U.S. NAVY ENGINEERING FIELD ACTIVITY, NORTHEAST REMEDIAL ACTION CONTRACT (RAC) CONTRACT NO. N62472-99-D-0032 CONTRACT TASK ORDER NO. 0089

DRAFT CLOSEOUT REPORT FOR SITE 4 THERMAL TREATMENT REMEDIATION

NAVAL WEAPONS INDUSTRIAL RESERVE PLANT BEDFORD, MASSACHUSETTS

April 26, 2005

Prepared by

Tetra Tech EC, Inc. 133 Federal Street Boston, Massachusetts 02110



Revision 0

<u>Date</u> 4/26/05 Prepared by Y. Zhang

Approved by J. Francis

Pages Affected All

CONTRACT NO N62472-99		CONTRACT TASK ORDER 0089	R NO.	ACTIVITY L	OCATION eapons Industria	al Reserve Pl	ant - Redford	MA
PROJECT TITI				114141	cupons maustra	<u> </u>	uni Deuroru,	
FROM:	reatment Phot 1	est				DATE		
Tetra Tecl	n EC, Inc.: Progr	am QC Manager T	homas Ke	elly		April 26, 20	05	
TO:	(CD C					DATE	0.5	
T. Bober	(CD-Copy)					April 26, 20	05	
1. (a) (b)	APPLY APPROPRIA	SUBMITTALS LISTED BE TE STAMP IMPRINT TO E OPY OF THIS TRANSMITT	ACH SUBMIT	TAL AND IN	DICATE REVIEW COM	IMENTS, AS REQ	UIRED.	DICC.
2.	THESE SUBMITTAL	S SHOULD BE RETURNED	D TO THIS OF	FFICE BY		_		
3.								
3.								
СД-Сору Т	o: EFANE: TRS:	R. Boucher, M J. Wolf	. Krivansky	7				
HARD COPY	To:							
ROICC	Г	RPM	CSO				A D	RIL 26, 2005
ROICC	L	Krw			SIGNATURE A	ND DATE	d API	KIL 20, 2003
FROM:	DESIGNER				DATE			
TO:					DATE			
	ROICC							
1.	THE SUBMITTALS	LISTED BELOW HAVE BE	EN REVIEWE	ED AND ARE I	RETURNED, WITH AC	TION TAKEN AS	INDICATED.	
2.								
COPY TO:								
ROICC		DESIGNER						
EDOM:					SIGNATURE AN	ID DATE		
FROM:	ROICC				DATE			
TO:	IONED A CEOP				DATE			
1.	CONTRACTOR THE SUBMITTALS	LISTED BELOW HAVE BE	EEN REVIEW	ED AND ARE	APPROVED/DISAPPR	OVED AS SHOW	N BELOW AND ON I	EACH STAMP
	IMPRINT.							
COPY TO:		OTHER						
Koicc		OTHER .			OFFICER, ENGIN - NAVAL FACILITIE	EERING FIELD ES ENGINEERING		DATE
ITEM NO.	SU	BMITTAL DESCRIPTION	1		PREPARED/ SUBMITTED BY	APPROVED	DISAPPROVED	REMARKS
1 SD		aft Closeout Report	for Site 4	Thermal	Amy			
116	eatment Remediati	IOII			Karaskevicus			

TABLE OF CONTENTS

1.0	INTR	ODUCT	ION	1-1
	1.1	Site Ba	ackground and History	1-1
	1.2	Overv	iew of ERH Remediation Program	1-4
		1.2.1	Project Team	1-4
		1.2.2	Site 4 Thermal Treatment Remediation Objectives	1-5
		1.2.3	Site 4 Thermal Treatment Remediation Design Basis	
		1.2.4	Site 4 Thermal Treatment Remediation Schedule	
		1.2.5	Site 4 Thermal Treatment Remediation Data, Analysis, and Reporting	1-7
2.0	ERH	REMED!	IATION	2-1
	2.1	Pre-Tr	reatment Soil and Groundwater Characterization	2-1
		2.1.1	Pre-Treatment Soil Sampling	2-1
		2.1.2	Pre-Treatment Groundwater Sampling	2-2
		2.1.3	Pre-Treatment Soil Sample Results	2-3
		2.1.4	Pre-Treatment Groundwater Results	2-3
	2.2	Installa	ation and Start-Up	2-4
		2.2.1	Subsurface Components	2-4
		2.2.2	Above Ground Components	2-4
		2.2.3	Start-up and System Shakedown	2-6
		2.2.4	Safety Considerations	
	2.3	ERH (Operation	2-9
		2.3.1	Oversight Activities	2-9
		2.3.2	Description of Routine Operation	2-9
			2.3.2.1 Electrode Operation	2-9
			2.3.2.2 VR and Treatment System	2-10
			2.3.2.3 Vapor Flow Rates and Vacuums	2-10
		2.3.3	Description of Maintenance Activities	2-10
			2.3.3.1 Excessive Water and Silt Recovery	2-10
			2.3.3.2 PCU Auto Dialer	2-13
			2.3.3.3 GAC Changeout	2-13
			2.3.3.4 Electrode Water Addition System	2-13
			2.3.3.5 Condenser System Shutdowns	2-13
			2.3.3.6 Loss of Make-Up Water	2-13
		2.3.4	Summary of Monitoring Data	2-13
			2.3.4.1 Environmental Characteristics	2-14
			2.3.4.2 Vapor Flow and Vacuum Data	2-14
			2.3.4.3 Temperature Values	2-16
			2.3.4.4 Water/Condensate Levels and Amounts	2-16
			2.3.4.5 Blower and GAC Data	2-16
		2.3.5	Contaminant Removal Rate	2-17
	2.4	Mid-P	rocess Groundwater Characterization	2-17
		2.4.1	Mid-Process Groundwater Sampling	2-17
		2.4.2	Mid-Process Groundwater Analytical Results	2-18
	2.5	Post-T	reatment Groundwater Characterization	2-18
		2.5.1	Post-Treatment Groundwater Sampling	
		2.5.2	Post-Treatment Groundwater Analytical Results	2-19
	2.6		bilizationbilization	
	2.7	Long-	Term Groundwater Monitoring	2-20

TABLE OF CONTENTS – cont'd

		2.7.1	Long-Ter	m Groundwater Sampling	2-20
		2.7.2	Long-Ter	m Groundwater Monitoring Results	2-20
3.0	WAST	E MAN	AGEMEN'	Τ	3-1
	3.1			Storage, and Disposal	
	3.2			torage, and Disposal	
	3.3			Storage, and Disposal	
	3.4	PPE C	ollection, S	torage, and Disposal	3-2
4.0	DATA	ANAL`	YSIS AND	CONCLUSIONS	4-1
	4.1			ical Data for Groundwater and Vapor Samples	
		4.1.1		Chemical and Biological Processes in Groundwater at Site 4	
			4.1.1.1	Recharge	4-4
			4.1.1.2	Rebound	4-4
				Increased Dissolution/Solubility	
			4.1.1.4	Biodegradation	4-4
		4.1.2		ng Wells Inside the Treatment Area (MW-18SR, MW-63S,	
)	
		4.1.3		ng Wells on the Periphery of or Outside the Treatment Area	
				MW-61S and MW-64S	
				MW-42SR, MW-60S, and MW-62S	
				MW-66S	
		4.1.4		of Vapor Data	
	4.2				
	4.3			s	
5.0	REFE	RENCES	S		5-1
				LIST OF FIGURES	
Figure	1_1	Site A	ea Man		1-2
Figure					
Figure					
Figure				IP Construction Details.	
Figure				lead Detail	
Figure			_	els Monitoring Wells Located in or Adjacent to Site 4 ERH Zone.	
Figure				w Plan View	
Figure		MW-1	8SR Contai	minants of Concern	4-6
Figure		MW-6	3S Contam	inants of Concern	4-7
Figure		MW-6	5S Contam	inants of Concern	4-8
Figure		MW-6	1S Contam	inants of Concern	4-10
Figure	4-7	MW-6	4S Contam	inants of Concern	4-11
Figure	4-8	MW-4	2SR Contai	minants of Concern	4-13
Figure	4-9	MW-6	OS Contam	inants of Concern	4-14
Figure	4-10			inants of Concern	
Figure	4-11	MW-6	6S Contam	inants of Concern	4-17

TABLE OF CONTENTS – cont'd

LIST OF TABLES

Table 1-1	Summary of Roles and Responsibilities for the Site 4 Remediation	1-4
Table 2-1	Pre-Treatment Groundwater Sampling Well Water Level Readings	
Table 2-2	Site 4 Operations Summary Data ERH Thermal Treatment	
Table 2-3	Weather Conditions	
Table 2-4	Post-Treatment Groundwater Sampling Well Water Level Readings	
Table 3-1	GAC Adsorption Efficiency	
Table 4-1	MW-18SR Contaminants of Concern	
Table 4-2	MW-63S Contaminants of Concern.	
Table 4-3	MW-65S Contaminants of Concern	
Table 4-4	MW-61S Contaminants of Concern.	4-10
Table 4-5	MW-64S Contaminants of Concern	4-11
Table 4-6	MW-42SR Contaminants of Concern	4-13
Table 4-7	MW-60S Contaminants of Concern	4-14
Table 4-8	MW-62S Contaminants of Concern	4-15
Table 4-9	MW-66S Contaminants of Concern	4-17
	LIST OF APPENDICES	
Appendix A	Thermal Remediation Services, Inc. – Site 4 Thermal Treatment Final Report	
Appendix B	Photographic Documentation	
Appendix C	Monitoring Well Soil Boring Logs and Construction Details	
Appendix D	Groundwater Sample Collection Record	
Appendix E	Summary of Analytical Results – Soil	
	Table E-1 Soil Analytical Results Site 4 ERH Remediation	
Appendix F	Summary of Analytical Results – Groundwater	
	Table F-1 Groundwater Analytical Results Site 4 ERH Remediation	
Appendix G	Summary of Analytical Results – Vapor	
	Table G-1 Vapor Analytical Results Site 4 Remediation Influent (Vapor Sam	ples
	Collected Using Summa Canisters)	
	Table G-2 Vapor Analytical Results Site 3 and Site 4 Operation (Vapor Sample	es
	Collected Using Summa Canisters)	
Appendix H	Waste Management Tracking Sheets	

LIST OF ACRONYMS AND ABBREVIATIONS

ASTM American Society for Testing and Materials

bgs below ground surface

BTEX benzene, toluene, ethylbenzene, and xylene

°C Degrees Celsius

CGI Combustible Gas Indicator
COC Contaminants of Concern
CPVC chlorinated polyvinyl chloride

CTO Contract Task Order

EFANE Engineering Field Activity, Northeast

ENSR ENSR International

ERH Electrical Resistance Heating

°F Degrees Fahrenheit

FID Flame Ionization Detector GAC Granular Activated Carbon

Hg Mercury
hp horsepower
kW kilowatt
lb pound

LEL lower explosive limit

MCL maximum contaminant level MCLG maximum containment level goal

NWIRP Naval Weapons Industrial Reserve Plant

O&M Operation and Maintenance

PCU Power Control Unit

PESM Project Environmental and Safety Manager

PID Photo Ionization Detector

ppb parts per billion

PPE personal protective equipment ppmv parts per million by volume

OA/OC Ouality Assurance/Ouality Control

RAC Remedial Action Contract
scfm standard cubic feet per minute
SHSO Site Health and Safety Officer
SHSP Site-Specific Health and Safety Plan
SOP Standard Operating Procedure
SVOC Semi-Volatile Organic Compound

TCL Target Compound List

TMP Temperature Monitoring Point
TRS Thermal Remediation Services, Inc.

TtEC Tetra Tech EC, Inc.
ug/kg micrograms per kilogram
ug/L micrograms per liter

USDOT United States Department of Transportation
USEPA United States Environmental Protection Agency

VOC Volatile Organic Compound

VR Vapor Recovery

1.0 INTRODUCTION

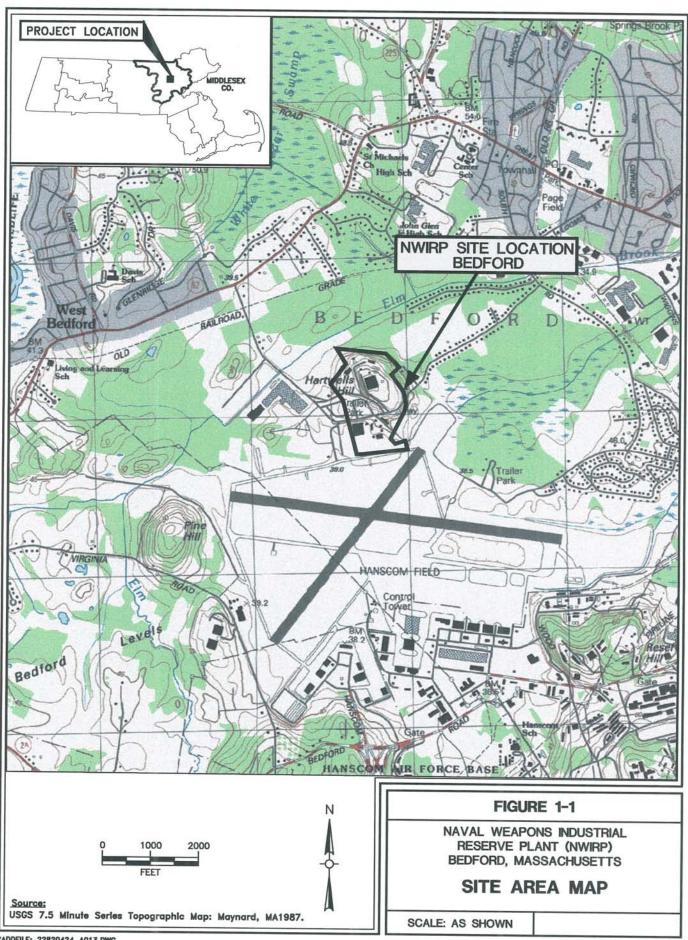
Tetra Tech EC, Inc. (TtEC) has prepared this Closeout Report for Site 4 Thermal Treatment Remediation under Contract Task Order (CTO) Number 0089, United States Navy Engineering Field Activity, Northeast (EFANE) Remedial Action Contract (RAC) Number N62472-99-D-0032. This Closeout Report for Site 4 describes the activities associated with the utilization of Electrical Resistance Heating (ERH), a thermal treatment technology, for the remediation of groundwater at the Naval Weapons Industrial Reserve Plant (NWIRP) located in Bedford, Massachusetts (the Site). The thermal treatment remediation at Site 4 was performed to remove benzene, toluene, ethylbenzene, and xylene (BTEX) contamination in soil and groundwater in the defined area.

During the period of operation for Site 4 remediation, an ERH pilot test was also conducted simultaneously in a nearby area identified as Site 3 to determine the applicability of the thermal treatment technology for full-scale treatment of chlorinated solvents in the groundwater source area. Activities and project results pertinent to the Site 3 pilot test are included in *Draft Closeout Report for Site 3 Thermal Treatment Pilot Test, Naval Weapons Industrial Reserve Plant, Bedford, Massachusetts* (TtEC, April 2004), and will not be discussed in this Closeout Report for Site 4. Where appropriate, this Closeout Report for Site 4 may reference the Closeout Report for Site 3, or discuss results from joint operations between Site 3 and Site 4, including a combined vapor recovery (VR) and treatment system as well as a combined waste disposal system.

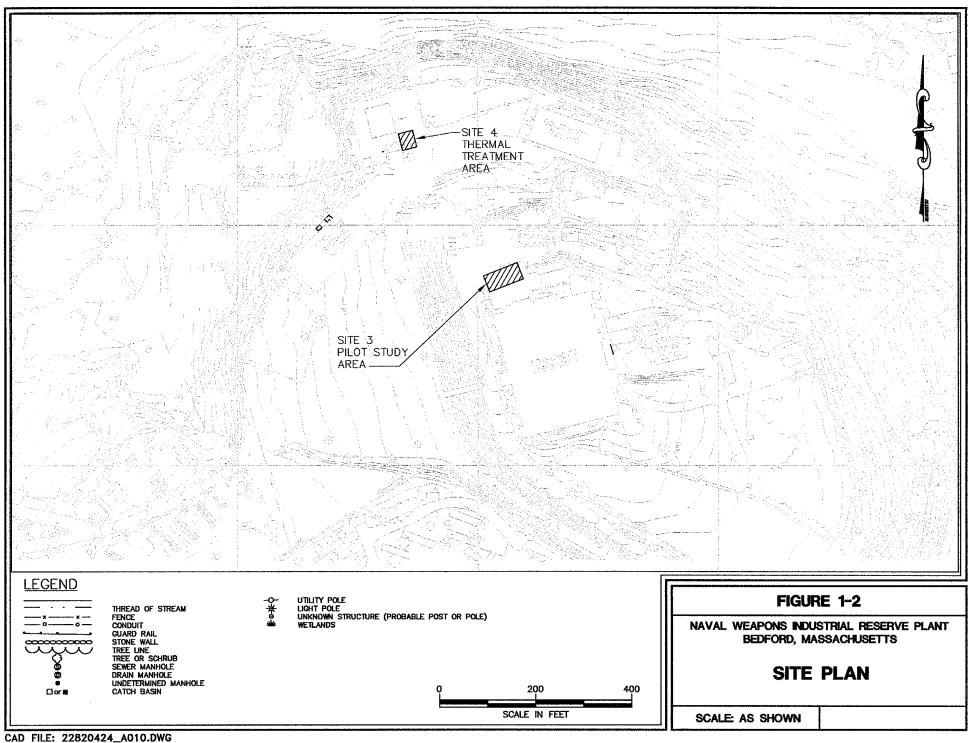
1.1 Site Background and History

The vicinity of NWIRP is depicted on Figure 1-1. The northern portion of the Site is located on Hartwells Hill. The northern slope of Hartwells Hill drops steeply at the northern-most property boundary, where the Site 4 thermal treatment project took place. Elm Brook and associated wetlands are present to the west and north of the facility, near the base of Hartwells Hill. A residential area and additional wetlands are located to the east and northeast. Other properties abutting the Site include Raytheon Missile Systems Division facilities to the west and Hanscom Field (formerly Hanscom Air Force Base) to the south.

Site 4 consisted of a subsurface source area and a dissolved-phase plume containing primarily BTEX constituents. The dissolved plume started at the source area near the former Transportation Building and migrated in a northwesterly direction across the Site and towards an off-site wetland area adjacent to Elm Brook (Figure 1-2). The date of the release that created this source area is not known, but it was due to the former presence of a 7,600-gallon underground storage tank which contained gasoline. This tank was removed by Raytheon between December 1988 and January 1989, along with some contaminated soil. Soil was not excavated beneath the building at that time in order to prevent any impacts to its structural integrity. Later groundwater sampling indicated levels of BTEX as high as 99,800 parts per billion (ppb) in MW-18S (1993). Between February 1997 and February 2000, the highest detected BTEX concentration in MW-18S was 56,300 ppb (1997). From November 2000 through January 2002, in situ chemical oxidation treatment was performed by GeoCleanse to reduce the mass of petroleum-related compounds in the source area. However, according to an investigation conducted in June 2002, the levels of BTEX in the groundwater of MW-18S still remained at above 20,000 ppb.



CADDFILE: 22820424_A013.DWG



1.2 Overview of ERH Remediation Program

The general strategy of the ERH remediation program at Site 4 was to implement an in situ thermal treatment technology that heated the shallow and intermediate groundwater for a set period of time while collecting and treating volatile organic compound (VOC) laden vapors in a combined VR and granular activated carbon (GAC) adsorption system for Site 3 and Site 4. Monitoring of various parameters, such as energy inputs, soil temperature, induced vacuum, extracted vapor flow rates, extracted vapor concentrations, and pre-treatment, mid-process, post-treatment and long-term monitoring groundwater VOC concentrations were performed to provide measurements of effectiveness of the thermal treatment technology.

1.2.1 Project Team

The design, installation, and operation of the ERH thermal treatment system for the simultaneous Site 3 pilot test and Site 4 remediation were performed by Thermal Remediation Services, Inc. (TRS), an experienced ERH subcontractor that TtEC procured. The final report for the Site 4 remediation prepared by TRS is included in Appendix A of this Closeout Report for Site 4. ENSR International (ENSR), under subcontract to TtEC, was also part of the team for the completion of the Site 4 remediation. Table 1-1 provides a summary of the major roles and responsibilities of TtEC, TRS, and ENSR for the Site 4 thermal treatment remediation project.

Table 1-1
Summary of Roles and Responsibilities for the Site 4 Remediation

Task	TtEC	TRS	ENSR
Work Area and Treatment	Lead Role	N/A	Review Role
Location			
Design of ERH Wells and Layout	Review Role	Lead Role	N/A
Additional Monitoring Well	Lead Role	N/A	Review Role
Installation and Baseline Survey			
Pre-Treatment Groundwater	Co-Lead Role	N/A	Co-Lead Role
Sampling			
ERH System Design and	Review Role; Supply power	Lead Role	N/A
Installation	connection.		
VR System Design and Installation	Review Role; Design and procure	Lead Role	N/A
	vapor collection system.		
Vapor Treatment System	Review role; Provide GAC vessels.	Lead Role	N/A
Installation		(installation)	
Thermal Treatment System	Review Role	Lead Role	N/A
Shakedown and Start-up			
Thermal Treatment System	Review Role	Lead Role	N/A
Operation and Maintenance			
(O&M)			
Thermal Treatment System	Lead Role	Review Role	N/A
Sampling			
Post-Treatment Performance	Lead Role	Review Role	Review Role
Testing and System Monitoring			
Long-term Monitoring	Co-Lead Role	N/A	Co-Lead Role
Groundwater Sampling			
(Six months after heating)			
Thermal Treatment Data Analysis	Lead Role	Review Role	Review Role
and Final Reporting			

1.2.2 Site 4 Thermal Treatment Remediation Objectives

The objective for Site 4 thermal treatment remediation was to significantly reduce the overall mass of petroleum-derived VOCs in the source area so that the remaining dissolved-phase plume could naturally attenuate to levels below the federal and state drinking water standards (maximum contaminant level (MCL) and non-zero maximum contaminant level goal (MCLG)) over time. Contaminants of concern (COCs) in the groundwater at Site 4 are BTEX compounds. Modeling of BTEX migration in groundwater of Site 4 indicated that achievement of a benzene concentration of 300 ppb in the groundwater source area by remediation would allow the remaining dissolved-phase plume to attenuate over time.

The groundwater benzene concentration was used as the key indicator of remediation performance at Site 4. This was based on the fact that benzene has the lowest federal and state drinking water standard (5 ppb) among the BTEX compounds. The remediation action objective for the Site 4 thermal treatment remediation was to achieve benzene concentration of 50 ppb in the Site 4 groundwater.

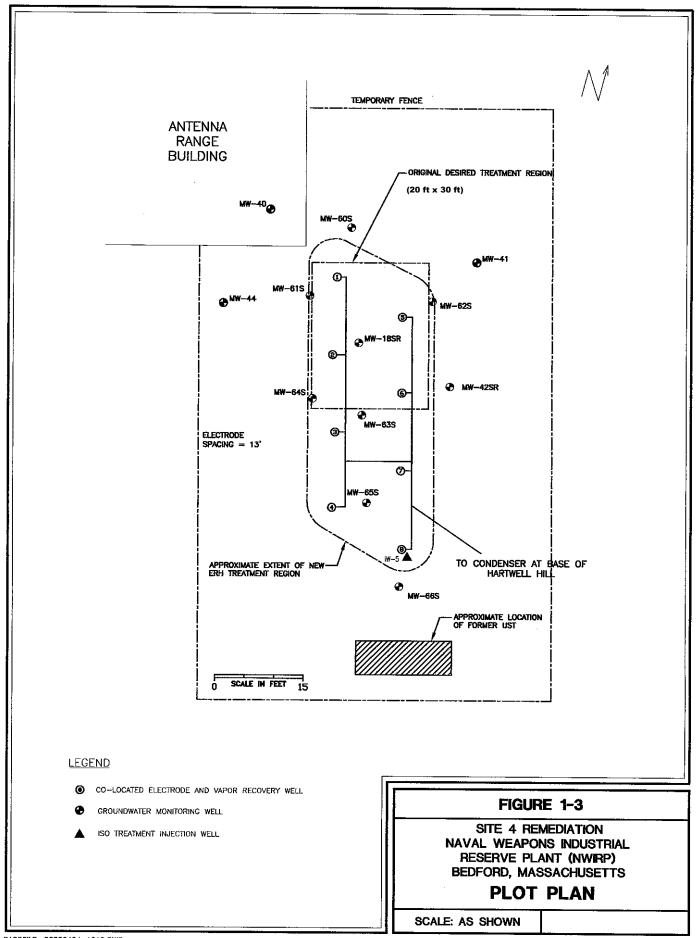
1.2.3 Site 4 Thermal Treatment Remediation Design Basis

The design of the Site 4 ERH remediation was based on several factors including treatment area and volume, site-specific geology and hydrogeology, and the project objective. The thermal treatment was performed in an area approximately 25 feet southeast of the Antenna Range Building. This area corresponded to the highest detected groundwater BTEX concentrations on Site 4.

The thermal treatment area at Site 4 was originally proposed to be 20 feet wide and 30 feet long. The actual treatment area was expanded from the original dimensions to 20 feet wide and 50 feet long after elevated BTEX concentrations were detected in an upstream monitoring well (MW-65S) during the pre-treatment groundwater sampling between May 29 and June 2, 2003. The proposed and actual Site 4 thermal treatment area is depicted in Figure 1-3.

The subsurface treatment interval of the ERH treatment area was from approximately 9.5 feet to 28 feet below ground surface (bgs), where contamination was largely present. The remediation area was approximately 20 feet wide by 50 feet long with a 9.5 feet to 28 feet bgs subsurface treatment interval, resulting in a treatment volume of 719 cubic yards. Eight electrodes with collocated VR wells were installed to a depth of 30 feet bgs (i.e., 2 feet beyond the treatment interval of 28 bgs). The electrode design allowed subsurface power application and VR to be performed simultaneously within each boring. Subsurface temperatures were measured at three temperature monitoring points (TMPs) located within the treatment area. The locations of the eight electrodes are also depicted in Figure 1-3.

Contaminants were removed from the vapor stream by four 1,000-pound (lb) GAC vessels. Condensate and recovered groundwater were treated using a single 30-gallon liquid GAC vessel and were either returned to the subsurface via drip lines installed in each electrode boring or were evaporated via the on-site condenser cooling tower.



1.2.4 Site 4 Thermal Treatment Remediation Schedule

The actual field efforts for implementation of the Site 4 remediation were from groundwater monitoring well installation and pre-treatment soil characterization in May 2003 to the conclusion of temperature and groundwater level monitoring in August 2004. The following is a summary of the timeline for the completion of the Site 4 thermal treatment remediation activities:

- Groundwater monitoring well installation and pre-treatment soil sampling: May 14 to May 17, 2003; well installation and pre-treatment soil sampling for MW-66S were conducted on June 26, 2003.
- Pre-treatment groundwater sampling: May 29 to June 2, 2003; pre-treatment groundwater sampling for MW-66S was conducted on June 30, 2003.
- Mobilization of the ERH system components commenced on April 16, 2003. Additional equipment arrived between May 1, 2003 and July 30, 2003.
- Installation of the ERH system components started on May 14, 2003. Installation of the subsurface components ended on July 22, 2003, while installation of the above ground piping, wiring, and equipment was completed on July 29, 2003.
- The system start-up, shakedown, and testing occurred on July 30 and 31, 2003.
- Routine ERH system operations were performed over 53 days, from July 31, 2003 until September 22, 2003.
- Electrodes were shut off permanently on September 19, 2003.
- Mid-process groundwater sampling: September 9, 2003.
- Post-treatment groundwater sampling: September 29 October 2, 2003.
- Final shutdown of the VR system occurred on October 9, 2003.
- Demobilization of the ERH system components and related supplies began on November 10, 2003. All system components were disassembled between November 10 and 14, 2003.
- Electrical power was disconnected from the power control unit (PCU) on December 19, 2003 and the office trailer was removed from the site on January 26, 2004.
- Long-term groundwater monitoring (6 months following the completion of the heating): August 2004.
- Temperature and groundwater level monitoring: May 2003 to August 2004.

1.2.5 Site 4 Thermal Treatment Remediation Data, Analysis, and Reporting

This Closeout Report for Site 4 presents data and information collected by TtEC, ENSR, and TRS. Data analysis has also been performed by TtEC, ENSR, and TRS with TtEC having the lead role in completing this Closeout Report for Site 4.

2.0 ERH REMEDIATION

The execution of the ERH remediation at Site 4 involved various distinct tasks beginning with pretreatment characterization and ending with long-term groundwater monitoring. These tasks are described in the following sections and include:

- Pre-treatment soil and groundwater characterization.
- Installation and start-up.
- ERH operation.
- Mid-process groundwater characterization.
- Post-treatment groundwater characterization.
- Long-term groundwater monitoring.

The information contained in Section 2.2, Installation and Start-Up, and Section 2.3, ERH Operation, references TRS's final report contained in Appendix A. Additional detailed information regarding these subjects can be found within Appendix A. Sections 2.1, 2.4, 2.5, and 2.7, Pre-Treatment Soil and Groundwater Characterization, Mid-Process Groundwater Characterization, Post-Treatment Groundwater Characterization, and Long-Term Groundwater Monitoring, respectively, discuss data that were collected, validated, and reported by TtEC.

Appendix B includes photographic documentation of the Site 4 ERH Thermal Treatment Remediation.

2.1 Pre-Treatment Soil and Groundwater Characterization

Soil samples were collected during the installation of seven new groundwater monitoring wells. Groundwater samples were collected from the 1 existing, 2 replacement and 7 new monitoring wells prior to the initiation of the ERH remediation at Site 4. Soil and groundwater samples were sent to Woods Hole Group Laboratories, Raynham, MA for the analyses of Target Compound List (TCL) VOC using United States Environmental Protection Agency (USEPA) Method 8260B and 2-methylnaphthalene using USEPA Method 8270C. Analytical results for the pre-treatment samples were used to compare with the results for the groundwater samples collected during and after the treatment.

2.1.1 Pre-Treatment Soil Sampling

Monitoring well installations for MW-60S, MW-61S, MW-62S, MW-63S, MW-64S, and MW-65S were conducted between May 14 and 17, 2003, and the installation for MW-66S was performed on June 26, 2003. The monitoring well construction diagrams for the seven new groundwater monitoring wells and two replacement wells (MW-18SR and MW-42SR) are included in Appendix C.

Soil samples were collected by TtEC from the seven soil borings drilled for the new groundwater monitoring well installations in 5-foot long lexan liners using a rotosonic drilling rig. The sample tube was cut open at 6-inch intervals using a utility knife, and a potential sample location was selected in every 5-foot interval based on field Flame Ionization Detector (FID) readings and visual observations of the soil boring. The soil boring logs produced from the drilling and soil sampling activities for the seven soil borings are included in Appendix C. FID screening results for the soil borings were recorded in the boring logs under the column titled "FID." Figure 1-3 depicts final locations of the existing and newly-installed monitoring wells.

One soil sample was collected per soil boring for laboratory analysis, based upon the FID readings and visual observations. One grab sample was collected from each boring for TCL VOC analysis using open-

barrel syringes and laboratory-preserved sample vials. One composite sample was also collected from each boring at the same interval as the VOC fraction for the analysis of semi-volatile organic compounds (SVOCs), particularly 2-methylnaphthalene. Samples were immediately placed in a cooler with ice following sampling. Sample collection was performed in accordance with procedures outlined in Standard Operating Procedure (SOP) 4 in the *Thermal Treatment Pilot Test and Remediation Quality Assurance/Quality Control (QA/QC) Plan, Naval Weapons Industrial Reserved Plant, Bedford, Massachusetts, Rev.* 2 (QA/QC Plan) (Foster Wheeler, July 2003). Sampling activities were documented on the soil boring logs and in the site logbook.

2.1.2 Pre-Treatment Groundwater Sampling

Groundwater samples were collected by TtEC using low-flow methods derived from the USEPA Region I Low Stress Purging and Sampling Procedure for the Collection of Ground Water Samples from Monitoring Wells. The low-flow sampling procedures were outlined in SOP S-2 in the QA/QC Plan. Groundwater samples were collected from the seven newly-installed and two replacement groundwater monitoring wells as well as an existing injection well located within or adjacent to the thermal treatment area between May 29 and June 2, 2003, and on June 30, 2003. These monitoring well locations are shown in Figure 1-3. One sample was collected from each of the monitoring wells MW-18SR, MW-42SR, MW-61S, MW-62S, MW-63S, MW-64S, IW-5, and MW-66S. One sample and one duplicate were collected from MW-60S. In addition, MW-65S was sampled twice during the pretreatment sampling on June 2 and June 30, 2003. A total of 12 samples were collected during the pretreatment groundwater sampling at Site 4.

Prior to the sampling activities, a round of water level measurements was conducted. The water level data are included in Table 2-1. Wells were purged and sampled using peristaltic pumps, and samples were collected after purging and water quality parameters had stabilized according to the criteria outlined in SOPs S-1 and S-2 in the QA/QC Plan.

Groundwater samples were immediately placed in a cooler with ice following sampling. All purging and sampling details were recorded on well purge data forms and in the site logbook. The well purge data forms for the pre-treatment sampling are included in Appendix D.

Table 2-1
Pre-Treatment Groundwater Sampling
Well Water Level Readings

Well ID	Sample Date	Water Level (ft below Top of Carbon Steel Riser)
MW-18SR	5/29/03	16.52
MW-42SR	5/29/03	15.59
MW-60S	5/29/03	20.30
MW-61S	5/29/03	17.59
MW-62S	5/29/03	17.79
MW-63S	5/29/03	15.36
MW-64S	5/29/03	14.95
MW-65S	5/29/03, 6/30/03	11.25, 11.30
MW-66S	6/30/03	10.44

2.1.3 Pre-Treatment Soil Sample Results

Pre-treatment soil samples were analyzed by Woods Hole Group Laboratories, Raynham, MA for TCL VOCs using USEPA Method 8260B and SVOCs (2-methylnaphthalene only) using USEPA Method 8270C. Analytical results for individual TCL VOCs, total VOCs, total BTEX, and 2-methylnaphthalene for the soil samples are tabulated in Table E-1 in Appendix E.

As indicated in Table E-1 in Appendix E, petroleum-related compounds including ethylbenzene, naphthalene, toluene, p/m xylene, and o-xylene were detected in the soil samples collected from the soil borings for the seven newly-installed groundwater wells at Site 4. Among these compounds, p/m-xylene had the highest concentrations in the soil samples with the exception of MW-66S-SBA-062603 in which only ethylbenzene was positively-detected at a low concentration (40 micrograms per kilogram (ug/kg)). Benzene, one of the COC and the key indicator compound for this remediation effort, was not detected in any of the soil samples. The soil sample data collected during the pre-treatment sampling event are consistent with the site history of petroleum-related contamination.

Total VOC concentration was the lowest in MW-66S (40 ug/kg) that was located outside the treatment area. Total VOCs ranged from low to moderate levels in the monitoring wells on the periphery of the treatment area including MW-62S (1330 ug/kg), MW-64S (91,200 ug/kg), MW-61S (119,800 ug/kg), and MW-60S (146,100 ug/kg). Soil sample data demonstrated the highest contamination levels in wells inside the treatment area including MW-63S and MW-65S with total VOC concentrations at 435,000 ug/kg and 363,000 ug/kg respectively.

Soil sample results for 2-methylnaphthalene also ranged from the lowest concentration (non-detect) in MW-66S to the highest concentration (770 ug/kg) in MW-63S.

2.1.4 Pre-Treatment Groundwater Results

Groundwater samples collected during the pre-treatment groundwater sampling event were analyzed by Woods Hole Group Laboratories, Raynham, MA for TCL VOCs using USEPA Method 8260B and SVOCs (2-methylnaphthalene only) using USEPA Method 8270C. Table F-1 in Appendix F contains analytical results for individual TCL VOCs, total VOCs, total BTEX, and 2-methylnaphthalene for all the groundwater samples collected during the Site 4 thermal treatment remediation, including the pre-treatment groundwater sample results.

Groundwater results generally followed similar contaminant distribution trend as observed in the soil samples, with monitoring wells outside the treatment area demonstrating lower contamination than wells inside the treatment area, while total VOC concentrations in the wells on the periphery of the treatment area varying from low to high levels. As indicated in Table F-1 in Appendix F, pre-treatment total VOCs ranged from 522.3 micrograms per liter (ug/L) (MW-66S) to 20,999 ug/L (MW-65S); total BTEX ranged from 502 ug/L (MW-66S) to 20,070 ug/L (MW-65S); benzene ranged from 14 ug/L (MW-42SR) to 360 ug/L (MW-IW-5); and 2-methylnaphthalene ranged from 5.8 ug/L (MW-42SR) to 80 ug/L (MW-65S).

Table F-1 in Appendix F shows that compounds positively-detected with the highest concentrations were mostly petroleum-derived compounds such as benzene, ethylbenzene, naphthalene, toluene, p/m xylene and o-xylene, with p/m xylene demonstrating the highest concentrations in most samples. Common laboratory contaminants including 2-butanone and acetone were also reported in most of the samples at concentration levels lower than the petroleum-derived compounds. In addition, chlorinated VOCs including trichloroethene and vinyl chloride were also detected in some samples at low concentrations, probably as a result of the Site's connected groundwater table with Site 3, which is known for chlorinated

VOC contamination. In summary, the Site 4 pre-treatment groundwater results indicated that petroleum-derived VOCs composed the majority of the total VOCs in most samples. This is consistent with the results from previous investigations and the site history of contamination from petroleum products.

2.2 Installation and Start-Up

Mobilization of the ERH system components commenced on April 16, 2003 with the delivery of the PCU for ERH operations. Additional equipment arrived between May 1, 2003 and July 30, 2003. Installation of the ERH system components started on May 14, 2003 with initiation of the drilling program for subsurface component installation. Installation of the subsurface components ended on July 22, 2003, while installation of the above ground piping, wiring, and equipment was completed on July 29, 2003. The system start-up, shakedown, and testing occurred on July 30 and 31, 2003, subsequent to the complete process installation. Operations officially began on July 30, 2003 with start-up and shakedown. The Site 4 thermal treatment remediation utilized various types of equipment installed in both subsurface and above ground locations.

2.2.1 Subsurface Components

ERH subsurface components included the following:

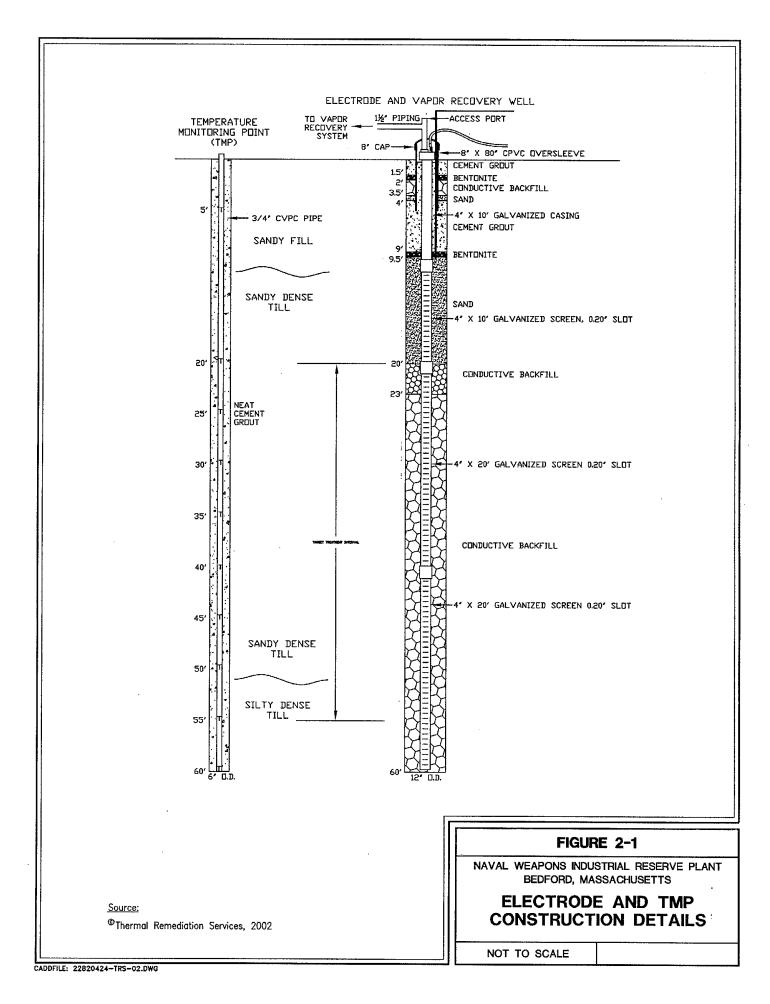
- Eight electrode/VR wells were installed to 30 feet bgs (see Figure 1-3).
- Seven new groundwater monitoring wells were installed to varying depths, depending upon the groundwater table depth and FID field screening results. Two existing monitoring wells (MW-18S and MW-42S) were abandoned and replaced so their construction materials were compatible with subsurface heating. In particular, screened intervals were constructed of stainless steel while riser sections were constructed of carbon steel. Appendix C contains well construction diagrams and soil boring logs completed during well installation and drilling. Soil sampling performed during installation is discussed in Section 2.1.1.
- Seven TMPs were installed concurrently with monitoring well installations. However, thermocouples were installed in only three of these TMPs.

Figure 2-1 provides a cross-section drawing of the electrode and TMP utilized during the Site 4 thermal treatment remediation.

2.2.2 Above Ground Components

During the subsurface installation, TRS installed the VR system, consisting of the VR manifold and above-surface process equipment, along with completing the piping and wiring connections to the electrodes and monitoring wells.

The heart of the ERH system was a PCU designed for 100% cycle duty and rated for a maximum power output of 2,000 kilowatts (kW). The VR manifold consisting of chlorinated polyvinyl chloride (CPVC) piping was connected from each VR well to the steam condenser that functioned to remove entrained liquids from the extraction process. The outlet of the steam condenser contains a knockout system that separates liquid from vapor phases. The condensate generated from the separated steam and groundwater passes through a liquid GAC treatment vessel and is used in the cooling loop to cool vapors and water removed during the VR process. Remaining condensate is recycled as electrode drip water and reinjected into the subsurface.



Air and vapor exiting the condenser skid following cooling was routed through vapor-phase GAC vessels to a VR blower unit, consisting of a 40 horsepower (hp) motor and vacuum pump capable of generating an original minimum of 6-inches of mercury (Hg) of vacuum. It had been re-sheaved soon after start-up in order to provide a range of 1-10-in Hg. Extracted hazardous vapors were treated using four 1,000-lb vapor-phase GAC vessels (provided by US Filter Westates) installed in a series-parallel configuration. Two parallel vessels served as the primary GAC vessel, while two others served as the secondary vessel. The GAC was provided and maintained by TtEC, including coordination of on-site changeouts.

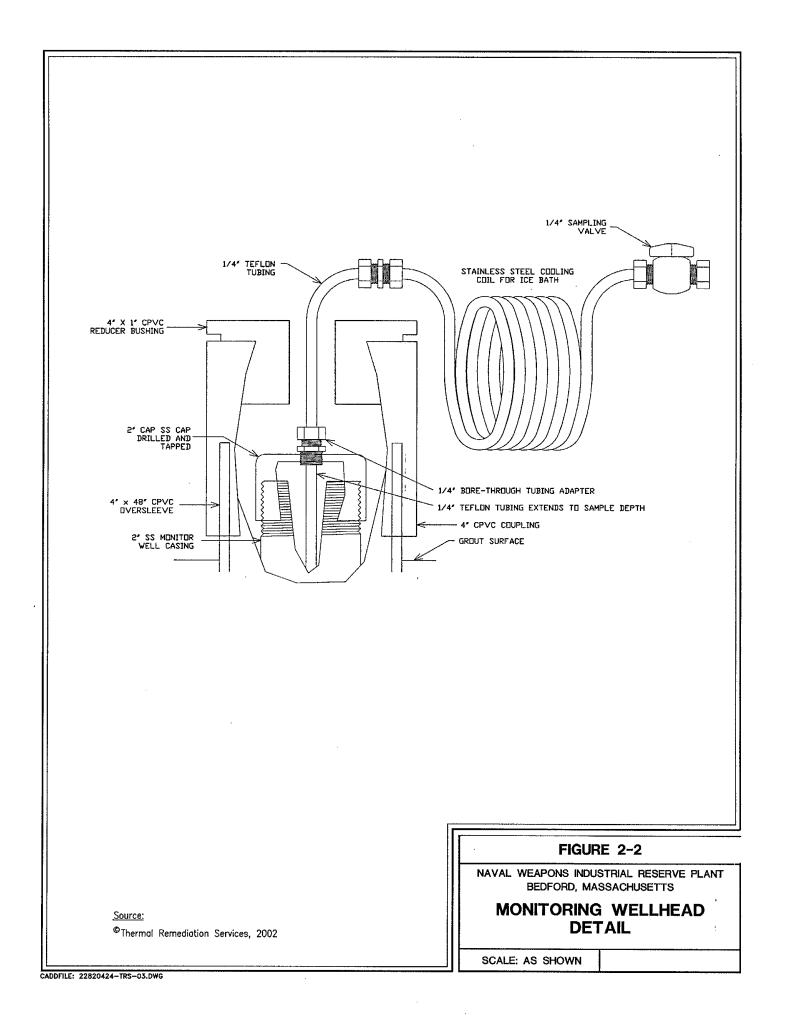
Groundwater monitoring well-heads for monitoring wells inside the ERH remediation area were modified for safety and sampling reasons, as seen in Figure 2-2. The capping of the well formed an enclosed system, where no gas or steam was allowed to escape from the top of the monitoring well. A stainless steel coil and valve were attached to the end of the groundwater sampling tubing, to be used during groundwater sampling. During sampling events, prior to purging a well, the coil was immersed in an ice water bath. The valve was opened and attached to a peristaltic pump. Sampling was progressed according to sampling procedures outlined in the QA/QC Plan. The coil apparatus functioned to enable the collection of cooled groundwater samples from heated groundwater without VOC losses.

<u>Instrumentation and Data Acquisition</u> - The data acquisition for the Site 4 thermal treatment remediation was performed by a combination of automatic and manual instrumentation. Much of the data was gathered through the control computer connected to the PCU. Temperature data from thermocouples installed in TMPs, in the vapor stream at the condenser influent and effluent, and at the blower stack, was routed to the computer system for the ability of automatic recording by TRS. Applied voltage to electrodes was able to be regulated and recorded by this PCU as well. Other operational data were able to be recorded on the PCU operations computer for use by TRS.

In order to determine energy input to individual electrodes, current surveys were to be performed using a clamping-type ampmeter. Various other instruments and gauges were available to collect data by TtEC personnel. Flow rates and temperatures of the vapor streams were to be measured through the use of an anemometer. Vacuum values, measured in inches of Hg were able to be measured through the use of vacuum gauges, of which several were available for various vacuum/pressure ranges. In addition, vapor samples were to be collected and screened using a Micro FID, MiniRAE Photo Ionization Detector (PID), and a VRAE Combustible Gas Indicator (CGI). Readings of the total cumulative volume of condensate generated during VR operations and the total volume reinjected into the subsurface as electrode drip water would be recorded as well, using permanently installed totalizers.

2.2.3 Start-up and System Shakedown

Start-up and system shakedown took place on July 30 and 31, 2003. TRS performed several tests and safety checks to ensure personnel safety during operations and successful working of the ERH system safety interlocks and emergency shutdowns. This work was in compliance with standard operating procedures as outlined in the *System Design and Work Plan, Electrical Resistance Heating Remediation Site 4, Naval Weapons Industrial Reserve Plant, Bedford, Massachusetts*, (TRS, April 2003).



Additionally, during the first week of full operations, several changes were made to address other deficiencies found and to adjust for site-specific geologic and hydrogeologic conditions:

- As the site heated over the first few days (and became more conductive) the power input to the pilot test cell was at over 800 kW. This caused a high rate of increase in subsurface temperatures at an average of 5.2 degrees Celsius (°C)/day and caused boiling near the electrodes at Site 3 only. This boiling led to mobilization of silt to the VR wells and, subsequently, the extracted vapor stream. Power application was reduced for both Sites 3 and 4, and later adjustments were made during operations.
- In order to lower the operating range for the vacuum provided by the blower, it was resheaved on August 12, 2003. The operating range was changed from a minimum of 6 in-Hg to having a range of 1-10 in-Hg. This adjustment was prompted by a need to have more control over the operating range of the blower, thus having the ability to lower steam (and groundwater) extraction rates.
- Excess water present in the cooling tower at Site 3 caused several operational shutdowns for both Sites 3 and 4 during the first week. Several causes of this were identified, and remedial measures were taken. See Section 2.2 of the Closeout Report for Site 3 for details regarding this adjustment.

2.2.4 Safety Considerations

- Although the Bedford NWIRP is surrounded by a barbed wire fence, temporary chain link fence with warning signs hung on it throughout its length was installed around the perimeter of the area to prevent unauthorized entry during unattended operations. This fence was installed to alleviate the requirement of 24-hour security during the test, and there were no unauthorized entries detected during the entire ERH operations.
- During the start-up period, stray voltage testing was conducted within and around the ERH treatment region to determine if any step-to-touch or step-to-step potentials existed. The testing and measures were taken to remove stray voltages, should any exist above the TRS safety limits of 30 volts for step-to-step potential and 15 volts for step-to-touch potential.
- Numerous system interlocks and safety systems exist within TRS's ERH equipment. These include water level switches and temperature interlocks for the steam condenser tank, cooling tower, and blower. Other safety systems and interlocks exist between system components, all of which were verified and checked during the start-up period. This testing was documented.
- During groundwater sampling events and any maintenance on electrodes or VR wells, the
 electrical power was turned off to the electrodes to prevent accidental contact with energized
 equipment. Power was then locked and tagged out by the personnel working on previously
 energized equipment. Additionally, when possible, the vapor extraction system was
 continuously kept in operation to prevent accumulation and/or fugitive emissions of steam
 and liberated vapors.

• Prior to entering the test area inside the perimeter fence for work-related reasons, any non-TRS employees were given a training session by TRS, detailing specific safety concerns and the means of eliminating any dangers to personnel. Additionally, specific activities were warned against, such as excavation or drilling near the area.

2.3 ERH Operation

2.3.1 Oversight Activities

During operations, TtEC was responsible for site management, project health and safety oversight and sampling/monitoring. A TtEC representative was on-site the majority of the time when any work was performed at the Site. For the greater part of the time spent on-site during Site 4 thermal treatment operations, one TtEC representative was present to perform these roles.

The Site Management role entailed monitoring, overseeing, and performing on-site observations/ inspection of work in progress to determine if the work was proceeding in accordance with the project QA/QC Plan. As part of this role, inspection and other quality-related reports were prepared and submitted. If any deficiencies on-site were found, the TtEC representative ensured resolution of these deficiencies and implemented any corrective action. This person also ensured that Site waste handling and manifesting were performed as required. The TtEC representative periodically reported to the Project Manager as to daily progress. The TtEC representative saw that all work performed by both TtEC and any subcontractors was completed in accordance with the *Final Work Plan For Site 4 Thermal Treatment, Naval Weapons Industrial Reserved Plant, Bedford, Massachusetts* (Work Plan) (Foster Wheeler, December 2003) and the QA/QC Plan.

In a related role, the TtEC representative served as the Site Health and Safety Officer (SHSO). The SHSO would ensure that all work on-site was being performed in accordance with the *Final Site -Specific Health and Safety Plan (SHSP) for Site 3 and Site 4 Thermal Treatment, Naval Weapons Industrial Reserved Plant, Bedford, Massachusetts* (Foster Wheeler, August 2003). Any operational changes that required modifications to health and safety procedures and the SHSP were identified, implemented, and documented by the SHSO. The SHSO maintained communication with both the Project Manager and the Project Environmental and Safety Manager (PESM) to ensure that the SHSP was being enforced for any TtEC employees and subcontractors and reported summaries of field operations.

TtEC personnel would also serve to perform monitoring of the ERH system components. This role is detailed in Section 2.3.4.

2.3.2 Description of Routine Operation

2.3.2.1 Electrode Operation

Routine operations were performed over 53 days, from July 31, 2003 until September 22, 2003.

Electrodes were shut off on August 12-13, 2003, for replacement of sheave on blower and repair to electrode water drip pump at Site 3. On August 14, 2003, a malfunction during a test of the PCU operating software caused a power and electrode shutdown that lasted approximately 20 hours until power was restored on August 15, 2003. In order to perform some cleaning of the VR system at Site 3, electrodes were turned off on August 19, 2003 for several hours. On August 20, 2003, for approximately four hours, on August 21, 2003 for approximately ten hours, and on August 27, 2003 for approximately

2.5 hours, electrodes were shut down for the addition of steel shot to VR wells at Site 3 for reduction of silting in the VR system.

During the week between September 1-6, 2003, electrodes were shut down for unknown amounts of time for addition of steel shot to VR wells at Site 4. During groundwater sampling on September 9, 2003 for approximately 7.5 hours, on September 10, 2003 for approximately eight hours, and on September 11, 2003 for approximately three hours, electrodes were turned off. A mid-process groundwater sampling round was conducted at Site 3 on September 18, 2003, when electrodes were turned off. Electrodes were shut off permanently on September 19, 2003, due to heat damage caused by a shut-off of the cooling water. Based on the mid-process groundwater sampling results for the monitoring wells at both Site 3 and Site 4, it had been determined that clean-up goals had been met, and therefore a decision was made to permanently leave off the electrodes. They were periodically turned off for other short periods throughout the thermal treatment operation in order to conduct both scheduled and unanticipated maintenance, as discussed in Section 2.3.3.

2.3.2.2 VR and Treatment System

The VR system was always in operation while electrodes were turned on, and during most times when electrodes were not turned on, as summarized in Section 2.3.2.1. The VR system did not operate during the power shutdown on August 14-15, 2003. Additionally, the shutdown on September 19, 2003 required repairs as described in Section 2.3.3.6. The VR system was restarted on October 2, 2003.

The majority of the problems associated with the ERH treatment were associated with the VR component. During the week of August 24-30, 2003, high power application rates to Site 4 electrodes began to occur, while boiling of the subsurface quickly took place immediately adjacent to electrodes. This caused very fine silts to become entrained in the boiling water and become transported into the recovered vapor stream, resulting in some problems as discussed in Section 2.3.3. While performing most maintenance activities, the vapor extraction system had remained operable.

An estimated total of 69.5 lbs of VOCs was removed from the subsurface at Site 4, as indicated in Table 2-2. Final shutdown of the VR system occurred on October 9, 2003.

2.3.2.3 Vapor Flow Rates and Vacuums

Throughout the duration of the vapor extraction system operation, several operational parameters and data values were recorded. The full list of these parameters is presented in Table 2-2. The influent vapor flow rate from Site 4 ranged from 24 to 183 standard cubic feet per minute (scfm). The vacuum on the Site 4 GAC influent ranged from 2 to 6.5 in-Hg. Section 2.3.4 describes the collection and use of the monitoring data gathered during the Site 4 remediation.

2.3.3 Description of Maintenance Activities

Throughout the course of the ERH operation, several maintenance issues occurred. The following summarizes these items, arranged according to the specific item of concern.

2.3.3.1 Excessive Water and Silt Recovery

High power and vacuum application rates became an issue during the week of August 24-30, 2003. High power caused boiling in the immediate vicinity of electrodes, which led to the introduction of silt into VR wells. Vacuum application was high enough to cause the extraction of this silt, along with groundwater

and steam. Silt would subsequently enter the VR system and build up inside places such as the condenser unit. As a remedy to this extraction, on the week of September 1-6, 2003, steel shot was added to the inside of the eight 4-inch diameter VR wells up to the approximate measured depth of groundwater. The condenser unit and discharge system was cleaned of the silt deposits during this week as well.

ND05-89-004 4/26/05 2-11

Table 2-2 Sites 4 Operations Summary Data ERH Thermal Treatment Bedford NWIRP Site

						Primary GAC Ir	ılet				Seconda	ary GAC Inlet					GAC Effluen	it				
	Daily SVE	Cumulative SVE	FID reading	PID reading	_	Summa canister	Influent	Influent Vacuur		FID reading	PID reading	LEL reading	Influent Vacuum	FID reading	PID reading	_	Summa canister	Effluent	Effluent Vacuum	Effluent Vapor	VOC removed	VOC removed
Date	Runtime (hours)	runtime (hours)	(ppmv)	(ppmv)	(%)	reading (ppmv)	Temperature	(in. Hg)	Flow (scfm)	(ppmv)	(ppmv)	(%)	(in. Hg)	(ppmv)	(ppmv)	(%)	reading (ppmv)	Temperature (°C)	(in. Hg)	Flow (scfm)	(lbs/day)	(lbs cumulative)
31-Jul-03	14	14	9800	NM*	20	14.8	20.3	4.0	162	5510	NM*	21	4.0	5240	NM*	21	0.028	21.8	4.5	172	0.5	0.5
1-Aug-03 2-Aug-03	22.5 24	36.5 60.5	9800 9800	NM*	20	14.8 14.8	20.3	4.0	162 162	5510 5510	NM* NM*	21 21	4.0	5240 5240	NM*	21	0.028 0.028	21.8 21.8	4.5 4.5	172 172	0.9	1.4
3-Aug-03	24	84.5	755	NM*	5	14.8	33.6	5.3	126	682	NM*	8	5.25	612	NM*	7	0.028	29.5	5.0	133	0.9	3.2
4-Aug-03	24	108.5	755	NM*	5	4.8	33.6	5.25	126	682	NM*	8	5.25	612	NM*	7	0.022	29.5	5.0	133	0.4	3.6
5-Aug-03	24	132.5	1585	NM*	8	4.8	37.2	6.5	71	1230	NM*	11	6.5	1233	NM*	10	0.022	34.0	5.5	152	0.2	3.8
6-Aug-03	24	156.5	836	NM*	5	4.8	34.6	5.5	144	718.0	NM*	10	5.5	707	NM*	8	0.022	30.9	5.5	127	0.4	4.2
7-Aug-03	24	180.5	515	NM*	6	4.8	33.2	5.0	137	445	NM*	8	5.25	452	NM*	11	0.022	32.5	5.5	155	0.4	4.6
8-Aug-03	24	204.5	2246	NM*	8	4.8	25.5	4.5	146	1733	NM*	9	4.75	1791	NM*	10	0.022	26.3	5.0	139	0.4	5.1
9-Aug-03	24	228.5	2246	41.9	8	4.8	25.5	4.5	146	1733	46	9	4.8	1791	31.2	10	0.022	26.3	5.0	139	0.4	5.5
10-Aug-03	24	252.5	389	41.9	3	4.8	28.3	5.5	143	328	46	7	5.5	280	31.2	4	0.022	29.6	5.5	147	0.4	6.0
11-Aug-03 12-Aug-03	24 21	276.5 297.5	389 288	41.9 64.5	3	3.8	28.3 31.6	5.5 5.5	143 160	328 239	46 105	4	5.5 5.25	280 216	31.2 97.4	2	0.053 0.053	29.6 28.7	5.5 5.5	147 158	0.2	6.2
13-Aug-03	20	317.5	990	54.9	4	3.8	31.5	3.2	127	374	2.5	4	3.8	505	27.1	3	0.053	30.0	4.0	143	0.2	6.5
14-Aug-03	14.5	332	591	4.7	5	3.8	41.1	6.0	137	509	0.3	8	5.8	414	0	5	0.053	34.0	4.0	215	0.1	6.7
15-Aug-03	14.5	346.5	591	4.7	5	3.8	41.1	6.0	137	509	0.3	8	5.8	414	0	5	0.053	34.0	4.0	215	0.1	6.8
16-Aug-03	24	370.5	591	4.7	5	3.8	41.1	6.0	137	509	0.3	8	5.8	414	0	5	0.053	34.0	4.0	215	0.1	6.9
17-Aug-03	23.5	394	316	189	4	3.8	23.2	2.5	159					217	21.6	4	0.053	25.6	3.0	186	0.2	7.0
18-Aug-03	24	418	316	189	4	3.8	23.2	2.5	159	258	88	4	2.5	217	21.6	4	0.053	25.6	3.0	186	0.2	7.3
19-Aug-03	16	434	324	1171	3	8.5	29.2	2.5	163	296	364	4	2.5	293	141	3	9.99	76.2	2.25	153	0.4	7.6
20-Aug-03	24	458	340	40.5	7	8.5	38.6	6.0	108	258	26	8	5.5	214	6.9	7	9.99	94.2	4.5	206	0.4	8.0
21-Aug-03 22-Aug-03	24 24	482 506	340 190	40.5 77.1	3	8.5 8.5	38.6 81.4	6.0 3.25	108 116	258 187	26 213	- 8 - 5	5.5 3.5	214 262	6.9 144	5	9.99 9.99	94.2 27.0	4.5 3.5	206 198	0.4	8.4 8.8
23-Aug-03	24	530	190	77.1	3	8.5	81.4	3.3	116	187	213	5	3.5	262	144	5	9.99	27.0	3.5	198	0.4	9.2
24-Aug-03	24	554	190	77.1	3	8.5	81.4	3.3	116	187	213	5	3.5	262	144	5	9.99	27.0	3.5	198	0.4	9.6
25-Aug-03	24	578	854	435	5	8.5	30.7	2.5	183	608	294	6	3	174	19.1	0	9.99	23.9	3	217	5.7	15.3
26-Aug-03	24	602	854	435	5	79.4	30.7	2.5	183	608	294	6	3.0	174	19.1	0	18.52	23.9	3.0	217	5.7	20.9
27-Aug-03	24	626	1275	960	12	79.4	32.6	3.5	113	574	460	12	4.0	465	147	10	18.52	28.2	4.0	180	3.5	24.4
28-Aug-03	24	650	4250	652	8	79.4	84.3	2.0	103	1364	169	7	3.0	939	55.1	5	18.52	28.2	3.0	256	3.2	27.6
29-Aug-03	24	674	4250	652	8	79.4	84.3	2.0	103	1364	169	7	3.0	939	55.1	5	18.52	28.2	3.0	256	3.2	30.8
30-Aug-03	24	698	4250	652	8	79.4 79.4	84.3	2.0	103	1364	169	7	3.0	939	55.1	5	18.52	28.2	3.0	256	3.2	34.0
31-Aug-03 1-Sep-03	24 24	722 746	4250 2846	652 707	8	79.4	84.3 18.7	2.0 3.0	103 145	1364 2216	169 480	7 5	3.0	939 1755	55.1 369	5 6	18.52 18.52	28.2 18.6	3.0	256 153	3.2 0.7	37.2 37.9
2-Sep-03	24	770	2846	707	4	12.4	18.7	3.0	145	2216	480	5	3.5	1755	369	6	0.213	18.6	3.5	153	0.7	38.6
3-Sep-03	14	784	2846	707	4	12.4	18.7	3.0	145	2216	480	5	3.5	1755	369	6	0.213	18.6	3.5	153	0.7	39.3
4-Sep-03	24	808	2846	707	4	12.4	18.7	3.0	145	2216	480	5	3.5	1755	369	6	0.213	18.6	3.5	153	0.7	40.0
5-Sep-03	17	825	1704	490	4	12.4	31.3	5.25	74	989	269	3	5.2	512	3.3	1	0.213	30.3	5.5	116	0.3	40.3
6-Sep-03	22.5	847.5	369	143	5	12.4	20.1	4.2	74	630	350	5	4.2	117	5.9	4	0.213	23.3	4.2	90	0.3	40.6
7-Sep-03	21.75	869.25	369	143	5	12.4		5.0	56	630	350	5	4.2	117	5.9	4	0.213	23.3	4.2	90	0.3	40.8
8-Sep-03	22.75	892	529	105	6	12.4	24.0	5.0	56	261	75	7	5.0	115	1.3	6	0.213	24.2	5.0	78	0.3	41.1
9-Sep-03	24	916	529	105	6	116.0	40 E	5.0	56	261	75 52	7	5.0	115	1.3	6	0.545	24.2	5.0	78	0.3	41.4
10-Sep-03 11-Sep-03	24 24	940 964	2236 1964	467 672	12 10	116.0 116.0	12.5 86.5	2.25 5.0	24 24	323 229	52 99.0	6	2.5 4.75	265 173	0.9	6 5	0.545 0.545	14.4 23.5	3.25 4.5	86 104	0.3 1.1	41.7 42.8
12-Sep-03	24	988	1550	406	10	116.0	19.9	4.0	33	229	107	3	4.75	226	3.0	4	0.545	23.9	4.5	79	1.5	44.3
13-Sep-03	24	1012	1550	406	10	116.0		4.0	33	298	107	3	4.3	226	3	4	0.545	23.9	4.5	79	1.5	45.8
14-Sep-03	24	1036	2750	467	6	116.0		5.5	33					403	32	5	0.545	30.9	5.5	110	1.5	47.3
15-Sep-03	24	1060	2750	467	6	116.0	28.7	5.50	33	531	120	6	5.5	403	32	5	0.545	30.9	5.5	110	1.5	48.8
16-Sep-03	24	1084	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	50.2
17-Sep-03	24	1108	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	51.7
18-Sep-03	24	1132	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	53.2
19-Sep-03	24	1156	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	54.7
20-Sep-03 21-Sep-03	24 24	1180 1204	2750 2750	413 413	16 16	116.0 116.0	85.9 85.9	5.25 5.25	33	531 531	150 150	10	5.5 5.5	403 403	47.2 47.2	8	0.545 0.545	29.6 29.6	5.5 5.5	96 96	1.5 1.5	56.2 57.7
22-Sep-03	11.5	1215.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	0.7	58.4
2-Oct-03	10	1225.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	0.6	59.1
3-Oct-03	24	1249.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	60.5
4-Oct-03	24	1273.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	62.0
5-Oct-03	24	1297.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	63.5
6-Oct-03	24	1321.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	65.0
7-Oct-03	24	1345.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	66.5
8-Oct-03	24	1369.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	68.0
9-Oct-03	24	1393.5	2750	413	16	116.0	85.9	5.25	33	531	150	10	5.5	403	47.2	8	0.545	29.6	5.5	96	1.5	69.5

- Bold summa results represent actual sample data.
- Shaded rows represent days on which data was not collected. Data shown for these days was estimated based upon nearby days' data. Most days on which data was not collected was because site personnel were not on-site.
- Only summa canister data was used to calculate mass removed. No FID data was used.
- All data for 7/31/03, except for summa canister results, was estimated; it was only measured for a combined flow from Sites 3 and 4.
- FID readings on 9/16/03 were estimated.
- Vapor flow for Site 4 influent on 9/6/03, 9/10/03, and 9/15/03 was estimated due to moisture present in piping.
- NM* = Not measured. The use of PID was not initially planned upon but was later added beginning on 8/11/03.
- The ERH system was shut down from 9/23/03 through 10/1/03, due to an equipment failure. Cooling water was accidentally shut off, resulting in shutdown.

 The mass of VOCs = summa canister reading*influent vapor flow*concentration units conversion factor*mass units conversion factor*mass-weight conversion factor*volume units conversion factor*time units conversion factor.

2.3.3.2 PCU Auto Dialer

During the week of August 16, 2003, the remote access PCU software locked, preventing remote access to the PCU central computer. The lock-up appeared to be due to the auto dialer residing on the same telephone line as the PCU modem. To resolve this problem, the auto dialer was rerouted to use the telephone line that the site fax was using.

2.3.3.3 GAC Changeout

In order for the vapor-phase GAC treatment vessels to maintain a performance treatment standard for VOCs in the vapor stream, VOC concentrations prior to, between, and after the vessels was monitored three times per week during every week of operation. Breakthrough of the primary vessel was determined when the vessel's adsorption efficiency percentage was below 95% removal, at which time the GAC in that vessel was changed. This entailed removal of the spent carbon by means of a vacuum truck; the spent GAC was placed into supersacs for later disposal or regeneration. The secondary GAC vessels were then moved to serve as the primary vessels. New or reactivated GAC was added to the former primary vessels, which then became the secondary unit, by means of loading through the vessel manway on the top.

Due to silt infiltration issues into the VR system, the liquid GAC vessel became restricted. The vessel was cleaned, and the GAC within it was changed out on September 5, 2003. The used GAC was vacuumed out and placed into a 55-gallon drum for later disposal or regeneration.

2.3.3.4 Electrode Water Addition System

On September 6 or 7, 2003, the electrode water addition system was placed into a "hand" operational mode in order to avoid "high-high" level shutdowns. However, this action caused the cooling tower water to drain and moisture to condense in the VR lines. When these negative effects were realized, the electrode water addition system was placed back into an "automatic" operations mode.

2.3.3.5 Condenser System Shutdowns

In order to further address shutdowns that resulted from low or high water levels in the cooling tower and condenser system, on September 11, 2003, float levels in the cooling tower were adjusted. Additional changes were made to condenser system float levels on September 7-14, 2003. This adjustment provided more vertical difference between high and low water shut off levels, therefore decreasing the number of shutdowns that occur.

2.3.3.6 Loss of Make-Up Water

The TtEC site personnel inadvertently turned off the make-up water supply for the VR condenser and cooling tower on September 19, 2003. This resulted in a shutdown of power supply to the electrodes but system interlocks cycled between the on and off positions. Cooling water was lost, but VR progressed. Some damage was incurred by the CPVC vapor lines after the condenser system, and failure of piping occurred near the heat exchanger and between GAC vessels.

2.3.4 Summary of Monitoring Data

Through the use of general observation, flow meters, vacuum/pressure gauges, thermometers, water level gauges, volt meters, amp meters, FIDs, PIDs, and lower explosive limit (LEL) meters, data were acquired

and recorded throughout the thermal treatment, from August 1, 2003 until September 16, 2003 on most of the days that the Site 4 remediation VR system was in operation. Most of these data were recorded by TtEC on a Daily Log Sheet that was sent to the Project Manager for review. See Table 2-2 for a summary of some of the daily monitoring data. Voltage data, current data, and thermocouple data were recorded by TRS and not included on Daily Log Sheets; these data were used as discussed in the TRS Final Report in Appendix A. System monitoring was performed in accordance with the project QA/QC Plan and Work Plan.

During the seven-week VR system operation, grab vapor samples were collected using summa canisters once every week from the separate inlet ports to the primary GAC units for Site 3 and Site 4 and from the combined GAC effluent. The sampling dates were: July 31, Aug. 7, Aug 14, Aug. 22, Aug. 28, Sept. 6, and Sept. 11. These vapor samples were sent to Air Toxics Ltd., Folsom, CA for analyses of TCL VOCs and methane using USEPA method TO-14A and American Society for Testing and Materials (ASTM) D-1946 respectively. All vapor samples were collected and analyzed in accordance with the project QA/QC Plan. Analytical data for the vapor samples collected from the Site 4 influent are summarized in Table G-1 in Appendix G, and data for samples collected from the combined effluent for Site 3 and Site 4 are summarized in Table G-2 in Appendix G.

The following sub-sections discuss results from these sampling and system monitoring activities.

2.3.4.1 Environmental Characteristics

FID readings from around the Site 4 perimeter fence were recorded on days during which a daily log was completed as health and safety screening data and were never higher than background values. In addition, an estimate of the precipitation that had accumulated for the previous 24-hour period was recorded; this data was recorded to potentially serve as justification for unusually high amounts of water being entrained by the VR system. The range of daily precipitation was from zero to 0.53 inches. All precipitation and ambient temperature data is shown in Table 2-3.

Visual observations were made daily. These include inspection of the electrode field to observe whether any steam or vapors were escaping from the tops of groundwater monitoring wells, VR wells, or from VR piping. The perimeter fences were observed to confirm that no unauthorized site entries had been attempted while the site was unattended.

2.3.4.2 Vapor Flow and Vacuum Data

Vapor flow on both the influent and effluent sides of the GAC vessels were measured using a portable electronic anenometer. The influent vapor flow was measured in the vapor stream pipe directly after the condenser unit, and the effluent flow was measured immediately after the secondary GAC vessel. The influent and effluent flow data are presented in Table 2-2. These data were used in conjunction with other data to calculate mass removal of VOCs, as discussed in Section 2.3.5 and Section 4.1.4 and calculated in Table 2-2. Site 4 influent vapor flow values ranged from 24 to 183 scfm, while the combined effluent flow values ranged from 78 to 256 scfm. Vacuum, measured in in-Hg, was monitored in the influent and effluent vapor streams at the same places that vapor flow was measured, and also in the vapor stream between the primary and secondary GAC units. Portable mechanical gauges were used to accomplish this. The influent and effluent vacuum data are included in Table 2-2. The influent vacuum measured in the vapor stream was between 2 and 6.5 in-Hg, while the GAC mid-point and effluent values ranged from 2.5 to 6.5 in-Hg and 2.25 to 5.5 in-Hg, respectively.

Note that mid-point and effluent vapor characteristics represent a combined vapor mass from the Site 3 pilot test and Site 4 remediation.

Table 2-3 Weather Conditions

Date	Temperati	Temperature (degrees Fahrenheit (°F))			ion (inches)
Date	Average	Minimum	Maximum	Daily	Monthly
7/31/2003	69.0	57.0	81.0	0	NR ²
8/1/2003	62.6	57.2	68.0	0.19	
8/2/2003	69.5	60.1	79.0	0.24	
8/3/2003	75.5	66.0	84.9	0.10	1
8/4/2003	76.3	71.6	81.0	0.42	
8/5/2003	77.0	71.6	82.4	0.15	1
8/6/2003	77	69.8	84.2	0	1
8/7/2003	74.6	66.2	82.9	0.01	
8/8/2003	73.4	68.0	78.8	0.53	
8/9/2003	77.6	71.1	84.2	0	
8/10/2003	79.0	73.0	84.9	0.02	
8/11/2003	78.8	71.6	86.0	0	
8/12/2003	75.0	69.1	81.0	0.48	
8/13/2003	76.1	64.4	87.8	0	
8/14/2003	76.1	64.4	87.8	NA ¹	
8/15/2003	68.6	62.1	75.2	0	
8/16/2003	77.0	66.2	87.8	NA^1	
8/17/2003	68.9	62.6	75.2	NA ¹	
8/18/2003	72.5	59.0	86.0	0.01	
8/19/2003	75.3	62.6	88.0	0	
8/20/2003	75.2	62.6	87.8	NA^1	
8/21/2003	77.0	66.0	88.0	0	
8/22/2003	80.6	69.8	91.4	0.03	
8/23/2003	69.0	57.0	81.0	0.01	
8/24/2003	61.1	48.2	73.9	0	
8/25/2003	68.1	57.2	79.0	0	
8/26/2003	70.0	59.0	81.0	0	
8/27/2003	74.3	64.4	84.2	0	
8/28/2003	63.5	53.1	73.9	0	
8/29/2003	64.5	48.0	81.0	0	
8/30/2003	69.8	57.2	82.4	0	
8/31/2003	59.1	48.2	70.0	0	2.19
9/1/2003	62.5	57.0	68.0	0	
9/2/2003	62.0	57.0	66.9	0.31	
9/3/2003	63.6	57.2	70.0	0	
9/4/2003	64.0	60.1	68.0	0.04	
9/5/2003	67.0	57.0	77.0	0	
9/6/2003	62.6	50.0	75.2	0	
9/7/2003	64.5	50.0	79.0	0	
9/8/2003	62.6	51.8	73.4	0	
9/9/2003	55.8	44.6	66.9	0	
9/10/2003	55.7	37.4	73.9	0.01	
9/11/2003	64.0	51.1	77.0	0	
9/12/2003	61.7	51.8	71.6	0	1
9/13/2003	62.2	51.1	73.4	0	1
9/14/2003	71.6	62.6	80.6	0	7

Table 2-3 – *cont'd* Weather Conditions

Date	Temperate	ure (degrees Fah	Precipitation	on (inches)	
Date	Average	Minimum	Maximum	Daily	Monthly
9/15/2003	67.0	57.0	77.0	0	
9/16/2003	67.1	57.2	77.0	NA ¹	
9/17/2003	66.5	59.0	73.9	0	
9/18/2003	60.8	48.2	73.4	NA ¹	
9/19/2003	59	66.5	73.9	NA ¹	
9/20/2003	72.5	62.6	82.4	0.04	
9/21/2003	63.5	53.1	73.9	0.01	
9/22/2003	61.9	51.8	72.0	0	0.41

Notes:

- Weather data obtained from www.wunderground.com, historical data for Bedford, Massachusetts.
- NA¹ Precipitation data for these dates was not available.
- NR² The ERH system only operated for one day this month; a monthly precipitation total was not necessary.
- The monthly precipitation total for September only represents that accumulated from September 1-22.

2.3.4.3 Temperature Values

The anenometer used to measure flow was also used to measure temperatures of influent and effluent vapors. Influent and effluent temperature values are presented in Table 2-2. Temperature values for the Site 4 influent vapor stream ranged from 12.5 to 86.5°C; the effluent vapor stream displayed a range of 14.4 to 34.0°C. Temperature values recorded by thermocouples in TMPs and installed along VR piping were downloaded onto the PCU's computer system and retained by TRS for operational use. These values are discussed in the TRS Final Report in Appendix A.

2.3.4.4 Water/Condensate Levels and Amounts

Using sight glasses, water and condensate levels were measured in the condenser unit and cooling tower. A high or low level in any of these tanks could be due to any number of circumstances; however, certain levels would cause system shutdown. These levels were observed qualitatively by TRS for operational reasons and were not recorded.

Condensate/water amounts that had been extracted through the VR system were recorded to monitor whether unusually large amounts of water were being collected by the VR system. This data was collected using a totalizer after the condenser unit. The total value recorded at the end of the Site 4 remediation was over 8,500 gallons. The total volume of water that was re-injected into the treatment zone was over 1,200 gallons. The remaining water, approximately 7,300 gallons, was used as cooling water and had evaporated from the cooling tower during operations.

2.3.4.5 Blower and GAC Data

The system blower runtime represented the total VR system operating time, and a final estimated value of 1,393.5 hours was made.

Vacuum readings collected at the influent and effluent to each GAC unit were made and recorded as discussed in Section 2.3.4.2. FID, PID, and LEL readings were taken from Tedlar bags filled with air collected from the inlet ports on the primary and secondary GAC units and on the GAC outlet prior to air discharge at the blower stack. FID data were collected using a PE Photovac MicroFID, while PID data

were collected using a MiniRAE 2000 PID. LEL was collected with a VRAE 7800 multi-gas meter. FID, PID, LEL, flow, and vacuum readings were obtained nearly daily from Monday through Friday during the ERH operation. FID, PID, and LEL data collected are summarized in Table 2-2.

Grab vapor samples were collected using Summa canisters once per week during the VR system operation, from the inlet port to the primary GAC unit and from the effluent of the GAC. The vapor sample data for the Site 4 influent and combined effluent are summarized in Tables G-1 and G-2 respectively in Appendix G. The total VOC values for the vapor samples are also presented in Table 2-2. During the seven summa canister collection events, the Site 4 influent values for total VOCs ranged from 4.8 to 116.0 parts per million by volume (ppmv) and the effluent values ranged from 0.022 to 18.52 ppmv.

2.3.5 Contaminant Removal Rate

Due to the poor correlation between the FID/PID readings and the laboratory results from the vapor sampling, VOC mass removal calculations were based on the data from the seven weekly vapor sampling events using Summa canisters. The Site 4 influent vapor analytical data, along with the Site 4 influent flow rate, vacuum, and temperature data, was used to calculate daily VOC mass removal amounts for the Site 4 thermal treatment remediation, as detailed in Table 2-2. Results for the Site 4 weekly influent samples were extrapolated to represent days when no grab vapor samples were collected.

Using the calculation presented in Table 2-2, it is estimated that the initial total VOC removal rate was approximately 0.5 lb/day on July 31, 2003. Due to fluctuations on the amount of vacuum employed on the well field, vapor flow, and influent vapor VOC concentration, the contaminant removal rates varied between 0.1 and 5.7 lb/day during the period of the VR system operation. The cumulative VOC removal during the Site 4 thermal treatment remediation was approximately 69.5 lbs.

2.4 Mid-Process Groundwater Characterization

2.4.1 Mid-Process Groundwater Sampling

To evaluate the on-going ERH process at Site 4 so that changes to the process could be made if required to optimize contaminant removal efficiency, mid-process groundwater samples were collected by TtEC on September 9, 2003 from monitoring wells MW-18SR, MW-63S, and MW-65S that were inside the thermal treatment area.

The mid-process groundwater samples were collected using a peristaltic pump in accordance with a modified version of the USEPA Region I low flow purging and sampling procedure (see SOP S-1/S-2 in Appendix C of the QA/QC Plan). Because of high sample temperature, special cooling procedures were adopted for the sampling using a peristaltic pump. When purging and sampling the well, the sampling valve on the wellhead was connected to a stainless steel cooling coil that was immersed in ice water. The outlet of the cooling coil was connected to the peristaltic pump. Using this technique, the hot groundwater was cooled. Groundwater wells were purged for more than an hour before the groundwater samples were collected. Sample bottles were placed in an iced cooler immediately upon filling.

Due to safety concerns, water levels of the wells were not measured during the mid-process groundwater sampling event. The water quality parameters were measured during the well purging. All sampling details were recorded on well purge data forms and in the site logbook. The well purge data forms are included in Appendix D.

ND05-89-004 4/26/05

2.4.2 Mid-Process Groundwater Analytical Results

Groundwater samples collected by TtEC from the mid-process sampling were sent to Woods Hole Group, Raynham, MA for TCL VOC analysis by USEPA Method 8260B. Tabulated analytical results for the mid-process groundwater samples are included in Table F-1 in Appendix F.

As indicated in Table F-1 in Appendix F, among the three monitoring wells that were sampled inside the treatment area during the mid-process sampling, total VOCs ranged from 226.1 ug/L (MW-18SR) to 5,488 ug/L (MW-65S), total BTEX ranged from 30.6 ug/L (MW-18SR) to 3,748 ug/L (MW-65S), and benzene ranged from non-detect (MW-18SR) to 14 ug/L (MW-65S). A comparison of the mid-process sample results with data from other sampling rounds will be discussed in Section 4.1.

2.5 Post-Treatment Groundwater Characterization

2.5.1 Post-Treatment Groundwater Sampling

The post-treatment groundwater sampling was conducted by TtEC after the ERH system was turned off and the groundwater temperature reached < 99°C. During the post-treatment sampling event that occurred between September 29 and October 2, 2003, monitoring wells MW-18SR, MW-42SR, MW-60S, MW-61S, MW-62S, MW-63S, MW-64S, MW-65S, and MW-66S were sampled using a peristaltic pump.

Because of high sample temperature, special cooling procedures were adopted for the post-treatment groundwater sampling using a bladder pump. When purging and sampling the well, the sampling valve on the wellhead was connected to a stainless steel cooling coil that was immersed in ice water. The outlet of the cooling coil was connected to the bladder pump. Using this technique, the hot groundwater was cooled. Depending on its water level, a monitoring well was purged for 30 minutes or a minimum volume of water before the groundwater sample was collected. Sample bottles were placed in an iced cooler immediately upon filling.

The water quality parameters were measured during the well purging. All sampling details were recorded on well purge data forms and in the site logbook. The well purge data forms are included in Appendix D.

Post-treatment water levels in the monitoring wells were measured on September 29, 2003, as presented in Table 2-4.

Table 2-4
Post-Treatment Groundwater Sampling
Well Water Level Readings

Well ID	Sample Date	Water Level (ft below Top of Carbon Steel Riser)
MW-18SR	9/29/03	20.77
MW-42SR	9/29/03	20.35
MW-60S	9/29/03	22.86
MW-61S	9/29/03	21.18
MW-62S	9/29/03	22.01
MW-63S	9/29/03	20.24
MW-64S	9/29/03	19.85
MW-65S	9/29/03	18.39
MW-66S	9/29/03	13.60

2.5.2 Post-Treatment Groundwater Analytical Results

Post-treatment groundwater samples collected by TtEC were sent to Woods Hole Group, Raynham, MA for TCL VOC analysis by USEPA Method 8260B. Tabulated analytical results for the post-treatment groundwater samples are included in Table F-1 in Appendix F.

As indicated in Table F-1 in Appendix F, among the nine monitoring wells that were sampled during the post-treatment sampling, total VOCs ranged from 259.4 ug/L (MW-42SR) to 14,114 ug/L (MW-64S), total BTEX ranged from 138 ug/L (MW-63S) to 11,900 ug/L (MW-64S), and benzene ranged from non-detect (MW-63S) to 140 ug/L (MW-60S). A comparison of the post-treatment sample results with data from other sampling rounds will be discussed in Section 4.1.

2.6 Demobilization

Shut down of the electrodes occurred on September 22, 2003. For health and safety reasons, the VR system remained operable until October 9, 2003. Demobilization of the ERH system components and related supplies began on November 10, 2003, after authorization to shut down was given to the TtEC Site Manager by the Project Manager.

All system components were disassembled between November 10 and 14, 2003. Any reusable items owned by TRS were placed into temporary storage for shipment off-site. Expendable items and condenser units were decontaminated (when necessary) and placed into a trash dumpster. Any trailer-mounted or skid-mounted equipment, such as the condenser skid, PCU, and cooling tower will be removed in the near future by flatbed truck. Rental items such as the Baker excess condensate storage tank, helium tanks, and perimeter fence, were returned between these dates.

Spent vapor-phase GAC and vessels were removed from the site on November 12, 2003; the GAC was shipped for regeneration as hazardous waste. Spent liquid-phase GAC was removed from the site on November 19, 2003 and shipped for regeneration as non-hazardous waste. Liquid GAC vessels were purchased by TRS and will be removed with their other remaining equipment. These GAC shipments are detailed in Section 3.0. Roll-off dumpsters containing soil cuttings and personal protective equipment (PPE)/miscellaneous trash that had contacted soil and water were removed from the site between October 20-23, 2003. Ten dumpsters were shipped off-site as non-hazardous waste, and one was removed for asphalt batching on October 24, 2003, as detailed in Section 3.0.

Reuseable items that were purchased by TtEC during site work and may be used in the future were placed into the Antenna Range Building. Electrical power was disconnected from the PCU on December 19, 2003, and the office trailer was removed from the site on January 26, 2004.

The TMPs and electrodes remain installed, with CPVC oversleeves and drip tubing remaining intact for possible future full-scale ERH operations. Groundwater monitoring wells were capped as previously, and flush mount lids were replaced.

ND05-89-004 4/26/05

2.7 Long-Term Groundwater Monitoring

2.7.1 Long-Term Groundwater Sampling

A long-term groundwater monitoring event was conducted by TtEC between April 13 and 14, 2004, more than six months after the completion of the heating. The purpose of the long-term monitoring was to evaluate the long-term effectiveness of the thermal treatment remediation at Site 4 and obtain information on the geological and chemical processes of the groundwater system after the thermal treatment. The two replacement wells (MW-18SR and MW-42SR) and the seven newly-installed wells (MW-60S, MW-61S, MW-62S, MW-63S, MW-64S, MW-65S, and MW-66S) were sampled using a peristaltic pump. The long-term monitoring groundwater samples were collected using the same low-flow procedures as the pre-treatment sampling described in Section 2.1.2. One sample was collected from each of the monitoring wells with the exception of MW-62S from which one sample and one duplicate were collected, resulting in a total of 10 groundwater samples.

Samples were collected from all wells for TCL VOC and SVOCs (2-methylnaphthalene only) in laboratory-preserved sample containers. Samples were immediately placed in a cooler with ice following sampling. The water quality parameters were measured during the well purging. All sampling details were recorded on well purge data forms and in the site logbook. The well purge data forms are included in Appendix D.

2.7.2 Long-Term Groundwater Monitoring Results

Groundwater samples collected during the long-term monitoring event were analyzed by Woods Hole Group Laboratories, Raynham, MA for TCL VOCs using USEPA Method 8260B and SVOCs (2-methylnaphthalene only) using USEPA Method 8270C. Table F-1 in Appendix F contains tabulated analytical results for the long-term monitoring groundwater samples collected.

As indicated in Table F-1 in Appendix F, among the nine monitoring wells that were sampled during the long-term monitoring, total VOCs ranged from 51.3 ug/L (MW-42SR) to 2,582 ug/L (MW-63S), total BTEX ranged from 35.2 ug/L (MW-42SR) to 2,047 ug/L (MW-63S), benzene ranged from non-detect (MW-61S) to 91 ug/L (MW-66S), and 2-methylnaphthalene ranged from 0.25 ug/L (MW-61S) to 76 ug/L (MW-64S). Results from the long-term monitoring sampling rounds will be compared with data from other sampling rounds in Section 4.1 to evaluate the effectiveness of the Site 4 thermal treatment remediation and whether the site-specific clean-up goal was achieved.

ND05-89-004 4/26/05

3.0 WASTE MANAGEMENT

Waste materials were generated during mobilization, remediation activities, and demobilization. The methods used to manage the materials are described in the Work Plan. The following sections describe the quantities of waste materials generated and disposition of these materials. Note that waste streams were the result of the combined Site 3 thermal treatment pilot test and Site 4 thermal treatment remediation. Appendix H contains copies of waste management tracking summary sheets.

3.1 Vapor Collection, Storage, and Disposal

As described in the Work Plan, vapor-phase GAC was used to collect VOCs from the extracted vapor during the thermal treatment. On September 5, 2003, the two primary GAC vessels were removed from service. After removing a GAC vessel from service, the spent carbon within it was removed from the unit and stored on-site in fabric bags for transport off-site. This carbon was sampled on September 5, 2003 and found to be hazardous waste. One spent carbon shipment was made; Appendix H indicates the details regarding this shipment. Four GAC vessels, each capable of holding 1,000 lbs of GAC, and two fabric bags, each holding 1,000 lbs of GAC, were transported off-site as hazardous waste for regeneration at Westates Carbon Arizona's facility in Parker, Arizona on November 12, 2003.

GAC usage was tracked using a PE Photovac MicroFID and by the total days each GAC unit was in service. The GAC usage log is contained in Appendix H.

The GAC system was used during the Site 4 remediation to continuously reduce VOCs in the air effluent stream to the target level of 95% (by weight) (see the Work Plan). Table 3-1 presents the GAC adsorption efficiency as determined by the summa canister vapor sampling events conducted weekly throughout the test. The GAC adsorption efficiency was measured to be greater than 95% in all but one of the seven sampling events. The date during which GAC adsorption efficiency was measured to be low was on August 28, 2003, and this value was 91.8%.

Table 3-1 GAC Adsorption Efficiency

Sampling Date Site 3 Influent Total VOCs (ppbv)		otal VOCs Total VOCs		Combined Effluent Total VOCs (ppbv)	Adsorption Efficiency (%)
07/31/03	18,230	14,752	32,982	28.1	99.91%
08/07/03	10,927	4,808	15,735	21.9	99.86%
08/14/03	108,640	3,793.2	112,433	52.8	99.95%
08/22/03	221,130	8,452	229,582	9,994	95.65%
08/28/03	147,400	79,420	226,820	18,520	91.83%
09/06/03	26,820	12,423	39,243	212.5	99.46%
09/11/03	40,620	116,020	156,640	544.9	99.65%

Note:

Analytical data for Site 4 influent and combined effluent are presented in Tables G-1 and G-2 respectively in Appendix G and summarized in Table 2-2. Analytical data for Site 3 influent are discussed in the Closeout Report for Site 3.

3.2 Soil Collection, Storage, and Disposal

Drill cuttings, consisting of soil only, were generated during the installation of electrodes/VR wells, groundwater monitoring wells, TMPs, and during VR operations (through becoming entrained in groundwater that was extracted). The soil was placed into four plastic-lined 25-yard (23 feet by 8 feet by 75 inches) roll-off containers, three of which were staged in the rear portion of the Site 3 parking lot. One other container was staged on Site 4 near the ERH treatment area. Soils from both the Site 3 ERH Pilot Test and Site 4 ERH treatment were combined in these containers. Waste characterization samples of the soil wastes were collected on August 6, 2003 and October 10, 2003, and most of the soils were found to be of non-hazardous nature. One roll-off was found to contain soils with contaminant concentrations that qualified it for use in asphalt batching. For shipment purposes, soils were stabilized using a polymer material (N²'s Waste Loc 770) and redistributed among eleven 25-yard roll-off containers. Ten of these containers were shipped off-site as non-hazardous waste between October 20-23, 2003 to Waste Management of New Hampshire's disposal facility in Gonic, New Hampshire. The last container was shipped off-site for asphalt batching on October 24, 2003 to Environmental Soil Management's facility in Loudon, New Hampshire. Appendix H provides details regarding these shipments.

3.3 Water Collection, Storage, and Disposal

Water was generated during the installation of electrodes/VR wells, groundwater monitoring wells, and TMPs, well development, groundwater sampling, and VR operation activities. During installation of components, groundwater monitoring well development, and baseline groundwater sampling, approximately 45,000 gallons of water (from both Sites 3 and 4 activities) was generated and stored in 21,000-gallon steel storage tanks. This water was pumped to a groundwater treatment facility located on-site for treatment and subsequent discharge into the Bedford sewage system. Prior to pumping of this water, it was sampled on June 3, 2003 and for VOCs only on July 16, 2003 and found to be acceptable for treatment at this facility. Approximately 71,300 gallons of groundwater and condensate were removed from VR wells during VR operations. Of this amount, approximately 37,500 gallons was recycled as drip water, placed back into the subsurface to maintain saturated conditions in soil adjacent to electrodes. The remainder was utilized as cooling water for the condenser. No excess condensate/groundwater required temporary storage on-site.

Any condensate/groundwater generated during VR operations was treated using liquid-phase GAC prior to its being recycled as drip water or as cooling water. This GAC was sampled on September 5, 2003 and found to be non-hazardous. It was shipped off-site in three United States Department of Transportation (USDOT) Type UN1A2 steel drums as spent non-hazardous GAC for regeneration on November 19, 2003 to US Filter's facility in Avon, Massachusetts. See Appendix H for details regarding this shipment.

3.4 PPE Collection, Storage, and Disposal

PPE used during the thermal treatment remediation was containerized as it was generated into several USDOT Type UN1A2 steel drums along with other general debris that had come into contact with soils or water (plastic, sampling equipment, etc.). The mixed trash was integrated into the soils during their stabilization by the use of polymers and sent off-site for disposal as non-hazardous waste with the soil containers to Waste Management of New Hampshire's disposal facility in Gonic, New Hampshire between October 20-23, 2003 (Appendix H).

4.0 DATA ANALYSIS AND CONCLUSIONS

The following sections present data analysis and conclusions for the Site 4 thermal treatment remediation. Section 4.1 discusses the chemical data collected from the four groundwater sampling rounds as well as the seven vapor sampling events. Section 4.2 assesses whether the objectives of the remediation were met and presents conclusions, and Section 4.3 provides recommendations for the Site 4 thermal treatment remediation project.

4.1 Analysis of Chemical Data for Groundwater and Vapor Samples

Groundwater levels of the monitoring wells were periodically measured by TtEC prior to and after the heating phase. Due to the potential for release of steam, groundwater levels could not be measured during the heating. The groundwater level data are presented in Figure 4-1. As indicated by Figure 4-1, the water levels in the nine monitoring wells inside and outside the treatment area generally followed the same trend. The pre-treatment groundwater levels in these wells measured on May 29, 2003 ranged from 11.25 ft (MW-65S) to 20.30 ft (MW-60S) below top of the carbon steel riser. The water levels measured immediately after the heating on September 29, 2003 indicated that groundwater levels dropped approximately five feet compared to the pre-treatment levels. It is not clear whether this water level drop was due to seasonal groundwater fluctuation, evaporation of the groundwater caused by heating, or a combination of both effects. Groundwater levels measured approximately a year later on August 6, 2004 showed slightly higher water levels than those measured on September 29, 2003 (see Figure 4-1). During the one-year period after the heating was completed, groundwater levels rose and fluctuated following their seasonal patterns.

Groundwater generally flows in a north-westerly direction across the Site 4 treatment area as shown in Figure 4-2. A significant water drop was not observed in the monitoring wells inside the treatment area during the mid-process sampling and immediately following the heating. This suggests that a temporary alteration of the groundwater flow caused by a depression of water table observed at Site 3 during and immediately after the heating did not occur at Site 4. It is assumed that the original north-westerly groundwater flow remained the dominant flow pattern during the heating and after the heating was completed.

As discussed in Section 2, four groundwater sampling rounds including pre-treatment, mid-process, post-treatment, and long-term monitoring sampling were performed for the three monitoring wells (MW-18SR, MW-63S, and MW-65S) located inside the treatment area. A discussion of the groundwater data for the three wells will be presented in Section 4.1.2. Monitoring wells on the periphery of the treatment area (MW-61S, MW-62S, and MW-64S) and wells adjacent to the treatment area (MW-42SR, MW-60S, and MW-66S) were sampled during the pre-treatment, post-treatment, and long-term monitoring sampling rounds. Data interpretation for these wells will be presented in Section 4.1.3.

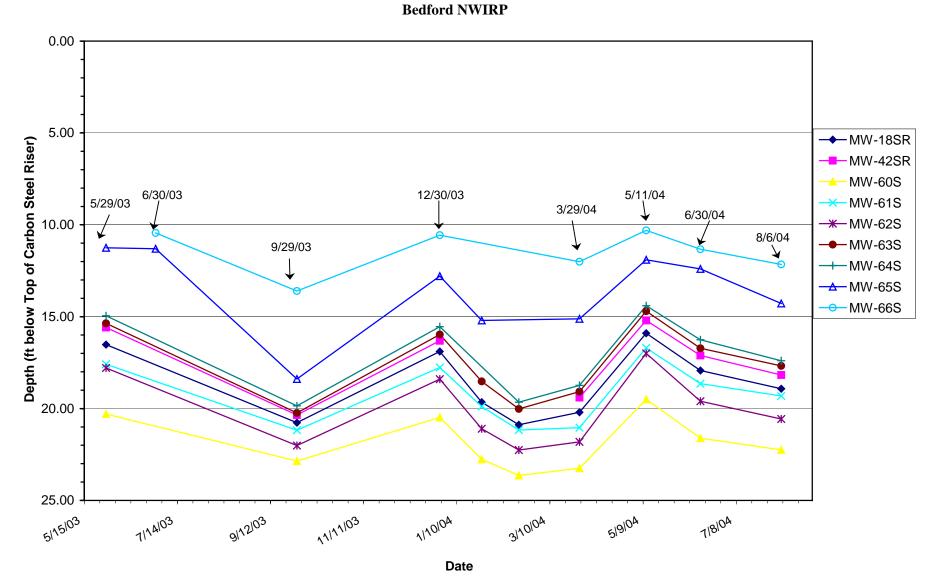
For the convenience of data analysis and presentation in this Closeout Report for Site 4, the analytical results of the four COCs (i.e., BTEX), as well as total VOCs and total BTEX, are summarized in Table 4-1 through Table 4-9 for the nine monitoring wells sampled at Site 4. In addition, analytical results for the four COCs for the nine wells are presented graphically in Figure 4-3 through Figure 4-11.

Analytical results for the vapor samples collected during the seven Summa canister sampling events is discussed in Section 4.1.4.

4-1

ND05-89-004 4/26/05

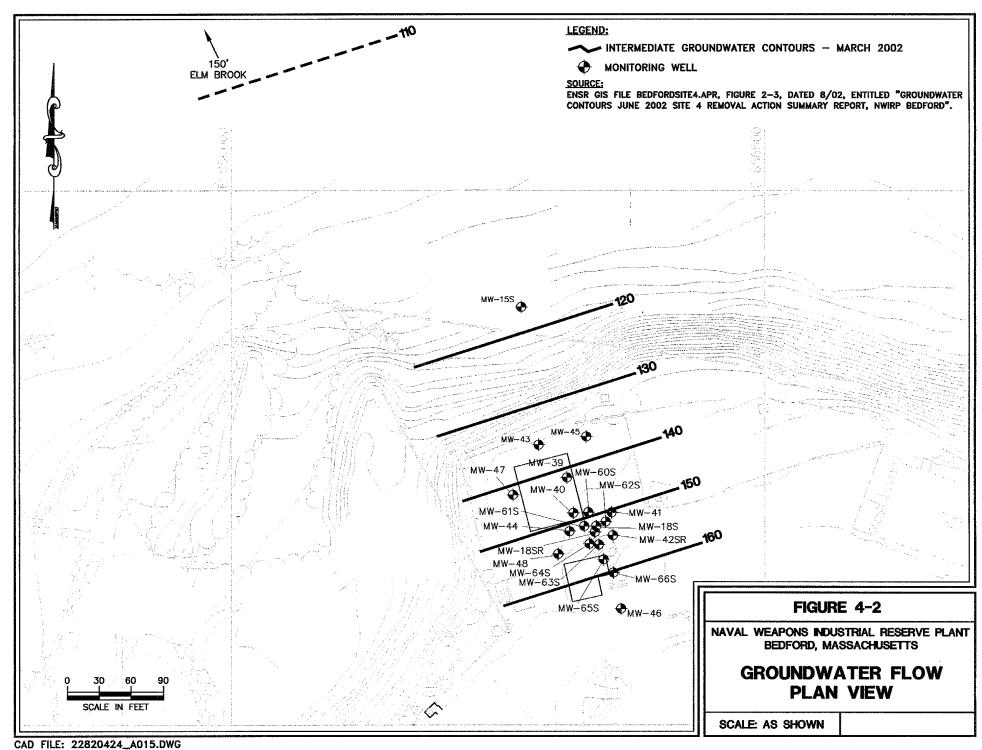
Figure 4-1
Groundwater Levels
Monitoring Wells Located in or Adjacent to Site 4 ERH Zone



4-2

ND05-89-004

4/26/05



4.1.1 Physical, Chemical and Biological Processes in Groundwater at Site 4

Physical, chemical and biological processes that may have affected the concentrations of contaminants in the Site 4 groundwater are recharge, rebound, increased dissolution/solubility, and biodegradation. These processes are described in the following sections.

4.1.1.1 Recharge

For the purpose of this Closeout Report for Site 4, recharge is defined as groundwater from other areas (e.g. upstream) flowing into the areas of interest. Depending on the concentration of contaminants in the groundwater flowing into the area of interest, an increase, decrease, or no change in concentration of contaminants within the area of interest may be observed.

In the case of Site 4 remediation, an effort was made to extend the treatment area far enough upstream to treat all areas of contaminated groundwater, thereby minimizing potential increases in concentration due to recharge after the thermal treatment.

4.1.1.2 Rebound

For the purpose of this Closeout Report for Site 4, rebound is defined as a contaminant concentration increase in the groundwater inside the treatment area as a result of soil-sorbed contaminants that were not completely removed from the treatment zone re-entering into the groundwater after the thermal treatment. Following the heating, the water-dissolved and soil-bound contaminants would gradually reach an equilibrium during which soil-bound contaminants may partition into the groundwater, causing observed increase in groundwater contaminant concentration in the treatment zone.

4.1.1.3 Increased Dissolution/Solubility

Increased dissolution/solubility is defined as an increase in groundwater contaminant concentration as a result of soil-sorbed contaminants dissolving into the groundwater at an increased rate due to enhanced contaminant solubility in the heated water. This process was thought to occur mostly in areas outside the treatment zone during and immediately after the heating. Groundwater and soil in these areas experienced an increase in temperature and thereby enhanced the dissolution of soil-bound contaminants into the groundwater. However, because these areas were outside or on the periphery of the treatment area, the groundwater temperature in these areas did not rise to a high enough degree for a long enough time to completely volatilize and remove the contaminants. The net result of this solubility enhancement and incomplete removal was the contaminant increase observed in some monitoring wells outside the treatment area during the post-treatment sampling round.

4.1.1.4 Biodegradation

Another process that is thought to be occurring in the groundwater following the heating is biodegradation. Biological breakdown of BTEX and other hydrocarbon compounds by bacteria in groundwater under aerobic (oxygenated) and anaerobic conditions has been widely reported. BTEX can be degraded rapidly by aerobic bacteria, but under anaerobic conditions biodegradation of BTEX is relatively slow (Reinhard et al. 1997).

It is generally believed that natural biological breakdown process ceases during the heating phase due to the extremely high temperature at about 100°C. After the heating the biological activity begins to increase as the groundwater cools down and would eventually exceed pre-heating biodegradation rates as a result of the warmer groundwater. It is believed that following the completion of the heating at Site 4, biodegradation of BTEX compounds occurred at an increased rate compared to the pre-treatment rate.

4.1.2 Monitoring Wells Inside the Treatment Area (MW-18SR, MW-63S, MW-65S)

The analytical results of the four COCs (BTEX) as well as total VOCs and total BTEX for MW-18SR, MW-63S, and MW-65S are summarized in Tables 4-1, 4-2, and 4-3, respectively. Analytical results for the four COCs for the wells are also plotted in Figures 4-3, 4-4, and 4-5, respectively. The depth of MW-18SR was 28 ft bgs, and the screened interval was 18 ft to 28 ft bgs. MW-63S, with a well depth of 24 ft bgs and a screened interval of 14 ft to 24 ft bgs, was installed on May 16, 2003. MW-65S, with a well depth of 23 ft bgs and a screened interval of 13 ft to 23 ft bgs, was installed on May 17, 2003. Of the three monitoring wells, MW-18SR was on the downstream side of the treatment area; MW-63S was in the center of the treatment area; and MW-65S was on the upstream side of the treatment area (see Figure 1-3).

As indicated by the pre-treatment groundwater results in Tables 4-1, 4-2, and 4-3, as well as Table F-1 in Appendix F, MW-63S demonstrated the highest pre-treatment total BTEX (19,080 ug/L) among the ten monitoring wells sampled during the pre-treatment sampling round. MW-65S also showed high BTEX concentrations at 16,520 ug/L, while MW-18SR had moderate BTEX level at 8,720 ug/L. The pre-treatment groundwater results for MW-63S and MW-65S were consistent with the pre-treatment soil sampling results. Soil samples from these two wells demonstrated the highest total BTEX values (419,000 ug/kg and 346,000 ug/kg respectively) among the seven newly-installed monitoring wells (see Table E-1 in Appendix E). MW-18SR was a replacement well, and no soil sample was collected from the well. In addition, the pre-treatment data for these wells indicated that BTEX compounds composed a major portion of total VOCs, consistent with the site history of contamination from petroleum products.

Significant reduction of groundwater BTEX compounds during the heating (see mid-process data in Tables 4-1 through 4-3) and immediately following the heating (see post-treatment data in Tables 4-1 through 4-3) was observed in the three wells, with reduction rates close to or above 95% for most of the individual COCs and total BTEX. Benzene, the key indicator of remediation performance at Site 4, was at 3.3 ug/L, non-detect, and 6.2 ug/L in MW-18SR, MW-63S, and MW-65S respectively, significantly below the remediation action objective of 50 ug/L.

In addition, unlike the pre-treatment data, the mid-process and post-treatment groundwater results for the three wells showed total BTEX composed only a small portion of total VOCs. A close examination of the mid-process and post-treatment results for individual compounds (see Table F-1 in Appendix F) indicated detections of acetone at higher concentrations than most of the other positively-detected compounds in the mid-process and post-treatment samples. Acetone was probably a by-product of the heating process, and was detected at similar concentration levels in the mid-process and post-test samples collected during the Site 3 pilot test study.

Tables 4-1 through 4-3 showed that compared with the post-treatment groundwater results, total BTEX generally increased in the long-term monitoring samples of the three monitoring wells collected approximately six months after the completion of the heating. With the exception of toluene in MW-18SR and MW-63S, and ethylbenzene in MW-65S, the concentrations of individual COCs all increased to a certain extent in the long-term monitoring samples compared to the results in the post-treatment samples. Nevertheless, benzene, the key indicator of remediation performance at Site 4, was at 41 ug/L, 26 ug/L, and 40 ug/L in MW-18SR, MW-63S, and MW-65S respectively during the long-term monitoring. These benzene concentrations were below the remediation action objective of 50 ug/L.

Table 4-1 MW-18SR Contaminants of Concern

Sample Location						MW-185	SR				
Date Collected	6/2/20	003		9/9/20	03	9/30/2003			4/14/2004		
Sampling Event	Pre-Trea	tment		Mid-Pro	cess	P	ost-Trea	tment	Long	g-Term N	Monitoring
Sample Collection Method	perista pum			perista pum		peristaltic pump			peristaltic pump		
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment
Comtaminants of Concern (COCs)											
Benzene	220		2.0	U	99.5%	3.3	J	98.5%	41		81.4%
Ethylbenzene	1200		3.1		99.7%	15		98.8%	650		45.8%
Toluene	2200		6.8		99.7%	24		98.9%	13		99.4%
Xylene	5100		20.7		99.6%	104		98.0%	850		83.3%
Total VOCs	9180		226.1		97.5%	1040		88.7%	1961		78.6%
Total BTEX	8720		30.6		99.6%	146		98.3%	1554		82.2%
2-Methylnaphthalene	42		NA			NA]		37]	

Figure 4-3 MW-18SR Contaminants of Concern

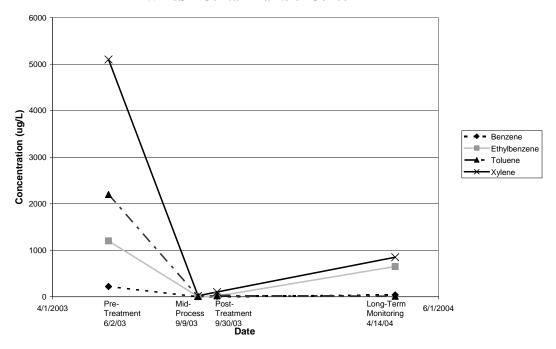


Table 4-2 MW-63S Contaminants of Concern

Sample Location	•		•	•		MW-635	3	•		•	
Date Collected	6/2/2	003		9/9/2	003	10/1/2003			4/14/2004		
Sampling Event	Pre-Trea	tment		Mid-Pro	ocess	Post-Treatment			Long-Term Monitoring		
Sample Collection Method	perist pun			perist pun			perista pum		peristaltic pump		
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment
Comtaminants of Concern (COC	Comtaminants of Concern (COCs)										
Benzene	180		10	U	97.2%	20	U	94.4%	26		85.6%
Ethylbenzene	1600		6.0	J	99.6%	25		98.4%	430		73.1%
Toluene	4400		14		99.7%	27		99.4%	27		99.4%
Xylene	12900		38.0		99.7%	86		99.3%	1590		87.7%
Total VOCs	19785		2332.0		88.2%	871		95.6%	2582		86.9%
Total BTEX	19080		58.0		99.7%	138		99.3%	2073		89.1%
2-Methylnaphthalene	44		NA			NA			60		

Figure 4-4 MW-63S Contaminants of Concern

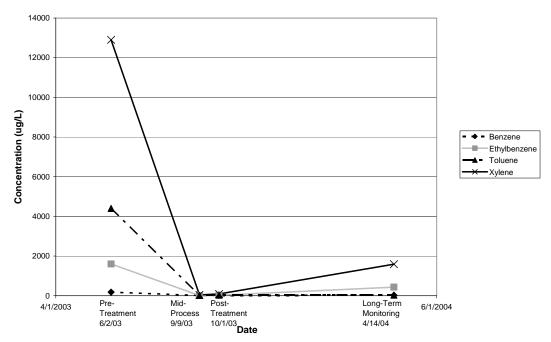
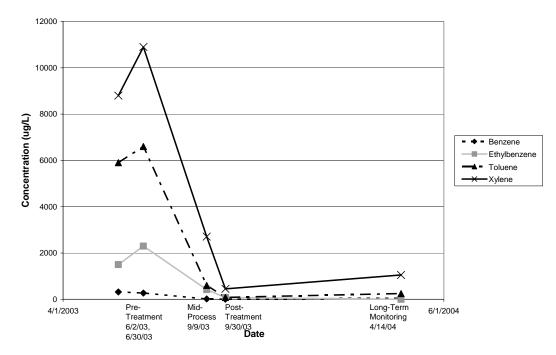


Table 4-3 MW-65S Contaminants of Concern

Sample Location		MW-65S														
Date Collected	6/2/2	003	6/30/2	003		9/9/2	2003	9/9/03, Duplicate 9/30/2003					4/14/2004			
Sampling Event	Sampling Event Pre-Treatment (1) Pre-Treatment (2) Mi		Mid-P	rocess	Mid-Pr	ocess		Post-Tr	eatment	Long-Term Monitoring						
Sample Collection Method	perist pun			peristaltic pump		peristaltic pump			peristaltic pump		peristaltic pump			peristaltic pump		
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment (1)	Conc. (ug/L)	Qual.	Conc.	Qual.	%Reduction from Pre- Treatment (1)	Conc.	Qual.	%Reduction from Pre- Treatment (1)	
	Comtaminants of Concern (COCs)															
Benzene	320		270		18	J	94.4%	14	J	6.2	J	98.1%	40		87.5%	
Ethylbenzene	1500		2300		420		72.0%	370		78		94.8%	2	U	99.9%	
Toluene	5900		6600		600		89.8%	520		81		98.6%	250		95.8%	
Xylene	8800		10900		2710		69.2%	2380		450		94.9%	1050		88.1%	
Total VOCs	17080		20999		5488		67.9%	4764		1124.1		93.4%	1560.2		90.9%	
Total BTEX	16520		20070		3748		77.3%	3284		615.2		96.3%	1342		91.9%	
		-		-			·	-							`	
2-Methylnaphthalene	34		80		NA			NA		NA			14			

Figure 4-5 MW-65S Contaminants of Concern



Compared to the post-treatment results, the increases of BTEX concentrations in the long-term monitoring samples may be explained by the combined effects of recharge of groundwater from other areas and rebound from soil-sorbed contaminants. The upstream groundwater that was not treated by ERH may still contain low levels of contaminants that may have been recharged into the wells inside the treatment area. However, the total BTEX concentrations in the long-term monitoring samples of MW-18SR, MW-63S, and MW-65S were at 1,554 ug/L, 2,073 ug/L, and 1,342 ug/L respectively, approximately two to three times of the BTEX concentration (655 ug/L) in MW-66S located upstream and outside the treatment area. This suggests that recharge alone could not account for all the BTEX increase in the long-term monitoring samples collected inside the treatment area.

The other process that may have contributed to the observed BTEX increase during the long-term monitoring was rebound. It is possible that the thermal treatment had not completely removed BTEX from the heavily-contaminated soils, and therefore some amount of soil-bound BTEX compounds may have been left in place inside the treatment area. During the six-month period between the post-treatment and long-term monitoring, the remaining soil-bound contaminants could have partitioned into the groundwater as the system was reestablishing groundwater-soil concentration equilibrium, resulting in the observed BTEX increase in groundwater.

In addition, biodegradation may also have occurred in the groundwater and soil during this period. However, the biodegradation breakdown of BTEX may not be fast enough to offset the concentration increase caused by the other two processes (recharge and rebound) mentioned above.

4.1.3 Monitoring Wells on the Periphery of or Outside the Treatment Area

Monitoring wells outside the treatment area include MW-42SR, MW-60S, MW-61S, MW-62S, MW-64S, and MW-66S that were on the periphery of or outside the treatment area (see Figure 1-3). Monitoring wells with similar contaminant distribution patterns will be grouped together in the following data discussions.

4.1.3.1 MW-61S and MW-64S

The analytical results of the four COCs (BTEX) as well as total VOCs and total BTEX for MW-61S and MW-65S are summarized in Tables 4-4 and 4-5 respectively. Analytical results for the four COCs are also plotted in Figures 4-6 and 4-7 respectively. MW-61S, with a well depth of 25 ft bgs and a screened interval of 15 ft to 25 ft bgs, was installed on May 15, 2003. MW-64S, with a well depth of 24 ft bgs and a screened interval of 14 ft to 24 ft bgs, was installed on May 16, 2003. As can be seen in Figure 1-3, MW-61S was located in the north side (downstream) of the west periphery of the treatment area, and MW-64S was in the center of the west periphery of the treatment area.

As indicated by the pre-treatment groundwater results in Tables 4-4 and 4-5 and Table F-1 in Appendix F, MW-61S and MW-64S demonstrated high pre-treatment total BTEX at 16,776 ug/L and 12,143 ug/L respectively. The pre-treatment soil sampling results also showed that soil samples from MW-61S and MW-64S had relatively high BTEX concentrations at 113,400 ug/kg and 87,700 ug/kg respectively. These values were approximately one-fourth of total BTEX observed in the pre-treatment soil samples collected from MW-63S and MW-65S that were located inside the treatment area (see Table E-1 in Appendix E).

Table 4-4
MW-61S Contaminants of Concern

Sample Location					MW-61S						
Date Collected	5/30/20	003		9/30/20	03	4/13/2004					
Sampling Event	Sampling Event Pre-Treatment			Post-Treat	ment	Long	g-Term Mo	nitoring			
Sample Collection Method	perista pum			peristaltic pump			peristaltic pump				
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment			
Comtaminants of Concern (COCs)											
Benzene	76	J	14	J	81.6%	2	U	98.7%			
Ethylbenzene	290		650		-124.1%	2	U	99.7%			
Toluene	3800		830		78.2%	2	U	100.0%			
Xylene	12600		5200		58.7%	50		99.6%			
Total VOCs	17306	I	7281		57.9%	63.2		99.6%			
Total BTEX	16766		6694		60.1%	56		99.7%			
2-Methylnaphthalene	42		NA			0.25	U				

Figure 4-6 MW-61S Contaminants of Concern

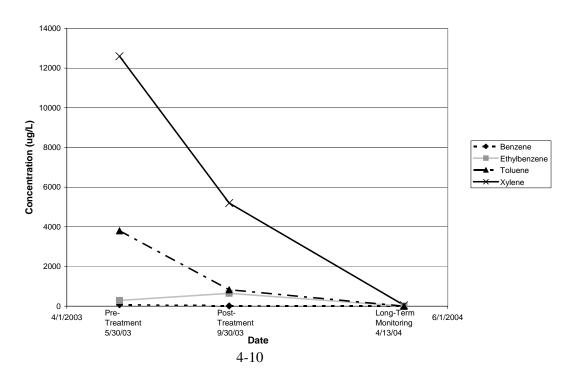
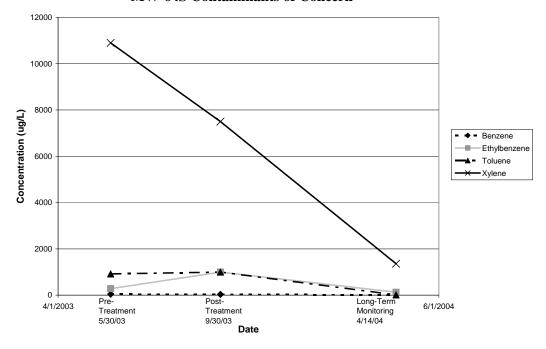


Table 4-5 MW-64S Contaminants of Concern

Sample Location					MW-64S				
Date Collected	5/30/20	003		9/30/200	3	4/14/2004			
Sampling Event	Sampling Event Pre-Treatment			ost-Treatn	nent	Long	-Term Mo	nitoring	
Sample Collection Method	perista pum			peristaltic pump			peristali pump		
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	
Comtaminants of Concern (COC	s)								
Benzene	43		32	J	25.6%	4.4		89.8%	
Ethylbenzene	280		1000		-257.1%	130		53.6%	
Toluene	920		1000		-8.7%	13		98.6%	
Xylene	10900		7500		31.2%	1360		87.5%	
Total VOCs	12887		14114		-9.5%	2002.1		84.5%	
Total BTEX	12143		9532		21.5%	1507		87.6%	
2-Methylnaphthalene	60		NA			76			

Figure 4-7
MW-64S Contaminants of Concern



In the post-treatment groundwater sample for MW-61S, benzene, toluene, and xylene demonstrated reduction rates of 81.6%, 78.2%, and 58.7% respectively compared to their pre-treatment levels, while ethylbenzene increased to 650 ug/L from its pre-treatment level of 290 ug/L. The post-treatment results for MW-64S generally demonstrated the same trend as MW-61S. However, in MW-64S, the reduction rates for benzene and xylene were at 25.6% and 31.2% respectively, lower than those in MW-61S. In addition, in the post-treatment sample for MW-64S, toluene remained at the same level as in the pre-treatment sample, and ethylbenzene increased to 1,000 ug/L from its pre-treatment level of 280 ug/L. Benzene concentrations in the post-treatment samples for MW-61S and MW-64S were at 14 ug/L and 30 ug/L respectively, below the remediation action objective of 50 ug/L.

The reduced reduction of contaminants in groundwater observed in MW-61S and MW-64S during the post-treatment sampling round may be attributed to their locations on the periphery of the treatment area. The groundwater and soil surrounding the two wells may have received some thermal treatment during the heating, but the treatment may not have been enough to remove all the contaminants in the groundwater and soil. Furthermore, immediately after the heating, the hot (but not boiling) water may have led to more soil-bound contaminants to be dissolved into the groundwater, thus increasing the groundwater BTEX concentrations (most notably ethylbenzene) in the post-treatment samples.

The groundwater concentrations of BTEX compounds in the long-term monitoring samples for MW-61S and MW-64S decreased significantly compared with the concentration levels in their pre-treatment and post-treatment samples. Benzene was at a low concentration level of non-detect and 4.4 ug/L in MW-61S and MW-64S respectively during the long-term monitoring, below the remediation action objective of 50 ug/L. Located in the downstream part of the treatment zone, MW-61S and MW-64S may have been receiving groundwater from upstream which was believed to contain low levels of contaminants. The recharge of relatively clean groundwater from upstream may partially be responsible for the significant decrease in contaminant concentrations observed in MW-61S and MW-64S during the long-term monitoring. Biodegradation may have also played a significant role in the reduction of soil and groundwater contaminants in MW-61S and MW-64S during the period between the post-treatment sampling and long-term monitoring.

It is also noted that although MW-61S and MW-64S showed a similar contaminant variation pattern, MW-61S demonstrated a more complete contaminant reduction than MW-64S, especially in the long-term monitoring sampling round. The total BTEX in the long-term monitoring sample for MW-61S was at a low level of 56 ug/L, while the corresponding BTEX concentration in MW-64S was at a moderate level of 1,507 ug/L. The total BTEX value in MW-64S was comparable to concentrations observed in the wells inside the treatment area (MW-18SR, MW-63S, and MW-65S) during the same sampling period.

4.1.3.2 MW-42SR, MW-60S, and MW-62S

The analytical results of the four COCs (BTEX) as well as total VOCs and total BTEX for MW-42SR, MW-60S, and MW-62S are summarized in Tables 4-6, 4-7, and 4-8 respectively. Analytical results for the four COCs for the three wells are also plotted in Figures 4-8, 4-9, and 4-10 respectively. MW-42SR has a well depth of 25 ft bgs and a screened interval of 15 ft to 25 ft bgs. MW-60S, with a well depth of 26 ft bgs and a screened interval of 16 ft to 26 ft bgs, was installed on May 14, 2003. MW-62S, with a well depth of 26 ft bgs and a screened interval of 16 ft to 26 ft bgs, was installed on May 15, 2003. As can be seen in Figure 1-3, MW-42SR was located adjacent to the center of the east periphery of the treatment area; MW-60S was adjacent to the north periphery of the treatment area; and MW-62S was in the corner of the east and north periphery of the treatment area.

Table 4-6 MW-42SR Contaminants of Concern

Sample Location					MW-42SR						
Date Collected	6/2/20	03		9/30/200	3	4/13/2004					
Sampling Event	Pre-Treat	tment	Po	ost-Treatr	ment	Long-Term Monitoring					
Sample Collection Method	perista pum			peristaltic pump			peristalt pump				
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment			
Comtaminants of Concern (COC	Comtaminants of Concern (COCs)										
Benzene	14		20		-42.9%	2.2		84.3%			
Ethylbenzene	34		65		-91.2%	15		55.9%			
Toluene	1.5	J	7.4	J	-393.3%	2	U	33.3%			
Xylene	23.2		89		-283.6%	16		31.0%			
Total VOCs	122.6		259.4		-111.6%	51.3		58.2%			
Total BTEX	72.7		181.4		-149.5%	35.2		51.6%			
2-Methylnaphthalene	5.8		NA			0.27	U				

Figure 4-8 MW-42SR Contaminants of Concern

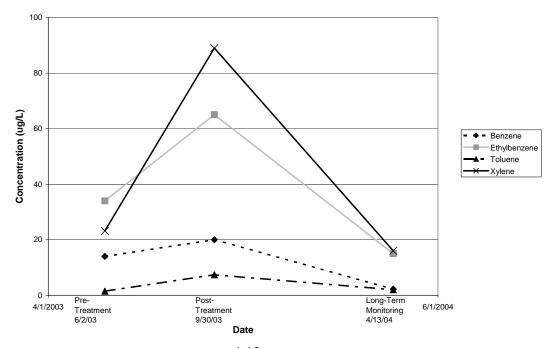


Table 4-7 MW-60S Contaminants of Concern

Sample Location					MV	V-60S		MW-60S										
Date Collected	5/29/20	003	5/29/03, Du	plicate		9/29/200	03	4/14/2004										
Sampling Event	Sampling Event Pre-Treatment		Pre-Treat	ment	F	ost-Treat	ment	Long-Term Monitoring										
Sample Collection Method	peristaltic pump		peristaltic pump			peristal pump		peristaltic pump										
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment	Conc. (ug/L)	Qual.	%Reduction from Pre- Treatment								
Comtaminants of Concern (COCs)																		
Benzene	250		250		140	J	44.0%	7.6		97.0%								
Ethylbenzene	1600		1700		2100		-31.3%	97		93.9%								
Toluene	1800		2300		670		62.8%	1.3	J	99.9%								
Xylene	4700		5600		5700		-21.3%	32.5		99.3%								
Total VOCs	8826		10550		9309		-5.5%	196.3		97.8%								
Total BTEX	8350		9850		8610		-3.1%	138.4		98.3%								
2-Methylnaphthalene	30		39		NA			6.9										

Figure 4-9
MW-60S Contaminants of Concern

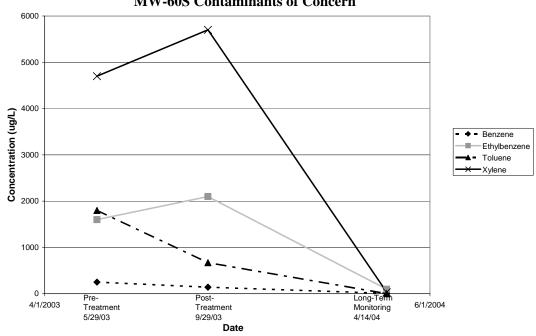
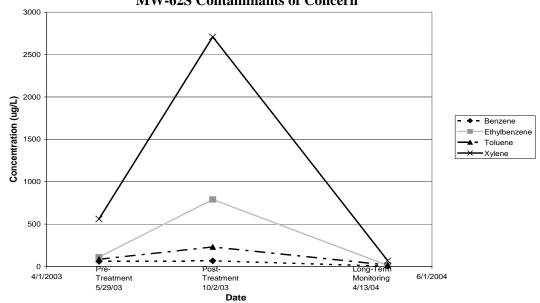


Table 4-8 MW-62S Contaminants of Concern

Sample Location					MW	-62S				
Date Collected	5/29/20	003		10/2/200)3		4/13/20	04	4/13/04, Duplicate	
Sampling Event	Pre-Trea	tment	P	ost-Treat	ment	Long	-Term Mo	Long-Term Mo	nitoring	
	perista	ıltic		peristal	tic		peristal	tic	peristaltic	
Sample Collection Method	pum	р		pump			pump)	pum	р
					%Reduction			%Reduction		
					from Pre-			from Pre-		
Analyte	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	Treatment	Conc. (ug/L)	Qual.	Treatment	Conc. (ug/L)	Qual.
Comtaminants of Concern (COCs)										
Benzene	59		66	J	-11.9%	3.4		94.2%	3.5	
Ethylbenzene	110		790		-618.2%	12		89.1%	12	
Toluene	85		230		-170.6%	17		80.0%	17	
Xylene	560		2710		-383.9%	67		88.0%	67	
Total VOCs	980		4509		-360.1%	119.1		87.8%	119.7	
Total BTEX	814		3796		-366.3%	99.4		87.8%	99.5	
		•			•					
2-Methylnaphthalene	29	•	NA	•		4.6			2.2	·

Figure 4-10 MW-62S Contaminants of Concern



As indicated by the pre-treatment groundwater results in Tables 4-6, 4-7, and 4-8, MW-60S demonstrated a moderate pre-treatment total BTEX concentration (8,350 ug/L) comparable to total BTEX in MW-18SR located inside the treatment area. MW-42SR and MW-62S showed low pre-treatment total BTEX concentrations at 72.7 ug/L and 814 ug/L respectively. The pre-treatment soil sampling results indicated that total BTEX in the soil sample from MW-60S was at a relative high level of 139,600 ug/kg, while the soil sample from MW-62S had total BTEX at a low level of 900 ug/kg. No soil sample was collected from replacement well MW-42SR.

In the post-treatment groundwater sample for MW-60S, benzene and toluene demonstrated reduction rates of 44.0% and 62.8% respectively compared to their pre-treatment levels, while ethylbenzene and xylene increased slightly relative to the pre-treatment results. MW-42SR and MW-62S showed similar increase in concentrations of all the four COCs in post-treatment samples compared with their pre-treatment levels. Benzene concentration in the post-treatment sample for MW-42S was at 20 ug/L, below the remediation action objective of 50 ug/L. However, post-treatment benzene concentrations for MW-60S and MW-62S were at 140 ug/L and 66 ug/L respectively, exceeding the remediation action objective.

The general increase in contaminant concentrations observed in the post-treatment samples for MW-42SR, MW-60S, and MW-62S may be attributed to the dissolution of originally soil-bound contaminants into the post-treatment groundwater. Due to their locations on the periphery of or outside the treatment area, these three wells may have received some heating during the thermal treatment, but the heating was not enough to completely remove the contaminants in the groundwater and soil. During and immediately after the heating, the warmer temperature in the surrounding groundwater and soil may have resulted in more soil-bound contaminants being dissolved into the groundwater. The net result of the incomplete contaminant removal and solubility enhancement may have led to the observed concentration increase in the post-treatment samples.

The concentrations of BTEX compounds in the long-term monitoring samples for MW-42SR, MW-60S, MW-62S decreased significantly compared with the concentration levels in their pre-treatment and post-treatment samples. Among the three wells, MW-60S demonstrated the most significant contaminant decrease with a reduction rate of 98.3% for total BTEX. More importantly, benzene concentrations in the long-term monitoring samples for MW-42SR, MW-60S and MW-62S were at low concentration levels of 2.2 ug/L, 7.6 ug/L, and 3.5 ug/L respectively. These values demonstrated a significant decrease from the elevated post-treatment results, and were below the remediation action objective of 50 ug/L.

Due to their location in the downstream part of the treatment area, recharge of relatively clean groundwater from south-east direction (upstream) may have contributed to the decrease in contaminant concentrations observed in MW-42SR, MW-60S, and MW-62S during the long-term monitoring. In addition, the contribution of biodegradation in the reduction of soil and groundwater contamination could not be ruled out. Among the three wells, the effect of biodegradation may have been most significant in MW-60S where a moderate pre-treatment BTEX concentration and a subsequent post-treatment increase were observed.

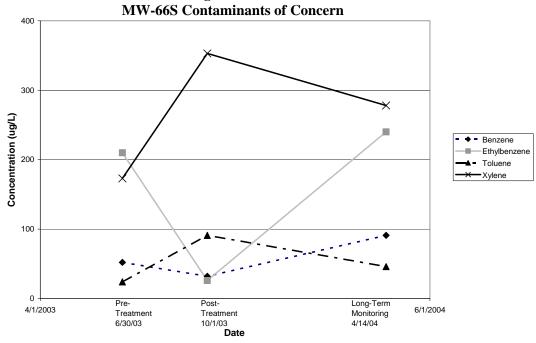
4.1.3.3 MW-66S

The analytical results of the four COCs (BTEX) as well as total VOCs and total BTEX for MW-66S are summarized in Table 4-9. Analytical results for the four COCs for the well is also plotted in Figure 4-11. MW-66S, with a well depth of 19 ft bgs and a screened interval of 9 ft to 19 ft bgs, was installed on June 26, 2003. As can be seen in Figure 1-3, MW-66S was located outside the south periphery of the treatment area.

Table 4-9 MW-66S Contaminants of Concern

Sample Location					M\	W-66S				
Date Collected	6/30/20	003		10/1/20	03	10/1/03, Du	plicate	4/14/2004		
Sampling Event	Pre-Trea	tment	I	Post-Trea	tment	Post-Treatment		Long-Term Monitoring		
Sample Collection Method	perista pum			perista pum		peristal pump			perist pun	
Analyte	Conc. (ug/L)		Conc. (ug/L)		%Reduction from Pre-Treatment	Conc. (ug/L)	Qual.	Conc. (ug/L)	Qual.	%Reduction from Pre-Treatment
Comtaminants of Concern (COCs)										
Benzene	52		32		38.5%	32		91		-75.0%
Ethylbenzene	210		26		87.6%	26		240		-14.3%
Toluene	24		91		-279.2%	86		46		-91.7%
Xylene	173		353		-104.0%	340		278		-60.7%
Total VOCs	522.3		559.7		-7.2%	538.4		719.5	I	-37.8%
Total BTEX	459		502		-9.4%	484		655		-42.7%
2-Methylnaphthalene	1.1		NA			NA		1.6		

Figure 4-11



As indicated by the pre-treatment groundwater results in Table 4-9 and Table F-1 in Appendix F, MW-66S demonstrated a low pre-treatment total BTEX at 459 ug/L. The pre-treatment soil sampling results (see Table E-1 in Appendix E) indicated that the soil sample from MW-66S only had ethylbenzene positively detected at 40 ug/kg, and total BTEX for the sample was the lowest among the soil samples collected from the seven newly-installed monitoring wells.

In the post-treatment sample for MW-66S, benzene and ethylbenzene demonstrated an increase while toluene and xylene showed a decrease compared to their pre-treatment levels. Post-treatment benzene concentration for MW-66S was at 32 ug/L, below the remediation action objective of 50 ug/L. Located in the upstream and outside of the treatment area, MW-66S was believed to have received minimum thermal treatment during the heating. However, some mixing of warm water from the treatment zone may still have occurred in this monitoring well during and immediately after the heating, which may explain the variations in BTEX concentrations observed in the post-treatment data.

The long-term monitoring results for MW-66S indicated that the contaminant composition (relative ratios among BTEX compounds) in the groundwater returned to the pre-treatment values, and a general increase in BTEX concentrations was observed. Benzene concentration in the long-term monitoring sample for MW-66S was at 91 ug/L, above the remediation action objective of 50 ug/L. The similarity of contaminant composition between the pre-treatment and long-term monitoring data for MW-66S indicated that recharge of the groundwater from further upstream was the dominant process that affected its long-term monitoring results.

It is also worth pointing out that due to the low level of contamination in MW-66S, the variation in contaminant concentrations observed in this well during the different sampling rounds were within the range of sampling and analytical errors.

4.1.4 Analysis of Vapor Data

As discussed in Section 2.3.4 and its sub-sections, seven vapor sampling events occurred on a weekly basis to monitor the VOC concentrations in the influents and effluent of the VR system. In addition, FID, PID LEL, vacuum, and vapor flow data were also collected nearly daily during the VR system operation. The analytical results for the Site 4 vapor influent and combined effluent are summarized in Tables G-1 and G-2 in Appendix G, and the system monitoring data are included in Table 2-2.

As indicated in Table 2-2, Site 4 influent FID, LEL and Summa canister readings on the VR system initialization day (July 31, 2003) were 9,800 ppmv, 20%, and 14.8 ppmv respectively. The corresponding combined effluent readings for these parameters were 5,240 ppmv, 21%, and 0.028 ppmv respectively. Although the Summa canister vapor data showed a significant reduction of total VOCs by the VR system, the effluent LEL reading was higher than the influent reading, indicating no removal of certain constituents by the VR system. This observation promoted additional collection of grab vapor samples (using Summa canisters) for the analysis of methane to determine the possible cause of the poor removal of constituents with high FID and LEL readings.

Methane results in Tables G-1 and G-2 in Appendix G indicated that on July 31, 2003, the methane concentration was 0.22% at the Site 4 influent and 0.31% at the effluent. The high methane concentration and low reduction rate of LEL constituents in the combined effluent vapor stream suggested that methane may be a significant constituent responsible for the high FID and LEL readings on the system initialization day. The significant presence of methane in the vapor stream was unexpected, and the sources of the methane have not been determined. In the subsequent two weeks of vapor sampling events, methane concentrations decreased to 0.025% and 0.045% respectively at Site 4 influent and

0.027% and 0.036% respectively at the combined effluent. Methane analysis was discontinued after the third week of vapor sampling due to the dissipating levels. The use of a PID in addition to a FID was incorporated into the sampling procedures in an attempt to differentiate the methane levels.

The individual VOC results shown in Table G-1 in Appendix G indicated that the chemical composition of the Site 4 vapor stream generally matched well with the compounds detected in the Site 4 groundwater samples, with the BTEX compounds as the dominant contaminants.

The Site 4 influent vapor Summa canister data, along with the Site 4 influent flow rate, vacuum, and temperature data, was used to calculate daily VOC mass removal amounts for Site 4 (see Table 2-2). Daily VOC removal rates ranged from 0.1 to 5.7 lbs VOC per day. It is estimated that approximately 69.5 lbs of VOCs were removed during the period of the ERH system operation.

The ERH operation was performed for 53 days, from July 31 to September 22, 2003. Based on the information that the mid-process groundwater samples collected from both Site 3 and Site 4 met the clean-up goals, a decision was made to permanently leave off the electrodes on September 22, 2003. To fully collect the vapor contaminants that were still coming out of the groundwater after the ERH system was turned off, VR system remained in operation for an extended period of time until October 9, 2003.

During the 53-day ERH operation period, changes in the VOC concentrations of the Site 3 and Site 4 influent vapor reflected the variation in contaminant removal rates by the ERH system. The influent VOC concentration was expected to increase from a low point near the beginning, reach a maximum near the middle of the operation, and then decrease to a low point indicating completion. The low influent VOC concentration near the end of the operation would indicate that the majority of the contaminants in the groundwater and soil had been removed. VOC concentrations in the Site 3 influent generally followed this trend, with the highest concentration observed in the middle of the ERH operation on August 22, 2003. However, at Site 4, the highest vapor VOC concentration was observed in the last Summa canister sampling round on September 11, 2003, suggesting that the maximum contaminant removal rate was reached close to the end of the ERH operation. Since additional Summa canister samples were not collected near the end of the treatment, it was not clear whether VOC concentration in the Site 4 influent had decreased to a low level at the time of the ERH system shut-off. It is possible that the Site 4 influent vapor still contained a relatively high level of contaminants at the time heating was terminated, indicting that some contamination may have been left untreated in the treatment zone.

4.2 Conclusions

The objectives for Site 4 thermal treatment remediation were to significantly reduce the overall mass of petroleum-derived VOCs in the source area and to achieve benzene concentration of 50 ug/L in the Site 4 groundwater. The analytical results from the various groundwater sampling events, primarily the long-term monitoring data in comparison with the pre-treatment data, were used to evaluate whether these objectives have been achieved. The evaluation of the objectives focused on the monitoring wells inside and on the periphery of the treatment area including MW-18SR, MW-61S, MW-62S, MW-63S, MW-64S, and MW-65S. The project objectives were also compared with results from monitoring wells outside the treatment area including MW-42SR, MW-60S and MW-66S, where complete removal of the BTEX contaminants was not expected.

ND05-89-004 4/26/05 4-19

The long-term monitoring results indicated that compared to the pre-treatment data, the overall mass of petroleum-derived VOCs in the source area has been significantly reduced. The reduction rates of total BTEX observed during the long-term monitoring for MW-18SR, MW-61S, MW-62S, MW-63S, MW-64S, and MW-65S were 82.2%, 99.7%, 87.8%, 89.1%, 87.6%, and 91.9% respectively. The concentrations of benzene, the key indicator of remediation performance at Site 4, were at 41 ug/L, non-detect, 3.4 ug/L, 26 ug/L, 4.4 ug/L, and 40 ug/L respectively, all below the site remediation action objective of 50 ug/L. All these long-term monitoring results indicated that the remediation objective for Site 4 has been achieved.

MW-42SR and MW-60S, the two downstream monitoring wells outside the treatment area, had benzene concentrations below the remediation objective at 2.2 ug/L and 7.6 ug/L respectively in their long-term monitoring samples. The only exceedance to the remediation objective in the long-term monitoring data set was a benzene concentration at 91 ug/L detected in MW-66S. Because MW-66S is located upstream and outside of the treatment area, a significant reduction of the contaminants from the area was not expected.

Inside the treatment area, groundwater BTEX contamination had been reduced to low levels during and immediately after the heating, as indicated by the mid-process and post-treatment sampling results. However, the long-term monitoring data collected six months after the heating demonstrated a moderate increase in BTEX concentrations compared to the post-treatment results. Recharge of groundwater from upstream of the treatment area could not account for all the contaminant increase, because the BTEX concentration in the upstream groundwater was only one-third of the concentrations observed in the groundwater inside the treatment area. It is hypothesized that a fraction of the observed contaminant increase may be due to rebound of the soil-sorbed contaminants that were not completely removed by the thermal treatment. During the period between the pre-treatment sampling and long-term monitoring, these soil-bound contaminants may have partitioned into the groundwater, contributing to the observed BTEX increase. The hypothesized rebound effect was further supported by the fact that the VOC concentration in the Site 4 influent vapor reached its maximum close to the end of the operation. This suggested that some amount of contaminants may have been left untreated inside the treatment area at the time heating was terminated and subsequently contributed to the BTEX increase in groundwater. In addition, biodegradation is believed to be occurring inside the treatment area at an increased rate compared to the corresponding biodegradation rate prior to the thermal treatment. biodegradation was also observed at Site 3 after the thermal treatment. However, biological breakdown process may not be fast enough inside the treatment area at Site 4 to offset any effects of recharge and rebound.

On the periphery of and outside the treatment area, a temporary BTEX concentration increase was observed immediately after the heating due to increased solubility of the contaminants in the groundwater. The contaminants in these areas were significantly reduced to low concentration levels during the long-term monitoring, probably as a result of accelerated biodegradation, or a combined result of recharge of clean groundwater from other areas and biodegradation.

4.3 Recommendations

It is recommended that additional groundwater monitoring be conducted in the future to monitor the contamination levels to see if they continue to remain below site remediation goal of 50 ug/L benzene in the groundwater. The availability of the future monitoring data may help elucidate the roles the chemical, physical, and biological processes are playing in the transport and fate of the BTEX contaminants, and predict the trend of natural attenuation throughout the site.

ND05-89-004 4/26/05 4-20 Furthermore, it is recommended that an additional round of soil sampling be conducted at the site. The soil samples should be collected from the same locations and depths where the pre-treatment soil samples were taken. As discussed in Section 4.1.2, rebound of soil-sorbed contaminants that were not completely removed by the thermal treatment may be one of the processes that were responsible for the moderate BTEX increase in the long-term monitoring samples collected inside the treatment area. The soil data from the recommended additional sampling, in combination with the pre-treatment soil data, will help clarify whether rebound process is occurring and its contribution to the overall contaminant distribution.

5.0 REFERENCES

- Foster Wheeler Environmental Corporation. July 2003. Thermal Treatment Pilot Test and Remediation QA/QC Plan, Naval Weapons Industrial Reserved Plant, Bedford, Massachusetts, Rev. 2.
- Foster Wheeler Environmental Corporation. August 2003. Final Site -Specific Health and Safety Plan for Site 3 and Site 4 Thermal Treatment, Naval Weapons Industrial Reserved Plant, Bedford, Massachusetts, Rev. 0.
- Foster Wheeler Environmental Corporation. December 2003. Final Work Plan for Site 4 Thermal Treatment, Naval Weapons Industrial Reserved Plant, Bedford, Massachusetts, Rev. 0.
- Reinhard, M., S. Shang, P. K. Kitanidis, E. Orwin, G. D. Hopkins, and C. A. Lebron, 1997. *In Situ BTEX Biotransformation Under Enhanced Nitrate- and Sulfate-Reducing Conditions*. Environmental Science and Technology, 31: 28-36.
- Tetra Tech EC, Inc. April 2005. Draft Closeout Report for Site 3 Thermal Treatment Pilot Test, Naval Weapons Industrial Reserve Plant, Bedford, Massachusetts, Rev. 0.
- TRS. April 2003. System Design and Work Plan, Electrical Resistance Heating Remediation Site 4, Naval Weapons Industrial Reserve Plant, Bedford, Massachusetts.

5-1

ND05-89-004 4/26/05

APPENDIX A

Thermal Remediation Services, Inc. Site 4 Thermal Treatment Final Report

FINAL REPORT

Electrical Resistance Heating Operations Site 4 Extended Thermal Treatment Area Bedford Naval Weapons Industrial Reserve Plant (NWIRP)

Bedford, MA.

U.S. NAVY REMEDIAL ACTION CONTRACT
N62472-99-R-0032



Prepared by

Thermal Remediation Services, Inc.

2325 Hudson Street Longview, Washington 98632

CONTENTS

Exec	cutive Summary	ES-1
1.0	INTRODUCTION	1
1.1	PURPOSE OF THE REPORT	1
1.2	BACKGROUND INFORMATION	
1.2	1.2.1 Site Location, Geology and Description	
	1.2.2 Historic and Current Land Use	
1.3	PREVIOUS INVESTIGATIONS AND REMEDIATION EFFORTS	2
1.4	REPORT ORGANIZATION	
	SITE 4 ERH EXTENDED TREATMENT AREA OBJECTIVES	
2.0	SITE 4 ERH EXTENDED TREATMENT AREA OBJECTIVES	4
2.1	ERH OBJECTIVE	4
2.2	EXTENDED ERH TREATMENT AREA DESIGN	
	2.2.1 ERH Remediation Planned Performance Period	
2.3	ERH PILOT TEST AT SITE 3	6
3.0	SITE 4 ERH REMEDIATION SYSTEM INSTALLATION	7
3.1	ERH MOBILIZATION AND DEMOBILIZATION	7
3.2	ERH PILOT TEST INSTALLATION AND CONSTRUCTION ACTIVITIES	8
	3.2.1 Drilling Activities and Schedule	
	3.2.2 Electrode Installation	
	3.2.3 Co-located Vapor Recovery Wells and Piping	8
	3.2.4 Temperature Monitoring Points	
	3.2.5 Power Control Unit	
	3.2.6 ERH Process Treatment Equipment	
	3.2.7 Monitoring Wells	10
4.0	SITE 4 ERH REMEDIATION	12
4.1	SYSTEM START UP AND INTERLOCK TESTING	12
4.2	ERH REMEDIATION OPERATIONS	
	4.2.1 Site 4 and Site 3 ERH Power Ratio	13
4.3	VAPOR RECOVERY SYSTEM	
	4.3.1 Condensate Production	
4.4	SUBSURFACE TEMPERATURES	
	4.4.1 Site 4 Average Subsurface Temperatures	15
5.0	SAMPLING ACTIVITIES AND ANALYTICAL RESULTS	17
5.1	GROUNDWATER SAMPLING	17
• • •	5.1.1 Data Validation	
	5.1.2 Analytical Results for Site 4 Groundwater Samples	
	5.1.3 Pre-ÉRH Remediation Analytical Results for Site 4 Groundwater Samples	
	5.1.4 September Analytical Results for Site 4 Groundwater Samples	
	5.1.5 Post-ERH Remediation Analytical Results for Site 4 Groundwater Samples	
	5.1.5.1 Site 4 Late September and Early October Groundwater Sample Results	
	5.1.5.2 Site 4 April 2004 Groundwater Sample Results	
5.2	VAPOR SAMPLING	
	5.2.1 Data Validation	
_	5.2.2 Analytical Results for Site 4 Vapor Recovery	
5.3	REMEDIATION-DERIVED WASTE STREAM SAMPLING	24

6.0 6.1			NSONCENTRATION REDUCTION	
7.0	REFE	ERENCE	ES	27
<u>L</u>	ist of	<u>Tables</u>		
Table	e 1: Bo	oiling Po	ints for Groundwater and Contaminants of Concern	5
Table	2: Si	te 4 Moi	nitoring Well Construction Information	11
Table	9: A	verage S	Soil Vapor Recovery Flow Rate for the Site 4 and Site 3 Pilot Test Period	14
Table	e 4: El	RH Rem	ediation Temperature Results Per TMP Location	16
Table	e 5: Pr	e-ERH	Remediation May and June Baseline Sampling and Analytical Results	19
Table	e 6: El	RH Rem	ediation Early September Operations Sampling and Analytical Results	20
Table	e 7: In	itial Pos	t-ERH Remediation Sampling and Analytical Results	21
Table	e 8: Ap	oril 2004	Post-ERH Remediation Sampling and Analytical Results	22
Table	9: El	RH Rem	ediation Vapor Recovery Sampling and Analytical Results	24
<u>L</u>	ist of	Figures		
Figur	e 1:	Bedford	d NWIRP Location Map and Aerial Photo	
Figur	e 2:	Site 4 L	Location Map	
Figur	e 3:	Site 4 E	ERH Extended Treatment Area	
Figur	e 4:	ERH E	lectrode, TMP and Monitoring Well Construction Details	
Figur	e 5:	ERH P	rocess Flow Diagram/Piping and Instrumentation Diagram	
Figur	e 6:	Site 4 7	Temperature Results Per TMP Location	
Figur	e 7:	TMP-1:	Average Temperatures Per Depth Interval During Operations	
Figur	e 8:	TMP-2	Average Temperatures Per Depth Interval During Operations	
Figur	e 9:	TMP-3	Average Temperatures Per Depth Interval During Operations	
Figur	e 10:	Site 4 A	Average Subsurface Temperature Decrease Per TMP Location	
Figur	e 11:	Predict	ed Trend Line for Site 4 Subsurface Temperature Decrease	
Figur	e 12:	Monito	ring Wellhead Sample Collection Configuration	
<u>L</u>	ist of	Append	<u>lices</u>	
А	Append	dix A:	Analytical Results	
А	Append	dix B:	Memorandums, Field Logs and Construction Reports	
А	Append	dix C:	Complete Temperature Interval Data Tables	

LIST OF ACRONYMS AND ABBREVIATIONS

Term Definition

°C Degrees Celsius

1,1,1-TCA 1,1,1-Trichloroethane

1,1-DCA 1,1-Dichloroethane

cis 1,2-DCE 1,2-Dichloroethene

acfm Actual Cubic Feet Per Minute

bgs Below Ground Surface

BTEX Benzene, toluene, ethylbenzene, xylene

cm/s Centimeters Per Second

CPVC Chlorinated Polyvinyl Chloride

CVOCs Chlorinated Volatile Organic Compounds

Electrical Resistance Heating

DNAPLs Dense Non-Aqueous Phase Liquids

ft³ Cubic Feet

ERH

GAC Granular Activated Carbon

gpm Gallons per minute kW-hr Kilowatt Hour

MCM One thousand circular mils

MW Monitoring Well

NWIRP Naval Weapons Industrial Reserve Plant

μg/lPCEPCUPower Control Unit

ppmv Parts Per Million By Volume

PVC Polyvinyl Chloride

scfm Standard Cubic Feet Per Minute

TCE Trichloroethene

TRS Thermal Remediation Services, Inc.

TTFW Tetra-Tech Foster Wheeler

TTNUS Tetra-Tech NUS

TMPs Temperature Monitoring Points

USEPA United States Environmental Protection Agency

VOCs Volatile Organic Compounds

VR Vapor Recovery yd³ Cubic Yard

EXECUTIVE SUMMARY

An Electrical Resistance Heating (ERH) extended treatment area application was conducted at Site 4 of the Bedford Naval Weapons Industrial Reserve Plant (NWIRP), Bedford, Massachusetts by Thermal Remediation Services, Inc. (TRS) under subcontract to Tetra Tech Foster Wheeler Environmental Corporation (TTFW) for the U.S. Navy Engineering Field Activity Northeast Remedial Action Contract (RAC) N62472-99-R-0032, Task Order 0089. The extended treatment area was conducted to remediate benzene in groundwater to 50 parts per billion (ppb).

Concentrations of benzene, toluene, ethylbenzene and xylene (BTEX) were detected in groundwater samples collected after an underground storage tank (UST) removal was completed in 1990. The UST previously contained gasoline and post removal groundwater sampling activities reported BTEX concentrations in an existing monitoring well, MW-18, ranging from 50 to 60 parts per million (ppm). Previous remediation activities included three rounds of chemical oxidation treatment from 2000 to 2002; however, post chemical oxidation treatment groundwater results reported that BTEX concentrations still exceeded 20 ppm (TTFW Statement of Work 2002).

The ERH treatment application was conducted as an extension of an ERH Pilot Test at Site 3 which was being evaluated for potential full-scale application for removal of chlorinated volatile organic compounds (CVOCs) at a previously-delineated source area near the Chemical Storage Building and Components Laboratory (Site 3). The Site 4 extended treatment was operated concurrently with the Site 3 Pilot Test via the same Power Control Unit (PCU). As indicated in the TTFW Statement of Work, the goal of the Site 4 extended ERH treatment was to reduce existing benzene concentrations in groundwater to the 50 ppb cleanup level.

A treatment volume 20 feet wide, 50 feet long, and 28 feet deep was delineated east from the southeast corner of the Antenna Range Building, which is approximately 3,150 feet northwest from the Site 3 ERH Pilot Test. The proposed treatment area at Site 4 was expanded from the original dimensions of 20 feet wide by 30 feet long after increased BTEX concentrations were detected upgradient from the site. The extended treatment area subsurface ERH treatment interval was from approximately 9.5 feet to 28 feet below grade surface (bgs), resulting in a potential treatment volume of 719 cubic yards (yd³). A total of eight electrodes with co-located vapor recovery wells were installed to a depth of 30 feet bgs (i.e., two feet beyond the proposed treatment interval of 28 bgs). The electrode design allowed subsurface power application and vapor recovery to be performed simultaneously within each boring. Subsurface temperatures were measured at three temperature monitoring points (TMPs) located within the treatment area.

Recovered groundwater, soil vapors, and steam from Site 4 were separated in the condenser unit of the ERH process treatment system. The vapor stream was processed through four, 1000-pound (lb) granular activated carbon (GAC) vessels for contaminant removal. Condensate and recovered groundwater was treated using a single 55-gallon liquid GAC vessel and was either returned to the subsurface via drip lines installed in each electrode boring or was evaporated via the on-site condenser cooling tower. Approximately 167,070 kilowatts hours (kW-hr) of energy was applied to the subsurface during the 53 days of operation (operational period for Site 3 ERH Pilot Test). The average temperature within the treatment volume, based on the average temperatures recorded at the three TMP locations, reached a high of 93 degrees Celsius (°C) on day 51 of operations. The average subsurface treatment interval temperatures at the three TMP locations were 93 °C, 100 °C, and 84 °C at TMP-1, -2 and -3, respectively.

The Site 4 ERH operations were shutdown when the directive from TTFW was given to officially shutdown the Site 3 ERH Pilot Test on September 22, 2003. The analysis of groundwater samples collected from Site 4 September 2003 after the cessation of ERH operations indicated that benzene concentration was below the 50 ppb remediation goal at all monitoring well locations within the treatment area. Subsequent sampling events in October 2003 and April 2004 reported that benzene concentrations remained below the cleanup goal; however, there was a laboratory qualifier (J for estimated value) added to the October 2, 2003 sample collected from MW-62S. The April 2004 sample results, including a duplicate sample, confirmed that the benzene concentration at that location (3.4 micrograms per liter (μ g/L) or ppb) remained below 50 μ g/L cleanup goal.

Monitoring well location MW-66S indicated a rise in benzene concentrations from 14J μ g/L in September 2003 to 91 μ g/L based on the analytical results of the April 2004 groundwater sampling event. Based on the location of MW-66S south of the Site 4 treatment area, the monitoring well is likely upgradient of the site with regards to general groundwater flow direction, and its increase in benzene concentration indicates the potential for recontamination of the treatment area.

1.0 INTRODUCTION

1.1 PURPOSE OF THE REPORT

This report presents the results of the Electrical Resistance Heating (ERH) remediation application at Site 4 of the Bedford Naval Weapons Industrial Reserve Plant (NWIRP), Bedford, Massachusetts. The operations were officially titled Extended Treatment Area in reference to the fact that Site 4 was operated concurrently via the same Power Control Unit (PCU) as the Site 3 ERH Pilot Test. The ERH application at Site 4 was conducted to remediate known and suspected concentrations of benzene in the groundwater attributable to a former underground storage tank (UST) to a cleanup level of 50 micrograms per liter (µg/L).

Thermal Remediation Services (TRS) has prepared this report under subcontract to Tetra Tech Foster Wheeler Environmental Corporation (TTFW) for the U.S. Navy Engineering Field Activity Northeast (EFA NE) Remedial Action Contract (RAC) N62472-99-R-0032, Task Order 0089. The information presented in this report is based on ERH operations results and data collected from various media during and after ERH operations at the site. This report presents the data from Site 4 operations as well as associated conclusions and recommendations.

1.2 BACKGROUND INFORMATION

1.2.1 Site Location, Geology and Description

The Bedford NWIRP is located approximately 15 miles northwest of Boston, in Bedford, Massachusetts (refer to Figure 1: Bedford NWIRP Location Map and Aerial Photo). The former NWIRP is comprised of approximately 46-acres of densely developed land with a geographical high to the north (Hartwells Hill) with some wetlands located north and west of Hartwells Hill and to the east and northeast as well.

The ERH system was constructed and operated at Site 4, a subsurface source area with a dissolved phase constituent plume east from the southeast corner of the Antenna Range Building on the northern slope of Hartwells Hill (refer to Figure 2: Site 4 Location Map). The Site 4 location is approximately 3,150 feet northwest and down the slope of Hartwells Hill from the Site 3 ERH Pilot Test. The ERH treatment area, as shown on Figure 3: Site 4 Extended Treatment Area, comprised an area 20 feet wide by 50 feet long, with a remediation design interval of approximately 9.5 to 28 feet below ground surface (bgs).

The Bedford NWIRP was primarily constructed on Hartwells Hill, within the drainage basin of the Shawsheen River (refer to Figure 1). The hill, a diorite knob capped by glacial till, rises approximately 70 feet above the surrounding wetlands (http://5yrplan.nfesc.navy.mil/1997). The glacial deposits are comprised of sandy till, silty till and dense, clayey till. The upper 10 feet of

the pilot study area is considered fill (i.e., re-worked till of sand and gravel) from the construction of the NWIRP and its various buildings and structures (TTFW 2002). Groundwater is primarily influenced by topography: precipitation at the site generally migrates radially off the hill with slow to minor penetration of the poorly drained soil due to the lack of remaining natural surface cover (http://5yrplan.nfesc.navy.mil/1997). Previous investigation results and groundwater contours based on shallow and intermediate zones support a primary groundwater flow in a north/northwesterly direction from Hartwell Hill. Permeability tests (i.e., slug tests) and geotechnical laboratory tests indicate a low hydraulic conductivity in the pilot test area ranging from an average of 3.5×10^{-5} centimeters per second (cm/s) to 11.20×10^{-7} cm/s (TTFW 2002).

1.2.2 Historic and Current Land Use

Former Bedford NWIRP activities included the design, fabrication and testing of prototype weapons and missile guidance systems. The facility was operated by Raytheon Company of Waltham, Massachusetts until operations ceased in December 2002. Raytheon Company removed the UST in the vicinity of Site 4 in 1990. The NWIRP facility is currently vacant (TTFW 2002).

1.3 PREVIOUS INVESTIGATIONS AND REMEDIATION EFFORTS

According to information provided in the 2002 TTFW Statement of Work, previous investigations conducted at Site 4 after the UST was removed indicated benzene, toluene, ethylbenzene and xylene (BTEX) concentrations in groundwater in excess of 50 milligrams per liter (mg/L) at monitoring well location MW-18. Additional groundwater samples also indicated that benzene concentrations were near 600 µg/L. Consequently, three separate chemical oxidation remediation efforts were conducted by GeoCleanse for the US Navy from 2000 to 2002. Post chemical oxidation treatment groundwater results from MW-18 indicated that BTEX concentrations at MW-18 still exceeded 20 mg/L (TTFW, 2002).

1.4 REPORT ORGANIZATION

In order to reduce the length and redundancy of this ERH Extended Treatment Area Report for Site 4, the reader will be referred to previous materials when appropriate to minimize reiteration of information that has not changed from previous documents (e.g., site history, regional and local geology and hydrogeology, and general design information and theory regarding ERH technology). The majority of the aforementioned information is provided in the Tetra Tech Foster Wheeler Statement of Work, for In-Situ Thermal Treatment Pilot Test, NWIRP, Bedford Massachusetts, July 2002 (TTFW, 2002) for the U.S Navy; the Thermal Remediation Services (TRS) System Design and Work Plan, Electrical Resistance Heating Remediation, Site 4,

Bedford NWIRP, April 2003 (TRS 2003); and the ERH Site 3 Pilot Test Report, March 2004 (TRS 2004).

This report presents the results of the Site 4 ERH Extended Treatment Area in terms of the purpose of the report outlined in Section 1.1 and presents the analytical results of the samples collected prior to, during and post-remediation application. In addition, the report briefly describes the construction, installation and operations of the Site 4 ERH application. The ERH project objectives are presented in Section 2.0 and the construction, installation and operation activities are presented in Section 3.0. Section 4.0 presents the Site 4 sampling activities and analytical results. The conclusions of the Site 4 ERH Extended Treatment Area and TRS recommendations for potential follow-on activities are presented in Section 5.0. Reference Materials are presented in Section 6.0. The figures and drawings associated with the pilot test are presented at the end of the report. Laboratory results and associated tables are presented in Appendix A. Field forms such as Monitoring Well Construction Completion Reports developed by ENSR are provided in Appendix B. Comprehensive temperature data has been tabulated and is presented in Appendix C.

2.0 SITE 4 ERH EXTENDED TREATMENT AREA OBJECTIVES

The Site 4 ERH remediation objective in the following sections is summarized from the TTFW Statement of Work (2002) and the TRS Work Plan (2003). The ERH Site 3 Pilot Test conducted by TRS is also briefly summarized in this section (and as appropriate in other sections of this report based upon relevance to the subject matter); however, complete details regarding the Site 3 pilot test scope of work, project objectives and performance goals, operations, and results have been provided in a separate Site 3 ERH Pilot Test Report submitted to TTFW for review in March 2004.

2.1 ERH OBJECTIVE

The sole objective of the Site 4 ERH remediation was to reduce benzene concentrations in groundwater within the treatment area to $50 \mu g/L$ (refer to Figure 3 for treatment area location). The objective was presented in Section 1.3.1 of the TTFW Statement of Work, (TTFW 2002). The Site 4 ERH remediation project was planned for either consecutive or concurrent operations with regards to the Site 3 ERH Pilot Test.

2.2 EXTENDED ERH TREATMENT AREA DESIGN

The design of the Site 4 ERH remediation was based on several factors including treatment area and volume, site-specific geology and hydrogeology, and the project objective. The original proposed treatment area and subsurface depth interval was based on information presented in the TTFW Statement of Work (TTFW 2002). The area designated for the Site 4 ERH remediation was based on the analytical results of previous investigations at the Bedford NWIRP. Based on this information, TRS provided TTFW with an ERH design and work plan specific to the project objective presented in the TTFW Statement of Work. The original Work Plan presented a design for Site 4 that would remediate an area approximately 20 feet wide by 36 feet long with a subsurface treatment interval of 9.5 feet to 28 feet bgs.

The TTFW proposed treatment length of 30 feet long was extended to 50 feet long based on groundwater concentrations of benzene detected in an upgradient well, MW-65S, during the baseline groundwater sampling in June 2003. The extension was approved by TTFW based on the pre-ERH remediation application data and a letter from TRS stating the need for complete remediation of the impacted area at Site 4 and recommending the aforementioned expansion of the treatment area. TRS also indicated that a more complete delineation of the remediation area was necessary to avoid potential recontamination of the site from untreated soil and groundwater. The letter from TRS has been included in Appendix B of this report since it pertains to modifications in the originally proposed treatment area. The actual operational treatment area is

shown on Figure 3 which details the location of the eight electrodes installed at the site as well as the original proposed treatment boundary (TTFW 2002; TRS 2003).

As previously indicated, the length of the treatment area was extended to 50 feet resulting in an ERH application treatment volume of 19,425 cubic feet (ft³) or approximately 719 cubic yards (yd³). In order to remediate this area, the TRS Site 4 ERH remediation design incorporated the installation of eight electrodes with co-located vapor recovery systems as shown in Figure 4: Subsurface Component Construction Details), as well as the installation of three temperature monitoring points (TMPs) to monitor and record subsurface temperature during ERH operations.

While the Site 4 ERH remediation system was provided energy via the PCU located at Site 3, there was a separate ERH condenser unit located at Site 4. The effluent vapors, condensation and recovered groundwater were run through the Site 4 condenser as well as the four granular activated carbon (GAC) vessels located at Site 3 to treat vapors recovered by both the Site 4 ERH remediation and the Site 3 pilot test vapor recovery systems (TRS 2003, TTFW 2002).

As detailed in the TRS Work Plans for Site 4 and Site 3, the ERH system essentially heats the subsurface to temperatures necessary to volatize the contaminants of concern (TRS 2003). For ease of reference, Table 1 from the TRS Work Plan has been repeated in this document to provide information regarding the boiling point distribution at depths corresponding to the treatment intervals at Site 4 (Heron, et al, 1996).

Table 1: Boiling Points for Groundwater and Contaminants of Concern

O a man a um d	Boiling Temperature of Compound in degrees Celsius (°C) In Various Medium							
Compound	A.i.	Water						
	Air	(18-feet bgs)	(28-feet bgs)					
Pure water	100	100	109					
benzene	80	69	77					
toluene	111	84	91					
ethylbenzene	136	89	97					
xylene	140	92	100					

2.2.1 ERH Remediation Planned Performance Period

Based on the information summarized in Section 2.2, the Site 4 ERH remediation application was designed and planned to provide ERH for approximately 30 days to achieve the project objective set forth by the TTFW Statement of Work and the TRS Work Plan. Since the Site 4 ERH application was operated in conjunction with the Site 3 ERH Pilot Test via the same PCU and the majority of the power input was directed toward Site 3, the pilot test operations would essentially dictate the overall operational period for the Site 4.

2.3 ERH PILOT TEST AT SITE 3

The installation and operation of the Site 4 ERH remediation was predicated on the approved installation and operation of an ERH pilot test at Site 3. The Site 4 ERH application was implemented to take advantage of the available power source (and personnel) at Site 3. The Site 3 ERH Pilot Test results and details regarding subsurface installations and ERH operations were addressed in a final report submitted to TTFW in April 2004. Discussion of the Site 3 ERH Pilot Test within this document is limited to ERH power output and a discussion of the soil vapor recovery rates.

The Site 3 ERH Pilot Test was conducted at a previously-delineated source area near the Chemical Storage Building and Components Laboratory to evaluate ERH as a viable full-scale remediation technology for removing volatile organic compounds (VOCs) from soil and groundwater. The goal of the Site 3 ERH Pilot Test was to apply electrical energy to the subsurface in order to raise subsurface temperatures to a sufficient level to volatilize, and subsequently recover, VOCs; thereby reducing total VOC concentrations in the groundwater by at least 95 percent. The pilot test, located approximately 50 feet north of the Components Laboratory, was designed to treat the subsurface interval from 20 to 55 feet below ground surface (bgs). A total of 24 electrodes with co-located vapor recovery wells were installed to a depth of 60 feet bgs (i.e., five feet beyond the bottom of the treatment interval).

.

3.0 SITE 4 ERH REMEDIATION SYSTEM INSTALLATION

The following sections will briefly discuss in the Site 4 ERH remediation system construction and installation activities, as well as the mobilization and demobilization tasks which include the PCU from Site 3. The details regarding the system design of the various ERH components including the PCU, condenser and vapor recovery system are provided in the TRS Work Plan under their respective section headings (TRS 2002). Only modifications to the ERH design detailed in the TRS Work Plan will be presented in this report; otherwise the reader is directed to reference the aforementioned plan for specific details regarding the ERH system components, including the subsurface installation.

In general, the Site 4 ERH remediation system included eight electrodes and three TMPs with individual thermocouple points at five-foot depth intervals from 5 feet bgs to 30 feet bgs, as well as the necessary chlorinated poly vinyl chloride (CPVC) piping (temperature/chemical-resistant material) for vapor recovery. Power was supplied to the Site 4 electrodes from the PCU at Site 3 via individual 350 MCM power cables.

3.1 ERH MOBILIZATION AND DEMOBILIZATION

As detailed in the Site 3 ERH Pilot Test report, drilling, construction and installation of the ERH system for Site 3 and Site 4 began in early spring 2003 and was completed during that summer. The ERH PCU arrived at the Bedford NWIRP on April 4, 2003, while the remainder of the ERH process equipment arrived on April 30 and May 1, 2003 (TRS Pilot Test Report 2004).

Demobilization activities, including decommissioning and decontaminating ERH pilot test equipment, were initiated on November 10, 2003 and completed on November 14, 2003. The Site 3 and Site 4 ERH condensers, including the cooling towers, as well as the piping from the vapor recovery and drip systems, were decontaminated using a pressure washer. All of the decontamination water and other waste associated with decontamination activities was collected and stored in drums on site for disposal by TTFW. The granular activated carbon (GAC) vessels used during the pilot test and Site 4 operations, as well as the remaining carbon filter replacement sacks, were removed by the vendor, US Filter-Westates. The thermocouples used to monitor subsurface temperatures were disconnected from the automated monitoring system, labeled, and left in place for further monitoring via a hand-held meter by TTFW during the post-treatment cool down period at Site 3 and Site 4 (TRS Pilot Test Report 2004).

3.2 ERH PILOT TEST INSTALLATION AND CONSTRUCTION ACTIVITIES

3.2.1 Drilling Activities and Schedule

Drilling activities for the Site 4 ERH Remediation began May 13, 2003, and were completed on July 21, 2003. The drilling service provider, Bowser-Morner of Dayton, Ohio, used a sonic drill rig to advance the boreholes for the eight electrodes, three TMPs, and nine monitoring wells as specified in the TRS Work Plan (TRS 2003). The monitoring well installation, supervised and logged by a geologist from TTFW, was completed on May 18, 2003. The installation of the electrodes, TMPs and monitoring wells associated with Site 3 superceded the installation of the remaining subsurface components at Site 4. After completing installation of the Site 3 ERH pilot test subsurface components, the remaining electrodes and TMPS were constructed and installed at Site 4 by July 21, 2003.

Site Survey

All of the subsurface installation points, including the electrodes and TMP locations, were located at the site using handheld tape measurements and existing structures as benchmarks. The electrode and monitoring well locations were selected and located in the field according to the design layout in the TRS Work Plan and subsequent modifications based on the extension of the treatment area at Site 4 (TRS 2003). The installed electrode, TMP and monitoring well locations are presented in Figure 3: Site 4 ERH Extended Treatment Area.

As of the date of this report, a site survey has not been completed. The site survey of all locations at the two ERH sites will be completed by TTFW. Figures associated with this report will be updated accordingly and submitted as amendments when the survey information is available.

3.2.2 Electrode Installation

The eight electrodes were located at Site 4 as shown on Figure 3 and installed to a depth of 30 feet bgs. Each electrode was constructed and installed in a 12-inch borehole per the construction specifications shown on Figure 4: ERH Electrode, TMP and Monitoring Well Construction Details in this report and as detailed in the TRS Work Plan (TRS 2003). According to the TRS design specifications for the Site 4 ERH remediation, the electrode boreholes were spaced on 13 foot centers from other electrodes (refer to Figure 3 for the treatment area plot plan).

3.2.3 Co-located Vapor Recovery Wells and Piping

A vapor recovery well (VR well) was co-located with each electrode as shown on Figure 4 of this document and per the design specifications of the TRS Work Plan (TRS 2003). The VR well screen intervals for the Site 4 ERH remediation were installed from 10 to 30 ft bgs with

conductive material backfill in the annulus. The vapor recovery piping was installed above grade as shown on the plot plan Figure 3 and vapor recovery flow was controlled by a 1.5-inch ball valve installed at each electrode/VR well recovery header. Ports for measuring vacuum, flow, and concentration, as well as a thermocouple, were also installed in the above-grade piping at each electrode/VR well location to enable measurement of vapor recovery parameters (i.e., flow rate, temperature, and pressure).

3.2.4 Temperature Monitoring Points

The TMPs for the pilot test were installed according to the TRS Work Plan to a depth of 30 feet bgs to enable remote monitoring and recording of subsurface temperatures during operations. As shown on Figure 3, the three TMP locations were located inside the ERH treatment region to monitor the subsurface treatment temperatures (TRS Work Plan 2003). The TMP-1 and -2 locations were situated within the treatment area, essentially surrounded by electrodes. The remaining location, TMP-3 as shown on Figure 3, was located along the western boundary of the Site 4 ERH remediation to provide some documentation regarding the extent of subsurface heating along the periphery of the treatment area.

As specified in the TRS Work Plan and shown on Figure 4 of this document, 6 Type-T thermocouples were installed within each TMP borehole (TRS Work Plan 2003). All of the thermocouples were connected to a field instrument box which transferred the subsurface temperature data to the ERH PCU computer via fiber optic cable for continuous data collection and real-time system monitoring.

3.2.5 Power Control Unit

As stated in Section 3.1, the PCU was delivered to Site 3 at the Bedford NWIRP on April 4, 2003. Details regarding the installation of the PCU are provided in the April 2004 Site 3 ERH Pilot Test Report. The location of the PCU within the process treatment system is identified on Figure 2 and Figure 5: ERH Process Flow Diagram/Piping and Instrumentation Diagram.

The existing electrical feed (a 13.2 kilovolt (kV) power source) for the Components Building at Site 3 was utilized to provide electrical service to the PCU. The electrical service was routed to the PCU via the line side of the main facility step-down transformer at the rear of the building which eliminated the need for a new and separate electrical service to provide electrical power to the PCU, which in turn, provided an electrical power source for ancillary processing equipment.

3.2.6 ERH Process Treatment Equipment

The Site 4 ERH remediation had a separate condenser with a cooling tower, as well as a separate liquid GAC vessel, which was connected to the process treatment equipment at Site 3 (refer to Figures 2 and 5 for details). The process treatment equipment at Site 3 included a 40 horsepower

(hp) blower for vapor recovery and four vapor GAC vessels (refer to Figure 5). The combined outlet of the secondary GAC vessels was connected to the blower inlet which was connected to the atmosphere discharge stack. Sampling ports and gauges were supplied to measure vacuum and flow at the blower inlet and temperature at the blower outlet. Vapor recovery from Site 3 and Site 4 was processed through the same GAC vessels; however the effluent lines from each site to the ERH process treatment equipment had sample ports allowing for the differentiation of effluent recovery rates and concentrations between Site 3 and Site 4.

3.2.7 Monitoring Wells

The scope of work for the Site 4 ERH remediation included the installation of nine monitoring wells for collecting groundwater samples to monitor the contaminant concentrations within the treatment area and to ensure that the benzene concentration remediation objective was achieved at the end of operations. In addition to the installation of the new monitoring wells at Site 4, existing monitoring well locations MW-18 and MW-42 were abandoned and replaced with new wells constructed using temperature-resistant material. The same well identification was kept for consistency, but an "R" was added to indicate a replacement well.

The monitoring wells at Site 4, consisting of carbon steel riser pipes (blanks) and stainless steel screens, were installed under TTFW supervision. The location of the monitoring wells was based on the TTFW Statement of Work and the TRS Work Plan (TTFW 2002 and TRS 2003). As briefly discussed in the Site Survey subsection in Section 3.2.1 of this report, the monitoring well locations were identified at the site based on field measurements during pre-construction activities. The following monitoring well construction table, Table 2: Site 4 Monitoring Well Construction Information, is based on the field logs completed during installation by TTFW. Copies of the Monitoring Well Completion Reports are presented in Appendix B of this report.

Monitoring well development activities were also completed by TTFW. Information regarding the well volumes purged from each monitoring well, as well as the monitoring well development methods (e.g., surge block, pump, turbidity standards, etc) is available through TTFW, but has not been included in this report.

Table 2: Site 4 Monitoring Well Construction Information

Monitoring Well Location	Northing	Easting	Top of Casing Elevation (Flushmount)	ation (5.010 slot) Interval (feet bgs)		Casing Diameter	Total Borehole Depth (feet bgs)	Borehole Diameter (inches)
			,	Top	Bottom		, ,	
MW-18SR	NA	NA	NA	18	28	2-inch	28	6
MW-42SR	NA	NA	NA	15	25	2-inch	25	6
MW-60S	NA	NA	NA	16	26	2-inch	27	6
MW-61S	NA	NA	NA	15	25	2-inch	26	6
MW-62S	NA	NA	NA	16	26	2-inch	27	6
MW-63S	NA	NA	NA	14	24	2-inch	25	6
MW-64S	NA	NA	NA	14	24	2-inch	25	8
MW-65S	NA	NA	NA	13	23	2-inch	24	6
MW-66S	NA	NA	NA	9	19	2-inch	24	6

Information is based on Tetra Tech Foster Wheeler Monitoring Well Construction Detail Reports.

NA: Not available at this time (see Site Survey subsection of Section 3.2.1 of this report for details); R: replacement.

4.0 SITE 4 ERH REMEDIATION

The following sections discuss the ERH operations and present the data collected from operational monitoring. All operations-related activities specific to the ERH system, including systems monitoring, maintenance and repair, were conducted by TRS site operations personnel. The data presented in the following sections, such as power input and subsurface temperatures, was primarily derived from automatic sensing equipment associated with the ERH system.

4.1 SYSTEM START UP AND INTERLOCK TESTING

As detailed in the Site 3 ERH Pilot Test Report, power was supplied to all of the ERH system components, including the electrodes, during the startup and testing shakedown period. Prior to applying power to the treatment volume, TRS site operations personnel completed various forms including an ERH Startup Checklist, ERH PCU Checklist, and a Component/Interlock Test form which are provided in Appendix B of the April 2004 Site 3 ERH Pilot Test Report. The startup testing, which included current and voltage surveys, was performed to ensure the safety of those working around the ERH equipment, and to verify the proper operation of the ERH system safety interlocks and emergency shutdown control systems. Greater details regarding the start up testing procedures are provided in the April 2004 Site 3 ERH Pilot Test Report and the April 2003 TRS Work Plan.

4.2 ERH REMEDIATION OPERATIONS

The operations phase of the Site 4 ERH remediation began in conjunction with the Site 3 ERH Pilot Test on July 31, 2003. The pilot test at Site 3 was officially completed on September 22, 2003, resulting in an operational period of 53 days. Consequently, operations at Site 4 also ceased on September 22, 2003, based on the official shutdown of ERH operations at the NWIRP, as well as groundwater data which indicated that benzene concentrations were below the remediation goals at all monitoring well locations within the Site 4 treatment area.

The treatment area average subsurface temperature increased from an ambient subsurface temperature of 14 °C prior to operations to a daily site average ranging from 88 °C to 93 °C for the week ending September 22, 2003 (based on the overall temperature average of the three TMPs within the treatment area). Cumulative energy input for both the Site 3 Pilot Test and the Site 4 Remediation totaled 726,391 kW-hr, with approximately 23 percent, or about 167,070 kW-hr, applied directly to Site 4 ERH remediation.

4.2.1 Site 4 and Site 3 ERH Power Ratio

Power was simultaneously applied to the Site 4 ERH remediation application and the Site 3 ERH Pilot Test by the TRS PCU. As detailed in the Site 3 ERH Pilot Test Report, the initial percentage of power applied to the Site 4 remediation was approximately eight percent, while the remaining 92 percent was applied to the Site 3 pilot test. The lowering of the water table at Site 3, though, resulted in a 14 percent change in the ratio of power input to either site (i.e., decreased power to Site 3 and increased power to Site 4). The ratio of power input to each site was extrapolated based on the current surveys conducted by site operations personnel and the total energy input applied by the PCU.

Due to its location (i.e., lower on the northern slope and subject to higher rate of groundwater recharge) and the lower power input, Site 4 did not experience the water table elevation decreases observed at Site 3. Consequently, Site 4 was able to maintain a higher level of electrical conductivity and higher electrical current flow.

4.3 VAPOR RECOVERY SYSTEM

Vapor recovery during the Site 4 ERH remediation was achieved via the 40-hp rotary lobe blower and the eight co-located VR wells within each electrode borehole (refer to Figures 5 and 4 for process flow and electrode/VR well construction details). In addition, vapor recovery was also performed at the Site 3 ERH Pilot Test using the 24 co-located electrode/VR wells. Both sites were operated simultaneously and used the same 40-hp blower, as well as the four vapor phase GAC vessels for vapor treatment.

Site personnel for TTFW provided the staffing for collection of vapor recovery flow rates using a hot-wire anemometer, as well as vapor recovery system pressure and temperature readings in the independent four-inch conveyance lines from Site 3 and Site 4. A table of vapor recovery flow rate data for the two ERH sites, as well as collection dates is provided in Appendix A of this report. The table also provides the calculation for conversion to standard cubic feet per minute (scfm) from actual cubic feet per minute (acfm) provided by the hot wire anemometer.

A comparison between the Site 4 ERH remediation and the Site 3 ERH Pilot Test vapor recovery systems is provided in the following table.

Table 3: Average Soil Vapor Recovery Flow Rate for the Site 4 and Site 3 Pilot Test Period

Site Location and Specifications	August 1, 2003	September 16, 2003	Average Vapor Recovery Flow Rate ^a
Site 3 Vapor Recovery Flow Rate(scfm)	57	52	49
Site 4 Vapor Recovery Flow Rate(scfm)	178	36	138
TRS Work Plan Vapor Recovery Flow Rate (scfm) Estimate (April 2003)		480	

a: Average recovery flow rate is based on 25 sample collection dates; see table in Appendix A.

The GAC units previously described in Section 3.2.6 of this report were changed once during the ERH operations, on September 5, 2003. The spent primary GAC was returned to US Filter Westates and the secondary units were moved into the primary position. Fresh carbon sacks were subsequently replaced in the secondary unit containers.

4.3.1 Condensate Production

As previously stated in Section 4.2, steam and condensate removal from July 31, 2003 through September 19, 2003 (last reading available prior to the official completion of the pilot test on September 24, 2003), resulted in a condensate production of 7,526 gallons of water from Site 4. The average removal rate for condensate based on the totalizer readings over time was approximately 0.1 gpm. The vapor recovery system continued operating until October 10, 2003, resulting in an additional removal of approximately 994 gallons of condensate (active steam production ceased on September 22, 2003, shortly after the cessation of power input to the treatment area). As stated earlier, site operations personnel noted a problem with the condensate totalizer readings on September 16, 2004, due to sand in the line, which was subsequently removed. All the condensate produced during ERH operations was treated with liquid GAC prior to being reinjected in to the electrodes.

4.4 SUBSURFACE TEMPERATURES

The average subsurface temperature from 10 to 25 feet bgs within the ERH treatment area prior to the start of operations was 14 °C based on TMP locations -1, -2 and -3. As shown on Figure 6: Site 4 Temperature Results Per TMP Locations, appropriate boiling point temperatures for

benzene between 18 and 28 feet bgs (approximately 69 to 77 °C according to Table 1 in this report) were achieved during the last week of August at TMP locations -1 and -2 and on September 15, 2003 at TMP-3. The Site 4 average subsurface temperature reached an operational high of 93 °C from September 16, 2003 through September 22, 2003. The daily site average temperature ranged from 88 to 93 °C during that period.

4.4.1 Site 4 Average Subsurface Temperatures

Subsurface temperatures were monitored continuously and recorded daily at each TMP location (refer to the TRS Work Plan 2003 for operational details). As shown on Figure 4 of this report, thermocouples were installed at five-foot intervals from five to 30 feet bgs resulting in a total of six thermocouples (subsurface temperature monitoring points) within each TMP location. The treatment interval for the Site 4 ERH remediation application was 9.5 to 28 feet bgs in accordance with the TRS Work Plan and the TTFW Statement of Work (TRS 2003 and TTFW 2002). The electrode conductive interval, as shown on Figure 4, was from 9.5 feet to 30 feet bgs.

The overall weekly average for each temperature monitoring interval on August 27, 2003 and September 20, 2003 is provided in Table 4: ERH Remediation Temperature Results per TMP Location. The dates selected essentially reflect the middle of the operational period and the documented highest daily average for subsurface temperatures several days before ERH power was shutdown (the official completion of the Site 3 pilot test was on September 24, 2004, however, ERH power input ceased on September 22, 2004 due to a system interlock shutdown).

It should be noted that TMP-3 was located at the perimeter of the target treatment area, and therefore was not subjected to strong active heating. This resulted in lower peak temperatures being achieved at this TMP location. The temperature increase at specific depth intervals (5 to 30 feet bgs) for each TMP location at Site 4 for the duration of the ERH remediation application is presented in Figures 7 through 9.

Table 4: ERH Remediation Temperature Results Per TMP Location

TMP	Date	Average Temperature for Treatment Interval	Subsurface Interval Temperature Average (feet bgs/°C)					ature
Location	(Week Ending)	(°C)	5	10	15	20	25	30
08/27/0	08/27/03	68	37	40	58	83	89	67
TMP-1	09/20/03	94	36	74	99	99	99	95
TMD 0	08/27/03	83	45	44	84	101	104	71
TMP-2	09/20/03	100	55	85	101	101	101	86
TMP-3	08/27/03	49	37	30	38	60	67	48
I IVIE -3	09/20/03	85	45	59	94	86	81	62

Temperature data has been rounded to nearest whole number

As shown in Table 4, there was some fluctuation in temperatures at the various subsurface intervals, however, by September 17, 2003, the average TMP temperature for the ERH application treatment interval (10 to 30 feet bgs) exceeded 90 °C at TMP location -1 and -2 and exceeded 80 °C at TMP-3. According to the information provided in Table 1, 80 °C was above the boiling point for benzene at depth.

The lower subsurface temperatures exhibited at TMP-3, though registering temperature levels necessary to boil benzene, were due to its location on the periphery of the Site 4 treatment area. The other TMP locations, -1 and-2, were located as shown on Figure 3 within close proximity to the center of the treatment area and, consequently, essentially surrounded by ERH electrodes.

Personnel from TTFW continue to measure water levels and subsurface temperatures at Site 3 and Site 4 at the Bedford NWIRP. Graphic representations of the average subsurface temperature decrease per TMP location for Site 4, as well as the predicted trend line for temperature decrease over time, are provided in Figures 10 and 11, respectively. Complete data tables for recorded temperature intervals recorded by TRS prior to, during and after the completion of the ERH remediation are provided in Appendix C.

5.0 SAMPLING ACTIVITIES AND ANALYTICAL RESULTS

The following sections discuss the field sampling activities and present the analytical results for the Site 4 ERH remediation application. The sampling activities conducted prior to, during and after the ERH application and the analytical results provided information to monitor the reduction of BTEX concentrations, specifically benzene (cleanup goal specified by the 2002 TTFW Statement of Work as $50 \mu g/L$).

Sampling events included the collection of groundwater samples from select monitoring wells at the site, as well as the collection of influent vapor samples from Site 3 and Site 4 prior to the GAC inlet; and GAC effluent vapor samples. All sampling activities including field logs, sample collection sheets, as well as sample packaging and shipping were conducted by TTFW personnel, except for the pre-ERH remediation groundwater samples which were collected by Tetra Tech NUS. The tables included within this section of the report were developed by TRS based on sample report information presented by TTFW.

For reference, the available analytical data from the offsite laboratories for the Site 4 remediation are located in Appendix C of this report.

5.1 GROUNDWATER SAMPLING

In accordance with the TRS Work Plan, groundwater sampling events for the Site 4 ERH remediation were conducted prior to, during and after the completion of operations at Site 4 (TRS 2003). The groundwater samples were collected in an effort to monitor the progress of the benzene concentration reduction toward the cleanup goal of 50 µg/L established by the TTFW Statement of Work (TTFW 2002). Cleanup goals were not established for the remaining BTEX constituents (toluene, ethylbenzene and xylene) and, therefore, those constituents are not addressed in this document.

The collected groundwater samples were shipped to an offsite laboratory for VOC analysis using USEPA SW 846 Method 8260a.

Field Sampling Methodology

As detailed in the TRS Work Plan and shown on Figure 12: Monitoring Wellhead Sample Collection Configuration, groundwater samples collected via a peristaltic pump were processed through a stainless steel coil immersed in an ice bath to effectively cool the sample water down to safe handling levels and further minimize any volatilization loss associated with agitation of the groundwater during the sample process (TRS 2003).

As indicated in the late September and early October 2003 Sample Collection Field Sheets maintained by TTFW personnel and presented in Appendix B of this report, some well locations

experienced slow recharge and occasionally dried out during the low flow sample purging process. The reduced yield from ground water monitoring wells observed in the Site 4 monitoring well locations should be attributed to the aforementioned slow recharge and not equated with the decreased water table documented at Site 3 (please refer to the April 2004 Site 3 ERH Pilot Test Report for greater details).

5.1.1 Data Validation

Any data validation of the sample results was the responsibility of TTFW and has not been included in this report, other than laboratory qualifiers. The laboratory results presented in this section of the report and in Appendix A have been assigned data qualifiers by the offsite laboratory. The following laboratory-assigned qualifier codes appear in connection with the analytical results presented in Section 5.0 of this report:

Qualifier Code	Explanation					
U	Not Detected; Detection Limit Listed					
J	Quantification Approximate					
E	Estimated Value					
Oth	ner Notes Assigned to Analytical Results					
ND Not Detected; Detection Limit Unknown						
NA Not Available						

The analytical results tables presented in Section 5 have been reproduced and summarized from tables within Appendix A of this document.

5.1.2 Analytical Results for Site 4 Groundwater Samples

The following tables present the analytical results for the groundwater sampling events conducted prior to, during and after the ERH remediation application at Site 4 for each monitoring well location. Each table presents a separate groundwater sampling event as well as the baseline value for comparison.

The analytical results for the BTEX analyzed via a gas chromatograph/mass spectrometer (GC/MS) have been summarized within this section of the report in order to minimize the size of the tables. A full accounting of all VOCs analyzed per monitoring well location and sample collection date is provided in Appendix A of this report. Values shown in bold represent detections of BTEX constituents during that sample collection event. Other necessary information has either been presented in a regular font or gray-scale to minimize complexity of the tables. In most cases, samples results were based on two dilution factors. While all of the

available data from the laboratories has been provided in this report, TRS has only tabulated on set of data (i.e., the initial sample analysis).

5.1.3 Pre-ERH Remediation Analytical Results for Site 4 Groundwater Samples

Baseline groundwater samples prior to the start of operations at the two ERH sites (July 31, 2003) were collected by TTFW in May and June of 2003 (see table for specific sample collection dates).

Table 5: Pre-ERH Remediation May and June Baseline Sampling and Analytical Results

May and June 2003 Groundwater Sample Event Dates (Site 4 Pre-ERH Remediation)										
Treatment			Analytical Results							
Area Location	Sample Dates		Compound							
		Units	Benzene	Toluene	Ethylbenzene	p/m- Xylene	o- Xylene	Total- Xylene		
MW-18SR	6/15/2003	μ g /L	220	2200	1200	3600	1500	NA		
IW-5	6/30/2003	μ g /L	360	1400	800	1800	600	NA		
MW-61S	5/30/2003	μ g /L	76J	3800	290	7800	4800	NA		
MW-62S	5/29/2003	μ g /L	59	85	110	410	150	NA		
MW-63S	6/2/2003	μ g /L	180	4400	1600	8700	4200	NA		
MW-64S	5/30/2003	μ g /L	210	920	280	6700	4200	NA		
MW-65S	6/2/2003	μ g /L	320	5900	1500	6200	2600	NA		
			Outside	of ERH Tre	eatment Area					
MW-42SR	6/2/2003	μ g /L	14	1.5J	34	22	1.2J	NA		
MW-60S	5/29/2003	μ g /L	250	1800	1600	3500	1200	NA		
MW-60S	5/29/03D	μ g /L	250	2300	1700	3800	1800	NA		
MW-66S	6/30/2003	μ g /L	52	24	210	130	43	NA		

Bold value indicates detected concentration; D: Duplicate sample

Grayscale represents well locations outside treatment area.

Please refer to Appendix A for complete analytical results for the baseline samples collected in May and June 2003 (Pre-ERH remediation) groundwater sampling event.

5.1.4 September Analytical Results for Site 4 Groundwater Samples

Groundwater sampling was conducted twice by TTFW during September of 2003 (see Table 6 for specific sample collection dates). As outlined in the TRS Work Plan, groundwater sample collection was planned for the 60 and 80 percent completion periods of the ERH remediation at Site 4. Based on the extended length of operations, samples were actually collected during the 75 percent completion period of the ERH Remediation.

As shown in Table 6, benzene concentrations for all sampled well locations within the treatment area were below the remediation goal of $50 \mu g/L$. Cleanup goals were not established for the remaining BTEX constituents, however, a relatively significant (any value greater than 10 percent) decrease in groundwater concentrations for toluene, ethylbenzene and xylene is observable.

Table 6: ERH Remediation Early September Operations Sampling and Analytical Results

September (Early) 2003 Groundwater Sample Event Dates (Site 4: 75 percent ERH Remediation)											
		Analytical Results									
Treatment Area	Sample Dates		Compound								
Location	Dates	Units	Benzene	Toluene	Ethylbenzene	p/m- Xylene	o- Xylene	Total- Xylene			
MW-65S	6/2/2003	μ g /L	320	5900	1500	6200	2600	NA			
10100-055	9/9/2003	μg/L	18J	600	420	1800	910	NA			
MW-65D	9/9/2003	μg/L	14J	520	370	1600	780	NA			
MW-63S	6/2/2003	μ g /L	180	4400	1600	8700	4200	NA			
10100-033	9/9/2003	μg/L	10U	14	6.0J	31	7.0J	NA			
MW-18SR	6/15/2003	μ g /L	220	2200	1200	3600	1500	NA			
IVIVV-103K	9/9/2003	μ g /L	2.0U	6.8	3.1	18	2.7	NA			
Remediati	μg/L	50	NE	NE	NE	NE	NE				

Bold value indicates detected concentration; values in gray represent baseline data.

NE: Not established

Please refer to Appendix A for complete analytical results for the early September 2003 (75 percent ERH remediation) groundwater sampling event.

5.1.5 Post-ERH Remediation Analytical Results for Site 4 Groundwater Samples

Post-ERH remediation application groundwater sampling was conducted by TTFW during late September and early October of 2003 (see Table 7 for specific sample collection dates) and again in April 2004. As outlined in the April 2003 TRS Work Plan, post-Site 4 operations groundwater sample collection events were planned to evaluate the effectiveness of the ERH remediation application and to monitor any potential recontamination of the treatment area from potential upgradient sources.

5.1.5.1 Site 4 Late September and Early October Groundwater Sample Results

As shown on Table 7, benzene concentrations remained below the Site 4 ERH remediation cleanup goal of 50 μ g/L during the September 29 through October 1, 2003 sampling event. Monitoring well location MW-62S was flagged with a laboratory qualifier for an estimated value

above the remediation cleanup goal, however, as shown in the April 2004 sampling results in the next section, MW-62S benzene concentration was reported at $3.4~\mu g/L$.

Table 7: Initial Post-ERH Remediation Sampling and Analytical Results

	Late Sep	tember a			Groundwater Sa Remediation)	mple Event	Dates			
Treatment		Analytical Results								
Area Location	Sample Dates	Compound								
Location	Dates	Units	Benzene	Toluene	Ethylbenzene	p/m- Xylene	o- Xylene	Total- Xylene		
MW-18SR	6/15/2003	μ g /L	220	2200	1200	3600	1500	NA		
IVIVV-103R	9/30/2003	μg/L	3.3J	24	15	64	40	NA		
MW-61S	5/30/2003	μ g /L	76J	3800	290	7800	4800	NA		
10100-013	9/30/2003	μ g /L	14J	830	650	4700E	2600E	NA		
MW-62S	5/29/2003	μ g /L	59	85	110	410	150	NA		
10100-023	10/2/2003	μg/L	66J	230	790	2000	710	NA		
MW-63S	6/2/2003	μ g /L	180	4400	1600	8700	4200	NA		
10100-033	10/1/2003	μg/L	20U	27	25	62	24	NA		
MW-64S	5/30/2003	μ g /L	43	920	280	6700	4200	NA		
10100-043	9/30/2003	μg/L	32J	1000	1000	4900	2600	NA		
MW-65S	6/2/2003	μ g /L	320	5900	1500	6200	2600	NA		
10100-055	9/30/2003	μg/L	6.2J	81	78	330	120	NA		
			Outside	of ERH Tre	eatment Area					
MW-42SR	6/2/2003	μg/L	14	1.5J	34	22	1.2J	NA		
10100-42510	9/30/2003	μg/L	20	7.4J	65	71	18	NA		
MW-60S	5/29/2003	μg/L	250	1800	1600	3500	1200	NA		
10100-003	9/29/2003	μg/L	140	670	2100	4600	1100	NA		
MW-66S	6/30/2003	μg/L	52	24	210	130	43	NA		
10100-000	10/1/2003	μg/L	32	91	26	260	93	NA		
MW-66SD	10/1/2003	μg/L	32	86	26	250	90	NA		
Remediat	ion Goal	μg/L	50	NE	NE	NE	NE	NE		

Bold value indicates detected concentration; values in gray represent baseline data and locations outside of the treatment area. NE: Not established

Please refer to Appendix A for complete analytical results for the initial September and October post-ERH remediation groundwater sampling event.

5.1.5.2 Site 4 April 2004 Groundwater Sample Results

As shown on Table 8, benzene concentrations remained below the Site 4 ERH remediation cleanup goal of 50 μ g/L during the April 2004 sampling event.

Table 8: April 2004 Post-ERH Remediation Sampling and Analytical Results

	April 2004	Ground	dwater Sample	e Event Da	ites (Site 4 Post-	ERH Remed	diation)			
Treatment		Analytical Results								
Area Location	Sample Dates		Compound							
		Units	Jnits Benzene Toluene Ethylbenzer		Ethylbenzene	p/m- Xylene	o- Xylene	Total- Xylene		
MW-18SR	6/15/2003	μg/L	220	2200	1200	3600	1500	NA		
IVIVV-105K	4/14/2004	μg/L	41	12	650	800	43	NA		
MW-61S	5/30/2003	μg/L	76J	3800	290	7800	4800	NA		
10100-013	4/13/2004	μ g /L	2.0U	2.0U	2.0U	34	16	NA		
MW-62S	5/29/2003	μ g /L	59	85	110	410	150	NA		
10100-023	4/13/2004	μ g /L	3.4	17	12	47	20	NA		
MW-62SD	4/13/2004	μg/L	3.5	17	12	48	19	NA		
MW-63S	6/2/2003	μg/L	180	4400	1600	8700	4200	NA		
10100-033	4/14/2004	μg/L	26	27	480	1300	290	NA		
MW-64S	5/30/2003	μ g /L	43	920	280	6700	4200	NA		
10100-043	4/14/2004	μg/L	4.4	13	130	1100	260	NA		
MW-65S	6/2/2003	μg/L	320	5900	1500	6200	2600	NA		
10100-000	4/14/2004	μg/L	40	250	280	650	400	NA		
			Outside	of ERH Tre	eatment Area					
MW-42SR	6/2/2003	μ g /L	14	1.5J	34	22	1.2J	NA		
10100 7201	4/13/2004	μ g /L	2.2	2.0U	15	14	2.0U	NA		
MW-60S	5/29/2003	μg/L	250	1800	1600	3500	1200	NA		
10100-003	4/14/2004	μg/L	7.6	1.3J	97	26	6.5	NA		
MW-66S	6/30/2003	μg/L	52	24	210	130	43	NA		
10100-003	4/13/2004	μg/L	91	46	240	190	88	NA		
Remediat		μ g /L	50	NE	NE	NE	NE NE	NE		

Bold value indicates detected concentration; values in gray represent baseline data and locations outside of the treatment area. NE: Not established

The April 2004 analytical results for benzene indicate a rise in concentration at several treatment area monitoring well locations; however the concentrations are still below the $50 \mu g/L$ remediation goal. Based on the increased benzene concentration at monitoring well MW-66S,

located outside of the Site 4 treatment region, as well as the initial high level of benzene concentrations in the baseline samples, it is presumable that recontamination of the monitoring wells is attributable to groundwater flow from source area(s) within close proximity to Site 4 that were not within the ERH remediation boundaries.

Please refer to Appendix A for complete analytical results for the April 2004 post-ERH remediation groundwater sampling event.

5.2 VAPOR SAMPLING

In accordance with the TTFW Statement of Work and the TRS Work Plan, vapor sampling of the influent vapor samples from Site 4 and Site 3 prior to the GAC inlet and at the GAC effluent were conducted by TTFW immediately prior to and during ERH remediation at Site 4 as well as the Site 3 pilot test to monitor the effectiveness of the ERH remediation application and the mass recovery rate (TTFW 2002 and TRS 2003). The vapor sampling was also used to determine breakthrough of the primary GAC units and for determining the appropriate time to change and dispose of the GAC filter bags.

As previously discussed in this report, the vapor recovery piping and sampling ports from each site allowed for the differentiation of the vapor samples from Site 3 and Site 4. The vapor samples were shipped to an offsite laboratory for VOC analysis using modified USEPA Method TO14A. The available laboratory reports regarding vapor analysis are provided in Appendix A.

Field Sampling Methodology

Vapor samples from both of the ERH sites' vapor recovery piping were collected on a weekly basis by TTFW using summa canisters and a flame ionization detector (FID) for determining total VOC recovery prior to the GAC inlet. Due to the reliability issues of the FID (according to TTFW site personnel who used the FID most days of the week for measuring total VOCs), only the quantifiable laboratory data in parts per million by volume (ppmv) from the summa canisters was used to extrapolate the VOC mass removal.

5.2.1 Data Validation

Any data validation of the sample results was the responsibility of TTFW and has not been included in this report, other than laboratory qualifiers. The laboratory results presented in this section of the report and in Appendix A have been assigned data qualifiers by the offsite laboratory. The laboratory-assigned qualifier codes appear in connection with the analytical results presented in Appendix A of this report:

5.2.2 Analytical Results for Site 4 Vapor Recovery

The following table presents the analytical results for the vapor recovery sampling events conducted immediately prior to and during the Site 4 ERH remediation application.

The analytical results tables presented in this section have been reproduced and summarized from tables within Appendix A of this document. The summa canisters were collected on a weekly basis by TTFW personnel from the start of the remediation on July 31, 2003 through August 28, 2003, for Site 4.

Table 9: ERH Remediation Vapor Recovery Sampling and Analytical Results

		Compound							
Date	and Location	BENZENE	ZENE TOLUENE ETHYL BENZEN		M,P- XYLENE	O- XYLENE			
31-Jul-03	SITE 4 INFLUENT	92	1600	260	9200	3600			
31-Jul-03	GAC EFFLUENT	0.86 U	0.86 U	0.86 U	0.86 U	0.86 U			
07-Aug-03	SITE 4 INFLUENT	12	330	66	3000	1400			
07-Aug-03	GAC EFFLUENT	0.90 U	0.90 U	0.90 U	0.90 U	0.90 U			
14-Aug-03	SITE 4 INFLUENT	16.00	140.00	30.00	2300.00	1300.00			
14-Aug-05	GAC EFFLUENT	0.80 U	0.80 U	0.80 U	0.80 U	0.80 U			
22-Aug-03	SITE 4 INFLUENT	32	650	170	5200	2400			
22-Aug-03	GAC EFFLUENT	33 U	33 U	33 U	33 U	33 U			
28-Aug-03	SITE 4 INFLUENT	520	13000	4900	45000	16000			
20-Aug-03	GAC EFFLUENT	260 U	310 U	360 U	110	360 U			

U: Not Detected; Detection Limit Used; PPBV: parts per billion by volume

The fluctuations in VOC concentrations can be attributed to the initial vapor recovery at the site during startup. The following decrease and subsequent peak BTEX concentrations reported in the early weeks of the ERH pilot test can be attributed to increased temperatures and corresponding volatilization of VOCs within the immediate vicinity of the co-located electrode/VR wells. A full accounting of all VOCs analyzed per sample collection dates is provided in tables in Appendix A of this report.

Based on the analytical vapor recovery results in conjunction with the flow rates of the vapor recovery system (measured in scfm), TTFW estimated 95 pounds of VOCs were recovered by the Site 4 VR wells from the start of operations on July 31, 2003 through September 16, 2003. The average rate of VOC removal via the vapory recover system was 2.0 pounds per day (estimated). The daily vapor flow rates and extrapolated mass removal measured and calculated by TTFW are presented in Appendix A.

5.3 REMEDIATION-DERIVED WASTE STREAM SAMPLING

All waste streams, such as water associated with drilling and decontamination, were containerized on site for sampling and disposition by TTFW. Analytical results pertaining to the aforementioned waste stream analysis are not presented in the TRS Site 4 ERH Remediation Report.

6.0 CONCLUSIONS

The Site 4 ERH Remediation was conducted in response to the TTFW Statement of Work (2002) under contract to the U.S. Navy Engineering Field Activity Northeast RAC N62472-99-R-0032, Task Order 0089. The ERH Remediation was designed, constructed and operated to reduce benzene concentrations in groundwater to a cleanup level of 50 µg/L within the treatment volume. The construction of the Site 4 ERH Remediation began in May 2003 and site ERH operations began on July 31, 2003. The official cessation of ERH operations was September 22, 2004, based on available groundwater analytical results, as well as cessation of the Site 3 ERH Pilot Test.

As shown in the data presentation in Section 5 of this report, the benzene remediation goal was achieved at all monitoring well locations within the treatment volume. The April 2004 data results indicate an increase in BTEX concentrations at several locations, including some monitoring wells within the treatment volume. While the treatment volume monitoring well groundwater results are still below the benzene remediation goal, the observed increases indicate a potential recontamination of the treatment area from an outside source location. TRS has submitted a second memorandum to TTFW on April 29, 2004, discussing this observed condition at Site 4 and potential recontamination of the site due to groundwater flow through unremediated soil located outside the ERH treatment volume.

Prior to the start of the ERH operations, the Site 4 ERH Remediation source volume was presumed to be fully delineated, however, initial baseline results of monitoring well locations beyond the periphery of the ERH treatment boundary indicated BTEX concentrations in excess of the benzene cleanup goal established in the November 2002 TTFW Statement of Work. TRS advised TTFW in a letter dated June 19, 2003, of the need for potential expansion of the ERH treatment area to adequately remediate the benzene concentrations in groundwater and to minimize or eliminate the potential for recontamination of the site based on groundwater flow through unremediated soil. The site was expanded beyond the initially proposed treatment volume, however, the baseline sample results indicated the potential for further ERH treatment volume expansion.

Both TRS memorandums have been included in Appendix B of this report.

6.1 BENZENE CONCENTRATION REDUCTION

The primary objective of the Site 4 ERH Remediation was to reduce the pre-ERH application benzene concentrations within the treatment volume to below 50 µg/L. While Site 4 was determined to be a BTEX groundwater contamination source area, the only established reduction goal was for the benzene constituent. The data presented in Section 5.0 indicates that the Site 4

ERH Remediation goal for benzene was met during the operational period from July through September 2003.

As indicated in this report, energy input via the design electrode configuration resulted in subsurface temperatures rising to a level adequate to boil benzene in groundwater (refer to Table 1 for details). Consequently, the Site 4 ERH Remediation system was successful in achieving the benzene cleanup goal. It should be noted, though, that there was significant (i.e., greater than 10 percent) reduction in all BTEX constituent concentration levels, as a result of the remediation efforts.

Since Site 4 was operated in conjunction with the Site ERH Pilot Test, the system was shutdown per the direction of TTFW on September 22, 2003. The groundwater data from Site 4 indicated that prolonged operations beyond the Site 3 ERH Pilot Test would not be necessary since benzene concentrations within the treatment volume monitoring wells were below the 50 μ g/L cleanup goal.

.

7.0 REFERENCES

- (Heron, et al, 1996) "Temperature Effects on the Distribution of Organics in Soil and Groundwater and Implication for Thermally Enhanced In-Situ Remediation," Environmental Science Technology. December.
- Tetra Tech Foster Wheeler (TTFW). 2002. Statement of Work for In-Situ Thermal Treatment Pilot Test, Naval Weapons Industrial Reserve Plant (NWIRP), Bedford, Massachusetts. July.
- Thermal Remediation Services, Inc (TRS). 2003. System Design and Work Plan, Electrical Resistance Heating Remediation, Site 4, Naval Weapons Industrial Reserve Plant (NWIRP), Bedford, Massachusetts. April.
- Thermal Remediation Services, Inc. 2004. Final Report, Site 3 Electrical Resistance Heating Pilot Study, Naval Weapons Industrial Reserve Plant (NWIRP), Bedford, Massachusetts. April.
- DON Environmental Restoration Plan for Fiscal Years 1997-2001. Bedford Naval Weapons Industrial Reserve Plant, Bedford, Massachusetts. Executive Summary.

 (http://5yrplan.nfesc.navy.mil/1997)

 (http://5yrplan.nfesc.navy.mil/previous/mar_1997/ma.pdf)

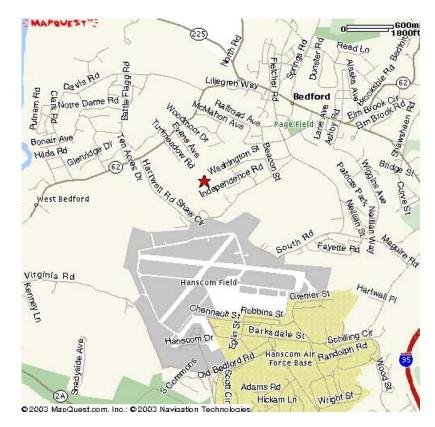
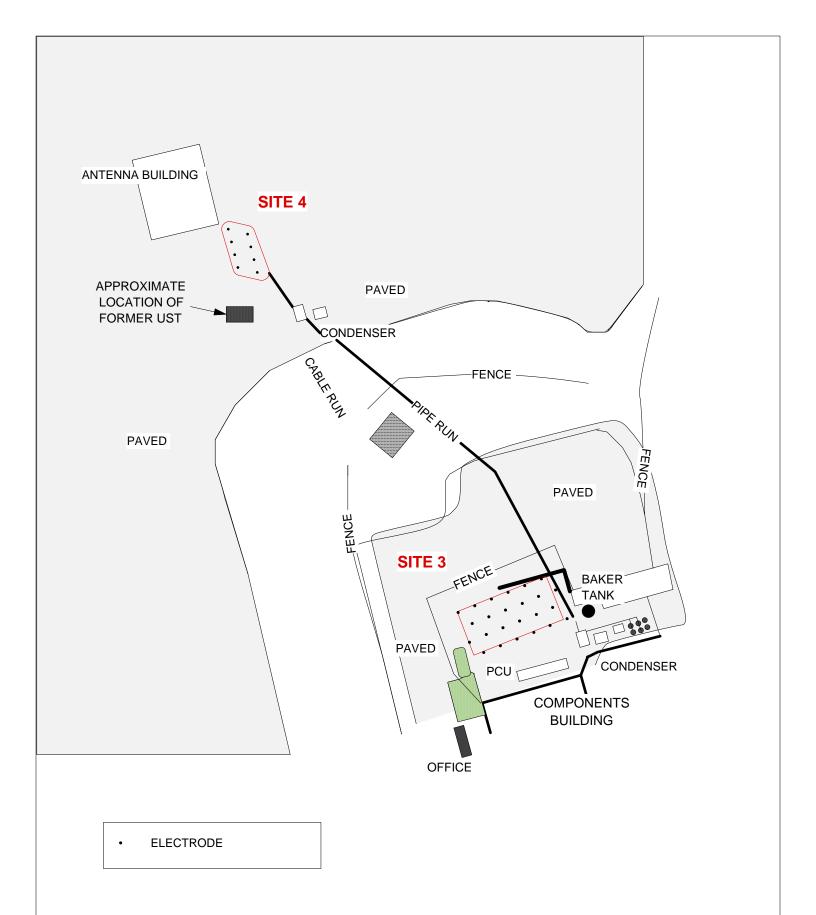




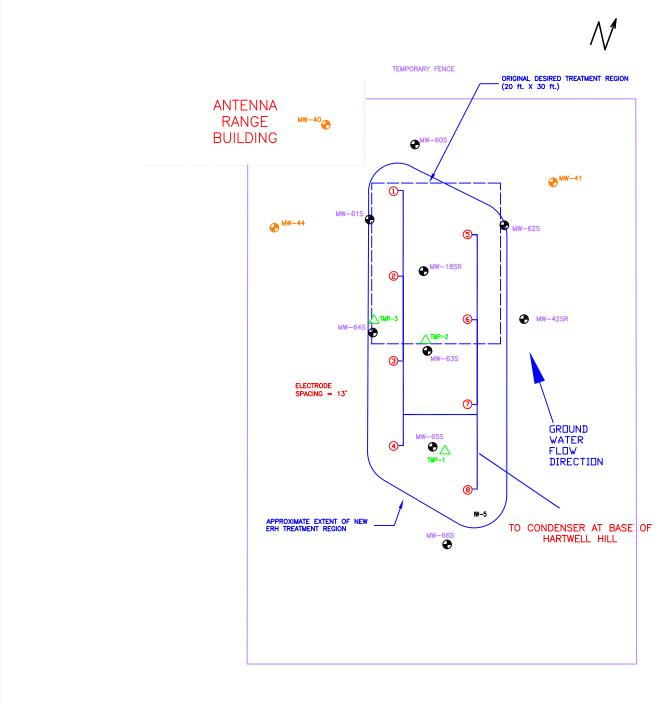
Figure 1: Bedford NWIRP Area Map and Aerial Photo





BEDFORD NWIRP

PROJECT NO.	BED-02
DATE	4/8/03
DRAWN BY	TDP
CHECKED BY	
SCALE:	NONE
FIGURE #	2



LEGEND

NEW OR REPLACEMENT GROUNDWATER MONITORING WELL

(8) CO-LOCATED ELECTRODE AND VAPOR RECOVERY WELL

▲ TMP LOCATION

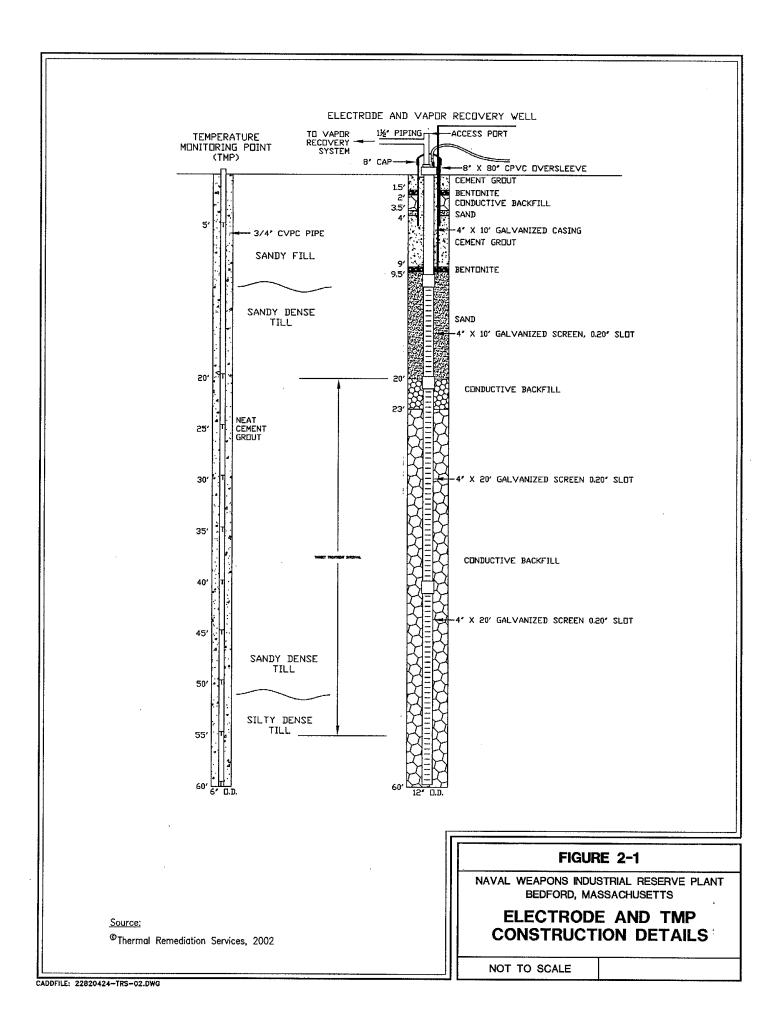
Ó	SCALE IN FEET	15	

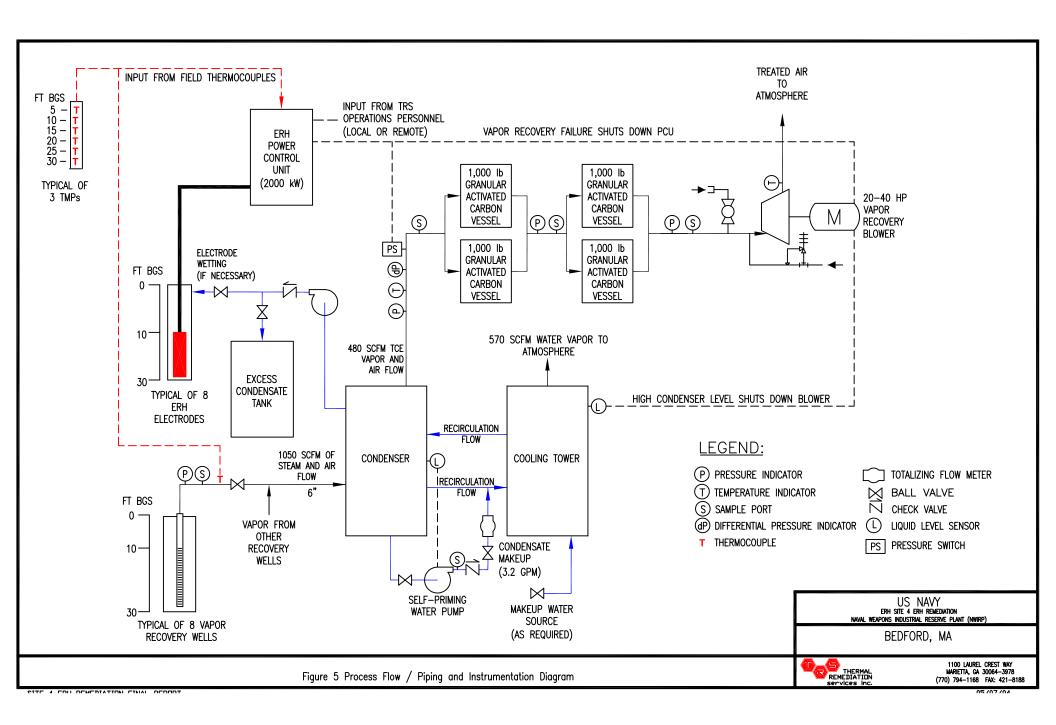
	NO.	DATE	BY	REVISIONS	DESIGN BY:	GB
					DRAWN BY:	GB
					CHECKED BY:	TP
					PROJECT MANAGER:	GS
					DATE:	04/04/03
					SCALE:	ON DWG
					FIGURE NUMBER:	3
					PROJECT NUMBER:	BED02
ENGINEER'S SEAL						

SITE 4 PLOT PLAN

NWIRP BEDFORD, MA







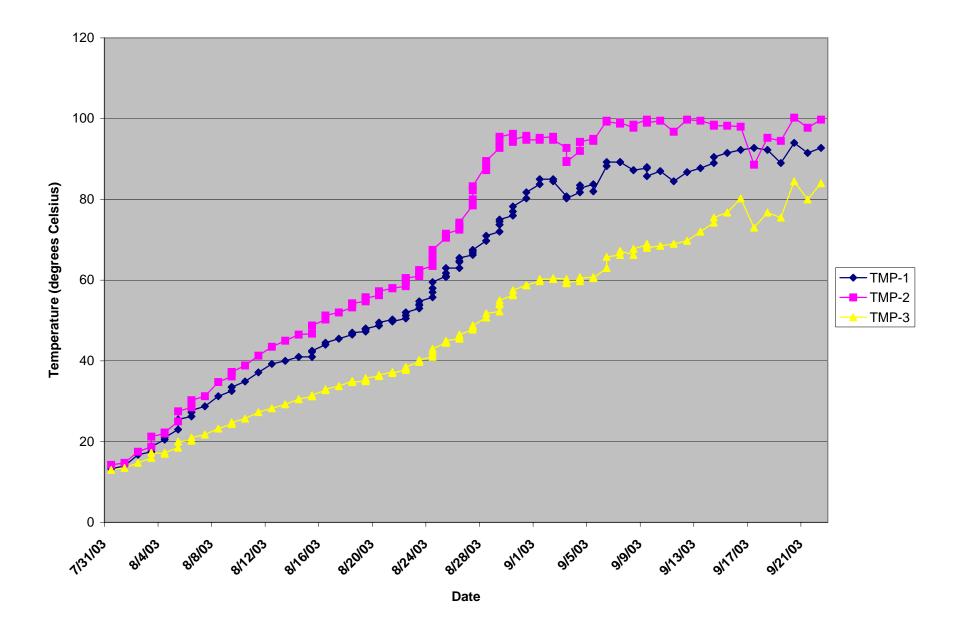


Figure 6: Site Temperature Results Per TMP Location

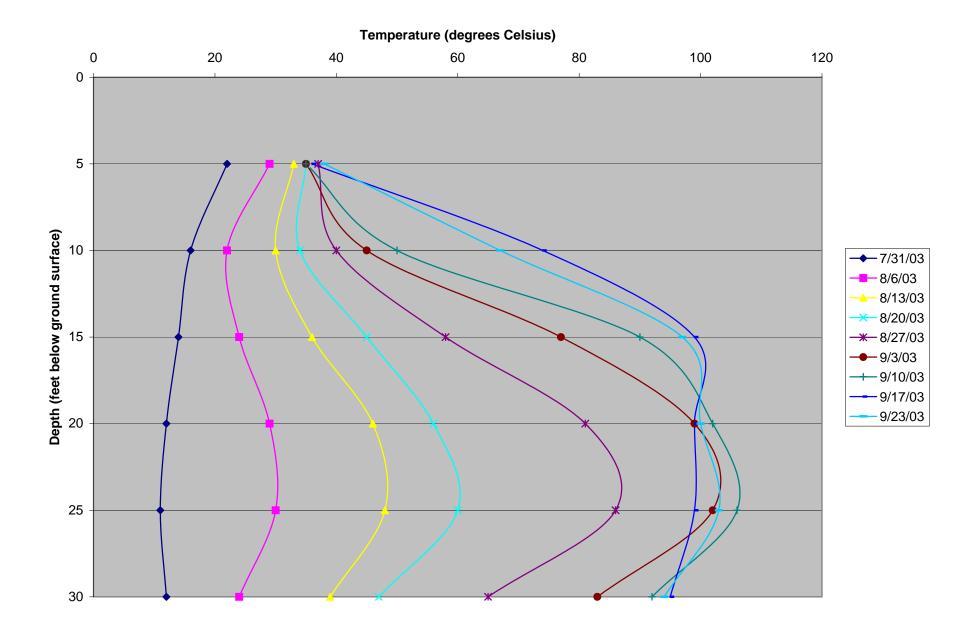


Figure 7: TMP-1 Average Temperatures Per Depth Interval During Operations

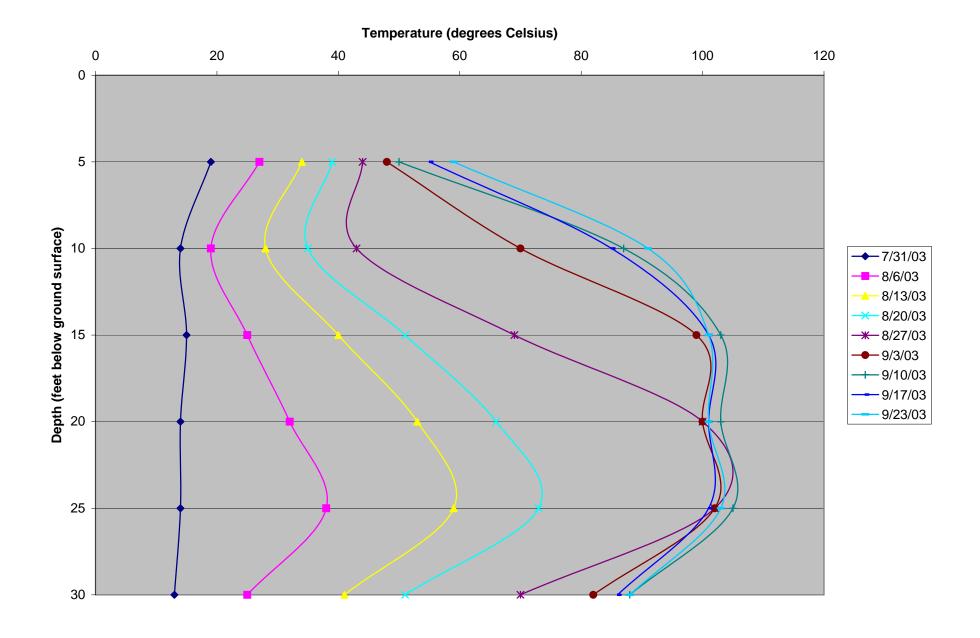


Figure 8: TMP-2 Average Temperatures Per Depth Interval During Operations

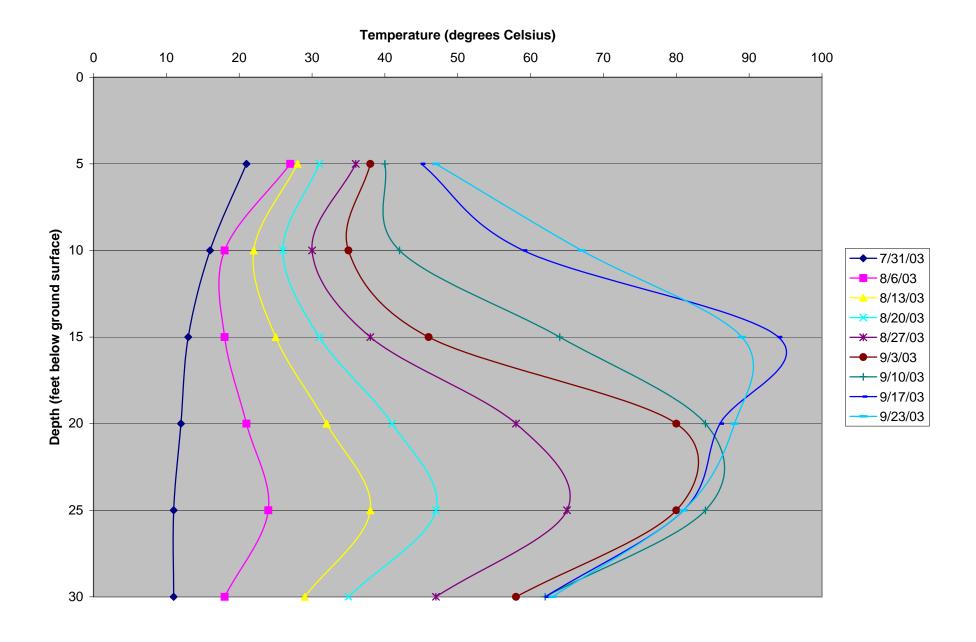


Figure 9: TMP-3 Average Temperatures Per Depth Interval During Operations

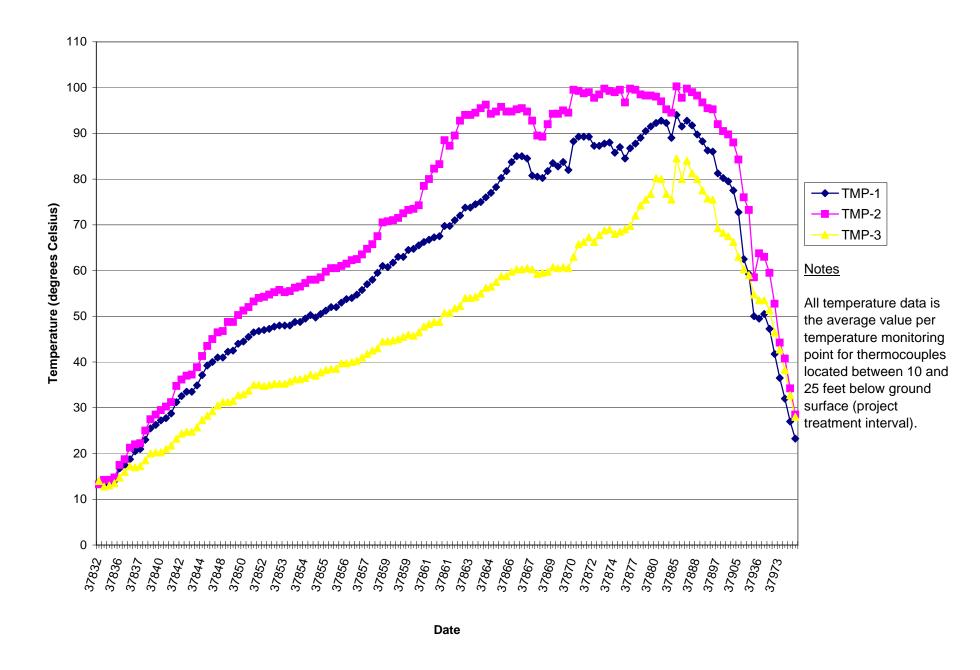


Figure 10: Site 4 Average Subsurface Temperature Decrease Per TMP Location

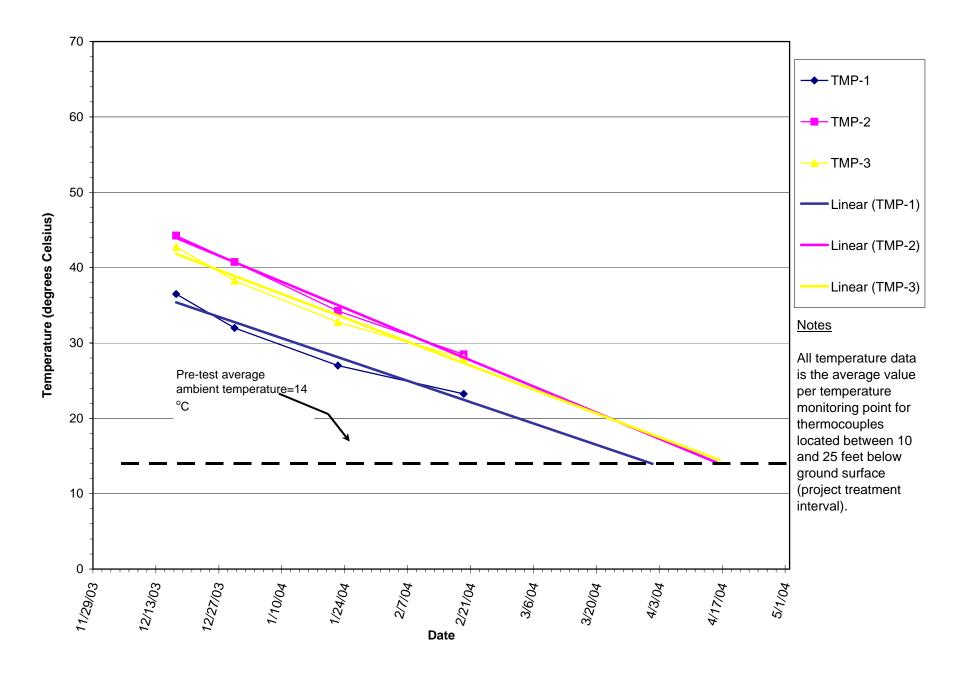
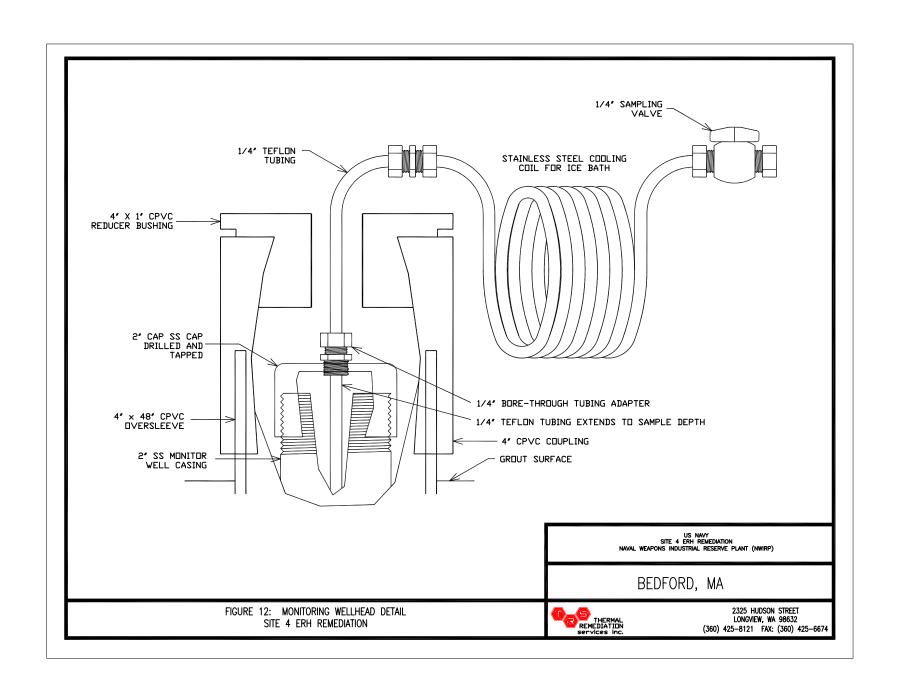


Figure 11: Predicted Trend Line for Site 4 Subsurface Temperature Decrease



APPENDIX A Analytical Results

Site 4 ERH Remediation

		June	2003 Grour	ndwater San	nolina Even	t Dates (Site	4 Pre-Pilot	t Test)				
	Treatmen				, 3		alytical Res					
0	t Area	Treatment A	rea Location	ns and Sam	pling Dates		,					
Compound	Location	5/29/03	5/29/03D	5/29/03	6/2/03	6/15/03	6/30/03	6/30/03				
	Units	MW-60S	MW-60S	MW-62S	MW-61S	MW-64S	MW-65S	MW-42SR	MW-63S	MW-18SR	IW-5	MW-66S
			Previously	y Identified I	Primary Cor	ntaminants o	f Concern					
Benzene	μg/L	250	250	59	76J	43	320	14	180	220	360	52
Toluene	μ g/L	1800	2300	85	3800	920	5900	1.5J	4400	2200	1400	24
Ethylbenzene	μ g/L	1600	1700	110	290	280	1500	34	1600	1200	800	210
p/m-Xylene	μg/L	3500	3800	410	7800	6700	6200	22	8700	3600	1800	130
o-Xylene	μg/L	1200	1800	150	4800	4200	2600	1.2J	4200	1500	600	43
Total-Xylene	μg/L	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
				Other Volat	ile Organic	Compounds						
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
1,1,2,2-Tetrachloroethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
1,1,2-Trichloroethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
1,1 Dichloroethane (1,1-DCA)	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
1,1-Dichloroethene	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
1,2-Dichloroethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
1,2-Dichloroethene (total)	μg/L	NA	NA	NA	NA	40U	100U	NA	100U	NA	20U	4U
1,2-Dichloropropane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
2-Butanone (MEK)	μg/L	46	110	NA	110	150	100U	8.7	75J	42	39	4.8
2-Hexanone	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
4-Methyl-2-pentanone	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Acetone	μg/L	110	210	51	190J	210	200J	29	220J	99J	100	18
Bromodichloromethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Bromoform	μ g/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Bromomethane	μ g/L	100U	100U	NA	250U	100U	250U	5.0U	250U	100U	50U	10U
Carbon Disulfide	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Carbon Tetrachloride	μ g/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Chlorobenzene	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Chloroethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Chloroform	μg/L	40U	40U	26	100U	40U	100U	2.0U	100U	40U	20U	4.1
Chloromethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Cis-1,2-Dichloroethene (cs-1,2-DC)	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
cis-1,3-Dichloropropene	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Dibromochloromethane	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Methylene Chloride	μg/L	100U	100U	NA	250U	100U	250U	5.0U	250U	100U	50U	10U
Methyl tert-butyl ether (MTBE)	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Methyl isobutyl ketone (MIBK)	μg/L	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
Naphthalene	μg/L	320	380	89	240	360	360	11	410	290	190	31
Styrene	μg/L	NA	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Tetrachloroethene (PCE)	μg/L	NA	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Trans-1,2-Dichloroethene	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
trans-1,3-Dichloropropene	μg/L	40U	40U	NA	100U	40U	100U	2.0U	100U	40U	20U	4U
Trichloroethene (TCE)	μg/L	40U	40U	NA	100U	40U	100U	1.2J	100U	29J	16J	5.4
Vinyl Chloride	μg/L	40U	40U	NA	100U	24J	100U	2.0U	100U	40U	20U	4U

Notes
Laboratory Qualifiers
U = Not Detected; Detection Limit Listed
J = Quantitation Approximate
ND = Not Detected; Detection Limit Unknown
NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration D= Duplicate

Other
Analytical Data Table developed from laboratory reports and samples collected by TTFW
TTFW = Tetra Tech Foster Wheeler
VOC= volatile organic compound
µg/L = micrograms per lites
NE = Not established

Location outside of treatment volume

			Septe	mber 2003 Mid-	Heating Grou	ndwater Sa	mpling Event (Si	ite 4 Operatio	ns)				
		1			ent Per Treatr		Monitoring Well L	ocation	MW-65				
Compound		MW-18SR			MW-63S					MW-65S (D)			
	Units	May/June Baseline	9/9/03 Results	Remediation Goal (µg/L)	May/June Baseline	9/9/03 Results	Remediation Goal (µg/L)	May/June Base	9/9/03 Results	Remediation Goal (µg/L)	May/June Base	9/9/03 Results	Remediation Goal (µg/L)
		Daseille	Results	, 0			aminants of Con		Results	Goai (μg/L)	Dase	Results	Goai (μg/L)
Benzene	μg/L	220	2.0U	50	180	10U	50	320	18J	50	320	14J	50
Toluene	μg/L μg/L	2.200	6.8	NE	4.400	14	NE	5.900	600	NE	5,900	520	NE
Ethylbenzene	μg/L	1,200	3.1	NE NE	1,600	6.0J	NE NE	1,500	420	NE NE	1,500	370	NE NE
p/m-Xylene	μg/L	3,600	18	NE NE	8,700	31	NE NE	6,200	1800	NE NE	6,200	1600	NE NE
o-Xylene	μg/L	1,500	2.7	NE NE	4,200	7.0J	NE NE	2,600	910	NE NE	2,600	780	NE NE
Total-Xylene	μg/L	NA	NA	NE NE	4,200 NA	NA	NE NE	2,000 NA	NA	NE NE	NA	NA	NE NE
Total-Aylerie	μg/L	INA	INA		Other Volatile			NA	IVA	INC	INA	INA	INE
Chloromethane	μg/L	40U	2.0U	NE	100U	10U	NE NE	100U	20U	NE	100U	20U	NE
Cis-1,2-Dichloroethene (cs-1,2-DCI	μg/L	40U	NA	NE	100U	NA	NE	100U	NA	NE	100U	NA	NE
Trans-1.2-Dichloroethene	μg/L μg/L	40U	NA	NE	100U	NA	NE	100U	NA	NE	100U	NA	NE
1,2-Dichloroethene (total)	μg/L μg/L	NA	5.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
1,1 Dichloroethane (1,1-DCA)	μg/L μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L μg/L	40U	2.0U	NE NE	100U	10U	NE NE	100U	20U	NE	100U	20U	NE NE
Trichloroethene (TCE)	μg/L μg/L	29J	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Tetrachloroethene (PCE)	μg/L μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Vinyl Chloride	μg/L μg/L	40U	2.0U	NE NE	100U	10U	NE NE	100U	20U	NE NE	100U	20U	NE NE
Bromomethane	μg/L	100U	5.0U	NE	250U	25U	NE	250U	50U	NE	250U	50U	NE
Chloroethane	μg/L μg/L	40U	2.0U	NE NE	100U	10U	NE NE	100U	20U	NE NE	100U	20U	NE NE
Acetone	μg/L μg/L	99J	2.00 220E	NE NE	220J	2300E	NE NE	200J	840	NE NE	200J	710	NE NE
1.1-Dichloroethene	μg/L μg/L	40U	2.0U	NE NE	100U	10U	NE NE	100U	20U	NE NE	100U	20U	NE NE
Carbon Disulfide	μg/L μg/L	40U	1.0J	NE NE	100U	13	NE NE	100U	20U	NE NE	100U	20U	NE NE
Methylene Chloride	μg/L μg/L	100U	5.0U	NE NE	250U	25U	NE NE	250U	50U	NE NE	250U	50U	NE NE
Methyl tert-butyl ether (MTBE)	μg/L μg/L	40U	2.0U	NE	100U	10U	NE NE	100U	20U	NE NE	100U	20U	NE NE
2-Butanone (MEK)	μg/L μg/L	400	12	NE NE	75J	250	NE NE	100U	110	NE NE	100U	100	NE NE
Chloroform	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Carbon Tetrachloride	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
1.2-Dichloroethane	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
1,2-Dichloropropane	μg/L μg/L	40U	2.0U	NE NE	100U	10U	NE NE	100U	20U	NE NE	100U	20U	NE NE
Bromodichloromethane	μg/L μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	5.0U	NE	NA	25U	NE	NA	50U	NE	NA	50U	NE
cis-1,3-Dichloropropene	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
trans-1,3-Dichloropropene	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
1.1.2-Trichloroethane	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
2-Hexanone	μg/L	40U	5.0U	NE	100U	25U	NE	100U	50U	NE	100U	50U	NE
Dibromochloromethane	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Chlorobenzene	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Styrene	μg/L	40U	5.0U	NE	100U	25U	NE	100U	50U	NE	100U	50U	NE
Bromoform	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
1.1.2.2-Tetrachloroethane	μg/L	40U	2.0U	NE	100U	10U	NE	100U	20U	NE	100U	20U	NE
Naphthalene	μg/L	290	2.5J	NE	410	11J	NE	360	790	NE	360	670	NE NE
ivapriirialerie	μ9/⊏	290	2.5J	INE	410	HJ	INE	300	790	INE	300	070	INE

Notes

<u>Laboratory Qualifiers</u>
U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

Other

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

μg/L = micrograms per lites

NE = Not established

Location outside of treatment volume

				Groundwater Sa						
2	-	VOC		t Per Treatment	Area Monito				1111010	
Compound	110:40	MW-60S			May/June	MW-615		MW-64S		
	Units	May/June Baseline	9/29/03 Results	Remediation Goal (µg/L)	Baseline	9/30/03 Results	Remediation Goal (µg/L)	May/June Base	9/30/03 Results	Remediation Goal (µg/L)
				dentified Primar			,, ,	Dase	Results	Goai (μg/L)
Benzene	μg/L	250	140	50	76J	14J	50	43	32J	50
Toluene	μg/L	1.800	670	NE	3,800	830	NE	920	1000	NE
Ethylbenzene	μg/L	1,600	2100	NE NE	290	650	NE NE	280	1000	NE NE
p/m-Xylene	μg/L	3,500	4600	NE NE	7.800	4700E	NE NE	6.700	4900	NE NE
o-Xvlene	μg/L	1,200	1100	NE NE	4.800	2600E	NE NE	4.200	2600	NE NE
Total-Xylene	μg/L	NA	NA	NE NE	NA	NA NA	NE NE	NA	NA	NE NE
Total-∧ylerie	μg/L	INA		ther Volatile Org			INE	NA	IVA	INC
Chloromethane	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
Cis-1,2-Dichloroethene (cs-1,2-DCI	μg/L	40U	NA	NE	100U	NA	NE	40U	NA	NE NE
Trans-1.2-Dichloroethene	μg/L μg/L	40U	NA	NE	100U	NA	NE	40U	NA	NE
	μg/L	NA	40U	NE	NA	20U	NE	40U	40U	NE NE
	μg/L μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
	μg/L μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE NE
	μg/L	NA	40U	NE	100U	20U	NE	40U	40U	NE
	μg/L	40U	40U	NE	100U	20U	NE	24J	40U	NE NE
Bromomethane	μg/L	100U	40U	NE	250U	20U	NE	100U	40U	NE
	μg/L	40U	40U	NE NE	100U	20U	NE NE	40U	40U	NE NE
Acetone	μg/L	110	73J	NE	190J	320	NE	210	2400	NE
1,1-Dichloroethene	μg/L	40U	40U	NE	190J	20U	NE	40U	40U	NE
Carbon Disulfide	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE NE
Methylene Chloride	μg/L	100U	100U	NE	250U	50U	NE	100U	100U	NE
Methyl tert-butyl ether (MTBE)	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
2-Butanone (MEK)	μg/L	46	26J	NE	110	97	NE	150	460	NE
Chloroform	μg/L	40U	40U	NE NE	100U	20U	NE	40U	40U	NE NE
Carbon Tetrachloride	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
1,2-Dichloroethane	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
1,2-Dichloropropane	μg/L μg/L	40U	40U	NE NE	100U	20U	NE NE	40U	40U	NE NE
	μg/L	40U	40U	NE NE	100U	20U	NE NE	40U	40U	NE NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	40U	NE	NA	20U	NE	NA	40U	NE
cis-1,3-Dichloropropene	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
trans-1,3-Dichloropropene	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
1,1,2-Trichloroethane	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
2-Hexanone	μg/L	40U	40U	NE	100U	20U	NE	40U	22J	NE
Dibromochloromethane	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
Chlorobenzene	μg/L	40U	40U	NE NE	100U	20U	NE NE	40U	40U	NE
Styrene	μg/L	NA	40U	NE	100U	20U	NE	40U	40U	NE
Bromoform	μg/L	40U	40U	NE	100U	20U	NE	40U	40U	NE
1.1.2.2-Tetrachloroethane	μg/L	40U	40U	NE NE	100U	20U	NE NE	40U	40U	NE
Naphthalene	μg/L	320	600	NE	240	170	NE	360	1700	NE

Notes

Laboratory Qualifiers

U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

Other

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

Page 1 of 2

μg/L = micrograms per lites

NE = Not established

Location outside of treatment volume

		Septembe	r 2003 Gro	undwater Samp	ling Event Da	ates (Site 4	Operations)			
		VOC		t Per Treatment	Area Monito					
Compound		MW-18SR		MW-42SR			MW-65S			
	Units	May/June	9/30/03	Remediation	May/June	9/30/03	Remediation	May/June	9/30/03	Remediation
	ш	Baseline	Results	Goal (μg/L)	Baseline	Results	Goal (μg/L)	Baseline	Results	Goal (μg/L)
Danasa	/1	220		dentified Primar 50	y Contaminar 14	nts of Conce	ern 50	320	6.2J	50
Benzene	μg/L		3.3J	NE	1.5J	7.4J	NE		81	50 NE
Toluene Ethylbenzene	μg/L μg/L	2,200 1,200	24 15	NE NE	34	65	NE NE	5,900 1,500	78	NE NE
p/m-Xylene	μg/L μg/L	3,600	64	NE NE	22	71	NE NE	6,200	330	NE NE
o-Xylene	μg/L μg/L	1,500	40	NE NE	1.2J	18	NE NE	2,600	120	NE NE
Total-Xylene	μg/L	NA	NA	NE NE	NA	NA	NE NE	2,000 NA	NA	NE NE
Total-Aylerie	μg/L	NA		ther Volatile Ord			INE	NA	NA.	INE
Chloromethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Cis-1.2-Dichloroethene (cs-1.2-DCl		40U	4.00 NA	NE	2.0U	NA	NE	100U	NA	NE
Trans-1,2-Dichloroethene	μg/L	40U	NA	NE	2.0U	NA	NE	100U	NA	NE NE
1,2-Dichloroethene (total)	μg/L	NA	4.0U	NE	NA	10U	NE	NA	10U	NE
1,1 Dichloroethane (1,1-DCA)	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Trichloroethene (TCE)	μg/L	29J	4.0U	NE	1.2J	10U	NE	100U	6.9J	NE
Tetrachloroethene (PCE)	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Vinvl Chloride	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Bromomethane	μg/L	100U	4.0U	NE	5.0U	10U	NE	250U	10U	NE
Chloroethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Acetone	μg/L	99J	690E	NE	29	39	NE	200J	370	NE
1,1-Dichloroethene	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Carbon Disulfide	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Methylene Chloride	μg/L	100U	10U	NE	5.0U	25U	NE	250U	10U	NE
Methyl tert-butyl ether (MTBE)	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
2-Butanone (MEK)	μg/L	42	91	NE	9	11	NE	100U	42	NE
Chloroform	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Carbon Tetrachloride	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
1,2-Dichloroethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
1,2-Dichloropropane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Bromodichloromethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	4.0U	NE	NA	10U	NE	NA	10U	NE
cis-1,3-Dichloropropene	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
trans-1,3-Dichloropropene	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
1,1,2-Trichloroethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
2-Hexanone	μg/L	40U	2.7J	NE	2.0U	10U	NE	100U	25U	NE
Dibromochloromethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Chlorobenzene	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Styrene	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Bromoform	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
1,1,2,2-Tetrachloroethane	μg/L	40U	4.0U	NE	2.0U	10U	NE	100U	10U	NE
Naphthalene	μg/L	290	40	NE	11	28	NE	360	90	NE

Notes

Laboratory Qualifiers

U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

Other

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

 μ g/L = micrograms per lites

NE = Not established

Location outside of treatment volume

				October 2003	Groundwater	Sampling Ev	vent Results (Sit	te 4 Operation	ns)				
					stituent Per Tr		a Monitoring We	ell Location					
Compound	1.1		MW-669			MW-66S (D			MW-63S			MW-628	
	Units	May/June Baseline	10/1/03 Results	Remediation Goal (µg/L)	May/June Baseline	10/1/03 Results	Remediation Goal (µg/L)	May/June Base	10/1/03 Results	Remediation Goal (µg/L)	May/June Base	10/2/03 Results	Remediation Goal (µg/L)
		Daseillie	Results				ontaminants of C		Results	Goar (µg/L)	Dase	Results	Goal (μg/L)
Benzene	μg/L	52	32	50	52	32	50	180	20U	50	59	66J	50
Toluene	μg/L	24	91	NE	24	86	NE	4,400	27	NE	85	230	NE
Ethylbenzene	μg/L	210	26	NE NE	210	26	NE NE	1.600	25	NE NE	110	790	NE NE
p/m-Xvlene	μg/L	130	260	NE NE	130	250	NE NE	8.700	62	NE NE	410	2000	NE NE
o-Xylene	μg/L	43	93	NE NE	43	90	NE NE	4.200	24	NE NE	150	710	NE NE
Total-Xylene	μg/L	NA	NA	NE NE	NA	NA	NE NE	4,200 NA	NA	NE NE	NA	NA	NE NE
Total-Aylerie	μg/L	INA	INA	INL			Compounds	NA	IVA	INL	INA	IVA	INL
Chloromethane	μg/L	4U	10U	NE	4U	10U	NE NE	100U	20U	NE	NA	100U	NE
Cis-1,2-Dichloroethene (cs-1,2-DC)	μg/L	4U	NA	NE	4U	NA	NE	100U	NA	NE	NA	NA	NE
Trans-1.2-Dichloroethene	μg/L μg/L	4U	NA	NE NE	4U	NA NA	NE	100U	NA	NE	NA	NA	NE
1,2-Dichloroethene (total)	μg/L μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
1.1 Dichloroethane (1.1-DCA)	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
1.1.1-Trichloroethane (1.1.1-TCA)	μg/L μg/L	4U	10U	NE NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Trichloroethene (TCE)	μg/L	5.4	6.7J	NE	5.4	6.3J	NE	100U	20U	NE	NA	100U	NE
Tetrachloroethene (PCE)	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Vinvl Chloride	μg/L	4U	10U	NE NE	4U	10U	NE NE	100U	20U	NE	NA	100U	NE
Bromomethane	μg/L	10U	10U	NE	10U	10U	NE	250U	20U	NE	NA	100U	NE
Chloroethane	μg/L	4U	10U	NE NE	4U	10U	NE NE	100U	20U	NE	NA	100U	NE
Acetone	μg/L	18	25	NE	18	23J	NE	220J	620	NE	51	310	NE
1.1-Dichloroethene	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Carbon Disulfide	μg/L	4U	10U	NE NE	4U	10U	NE NE	100U	20U	NE	NA	100U	NE
Methylene Chloride	μg/L	10U	10U	NE NE	10U	10U	NE	250U	20U	NE	NA	100U	NE NE
Methyl tert-butyl ether (MTBE)	μg/L	4U	10U	NE NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
2-Butanone (MEK)	μg/L	5	9.8J	NE NE	5	9.3J	NE	75J	92	NE	NA	63J	NE
Chloroform	μg/L	4	10U	NE NE	4	10U	NE	100U	20U	NE	26	100U	NE
Carbon Tetrachloride	μg/L	4U	10U	NE NE	4 4U	10U	NE NE	100U	20U	NE	NA	100U	NE
1.2-Dichloroethane	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
1,2-Dichloropropane	μg/L	4U 4U	10U	NE NE	4U 4U	10U	NE NE	100U	20U	NE NE	NA NA	100U	NE NE
Bromodichloromethane	μg/L	4U	10U	NE NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	7.5J	NE NE	NA	7.2J	NE	NA	20U	NE	NA	100U	NE
cis-1,3-Dichloropropene	μg/L	4U	10U	NE NE	4U	10U	NE NE	100U	20U	NE	NA	100U	NE NE
trans-1,3-Dichloropropene	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
1,1,2-Trichloroethane	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
2-Hexanone	μg/L	4U	25U	NE	4U	25U	NE	100U	50U	NE	NA	250U	NE
Dibromochloromethane	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Chlorobenzene	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Styrene	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Bromoform	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
1.1.2.2-Tetrachloroethane	μg/L	4U	10U	NE	4U	10U	NE	100U	20U	NE	NA	100U	NE
Naphthalene	μg/L	31	8.7J	NE NE	31	8.6J	NE NE	410	21	NE NE	89	340	NE NE
rapridiatelle	rg/L	31	0.70	INL	31	0.00	INL	410	41	INL	03	340	INL

Laboratory Qualifiers
U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

Other

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

μg/L = micrograms per lites

NE = Not established

Location outside of treatment volume

							ent (Site 4 Opera						
			101/00/		ent Per Treat		Ionitoring Well L	ocation	1011010			101/00	2
Compound	Units		MW-603			MW-61S			MW-64S 4/14/04	In re		MW-66	
	Units	May/June Baseline	4/14/04 Results	Remediation Goal (µg/L)	May/June Baseline	4/13/04 Results	Remediation Goal (µg/L)	May/June Base	Results	Remediation Goal (µg/L)	May/June Base	4/13/04 Results	Remediation Goal (µg/L)
		Daseille	Results				minants of Con		Results	Goar (µg/L)	Dase	Results	Goar (µg/L)
Benzene	μq/L	250	7.6	50	76J	2.0U	50	43	4.4	50	52	91	50
Toluene	μg/L	1.800	1.3J	NE	3,800	2.0U	NE	920	13	NE	24	46	NE NE
Ethylbenzene	μg/L	1,600	97	NE	290	2.0U	NE	280	130	NE NE	210	290	NE
p/m-Xylene	μg/L	3,500	26	NE	7.800	34	NE	6.700	1100E	NE	130	190	NE
o-Xylene	μg/L	1,200	6.5	NE	4,800	16	NE	4,200	310E	NE	43	88	NE
Total-Xvlene	μg/L	NA	NA	NE	NA	NA	NE	NA	NA	NE	NA	NA	NE
retai rytene	F-9-			.,_	Other Volatil			10.1		.,		1.01	.,_
Chloromethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Cis-1,2-Dichloroethene (cs-1,2-DC	μg/L	40U	NA	NE	100U	NA	NE	40U	NA	NE	4U	NA	NE
Trans-1,2-Dichloroethene	μg/L	40U	NA	NE	100U	NA	NE	40U	NA	NE	4U	NA	NE
1,2-Dichloroethene (total)	μg/L	NA	4.5	NE	NA	2.0U	NE	40U	2.0U	NE	4U	2.7	NE
1,1 Dichloroethane (1,1-DCA)	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Trichloroethene (TCE)	μg/L	40U	1.4J	NE	100U	2.0U	NE	40U	2.0U	NE	5.4	3.5	NE
Tetrachloroethene (PCE)	μg/L	NA	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Vinvl Chloride	μg/L	40U	2.0U	NE	100U	2.0U	NE	24J	2.0U	NE	4U	2.0U	NE
Bromomethane	μg/L	100U	2.0U	NE	250U	2.0U	NE	100U	2.0U	NE	10U	2.0U	NE
Chloroethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	1.6J	NE
Acetone	μg/L	110	4.1J	NE	190J	4.0J	NE	210	13	NE	18	5.0U	NE
1,1-Dichloroethene	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Carbon Disulfide	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Methylene Chloride	μg/L	100U	5.0U	NE	250U	5.0U	NE	100U	5.0U	NE	10U	5.0U	NE
Methyl tert-butyl ether (MTBE)	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
2-Butanone (MEK)	μg/L	46	1.8J	NE	110	2.0J	NE	150	7.5	NE	5	14	NE
Chloroform	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4	2.0U	NE
Carbon Tetrachloride	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
1,2-Dichloroethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
1,2-Dichloropropane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Bromodichloromethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	2.0U	NE	NA	1.0J	NE	NA	1.7J	NE	NA	2.0U	NE
cis-1,3-Dichloropropene	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
trans-1,3-Dichloropropene	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
1,1,2-Trichloroethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
2-Hexanone	μg/L	40U	1.6J	NE	100U	4	NE	40U	4.2	NE	4U	2.0U	NE
Dibromochloromethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Chlorobenzene	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Styrene	μg/L	NA	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Bromoform	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
1,1,2,2-Tetrachloroethane	μg/L	40U	2.0U	NE	100U	2.0U	NE	40U	2.0U	NE	4U	2.0U	NE
Naphthalene	μg/L	320	52	NE	240	1.2J	NE	360	670E	NE	31	40	NE

Laboratory Qualifiers
U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

μg/L = micrograms per lites

NE = Not established

Location outside of treatment volume

							Dates (Site 4 Op						
					ent Per Treat		Ionitoring Well L	ocation					
Compound			MW-18S			MW-42SI			MW-65S	1		MW-62	
	Units		4/14/04	Remediation	May/June	4/13/04	Remediation	May/June	4/14/04	Remediation			Remediation
		Baseline	Results	Goal (μg/L)	Baseline	Results	Goal (μg/L) aminants of Cond	Baseline	Results	Goal (μg/L)	Baseline	Results	Goal (μg/L)
Benzene	μg/L	220	41	50	y identified P	2.2	50	320	40	50	59	3.4	50
Toluene	μg/L	2.200	13	NE	1.5J	2.0U	NE	5,900	310E	NE	85	17	NE
Ethylbenzene	μg/L	1.200	650E	NE NE	34	15	NE NE	1,500	330E	NE NE	110	12	NE NE
p/m-Xylene	μg/L	3,600	840E	NE NE	22	14	NE NE	6,200	740E	NE NE	410	47	NE NE
o-Xylene	μg/L	1,500	50 50	NE NE	1,2J	2.0U	NE NE	2,600	460E	NE NE	150	20	NE
Total-Xvlene	μg/L	NA	NA	NE NE	NA	NA	NE NE	NA	NA.	NE NE	NA	NA	NE
Total Aylene	μ9/-	1375	NA	IVL	Other Volatil			INA	11/4	INC	11/5	М	IVE
Chloromethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE NE	100U	2.0U	NE	NA	2.0U	NE
Cis-1,2-Dichloroethene (cs-1,2-DC	μg/L	40U	NA	NE	2.0U	NA.	NE	100U	NA	NE	NA	NA	NE
Trans-1.2-Dichloroethene	μg/L	40U	NA	NE	2.0U	NA	NE	100U	NA	NE	NA	NA	NE
1.2-Dichloroethene (total)	μg/L	NA	16	NE	NA NA	2.0U	NE	NA	4.4	NE	NA	2.0U	NE
1.1 Dichloroethane (1.1-DCA)	μg/L	40U	1.4J	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Trichloroethene (TCE)	μg/L	29J	1.9J	NE	1.2J	2.0U	NE	100U	5.6	NE	NA	2.0U	NE
Tetrachloroethene (PCE)	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Vinyl Chloride	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Bromomethane	μg/L	100U	2.0U	NE	5.0U	2.0U	NE	250U	2.0U	NE	NA	2.0U	NE
Chloroethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Acetone	μg/L	99J	11	NE	29	8.5	NE	200J	16	NE	51	2.7J	NE
1,1-Dichloroethene	μg/L	40U	1.6J	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Carbon Disulfide	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Methylene Chloride	μg/L	100U	5.0U	NE	5.0U	5.0U	NE	250U	5.0U	NE	NA	5.0U	NE
Methyl tert-butyl ether (MTBE)	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
2-Butanone (MEK)	μg/L	42	4.4	NE	9	2.5	NE	100U	6.6	NE	NA	2.0	NE
Chloroform	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	26	2.0U	NE
Carbon Tetrachloride	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
1,2-Dichloroethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
1,2-Dichloropropane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Bromodichloromethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	3.7	NE	NA	2.0U	NE	NA	2.0U	NE	NA	2.0U	NE
cis-1,3-Dichloropropene	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
trans-1,3-Dichloropropene	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
1,1,2-Trichloroethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
2-Hexanone	μg/L	40U	1.3J	NE	2.0U	2.0U	NE	100U	1.1J	NE	NA	2.0U	NE
Dibromochloromethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Chlorobenzene	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Styrene	μg/L	40U	3.2	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Bromoform	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
1,1,2,2-Tetrachloroethane	μg/L	40U	2.0U	NE	2.0U	2.0U	NE	100U	2.0U	NE	NA	2.0U	NE
Naphthalene	μg/L	290	480E	Е	11	5.1	NE	360	190	NE	89	15	NE

Laboratory Qualifiers

U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

μg/L = micrograms per lites

NE = Not established

Location outside of treatment volume

April 2	004 Gı	roundwater S	Sampling E	vent Dates (Site	4 Operations	3)	
VOC	Const	ituent Per Tr	eatment A	rea Monitoring V	Vell Location		
Compound			MW-62S	(D)		MW-63S	
	Units	May/June	4/13/04	Remediation	May/June	4/14/04	Remediation
		Baseline	Results	Goal (μg/L)	Baseline	Results	Goal (μg/L)
Previously Identified Primary Conta					, ,		
Benzene	μg/L	59	3.5	50	180	26	50
Toluene	μg/L	85	17	NE	4,400	27	NE
Ethylbenzene	μg/L	110	12	NE	1,600	510E	NE
p/m-Xylene	μg/L	410	48	NE	8,700	1200E	NE
o-Xylene	μg/L	150	19	NE	4,200	350E	NE
Total-Xylene	μg/L	NA	NA	NE	NA	NA	NE
Other Volatile Organic Compounds							
Chloromethane	μg/L	NA	2.0U	NE	100U	2.0U	NE
Cis-1,2-Dichloroethene (cs-1,2-DC		NA	NA	NE	100U	NA	NE
Trans-1,2-Dichloroethene	μg/L	NA	NA	NE	100U	NA	NE
1,2-Dichloroethene (total)	μg/L	NA	2.0U	NE	100U	6.8	NE
1,1 Dichloroethane (1,1-DCA)	μg/L	NA	2.0U	NE	100U	2.0U	NE
1,1,1-Trichloroethane (1,1,1-TCA)	μg/L	NA NA	2.0U 2.0U	NE NE	100U 100U	2.0U	NE NE
Trichloroethene (TCE)	μg/L	NA NA		NE NE		1.2J	NE NE
Tetrachloroethene (PCE) Vinvl Chloride	μg/L μg/L	NA NA	2.0U 2.0U	NE NE	100U 100U	2.0U 2.0U	NE NE
Bromomethane	μg/L	NA NA	2.0U	NE NE	250U	2.0U	NE NE
Chloroethane		NA NA	2.0U	NE NE	100U	2.0U	NE NE
Acetone	μg/L μg/L	51	2.6J	NE NE	220J	2.00	NE NE
1.1-Dichloroethene	μg/L	NA NA	2.0U	NE	100U	2.0U	NE
Carbon Disulfide	μg/L	NA	2.0U	NE	100U	2.0U	NE
Methylene Chloride	μg/L	NA	5.0U	NE NE	250U	5.0U	NE
Methyl tert-butyl ether (MTBE)	μg/L	NA	2.0U	NE NE	100U	2.0U	NE
2-Butanone (MEK)	μg/L	NA	2.6	NE	75J	11	NE
Chloroform	μg/L	26	2.0U	NE NE	100U	2.0U	NE NE
Carbon Tetrachloride	μg/L	NA	2.0U	NE	100U	2.0U	NE
1.2-Dichloroethane	μg/L	NA	2.0U	NE	100U	2.0U	NE
1,2-Dichloropropane	μg/L	NA	2.0U	NE	100U	2.0U	NE
Bromodichloromethane	μg/L	NA	2.0U	NE	100U	2.0U	NE
Methyl isobutyl ketone (MIBK)	μg/L	NA	2.0U	NE	NA	2.8	NE
cis-1,3-Dichloropropene	μg/L	NA	2.0U	NE	100U	2.0U	NE
trans-1,3-Dichloropropene	μg/L	NA	2.0U	NE	100U	2.0U	NE
1,1,2-Trichloroethane	μg/L	NA	2.0U	NE	100U	2.0U	NE
2-Hexanone	μg/L	NA	2.0U	NE	100U	2.2	NE
Dibromochloromethane	μg/L	NA	2.0U	NE	100U	2.0U	NE
Chlorobenzene	μg/L	NA	2.0U	NE	100U	2.0U	NE
Styrene	μg/L	NA	2.0U	NE	100U	2.0U	NE
Bromoform	μg/L	NA	2.0U	NE	100U	2.0U	NE
1,1,2,2-Tetrachloroethane	μg/L	NA	2.0U	NE	100U	2.0U	NE
Naphthalene	μg/L	89	15	NE	410	680E	NE

Laboratory Qualifiers

U = Not Detected; Detection Limit Listed

J = Quantitation Approximate

ND = Not Detected; Detection Limit Unknown

NA = Not Available

E= Estimtated value, exceeds the upper limit of calibration

D= Duplicate

<u>Other</u>

Analytical Data Table developed from laboratory reports and samples collected by TTFW

TTFW = Tetra Tech Foster Wheeler VOC= volatile organic compound

μg/L = micrograms per lites

NE = Not established

Location outside of treatment volume

Page 3 of 3

Sites 4 and 3 Influent Vapor Analytical Results Bedford NWIRP Site Bedford, Massachusetts

Vapor Sample Resu	Its (Site 4	ERH Rem	nediation C	peration	ns)
Sample Collection		Primary	VOCs (pp	mv)	
Analysis Date			Ethyl	Xylene	
Allalysis Date	Benzene	Toluene	benzene	(total)	PCE
7/31/03	0.025U	0.025U	0.025U	0.2	4.6
8/7/03	0.017U	0.088	0.048	0.229	1.20
8/14/03	0.16U	1.2	0.89	4.07	15
8/22/03	0.8U	1.40	1.40	5.8	17.00
8/28/03	0.31U	0.21	1.2	5.6	16
9/6/03	0.08U	0.21	0.17	0.85	2.00
9/11/03	0.25U	0.47	0.44	2.13	4
9/11/2003, Duplicate	0	0.45	0.42	2.00	3.8

Date Collected	_	7/31/03			8/7/03			8/14/03			8/22/03			8/28/03			9/6/03			9/11/03		9/11/2	003, Dup	olicate
Analyte	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ymad	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.
1,1,1-Trichloroethane	1800	1.8	Quu.	340	0.34	Quai.	12000	12	Quui.	6100	6.1	Quui.	1100	1.1	Quui.	390	0.39	Quai.	250	0.25	Quui.	250	0.25	Quui.
1.1.2.2Tetrachloroethan€	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
1.1.2-Trichloroethane	25	0.025	Ü	17	0.017	Ü	160	0.16	Ü	800	0.8	Ü	310	0.31	Ü	80	0.08	Ü	79	0.079	Ü		0	Ü
1,1-Dichloroethane	2100	2.1		520	0.52	- u	480	0.48		830	0.83	Ŭ	1100	1.1	Ŭ	210	0.21	Ŭ	230	0.073	Ŭ	240	0.24	- ŭ
1.1-Dichloroethene	3000	3		1100	1.1		13000	13		22000	22		8600	8.6		1500	1.5		1600	1.6		1500	1.5	
1,2-Dichloroethane	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U	1500	0	U
1,2-Dichloropropane	25	0.025	Ü	17	0.017	Ü	160	0.16	Ü	800	0.8	Ü	310	0.31	Ü	80	0.08	Ü	79	0.079	Ü		0	Ü
2-Butanone	100	0.023	Ü	160	0.16	U	640	0.64	Ü	3200	3.2	Ü	1200	1.2	Ü	320	0.32	Ü	320	0.32	Ü		0	Ü
2-Hexanone	100	0.1	Ü	68	0.068	U	640	0.64	Ü	3200	3.2	Ü	1200	1.2	Ü	320	0.32	Ü	320	0.32	Ü		0	Ü
4-Methyl-2-pentanone	100	0.1	Ü	68	0.068	Ü	640	0.64	U	3200	3.2	U	1200	1.2	Ü	320	0.32	Ü	320	0.32	Ü		0	Ü
Acetone	100	0.1	Ü	810	0.81	0	1000	1	0	5500	5.5	U	2400	2.4	U	1400	1.4	U	1700	1.7	U	1800	1.8	
Benzene	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U	1000	0	U
Bromodichloromethane	25	0.025	U	17	0.017	U	160	0.16	IJ	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
Bromoform	100	0.023	U	68	0.017	U	640	0.64	U	3200	3.2	U	1200	1.2	U	320	0.32	Ü	320	0.073	U		0	U
Bromomethane	25	0.025	Ü	17	0.008	U	160	0.04	U	800	0.8	U	310	0.31	U	80	0.32	U	79	0.079	U		0	U
Carbon disulfide	100	0.025	U	170	0.017	U	640	0.16	IJ	3200	3.2	U	1200	1.2	U	330	0.08	0	320	0.079	U		0	U
Carbon disulide Carbon tetrachloride	25	0.025	U	170	0.17	U	160	0.64	U	800	0.8	U	310	0.31	U	80	0.33	U	79	0.32	U		0	U
Chlorobenzene	25	0.025	Ü	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
	140	0.025	U	17	0.017	U		0.16	IJ	800	0.8	U			U		0.08	U	79	0.079	U		0	U
Chloroethane	25		U				160						310 310	0.31		80 80		U	79		U		0	
Chloroform Chloromethane	25	0.025 0.025	U	17 17	0.017	U	160 160	0.16 0.16	U	800 800	0.8	U	310	0.31	U	160	0.08	U	79	0.079	U		0	U
	3300		U	2100		U	2000		U			U	10000		U						U	2700		U
Cis-1,2-Dichloroethen∈		3.3			2.1			2		7400	7.4			10		2600	2.6		3600	3.6		3700	3.7	⊢ ⊢
Cis-1,3-dichloropropene	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
Dibromochloromethane	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U	400	0	U
Ethylbenzene	25 50	0.025	U	48	0.048		890	0.89		1400	1.4		1200	1.2 0.31		170	0.17		440 79	0.44		420	0.42	⊢ ⊢
Methylene chloride		0.05		28			160	0.16	U	1100	1.1		310		U	80	0.08	U			U		0	U
Methyl-tert-butyl ethe	100	0.1	U	68	0.068	U	640	0.64	U	3200	3.2	U	1200	1.2	U	320	0.32	U	320	0.32	U		0	U
Naphthalene	100	0.1	U	68	0.068	U	640	0.64	U	3200	3.2	U	1200	1.2	U	320	0.32	U	320	0.32	U		0	U
Styrene	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
Tetrachloroethene	2800	2.8	ļ	1200	1.2		15000	15		17000	17		16000	16		2000	2		4200	4.2		3800	3.8	ldot
Toluene	25	0.025	U	88	0.088	L	1200	1.2		4000	4		1400	1.4		210	0.21		470	0.47		450	0.45	⊢ ⊢
Trans 1,2-dichloroethene	110	0.11	ļ	68	0.068	U	640	0.64	U	3200	3.2	U	1200	1.2	U	320	0.32	U	320	0.32	U		0	U
Trans-1,3-dichloropropen€	25	0.025	U	17	0.017	U	160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
Trichloroethene	4600	4.6		4100	4.1		59000	59		150000	150		100000	100		17000	17		26000	26		24000	24	
Vinyl chloride	180	0.18		34	0.034		160	0.16	U	800	0.8	U	310	0.31	U	80	0.08	U	79	0.079	U		0	U
p/m - Xylene	110	0.11		160	0.16		3200	3.2		4600	4.6		4400	4.4		620	0.62		1600	1.6		1500	1.5	
o-Xylene	40	0.04		69	0.069	0.229	870	0.87	4.07	1200	1.2	5.8	1200	1.2	5.6	230	0.23	0.85	530	0.53	2.13	500	0.5	2
		0			0			0			0			0			0			0			0	ш
TVO (Total VOCs)	18230	18.23	l	10927	10.927		108640	108.64		221130	221.13	<u> </u>	147400	147.4		26820	26.82		40620	40.62		38160	38.16	Щ
TICs		ļ																	L				<u> </u>	igspace
Benzene, 1-ethyl-2-methyl														ļ					430					igspace
Benzene, 1,3,5-trimethyl-										L				<u> </u>					430				<u> </u>	igsquare
Octane	3100		ļ							5500														$oxed{oxed}$
Octane, 2-methyl-	1400			270			L						3700	<u> </u>									<u> </u>	igsquare
Octane, 3-methyl-							1800			L				<u> </u>									<u> </u>	igsquare
Octane, 4-methyl-										10000														ldot
Cyclohexane, ethyl-	4300			930	<u> </u>		2200						1800	<u> </u>					560			470	<u> </u>	ш
Cyclohexane, 1,3-dimethyl-, cis	3700			830	l	l	2700												630			570	1	
	3,00		1	030	-		2100					-		1				-	030	-		3/0	\vdash	\vdash
Cyclohexane, 1,3-dimethyl-,		l	l		l							1		1						l			1	1 /
trans-	1600		ĺ											<u> </u>										

Sites 4 and 3 Influent Vapor Analytical Results Bedford NWIRP Site Bedford, Massachusetts

Date Collected		7/31/03			8/7/03			8/14/03			8/22/03			8/28/03			9/6/03			9/11/03		9/11/2	003, Dup	plicate
Analyte	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual.	ppbv	ppmv	Qual
Cyclohexane, 1,4-dimethyl-							2300																	
Cyclohexane, 1,4-dimethyl-, cis				330			1800																	
Decane, 5,6-dimethyl-				370																				
Decane, 2,6,6-trimethyl-				570																				
Hexane, 2,3,5-trimethyl-	1600																							
Hexane, 1-(hexyloxy)-2-methyl																						480		
Heptane, 2-methyl-				400			2400						2100						560			530		
Heptane, 3-methyl-	1500			400			1700												410					
Heptane, 2,4-dimethyl-																						850		
Heptane, 2,5-dimethyl-							1600																	
Heptane, 2,6-dimethyl-	2800			640			4200																	
Heptane, 3-ethyl-2-methyl-	2400																							
Pentane, 2-methyl-										9600														
2-Propanol										13000														
Nonane	2800			690			2200						3000						400					
Undecane										4500														
Undecane, 5,7-dimethyl-										17000														
Undecane, 2,7-dimethyl-										25000														
Nonadecane, 4-methyl-										6800														
Dodecane										7300														
Hydroxylamine, O-decyl-																			910					
Nonahexacontanoic acic																			720					
Unknown										4900			8100			730			670			1240		
Methane	0.67%			0.014%			0.012%	1		NA			NA			NA		l	NA			NA		1

Notes
U = Non-detect
J = Analyte was detected below its reporting limit. The result was estimated.
NA = Not analyzed
TIC = Tentatively identified compound

TTFW collected samples and obtained analytical results

APPENDIX A

Laboratory Reports

Site 4 ERH Remediation

Raw Analytical Data and Field Documentation have been removed from this appendix and will be submitted in a separate volume at a later date.

APPENDIX B

Memorandums, Field Logs and Construction Reports Site 4 ERH Remediation

APPENDIX B

Memorandums

Thermal Remediation Services, Inc.

Site 4 ERH Remediation



June 19, 2003

Joe Francis
Foster Wheeler Environmental Corporation
133 Federal St., 6th Floor
Boston, MA 02110

Subject: Contaminated Region at Site 4 of the Bedford NWIRP

Dear Mr. Francis:

As you are aware, the newly installed monitoring wells at Site 4 were recently sampled. This sampling provided somewhat surprising results in that the region of contamination is larger and appears to be shifted further south than originally believed when the electrical resistance heating (ERH) remediation system was designed.

The most contaminated well was MW-65s, which contained 320 μ g/ ℓ of benzene. This is especially troubling because MW-65s is at the upgradient edge of the new MWs and is located about 30 feet downgradient of the former underground storage tank location. MW-65s might indicate that even greater levels of contamination would be found a little further south.

TRS believes that ERH is a powerful site remediation tool. However, ERH will only remediate the region in which it is applied. None of us (Foster-Wheeler, the US Navy, or TRS) would be well served by a very thorough remediation of only a portion of the remaining contaminated zone, especially if residual upgradient benzene were to re-contaminate the treated region. For this reason, TRS strongly urges Foster-Wheeler and the US Navy to make all practical efforts to determine the extent of the contaminated region prior to finalizing the ERH electrode locations and number.

TRS is eager to work with you in order to shift some contracted work into the next fiscal year. However, please note that a delay in start-up of the Site 4 ERH remediation or start-up of the Site 3 pilot test would lead to additional remediation equipment stand-by costs.

Please feel free to contact me at (770) 794-1168 should you have any questions about this letter. Please contact Greg Sandberg at (206) 524-6276 or Tom Powell at (360) 263-3615 if you have questions regarding work that can be deferred or any other measures we can take to provide the best overall remedial approach and cost structure for the site.

Sincerely,

Greg Beyke
VP - Engineering
Thermal Remediation Services



April 29, 2004

Mr. Joe Francis Project Manager Tetra Tech FW, Inc. 133 Federal St., 6th Floor Boston, MA 02110

Subject: Evaluation of Post ERH Groundwater Results at Site 4 of the Bedford NWIRP

Dear Mr. Francis:

Thank you for forwarding the April 2004 post cool-down analytical data for the Site 4 groundwater monitoring wells at the Bedford NWIRP. TRS has reviewed the data and would like to convey our assessment of these results.

The data provided indicates that all groundwater monitoring wells located downgradient of the ERH treatment region show a significant decrease in concentration between the end of operations at Site 4 and the April sampling event. These wells include MW-60S, MW-61S, and MW-64S. Additionally, wells MW-62S and MW-42SR, located slightly cross-gradient, show a significant decrease in concentration. The three wells located inside the treatment region, MW-18SR, MW-63S, and MW-65S, all have higher Benzene concentrations than were indicated immediately following ERH application. However, each of these eight monitoring wells remains below the Benzene cleanup concentration objective of 50 μ g/ ℓ .

The April sample results from monitoring well MW-66S, located up-gradient and outside of the treatment region, indicates higher Benzene concentrations than prior to ERH operations. In fact, this well has the highest Benzene concentration of any well at the Site, 91 μ g/ ℓ .

TRS believes that groundwater between the Site 4 treatment region and the former UST, located south and up gradient of the treatment region, contains significant Benzene concentrations, as we described in our letter to TfFW dated 19 June, 2003. As this up-gradient groundwater moves into the Site 4 treatment region, it is the likely source of any increase in Benzene concentrations within that region during this post ERH treatment period.

We conclude that the reduced Benzene concentrations indicated in the wells down-gradient of the Site 4 treatment region are attributable to treated groundwater flowing out of the ERH treatment volume in a north/northwesterly direction.

We are interested in hearing whether TfFW shares our view of the results of the post cool-down groundwater analytical data at Site 4. Please feel free to contact me at (817) 741-4361 with any questions or comments you have regarding this evaluation, particularly if you are not in agreement.

Sincerely,

Thermal Remediation Services, Inc.

Jerry L. Wolf VP - Operations

APPENDIX B

TtFW Field Logs and Construction Reports

Site 4 ERH Remediation

Raw Analytical Data and Field Documentation have been removed from this appendix and will be submitted in a separate volume at a later date.

APPENDIX C

Complete Temperature Interval Data Tables

Site 4 ERH Remediation

Site 4 ERH Remediation Subsurface Temperature Data Temperature Monitoring Point (TMP) Locations 1 through 3

	Area 4		,	Area 4	Cell A	verag	е					TMP-1							TMP-2							TMP-	3		
Date	Average	-5	-10	-15	-20	-25	-30	AVG.	5	10	15	20	25	30	AVG.	5'	10'	15'	20'	25'	30'	AVG.	5'	10'	15'	20'	25'	30'	AVG.
7/31/03	14	21	15	14	13	12	12	14	22	16	14	12	11	12	13	19	14	15	14	14	13	14	21	16	13	12	11	11	13
8/1/03 7:15	14	22	16	14	13	13	12	14	24	17	14	13	12	12	14	20	15	15	15	14	14	15	22	16	14	12	12	11	14
8/2/03 20:22	16	24	17	16	17	16	14	16	25	18	16	17	16	15	17	22	16	17	18	19	16	18	24	16	14	15	14	12	15
8/3/03 7:51	17	24	17	17	18	18	15	17	26	18	17	18	17	16	18	23	16	18	20	21	17	19	24	17	15	16	16	13	16
8/3/03 18:51	19	25	18	18	20	20	16	19	26	18	19	20	18	17	19	24	17	19	24	25	18	21	24	18	16	17	18	14	17
8/4/03 7:37	20	25	18	19	21	22	17	20	26	19	20	22	21	18	21	24	17	20	24	27	19	22	25	17	16	18	17	14	17
8/4/03 11:45	20	26	18	19	22	22	18	20	27	20	20	22	22	19	21	25	17	20	25	27	19	22	25	17	16	18	18	15	17
8/5/03 7:47	22	26	19	20	24	25	19	22	28	21	22	26	23	20	23	26	18	22	28	32	22	25	24	17	17	19	21	16	19
8/5/03 22:36	24	27	20	22	27	29	22	24	29	22	23	28	29	23	26	27	19	24	31	36	24	28	26	18	18	21	23	18	20
8/6/03 7:37	25	28	20	22	27	31	22	25	29	22	24	29	30	24	26	27	19	25	32	38	25	29	27	18	18	21	24	18	20
8/6/03 14:36	26	28	20	23	28	31	23	26	29	23	25	30	31	25	27	28	19	26	34	39	26	30	27	18	18	21	24	18	20
8/6/03 21:11	26	28	20	24	29	32	24	26	29	23	25	31	32	26	28	28	20	27	34	40	26	30	27	18	19	22	25	19	21
8/7/03 7:26	27	29	21	24	30	33	24	27	30	24	26	32	33	26	29	29	20	28	36	41	27	31	27	19	19	23	26	20	22
8/8/03 17:05	30	30	22	26	33	37	28	30	31	26	28	35	36	30	31	31	22	31	40	46	31	35	27	19	20	25	29	22	23
8/9/03 10:21	31	30	23	27	35	39	29	31	31	26	29	37	38	31	33	31	23	32	42	48	32	36	27	20	21	27	30	23	24
8/9/03 15:22	32	30	23	28	36	40	29	32	31	27	30	38	39	31	34	32	23	33	43	49	33	37	28	20	21	27	31	23	25
8/9/03 17:52	32	30	24	28	36	40	29	32	31	27	30	38	39	32	34	32	24	33	43	49	33	37	27	20	21	27	31	23	25
8/10/03 11:04	33	31	24	29	38	42	31	33	32	27	31	40	41	33	35	33	24	35	45	51	35	39	28	20	22	28	32	24	26
8/11/03	35	31	25	31	40	45	32	35	32	28	34	42	44	35	37	33	25	37	48	55	37	41	29	21	23	30	35	26	27
8/12/03 10:41	37	32	25	33	43	47	34	37	32	29	36	45	47	37	39	34	26	39	51	58	39	44	29	20	24	32	37	27	28
8/13/03 21:44	38	32	27	34	44	48	36	38	33	30	36	46	48	39	40	34	28	40	53	59	41	45	28	22	25	32	38	29	29
8/14/03 8:53	39	32	27	35	45	50	37	39	33	30	37	47	50	39	41	35	28	43	54	61	42	47	29	23	26	34	39	29	31
8/15/03 9:00	40	32	27	35	46	51	38	40	33	30	37	47	50	40	41	35	29	41	55	62	43	47	29	23	27	35	40	30	31
8/15/03 16:00	41	33	28	37	47	51	38	41	33	31	38	49	51	41	42	36	31	45	56	63	44	49	29	23	27	35	40	30	31
8/15/03 19:19	41	33	28	37	47	52	39	41	33	31	38	49	52	41	43	37	31	45	56	63	44	49	29	23	27	35	41	31	32
8/16/03 9:45	42	33	29	38	49	54	39	42	33	31	40	51	54	42	44	37	31	46	58	66	45	50	30	24	28	37	42	31	33
8/16/03 17:53	43	33	29	39	49	55	40	43	33	31	41	51	55	43	45	37	32	47	59	67	46	51	30	24	28	37	43	32	33
8/17/03 1:33	44	34	29	39	50	56	41	44	34	32	41	53	56	44	46	37	32	48	60	68	47	52	31	24	29	38	44	32	34
8/18/03 12:55	45	34	30	41	52	57	42	45	34	32	43	54	57	45	47	37	32	49	62	70	49	53	31	25	30	40	45	33	35
8/18/03	45	34	30	41	52	57	43	45	34	33	43	54	57	45	47	38	33	50	63	70	49	54	30	25	30	40	45	34	35
8/18/03 19:09	45	34	31	41	52	58	43	45	35	33	43	54	58	46	47	38	34	50	63	70	49	54	30	25	30	39	45	34	35
8/19/03 0:16	46	34	31	42	52	58	43	46	35	33	44	54	58	46	47	38	34	51	63	71	49	55	30	25	30	40	45	34	35
8/19/03 8:45	46	35	31	42	53	59	43	46	35	33	44	55	59	46	48	38	34	51	64	72	50	55	31	25	30	40	46	34	35
8/19/03 10:19	46	35	31	42	53	59	43	46	35	34	44	55	59	46	48	38	34	52	65	72	50	56	31	25	30	40	46	34	35
8/19/03 18:55	46	35	31	41	53	59	44	46	35	34	44	55	59	47	48	39	35	50	64	72	50	55	30	25	30	40	46	35	35
8/19/03 22:03	46	35	31	42	54	59	44	46	35	34	44	55	59	47	48	39	35	50	65	72	50	56	31	25	31	41	46	35	36
8/20/03 11:02	47	35	32	42	54	60	44	47	35	34	45	56	60	47	49	39	35	51	66	73	51	56	31	26	31	41	47	35	36
8/20/03 14:51	47	35	32	43	54	60	45	47	35	34	45	56	60	48	49	39	35	52	66	73	52	57	31	26	31	41	47	35	36
8/20/03 17:27	48	35	32	43	55	60	45	48	35	35	46	57	60	48	50	39	36	53	66	74	52	57	31	26	31	42	47	36	37
8/21/03 10:14	49	35	33	44	56	61	46	49	35	35	47	58	61	48	50	39	36	53	68	75	53	58	31	27	32	42	48	36	37
8/21/03 18:43	48	35	33	44	55	61	46	48	35	35	46	57	61	49	50	39	37	53	67	75	53	58	30	26	32	42	48	36	37
8/22/03 0:01	49	35	33	44	56	62	46	49	35	35	47	58	62	49	51	39	37	54	68	75	53	59	31	27	32	43	49	37	38
8/22/03 10:20	50	35	33	46	57	63	47	50	35	35	48	59	63	49	51	39	37	56	69	77	54	60	32	27	33	44	49	37	38
8/22/03 13:52	50	35	33	46	58	64	47	50	35	36	48	60	64	50	52	39	37	57	70	78	54	61	31	27	33	44	50	37	39
8/22/03 17:31	50	35	33	46	58	64	48	50	35	36	48	60	64	50	52	40	37	57	70	78	55	61	31	27	33	44	50	38	39
8/23/03 1:12	51	36	34	46	60	65	48	51	35	36	49	61	66	51	53	40	38	56	71	79	55	61	32	27	34	47	51	38	40
8/23/03 9:07	52	36	33	46	60	67	48	52	36	36	50	62	67	51	54	39	37	55	73	81	56	62	32	27	34	46	52	38	40
8/23/03 13:04	52	36	34	46	61	67	49	52	36	36	50	63	67	52	54	40	38	55	74	82	57	62	33	28	34	46	52	39	40

Site 4 ERH Remediation Subsurface Temperature Data Temperature Monitoring Point (TMP) Locations 1 through 3

	Area 4		-	Area 4	Cell A	verag	e					TMP-1							TMP-2							TMP-3	3		
Date	Average	-5	-10	-15	-20	-25		AVG.	5	10	15	20	25	30	AVG.	5'	10'	15'	20'	25'	30'	AVG.	5'	10'	15'	20'	25'	30'	AVG.
8/23/03 17:11	53	36	34	47	61	68	50	53	36	37	51	63	68	53	55	40	38	55	74	83	57	63	32	27	34	47	53	39	40
8/24/03 1:22	53	37	35	47	63	69	50	53	36	37	52	65	69	53	56	41	39	55	76	84	58	64	33	28	34	48	54	40	41
8/24/03 9:48	55	37	34	48	65	71	51	55	36	37	53	67	71	54	57	40	38	56	78	87	59	65	34	28	35	49	55	41	42
8/24/03 18:15	55	37	35	48	66	73	53	55	37	37	54	68	73	56	58	41	39	56	80	88	60	66	34	28	35	50	57	42	43
8/24/03 23:08	57	38	35	49	68	74	53	57	37	38	55	70	75	57	60	42	40	58	82	90	61	68	34	28	35	51	58	42	43
8/25/03 12:32	59	38	36	50	71	77	55	59	37	38	55	73	78	59	61	42	40	60	88	94	64	71	35	29	36	53	60	43	45
8/25/03 15:26	59	38	36	50	71	78	55	59	37	38	54	73	78	59	61	42	40	60	88	95	64	71	35	29	36	53	60	43	45
8/25/03 18:54	59	38	36	51	72	78	56	59	37	38	56	74	79	60	62	43	41	60	88	95	64	71	35	29	36	54	60	44	45
8/25/03 20:55	60	38	36	51	73	79	56	60	37	39	58	75	80	60	63	43	41	60	89	96	65	72	35	29	36	54	61	44	45
8/26/03 3:07	60	39	36	51	74	80	57	60	37	38	57	76	81	61	63	43	41	61	91	97	66	73	36	29	36	55	62	45	46
8/26/03 11:55	61	39	37	53	75	81	58	61	37	39	60	77	82	62	65	43	41	62	92	98	67	73	36	30	37	55	62	45	46
8/26/03 12:53	61	39	36	53	75	81	58	61	37	39	61	77	82	62	65	43	41	62	93	98	67	74	36	29	37	55	62	45	46
8/26/03 22:39	62	39	37	54	76	82	59	62	37	39	62	78	83	63	66	44	42	63	93	99	67	74	35	30	37	56	63	46	47
8/27/03 10:01	64	39	38	55	80	84	61	64	37	40	58	81	86	65	66	44	43	69	100	102	70	79	36	30	38	58	65	47	48
8/27/03 14:54	65	39	38	56	81	85	61	65	37	40	58	82	87	66	67	44	43	73	101	103	70	80	36	30	38	59	66	47	48
8/27/03 17:56	66	39	38	58	82	86	62	66	37	40	58	83	88	67	67	45	44	79	102	104	71	82	36	30	38	60	67	48	49
8/27/03 20:06	67	40	38	60	81	87	62	67	37	40	58	83	89	67	68	45	44	84	101	104	71	83	37	30	38	60	67	48	49
8/28/03 7:08	70	40	40	65	84	90	64	70	37	41	59	87	92	69	70	45	48	97	102	107	73	89	38	31	39	63	70	50	51
8/28/03 11:24	69	40	40	64	84	89	64	69	37	41	59	87	92	69	70	45	48	94	101	106	73	87	38	31	39	63	70	50	51
8/28/03 19:36	71	40	41	66	85	90	65	71	37	41	60	89	94	71	71	46	52	99	101	106	74	90	38	31	40	65	71	51	52
8/29/03 2:12	72	40	45	67	86	91	66	72	37	41	61	91	95	72	72	46	63	100	101	107	75	93	38	31	40	66	72	51	52
8/29/03 14:03	74	41	47	68	88	92	67	74	37	42	63	93	97	74	74	47	68	101	101	106	76	94	38	32	41	69	74	52	54
8/29/03 16:04	74	41	47	68	88	92	67	74	37	42	63	93	97	74	74	47	68	101	101	106	76	94	38	32	41	69	74	52	54
8/29/03 19:38	74	41	48	69	88	93	68	74	37	42	64	94	98	74	75	47	70	101	101	106	77	95	38	32	41	70	74	53	54
8/29/03 22:49	75	41	49	69	90	93	68	75	37	42	64	95	99	75	75	47	72	102	102	106	77	96	39	32	41	72	75	53	55
8/30/03 2:35	76	41	49	69	92	94	69	76	37	42	65	97	100	76	76	47	74	102	102	107	78	96	39	32	41	76	76	54	56
8/30/03 12:17	76	41	49	70	92	93	69	76	37	43	66	99	100	76	77	47	72	101	101	103	78	94	39	33	42	75	76	54	57
8/30/03 20:37	77	41	50	70	93	94	71	77	37	43	68	100	102	78	78	48	74	101	101	103	79	95	39	33	42	77	78	55	58
8/31/03 2:53	78	41	51	73	94	95	71	78	37	43	75	100	103	79	80	48	76	102	102	103	80	96	39	33	43	80	79	55	59
8/31/03 19:55 9/1/03 15:22	78 79	41	51 51	75 78	93 94	95 95	72 73	78 79	37 36	44	80 89	100 99	103	80 82	82 84	48 48	75 76	101	101	102	80 81	95 95	39 39	33 34	43	79 81	80	56 57	59 60
9/1/03 15.22	80	41	52	79	94	95	74	80	36	45	92	100	103	83	85	49	77	101	101	101	81	95	39	34	45	81	81	58	60
9/2/03 1:31	80	41	52	79	94	96	74	80	36	45	91	100	103	83	85	49	77	102	101	102	82	96	39	34	45	81	81	58	60
9/2/03 1:51	80	42	52	79	94	95	75	80	36	45	91	99	103	84	85	49	77	102	101	102	82	95	40	34	45	82	81	58	61
9/3/03 8:00	78	40	50	74	93	95	74	78	35	45	77	99	103	83	81	48	70	99	100	102	82	93	38	35	46	80	80	58	60
9/3/03 18:39	76	40	48	72	92	94	74	76	36	45	76	99	102	83	81	48	63	94	99	102	81	90	37	35	46	77	79	58	59
9/3/03 21:39	76	40	47	71	92	94	75	76	36	45	75	99	102	84	80	48	62	93	100	102	82	89	37	35	46	78	79	58	60
9/4/03 8:05	78	40	48	75	93	96	75	78	35	45	78	100	104	84	82	47	64	99	101	104	82	92	38	35	47	77	80	59	60
9/4/03 14:29	80	40	51	77	93	97	76	80	35	46	83	100	105	85	84	47	71	100	101	105	83	94	38	36	48	78	81	60	61
9/4/03 23:22	79	40	51	76	93	96	76	79	35	45	81	101	104	85	83	47	73	99	100	105	83	94	38	36	48	78	80	59	61
9/5/03 4:54	80	40	52	77	93	97	76	80	35	46	83	101	105	86	84	47	74	100	101	105	83	95	38	36	48	78	81	60	61
9/5/03 17:08	79	40	52	75	93	96	76	79	35	46	78	100	104	85	82	47	74	100	100	104	83	95	37	36	48	78	80	60	61
9/6/03 10:59	84	40	55	84	96	99	77	84	35	46	96	104	107	87	88	47	83	102	104	109	85	100	38	37	54	79	82	60	63
9/6/03 23:38	85	40	55	87	97	100	78	85	35	47	98	104	108	88	89	48	82	103	103	109	86	99	38	37	60	83	83	61	66
9/7/03 12:19	85	41	56	88	96	100	79	85	35	48	98	103	108	89	89	48	81	103	103	108	86	99	39	38	62	82	83	61	66
9/7/03 18:48	85	40	56	89	96	100	79	85	35	48	98	103	108	89	89	48	82	103	103	108	86	99	38	38	66	81	84	62	67
9/8/03 6:07	84	40	56	85	95	99	79	84	35	49	91	102	107	89	87	48	81	101	102	107	87	98	38	39	62	81	83	62	66
9/8/03 14:44	85	40	57	86	96	100	80	85	35	49	91	102	107	90	87	48	81	101	104	108	87	99	38	40	66	81	84	62	68

Site 4 ERH Remediation Subsurface Temperature Data Temperature Monitoring Point (TMP) Locations 1 through 3

Date	Area 4			Area 4	Cell A	verag	е					TMP-1							TMP-2	2						TMP-3	3		
Date	Average	-5	-10	-15	-20	-25	-30	AVG.	5	10	15	20	25	30	AVG.	5'	10'	15'	20'	25'	30'	AVG.	5'	10'	15'	20'	25'	30'	AVG.
9/9/03 1:23	85	41	58	87	97	100	80	85	35	49	93	102	107	91	88	49	84	102	104	109	88	100	39	40	67	84	84	62	69
9/9/03 6:35	85	41	58	87	97	100	80	85	35	49	94	102	107	91	88	49	84	102	103	108	88	99	39	41	66	85	84	62	69
9/9/03 16:21	84	41	59	84	95	98	80	84	35	50	87	101	105	91	86	49	87	102	102	105	88	99	39	41	64	83	84	62	68
9/10/03 4:38	85	42	60	86	96	98	81	85	35	50	90	102	106	92	87	50	87	103	103	105	88	100	40	42	64	84	84	62	69
9/11/03 9:23	83	42	60	83	95	96	80	83	35	51	83	100	104	91	85	50	83	101	101	102	87	97	40	45	65	83	83	62	69
9/12/03 12:23	85	42	61	86	96	99	81	85	35	51	88	102	106	92	87	51	86	102	103	108	88	100	40	46	67	83	83	63	70
9/13/03 2:15	86	43	62	88	96	99	82	86	35	52	91	102	106	93	88	52	87	102	102	107	89	100	41	47	72	85	84	64	72
9/14/03 14:17	87	44	64	92	96	97	82	87	36	56	97	99	104	95	89	53	87	102	102	103	88	99	43	50	78	86	83	63	74
9/14/03 23:57	88	45	66	94	95	96	82	88	36	61	99	99	103	95	91	54	87	102	101	103	88	98	44	51	82	86	83	63	76
9/15/03 7:57	89	45	68	96	95	96	82	89	36	65	99	99	103	95	92	54	87	102	101	103	87	98	44	52	87	86	82	63	77
9/16/03 7:33	90	45	72	99	95	94	81	90	36	72	99	99	99	93	92	55	89	102	100	101	86	98	44	56	97	86	82	63	80
9/17/03 8:31	85	45	73	98	95	94	81	85	36	74	99	99	99	95	93	55	85	101	101	101	86	89	45	59	94	86	81	62	73
9/18/03 7:16	88	45	71	94	94	93	80	88	36	73	99	99	98	94	92	56	81	100	100	100	85	95	44	60	83	84	80	62	77
9/19/03 7:32	86	45	68	91	94	93	79	86	36	65	94	98	99	92	89	55	79	99	100	100	84	95	44	61	79	83	79	62	76
9/20/03 12:13	93	46	76	100	97	98	81	93	36	71	99	100	106	94	94	55	91	101	101	108	87	100	46	67	99	91	81	62	85
9/21/03 23:30	90	47	74	95	95	95	81	90	37	68	97	99	102	94	92	57	89	101	100	101	87	98	46	65	87	87	81	63	80
9/22/03 11:16	92	47	75	99	98	97	82	92	38	67	98	101	105	94	93	57	91	102	102	104	88	100	47	66	98	91	81	63	84

APPENDIX B

Photographic Documentation

PHOTOGRAPHIC RECORD



Direction of View:
Northeast
Date:

5/1/02

Description:
Site 4 ERH Pilot Test
Area. Treatment area is
outlined in white.
Electrode locations are
marked in orange, and
monitoring wells in white.



Direction of View: West

Date:

__5/1/02_

Description:

Site 4 ERH Pilot Test
Area. Treatment area is
outlined in white.
Electrode locations are
marked in orange, and
monitoring wells in white.

PHOTOGRAPHIC RECORD



Direction of View:
North
Date:
7/14/03

Description:
Drill rig and related
Equipment set up on
electrode 1, while
advancing 10" casing.



Direction of View:
North
Date:

5/15/03

Description:
Advancing of 6" steel
casing at MW-61S

PHOTOGRAPHIC RECORD



Direction of View: Not Applicable _ Date:

6/14/03_

Description: Bottom of typical electrode, ready to be installed in boring.



Direction of View:

North_ Date:

7/14/03_

Description:
Installation of uppermost section of electrode 2 into boring.

PHOTOGRAPHIC RECORD



Direction of View:
North

_1101

Date:

7/14/03

Description:

Adding graphite sand for annular space of electrode conductive interval of electrode 2.



Direction of View:
Not applicable

Date:

__6/3/03_

Description:

Closeup of graphite sand used for filling annular space of electrodes.

PHOTOGRAPHIC RECORD



Direction of View:
Not applicable
Date:

___6/3/03_

Description:

Closeup of steel shot used for filling annular space of electrodes.



Direction of View:
Not applicable
Date:

6/3/03

Description:

Closeup of screened interval material used for electrode construction.

PHOTOGRAPHIC RECORD



Direction of View:
Not applicable
Date:

___6/14/03

Description:
Newly installed electrode,
without CPVC protective
casing yet placed over it.



Direction of View:
Not applicable
Date:

_7/14/03

Description:
Top of typical electrode,
with threaded opening for
VR pipe connection and
opening for bolt
connection of electrode
cable.

PHOTOGRAPHIC RECORD



Direction of View:
Not applicable
Date:

7/18/03_

Description:
Completed electrode, with cable, VR pipe, and water drip tubing shown.



Direction of View:

North__

Date:

7/24/03

Description:

Site 4 ERH treatment area.
TMP within monitoring
well casing seen in
foreground. Electrode
oversleeves are placed on
electrodes.

PHOTOGRAPHIC RECORD



Direction of View:
Southeast

Date:

Unknown

Description:

Aerial view of Site 4 ERH treatment region, consisting of eight

electrodes._



Direction of View:

North__

Date:

Unknown

Description:

ERH treatment region.
In foreground is cooling
tower (left) and condenser
unit (right). VR piping
runs from condenser unit
towards Site 3.

PHOTOGRAPHIC RECORD



Direction of View:

West____

Date:

___7/10/03_

Description:

Vapor-phase GAC vessels with hose connections.



Direction of View:

North__

Date:

Unknown

Description:

Cooling tower (left) and___

condenser unit (right).

PHOTOGRAPHIC RECORD



Direction of View:

South _

Date:

5/1/03

Description:

Power control unit, after delivery to site. Location is adjacent to Components Building.



Direction of View:

North

Date:

5/30/03

Description:

Groundwater sampling setup for Site 4 pre-treatment groundwater sampling.

PHOTOGRAPHIC RECORD



Direction of View:
West

Date: _9/10/03__

Description:

Groundwater sampling
equipment setup for hot
groundwater sampling
during ERH treatment.
Well being purged is MW56I. (An identical setup
was utilized for Site 4 hot
groundwater sampling.



Direction of View:
Not applicable
Date:
9/10/03

Description:

Groundwater sampling
equipment setup for hot
groundwater sampling
during ERH treatment.
Well being purged is MW56I. Note ice bath for
cooling sample during
purging.

APPENDIX C

Monitoring Well Soil Boring Logs and Construction Details

BORING NUMBER: MW-60S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

LOCATION: North end of treatment area

DATE STARTED: 5/14/03

DATE COMPLETED: 5/14/03

GROUDWATER DEPTH: 20.30' TIC on 5/29/03

GROUND ELEVATION:

X COORDINATE:

Y COORDINATE:

DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-9', lexan liner samples

DATUM:

at 10-30'

DRILLER: Bowser-Morner, Inc.

GEOLOGIST: Matthew Greenberg

		1			at 10-30 .		,		
Sample		BLOWS	1	I	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)					(ppm)	
	1-9		65		0-12" Asphalt.	1442	5/14/03	1.5	
					12-24" Tan silty SAND; some ang f-c gravel; trace clay; moist;				
					dense.				
					24-27" Dk gray SILT; little ang f-c gravel; moist; dense.				
					27-37" Olive gravelly (ang, f-c) SILT; moist; dense.				
					37-44" Dk gray fm SAND; moist; semi-loose.				
					44-54" M brown silty f-m SAND; trace subrounded mc gravel;				
					moist; semi-loose.				
					54-65" Rock fragment.				
	9-10		N/A		Core through rock/boulder from 9-10 feet.	1505	5/14/03	N/A	
	10-15		18		0-15" Orange-brown m-c SAND; little subang f-c gravel; semi-	1525	5/14/03	NAB	
					dense; wet.				
	15-20		41		0-8" Orange-brown m-c SAND; little subang f-c gravel; semi-	1600	5/14/03	See	Highest FID reading=
		<u></u>			dense; wet.			right.	7.1 ppm at 3.0 ft.
	20-25		31		0-17" Lt brown silty f-c SAND; some rounded f-c gravel; wet;	1620	5/14/03	See	Highest FID reading=
					dense.			right.	1000 ppm at 2.0 ft.
					17-31" Gray gravelly SILT; trace to some sand; dry; v dense.				
MW-60S-	25-30		60		Gray gravelly SILT; trace to some sand; dry; v dense.	1645	5/14/03	See	Sample collected at
SBC-								right.	25.5 ft bgs.
051403									Highest FID reading=
									3466 ppm at 0.5 ft.
		-			End of boring at 30 feet.				
]									
					`		<u> </u>		
NOTES:	N/A = N	ot applica	ble.		bas = below ground surface.		<u></u>		

NOTES: N/A = Not applicable.

bgs = below ground surface.

NAB = Not above background.

TIC = top of inner casing.

ft = feet.

1 OF PAGE

BORING NUMBER: MW-61S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

LOCATION: Northwest corner of treatment area

DATE STARTED: 5/15/03

DATE COMPLETED: 5/15/03

GROUDWATER DEPTH: 17.59' TIC on 5/29/03

GROUND ELEVATION:

X COORDINATE:

Y COORDINATE:

DRILLER: Bowser-Morner, Inc. DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-9', lexan liner samples

DATUM:

at 10-30'.

GEOLOGIST: Matthew Greenberg

Sample	Depth	BLOWS	Recov-	Luscs	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)		Description	111110	Date	(ppm)	Comments
	0-10"	P	N/A		Asphalt.	1043	5/15/03	N/A	
	10"-10'		57		0-26" Lt brown silty f-m SAND; trace subang-ang f-c gravel; moist.	1100	5/15/03	0.0	
					26-57" Brown f-m SAND; trace ang m gravel; moist.	'''	0. 10.00	0.0	
	10-15		60		0-12" Lt brown silty f-m SAND; trace subang-and f-c gravel; moist.	1115	5/15/03	See	Highest FID reading=
					12-60" Lt brown silty f SAND; little m-c sand; trace subrounded f-c				0.1 ppm at 1.5 ft.
					gravel; moist; v dense.				, ,
MW-61S-	15-20		60		0-36" Lt brown silty f SAND; little m-c sand; trace subrounded f-c	1125	5/15/03	See	Highest FID reading=
SBA-					gravel; moist; v dense becomes satd at 18.5 ft.			right.	2900 ppm at 5.0 ft.
051503	20-25		60		0-12" Orange f-c SAND; trace silt and rounded f-c gravel; wet to	1205	5/15/03	i i	Sample collected at
			`		satd; v dense.				20 ft bgs.
			1		12-60" Gray SILT; little clay and subrounded to rounded f-c gravel;			See	Highest FID reading=
					moist to wet; v dense.			right.	2300 ppm at 0.5 ft.
	25-30		58		Gray SILT; trace sand; little subrounded to rounded f-c gravel and	1215	5/15/03	See	Highest FID reading=
		· · · · · ·			clay; moist to wet; v dense.			right.	2.2 ppm at 0.5 ft.
					End of boring at 30 feet.				
									•
								٠	
									·
							İ		
NOTES					has - below around out of		•		i

NOTES: N/A = Not applicable.

bgs = below ground surface.

NAB = Not above background.

TIC = top of inner casing.

ft = feet.

1 OF PAGE

BORING NUMBER: MW-62S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

LOCATION: Northeast corner of treatment area

DATE STARTED: 5/15/03

DATE COMPLETED: 5/15/03

GROUDWATER DEPTH: 17.79' TIC on 5/29/03

GROUND ELEVATION:

X COORDINATE:

Y COORDINATE:

DRILLER: Bowser-Morner, Inc. DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-10', lexan liner samples DATUM:

at 10-301

GEOLOGIST: Matthew Greenberg

Sample	Depth	BLOWS	Recov-	USCS	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)					(ppm)	
	0-0.5		N/A		Asphalt.	1523	5/15/03		
	0.5-5		50		0-35" Lt brown f-m SAND; trace subrounded f-m gravel; moist;	1550	5/15/03	0.0	
					dense.				
				,	35-50" Dk gray f SAND; trace silt; moist; semi-loose.				
	5-10		28		0-12" Dk gray f SAND; trace silt; moist; semi-loose.	1610	5/15/03	0.0	
		•			12-21" COBBLE.				
					21-28" Lt brown f-m SAND; moist; loose.				
	10-15		28		0-20" Dk gray silty m-c subang GRAVEL; dry; loose.	1610	5/15/03	0.0	
					20-28" Orange-brown silty f-m SAND; little subang f-m gravel;				
					moist; v dense.				
	15-20		31		0-18" Lt gray-brown silty f-c SAND; little subang f-c gravel; dry;	1620	5/15/03	See	Highest FID reading:
					dense.			right.	234.8 ppm at 1.5 ft.
					18-31" Gray SILT; some f sand; little clay; wet; v dense.				
MW-62S-	20-25		53		0-20" Brown f-m SAND; little subang f-c gravel; dry to wet;	1630	5/15/03	See	Sample collected at
SBA-					v dense.			right.	17.5 ft bgs.
051503					20-27" Orange silty m SAND; black discoloration at 23-26"; wet;				Highest FID reading
					semi-loose.				501 ppm at 1.5 ft.
					27-53" Gray SILT; little subrounded f-c gravel; trace sand; moist;				
	05.00				v dense.	4700	5/45/00		
	25-30	<u> </u>	58		Gray SILT; little subrounded f-c gravel; trace sand; moist; v dense.	1700	5/15/03	0.0	
					End of boring at 30 feet.				
					•				
									,
NOTEC	NI/A - NI	r ot applicat			bas = below ground surface.				

NOTES: N/A = Not applicable.

bgs = below ground surface.

NAB = Not above background.

TIC = top of inner casing.

ft = feet.

PAGE

1 OF

BORING NUMBER: MW-63S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

LOCATION: Southern edge of treatment area

at 10-30'.

DATE STARTED: 5/16/03

DATE COMPLETED: 5/16/03

GROUDWATER DEPTH: 15.36' TIC on 5/29/03

GROUND ELEVATION:

X COORDINATE:

GEOLOGIST: Matthew Greenberg DRILLER: Bowser-Morner, Inc. Y COORDINATE:

DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-10', lexan liner samples

DATUM:

Sample	Depth	BLOWS	Recov-	uscs	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)					(ppm)	
	0-5		49		0-13" Brown f-m SAND; trace organics; moist; loose.	1525	5/16/03	0.0	
					13-49" Orange-brown f-m SAND; trace subang f-m gravel; wet;				
					loose.				
	5-10		36		0-20" Lt brown f-m SAND; little silt; moist; loose.	1530	5/16/03	0.0	
					20-21" Dk brown PEAT; moist.				
					21-36" Lt brown silty f-c SAND; little subang-ang f-c gravel; wet;				
					semi-loose.				
	10-15		56		Gray-brown silty f-c SAND; little subang-ang f-c gravel; wet;	1540	5/16/03	See	Highest FID reading=
					dense.				77.7 ppm at 4.0 ft.
MW-63S-	15-20		60		0-36" Orange silty f-c SAND; little subang-ang f-c gravel; wet;	1550	5/16/03		Highest FID reading=
SBA-					dense; satd at 16".			right.	1938 ppm at 2.5 ft.
051603					36-60" Gray SILT; little subrounded f-c gravel; moist; v dense.				Sample collected at
							,		17.5 ft bgs.
	20-25		60		Gray SILT; little subrounded f-c gravel; moist; v dense.	1605	5/16/03		Highest FID reading=
								right.	390 ppm at 1.0 ft.
	25-30		57		Same as above.	1640	5/16/03		
					End of boring at 30 feet.				
								*	

NOTES: N/A = Not applicable.

bgs = below ground surface.

NAB = Not above background.

TIC = top of inner casing.

ft = feet.

PAGE 1 OF

BORING NUMBER: MW-64S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

GEOLOGIST: Matthew Greenberg

DRILLER: Bowser-Morner, Inc.

LOCATION: Southwest corner of treatment area

DATE STARTED: 5/16/03

DATE COMPLETED: 5/16/03

GROUDWATER DEPTH: 14.95' TIC on 5/29/03

GROUND ELEVATION:

X COORDINATE:

Y COORDINATE:

DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-10' and 13.5-20', lexan liner samples at 10-13.5' and 20-30'

DATUM:

	····				liner samples at 10-13.5' and 20-30'.				
Sample		BLOWS	1	ı	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)					(ppm)	
	0-5		14"		0-4" Gray organic SILT; moist; loose.	0930	5/16/03	0.0	Cobble at base
			<u> </u>		4-14" Brown SILT; trace ang f-m gravel; dry; loose.				caused low recovery.
	5~10		24"		0-11" M brown f-m SAND; little silt; trace f-m subrounded gravel;	0945	5/16/03	0.0	
					moist; dense.				
					11-24" Rock, cored.				
	10-13.5		12"		Rock fragments.	1055	5/16/03	N/A	
	13.5-20		49"		0-20" Lt brown SILT; trace subrounded f-m gravel; dry; loose.	1105	5/16/03	See	Highest FID reading=
SBA-					20-49" Orange-brown silty f-m SAND; little subrounded f-m gravel;			right.	2850 ppm at 3.0 ft.
051603					wet to satd; semi-dense.				Sample collected at
	20-25		57"		Gray SILT; little subrounded f-c gravel; trace sand; moist; v dense.	1125	5/16/03	0.0	16.5 ft bgs.
	25-30		60"		Same as above.	1145	5/16/03	0.0	
					End of boring at 30 feet.				
								,	
									•
			:						
								į	
				:					
NOTEO	<u> </u>								

NOTES: N/A = Not applicable.

1 OF

bgs = below ground surface.

NAB = Not above background.

TIC = top of inner casing.

ft = feet.

PAGE

BORING NUMBER: MW-65S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

GEOLOGIST: Joseph Francis

LOCATION: South end of treatment area

DATE STARTED: 5/17/03

DATE COMPLETED: 5/17/03

GROUDWATER DEPTH: 11.25' TIC on 5/29/03

GROUND ELEVATION:

X COORDINATE:

DRILLER: Bowser-Morner, Inc. Y COORDINATE: DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-10' and 20-25', lexan DATUM:

liner samples at 10-20' and 25-30'.

Sample	Depth	BLOWS	Recov-	uscs	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)		'			(ppm)	
	0-5		40		0-8" Dk brown Topsoil and sandy GRAVEL. 8-14" Silty CLAY. 14-40" Lt brown and tan SAND.	0820	5/17/03	0.0	
	5-10		42		0-6" Lt brown and tan SAND. 6-12" Sandy GRAVEL. 12-42" Orange and brown coarse SAND.	0825	5/17/03	0.0	
	10-15		60		0-4" Dk brown SAND. 4-35" Red-tan c SAND with gravel. 35-43" Gray-brown SAND. 43-60" Lt brown m SAND.	0838	5/17/03	See right.	Highest FID reading= 1600 ppm at 14.5 ft.
MW-65S- SBA- 0517103	15-20		60		0-4" SAND. 4-8" Dk gray f SAND; wet 8-28" Lt gray-tan TILL. 28-60" Gray TILL.	0851	5/17/03	right.	Sample collected at 16.0 ft bgs. Highest FID reading= 2130 ppm at 1.0 ft.
	20-25		60		0-23" Gray TILL. 23-33" C SAND. 33-60" TILL.	NR	5/17/03	NR	Lexan tube had gotten jammed; switch to using bag sampler.
	25-30		60		TILL. End of boring at 30 feet.	1000	5/17/03	0.0	

NOTES: N/A = Not applicable.

bgs = below ground surface.

NAB = Not above background.

NR = Not recorded.

ft = feet.

TIC = top of inner casing.

PAGE

1 OF

BORING NUMBER: MW-66S

FIELD BORING LOG SHEET

PROJECT: Bedford NWIRP - ERH Thermal Treatment, Site 4

PROJECT NO.: 2282.0892

LOCATION: South of treatment area; adjacent to former underground storage

tank.

GEOLOGIST: Joseph Francis

GROUND ELEVATION:

X COORDINATE: Y COORDINATE:

DRILLING/SAMPLING METHOD: Rotosonic Drilling/plastic bag sample at 0-10', lexan liner samples

DATUM:

DATE STARTED: 6/26/03 DATE COMPLETED: 6/26/03

GROUDWATER DEPTH: 10,44' TIC on 6/30/03

at 10-25'.

DRILLER: Bowser-Morner, Inc.

Sample	Depth	BLOWS	Recov-	USCS	Description	Time	Date	FID	Comments
ID	(feet)	per 6"	ery (in)					(ppm)	
	0-1		N/A		0-12" Asphalt.		6/26/03		
	1-5		40		0-22" Brown fm SAND; moist; loose. 22-40" Orange-brown f-m SAND; little c sand; trace f-m gravel; wet; loose.	0830	6/26/03	2.6	
	5-10		38		0-29" Orange-brown f-m SAND; little c sand; trace f-m gravel; wet; loose. 29-38" Orange-brown f-m SAND; little c sand; trace f-m gravel; gray silt lens at 29"; wet; loose.	0832	6/26/03	32.2	
MW-66S- SBA- 062603	10-15		60		0-23" Orange-brown f-m SAND; little c sand; trace f-m gravel; wet; loose. 23-60" Gray-brown silty f-c SAND; little subang-ang f-c gravel; wet; satd at 27-44"; moist at 44-60"; dense.	0845	6/26/03		Highest FID reading= 433 ppm at 4.5 ft. Sample collected at 14.5 ft bgs.
	15-20		60		0-43" Gray-brown silty f-c SAND; little subang-ang f-c gravel; satd; dense. 43-60" Gray SILT; little subrounded f-c gravel; dry; v dense.	0900	6/26/03		Highest FID reading= 169 ppm at 3.5 ft.
	20-25		58		0-43" Orange-brown silty f-c SND; satd; v loose. 43-58" Gray SILT; little subrounded f-c gravel; dry; v dense. End of boring at 25 feet.	0920	6/26/03		Sample tube became jammed, plastic bag used for sample.

NOTES: N/A = Not applicable.

bgs = below ground surface.

NAB = Not above background.

NR = Not recorded.

ft = feet.

TIC = top of inner casing.

PAGE

1 OF

UNCONSOLIDATED WELL NO. MW-18SR MONITORING WELL CONSTRUCTION DIAGRAM PROJECT Bedford NWIRP – ERH Thermal Treatment, Site 4 DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING DATE BORING NO.: MW-18SR METHOD Rotosonic Drilling ELEVATION DEVELOPMENT FIELD METHOD GEOLOGIST Matthew Greenberg Whale pump/surge block **GROUND SURFACE ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete GROUND SURFACE ELEVATION: **ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 14 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 16 ft ELEVATION/DEPTH TOP OF SCREEN: 18 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 28 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 28 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: None ELEVATION/DEPTH OF HOLE: 28 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-42SR MONITORING WELL CONSTRUCTION DIAGRAM Bedford NWIRP - ERH Thermal Treatment, Site 4 **PROJECT** DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING DATE BORING NO.: MW-42SR METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT **FIELD METHOD GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND** SURFACE **ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 11 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 13 ft ELEVATION/DEPTH TOP OF SCREEN: 15 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 25 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 25 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: None **ELEVATION/DEPTH OF HOLE:** 25 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-60S MONITORING WELL CONSTRUCTION DIAGRAM Bedford NWIRP - ERH Thermal Treatment, Site 4 PROJECT DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING BORING NO.: MW-60S DATE METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT FIELD **METHOD** GEOLOGIST Matthew Greenberg Whale pump/surge block **GROUND** SURFACE **ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 12 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 14 ft ELEVATION/DEPTH TOP OF SCREEN: 16 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 26 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 26 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: #5 Quartz sand/native soils **ELEVATION/DEPTH OF HOLE:** 27 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-61S MONITORING WELL CONSTRUCTION DIAGRAM PROJECT Bedford NWIRP - ERH Thermal Treatment, Site 4 DRILLER Bowser-Morner, Inc. 2282.0892 PROJECT NO. DRILLING DATE BORING NO.: MW-61S METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT **FIELD** METHOD **GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND SURFACE ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 11 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 13 ft ELEVATION/DEPTH TOP OF SCREEN: 15 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 25 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 26 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: #5 Quartz sand **ELEVATION/DEPTH OF HOLE:** 26 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-62S MONITORING WELL CONSTRUCTION DIAGRAM PROJECT Bedford NWIRP - ERH Thermal Treatment, Site 4 DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING DATE BORING NO.: MW-62S METHOD Rotosonic Drilling ELEVATION DEVELOPMENT **FIELD METHOD GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND** SURFACE **ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 12 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 14 ft **ELEVATION/DEPTH TOP OF SCREEN:** 16 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 26 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 27 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: #5 Quartz sand **ELEVATION/DEPTH OF HOLE:** 27 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-63S MONITORING WELL CONSTRUCTION DIAGRAM Bedford NWIRP - ERH Thermal Treatment, Site 4 PROJECT DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING BORING NO.: MW-63S DATE METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT FIELD **METHOD GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND** SURFACE **ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout **ELEVATION/DEPTH TOP OF SEAL:** 10 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 12 ft ELEVATION/DEPTH TOP OF SCREEN: 14 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 24 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 25 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: #5 Quartz sand **ELEVATION/DEPTH OF HOLE:** 25 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-64S MONITORING WELL CONSTRUCTION DIAGRAM Bedford NWIRP - ERH Thermal Treatment, Site 4 PROJECT DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 **DRILLING** BORING NO.: MW-64S DATE METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT **FIELD METHOD GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND** SURFACE **ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 10 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 12 ft ELEVATION/DEPTH TOP OF SCREEN: 14 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 24 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 25 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: #5 Quartz sand **ELEVATION/DEPTH OF HOLE:** 25 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-65S MONITORING WELL CONSTRUCTION DIAGRAM PROJECT Bedford NWIRP - ERH Thermal Treatment, Site 4 DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING DATE BORING NO.: MW-65S METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT FIELD METHOD **GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND SURFACE ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 9 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK: 11 ft ELEVATION/DEPTH TOP OF SCREEN: 13 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 23 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 24 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: None **ELEVATION/DEPTH OF HOLE:** 24 ft **NOT TO SCALE**

UNCONSOLIDATED WELL NO. MW-66S MONITORING WELL CONSTRUCTION DIAGRAM PROJECT Bedford NWIRP - ERH Thermal Treatment, Site 4 DRILLER Bowser-Morner, Inc. PROJECT NO. 2282.0892 DRILLING DATE BORING NO.: MW-66S METHOD Rotosonic Drilling **ELEVATION** DEVELOPMENT **FIELD** METHOD **GEOLOGIST** Matthew Greenberg Whale pump/surge block **GROUND** SURFACE **ELEVATION OF TOP OF SURFACE CASING:** TYPE OF SURFACE SEAL: Concrete **GROUND SURFACE ELEVATION: ELEVATION OF TOP OF RISER:** I.D. OF SURFACE CASING: 8 in TYPE OF SURFACE CASING: Steel flush Mount RISER PIPE I.D. 2 in TYPE OF RISER PIPE: Carbon steel BOREHOLE DIAMETER: 6 in TYPE OF BACKFILL: Cement-bentonite grout ELEVATION/DEPTH TOP OF SEAL: 5 ft TYPE OF SEAL: Medium size bentonite chips ELEVATION/DEPTH TOP OF SAND PACK. 7 ft ELEVATION/DEPTH TOP OF SCREEN: 9 ft TYPE OF SCREEN: Stainless steel SLOT SIZE X LENGTH: .020 in X 10 ft TYPE OF SAND PACK: #5 Quartz sand ELEVATION/DEPTH BOTTOM OF SCREEN: 19 ft ELEVATION/DEPTH BOTTOM OF SAND PACK: 19 ft TYPE OF BACKFILL BELOW OBSERVATION WELL: None **ELEVATION/DEPTH OF HOLE:** 19 ft **NOT TO SCALE**

APPENDIX D

Groundwater Sample Collection Record



Well ID: WISS Page 1 of 2

(continued on back)

Date: 06/08/03

				Ground	wate	r San	npie C	onect	ion Re	ecora
Client: Project i Site Loc		068- ල	284	eeler) 3-006-30 -817c 4	<u> </u>		0-2-0		F	Start 1446 (24hr) Finish 1645
Weather		SOUL VIKE PG			2'C	Collecto	or(s): <u>M</u>	, Gre	enbû	rg. L. Burdick
Total Water Water	well length: r table depth r column len	733 : 5 gth:	.91 .91	sured from T Screen interva Casing type\di Pump intake o	al: iameter: depth:	iñ-2 steel 23	<u>/2"</u> Tu Mi ∖	ital tubing l ibing intern nimum pur	al diam.:	(ft)
Acce - Ten - pH - D.C	ptance Crit nperature	eria (EF 3% + 4	PA Reg 6 or - 0.1 % (0.	gion I low flow	groundw - ORI	vater sar > wdown	npling pro + or - < 0.3 f	10 mV		
Field	Testing Eq	uipment	used:	Make		Mod	el		Ser	rial number
<u> </u>				YSI		610			0	2R0485AN
				YSI		6820	or 6920)		AA FF (TS)
				LaMotte		2020) Turbidim	eter		549-3509
				Photovac		2020) PID '			
	Volume						Ţ,			
Time (24hr)	Removed (liters)	Temp.	рН	Spec. Cond.	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdow (feet)	vn Comments
1501	0.00	4 05	6.31	383	440.0	1,93	37	250	0.13	Flow cell full
IKIL	0.35	13,20	10.14	રુઉજ	-144 7	0.79	37	150	0,24	clear, oder
1516	0.50	13,33	10.18	350	-148.9	0.64	18	180	0.90	} (c
1501	C.75	13.38	6.26	424	-154, 7	0.59	15	180	0.30	2 10
1526	1.00	13.24	يلا. ما	424	-155, <i>ia</i>	0.49	13	150	11.30	0 4 4 4
1531	1.25	13,40	6.27	434	-15% 5	0.50	11	150	0.3	8 4 4
1536	1.50	13,40	6.38	416	-156.7	0.51	1-7	170	0.30	
1541	1.75	13.53		431	-155,5		_ لذ	170	0,30	
1546		13.43		431	-154.5	0.48	<u>q.7</u>	150	0.30	
1551	3.95	13.56		नं उत	-1500	0.47	%ે.}−	150	(1.30	
عا555	2.50	13.52	6.38	431	-150.0	0.43	(0:0)	150	0.30) 11 11
 			į	1			_		l	
			<u> </u>							
0.1.	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	9.0		10						
رون	diffe	Sa	ng	\p						
			,							
	d: , to	sa sa	161							

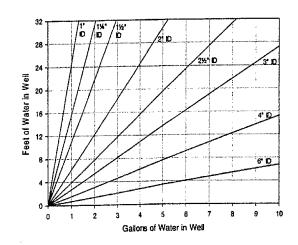
Sample Collector(s): <u>La Bundur</u>

Well ID: MW - 185R

	Volume	(continu	ued fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp. (°C)	pН	Spec. Cond. (uS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
				\smile		,				
				Z B	inde		<u> </u>			
						E				
·										
		:	_							
							<u> </u>			

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	<u>Analysis</u>	Time (24 hr)
MW-1852-GW-Clo	don3 3	40 ml	HCL	TCL NOCS -	1605
11W0 1322 302 CA	2	11	با و	2-MethinaDthalene	1605
MW-1838	1	500ml Dlastic	400	test kit	1605



Calculations:

3 (add 3ft for pump) 0.0217 Liters per foot tubing length =

tubing vol. 0.065

0.25 (flow cell vol., L) 0.315 (liters)

system vol.

Volume p	Volume per linear ft of tubing									
ID (in)	Gallon	Liter								
0.250	0.0025	0.0097								
0.375	0.0057	0.0217								
0.500	0.0102	0.0386								
0.750	0.0229	0.0869								
1.000	0.0408	0.1544								
1.250	0.0637	0.2413								
1.500	0.0918	0.3475								
2.000	0.1632	0.6178								
2.500	0.2550	0.9653								
3.000	0.3672	1.3900								
4.000	0.6528	2.4711								
6.000	1.4688	5.5600								

Comments: A flow rate around 180 m	ıl/min is appropr	iate	
PID reading of purge wa	ater = ppm		·
	1	1	

Collector(s): Lai Burdie Date: <u>06/03/03</u>



ound Water Sample Collection Record

				Ground							70.14
Client:	Navy (oster	Wh	eeler)		Date: 💪	و - ديـر	3	Time:	Sta	rt <u>i 508</u> (24hr)
Project N	lo: <u>5060-</u>	068- ල	2840	2-006-30	<u>\$</u>					Fini	sh <u>1603</u>
Site Loca				-8:tc 4		~ " ·	IA	· Gree	Alne	ive	I Buntal
Weather	Conds:	<u> </u>	NK 1	migh 60's		Collecto	or(s): <u> </u>	. 618	- PVOC	477	C. SUNGOE
Total v Water Water	well length: table depth column leng	ابنان : <u>الا</u> gth: DATA	62111 1.9.311	Sured from T Screen interval Casing type\di Pump intake of	al: iameter: lepth:	15 2 Steel 30	<u>/2''</u> Tu <u>၆ရ3်</u> Mi	tal tubing lo bing intern nimum pur	al dian	٦.:	22 (ft) 6.375 (inches) (calculations on reverse)
Accer		eria (EF 3%	PA Reg	gion I low flow	groundw - ORI	ater sar		10 mV			
- D.O - Spe	c. Cond.	10 39		5 mg/L if <1)	- Turt	oidity	< withi	in 10%			
Field	Testing Eq	uipment	used:	Make		Mod	ef			Serial	number
				YSI		610					
				YSI			0 or 6920				F0329 A)
				LaMotte Photovac			O Turbidim O PID	eter			0639-1299
1	Volume	1		II Hotovac		1202	!				
Time	Removed :	Temp.	рН	Spec. Cond.	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawd		Comments
(24hr) 3 5 1 1	0.00	14.50	7.52	107	-9.0	·	45			7	<u> </u>
						10.171	45	150	LLA.	ï/	Flow cell full
1 521	0.5		6.19	109	3.3	0.01	38	150	15.5	0	Flow cell full
1236	0.8	14.33 14.33	6.19 6.17	109	3. § 5, 9	1.76	3'8 45	170	15.5 15.	67	Flow cell full
1536 1531	0.8	14.33 14.33	6.19 6.17 c.61	109	3.8 5.9 6.9	1.54 1.76 1.60	3'8 45 40	170 170 130	डि.ह 15. 15.	67 57	Flow cell full
	0.8	14.33 14.33 14.33	6.19 6.17 6.71	109	3.8 5.9 6.9 6.4	1.76	3'8 45	170 170 175	15.5 15.	6 7 5 7	Flow cell full
1526 1536 1541	0.8 1.0 1.4 1.6	14.33 14.33 14.33 14.33 14.32	6.18 6.17 6.17 6.15	109	3.8 5.9 6.9	1.54 1.76 1.60	3'8 45 40	170 170 175 150	1000	67 57	Flow cell full
526 1531 1536 1546	0.8 1.0 1.4 1.6	14.33 14.33 14.18 14.37 14.37 14.47	6.18 6.17 6.17 6.15	109	3.8 5.9 6.9 6.4	1.54 1.76 1.55 1.62	3'8 45 40 50 55	170 170 175	15.5 15.	67 57 17	Flow cell full
1526 1536 1541	0.8 1.0 1.4 1.6	14.33 14.33 14.33 14.37 14.32 14.47	679 677 677 675 688	105 105 113 116 119	3.8 6.4 3.8 C.4	1.54 1.76 1.55 1.62	3'8 45 40 50 55	170 170 130 150 160	15.15.15.15.15.15.15.15.15.15.15.15.15.1	67 57 17	Flow cell full
536 1536 1536 1536 1536	0.9	14.33 14.33 14.33 14.33 14.33 14.43 14.41	6777 6677 6677 6666 6666 6666	105 105 119 119 119 119 115 121	3.8 6.4 3.8 C.4 3.7.0	1.54 1.76 1.60 1.55 1.62 1.49 1.57	3'8 45 45 55 55 55 55	170 135 155 160 160	15.55 15.55 15.55 15.55 15.55	10 7 17 9 17 9 17 9 17 9 17 9 17 9 17 9 17	Flow cell full
1536 1536 1536 1536 1536	0.9	14.33 14.33 14.33 14.37 14.32 14.47	6777 6677 6677 6666 6666 6666	105 105 113 116 119	3.8 6.4 3.8 C.4	1.54 1.76 1.60 1.55 1.62 1.49 1.57	3'8 45 45 55 55 55 55	170 130 135 150 160 160	15.15.15.15.15.15.15.15.15.15.15.15.15.1	10 7 17 9 17 9 17 9 17 9 17 9 17 9 17 9 17	Flow cell full
536 1536 1536 1536 1536	0.9	14.33 14.33 14.33 14.33 14.33 14.43 14.41	6777 6677 6677 6666 6666 6666	105 105 119 119 119 119 115 121	3.8 6.4 3.8 C.4 3.7.0	1.54 1.76 1.60 1.55 1.62 1.49 1.57	3'8 45 45 55 55 55 55	170 135 155 160 160	15.55 15.55 15.55 15.55 15.55	10 7 17 9 17 9 17 9 17 9 17 9 17 9 17 9 17	Flow cell full
536 1536 1536 1536 1536	0.9	14.33 14.33 14.33 14.33 14.33 14.43 14.41	6777 6677 6677 6666 6666 6666	105 105 119 119 119 119 115 121	3.8 6.4 3.8 C.4 3.7.0	1.54 1.76 1.60 1.55 1.62 1.49 1.57	3'8 45 45 55 55 55 55	170 135 155 160 160	15.55 15.55 15.55 15.55 15.55	10 7 17 9 17 9 17 9 17 9 17 9 17 9 17 9 17	Flow cell full
536 1536 1536 1536 1536	0.9	14.33 14.33 14.33 14.33 14.33 14.43 14.41	6777 6677 6677 6666 6666 6666	105 105 119 119 119 119 115 121	3.8 6.4 3.8 C.4 3.7.0	1.54 1.76 1.60 1.55 1.62 1.49 1.57	3'8 45 45 55 55 55 55	170 135 155 160 160	15.55 15.55 15.55 15.55 15.55	10 7 17 9 17 9 17 9 17 9 17 9 17 9 17 9 17	Flow cell full
5006 1506 1506 1506 1506 1506 1506 1506	0.9	14.33 14.33 14.33 14.33 14.33 14.43 14.41	6777 6677 6677 6666 6666 6666	105 105 119 119 119 119 115 121	3.8 6.4 3.8 C.4 3.7.0	1.54 1.76 1.60 1.55 1.62 1.49 1.57	3'8 45 45 55 55 55 55	170 135 155 160 160	15.55 15.55 15.55 15.55 15.55	10 7 17 9 17 9 17 9 17 9 17 9 17 9 17 9 17	Flow cell full

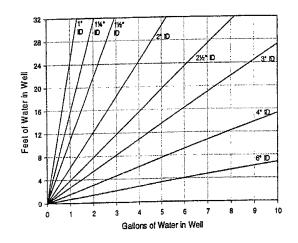
Sample Collector(s): M. Greenberg Date: 6-2-03

Well ID: MW-42SR

	Volume	(continu	ued fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp. (°C)	рH	Spec. Cond. (µS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
\ <u>\</u>										
				,						
		<u> </u>			:					

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
MW-425R-6W-0602	19 3	40 ml	HCL	TCL NOCS =	1625
MW-425R-GW060		11	4°C	2-MethInasthalene	1625
440-4252		500 ML DUSTIC	400	1+est kits	1629



Calculations:

tubing length = 3 (add 3ft for pump)

x 0.0217 Liters per foot

tubing vol. = 0.065

+ 0.25 (flow cell vol., L)

	+	0.25	(flow cell	vol
system vol.	=	0.315	(liters)	

		·							
Volume p	Volume per linear ft of tubing								
ID (in)	Gallon	Liter							
0.250	0.0025	0.0097							
0.375	0.0057	0.0217							
0.500	0.0102	0.0386							
0.750	0.0229	0.0869							
1.000	0.0408	0.1544							
1.250	0.0637	0.2413							
1.500	0.0918	0.3475							
2.000	0.1632	0.6178							
2.500	0.2550	0.9653							
3.000	0.3672	1.3900							
4.000	0.6528	2.4711							
6.000	1.4688	5.5600							

	A flow rate around 180 ml/min is appropriate
Comments:	A How rate around 100 minimus appropriate
	PID reading of purge water = ppm
ł	

Collector(s):	Date:	, •
Concolor (C).		



Well ID:	MW-603	

Page 1 of 2

Ground Water Sample Collection Record

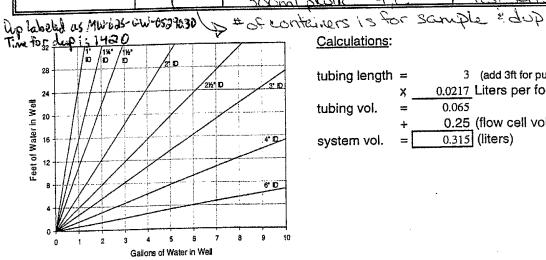
Total Wate Wate	r Conds: ER LEVEL weil length: r table depth r column len	DATA:	edford d: (mea 5.85 5.30 5.55	sured from 1 Screen interview Casing type of pump intake of the page of the pa	Top of Ca al: liameter: depth:	sing) Steel	т. / <u>2"</u> т. м	, Burd otal tubing l ubing interr linimum pur	length: nal diar	n.:	(ft) (s) 375 (inches) (calculations on reverse)	
- Ter pH - D.0	nperature	3%	6 or - 0.1)% (0.1	gion I low flow I ι 5 mg/L if <1)	- ORI - Dra		+ or - < 0.3	10 mV				
Field	Testing Eg	uipment	used:	Make		Mod	el			Serial	number	İ
<u>النست</u> ين			5	YSI			DM				Z4 PGE'05	
				YSI		6820	0 or 6920				790777	1
				LaMotte		2020	0 Turbidir	neter			(42 - 3505	
				Photovac		2020) PID					
	Volume	1		(!	V				1
Time (24hr)	Removed (liters)	Temp. (°C)	рН	Spec. Cond.	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)		down et)	Comments	-
1315	0.00	14.44	6.41	916	-93.3	1.40	10	250	0,0	53	Flow cell full clear odo	c
1325	0,95	13.34	6.25	848	-125,7	0.04	300	222	٠,٦,٠٠	50	cloude odor	[`
1335	0,50	13,42		168	-121.5	0.50	31	180	0.	80	W W	
340	0/00	13:56			-120,4	0.47	15	200		75	slear, ador	
345	1,55	13,57			-133.1	0.44	10	150	1.0	53		pike 1.1 on
1350	1,50	13.37		ે હો	-126.5		5.6	150		v	1.3 - PID : 0000	7,-0,,, 0,,
1355	11.75	13,12		790	-1259		5.5	150	1.6	18	clear-ador	
1400			6.20		-124.4		₹,4	150	1, 2		ilear-cosc	
1405	2.35	1310		783	-127.2		4.8	150	1,5		:1 c(
<u> </u>												
0141	readu	to	Sa	wile								
	1,2,2,1			7		-			1			
								T				
												ĺ
			1									
										-X/		
											(continued on back)	

Well ID: MW-60S

ſ	Volume	(continu	ued fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp. (°C)	рН	Spec. Cond. (μS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
				***	2010					
					-					
<u> </u>										·
									11.00	
									`t +	
<u> </u>										,
					 				<u> </u>	
11	1			l				<u> </u>	1	<u> </u>

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
MW-625-6W-05340	2 3/12	40 ml	HCL	TCL MOCS =	1415
MW-635-6W-0529		1 \	4°C	2-MethInadthalene	1415
MW. 607 - 10 10 - 0.00-1	1	500ml Dicoti	400	test kits	1415



Calculations:

3 (add 3ft for pump) tubing length = 0.0217 Liters per foot

tubing vol. 0.065 0.25 (flow cell vol., L)

system vol. 0.315 (liters)

Volume per linear ft of tubing							
ID (in)	Gallon	Liter					
0.250	0.0025	0.0097					
0.375	0.0057	0.0217					
0.500	0.0102	0.0386					
0.750	0.0229	0.0869					
1.000	0.0408	0.1544					
1.250	0.0637	0.2413					
1.500	0.0918	0.3475					
2.000	0.1632	0.6178					
2.500	0.2550	0.9653					
3.000	0.3672	1.3900					
4.000	0.6528	2.4711					
6.000	1.4688	5.5600					

Comments: A flow rate around 180 ml/min is appropri	ate
PID reading of purge water = ppm	
PID reading of purge water = ppm	
·	

Collector(s): La Bundine Date: <u>5/29/03</u>



Well ID: MW-615

age 1 of 2

Ground Water Sample Collection Record

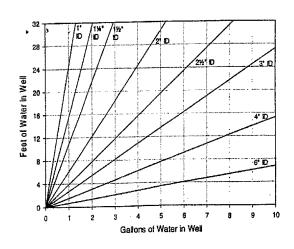
	Faster				Date: <u>5</u>	-3D·	· 03	Time: Sta Fini		(24hr)
roject No: 500 ite Location: /eather Conds:	NWIRP Be	edford -	-8:tc 4		Collecto	r(s): <u>M</u>	.Gre	enberg	L. Berry	lick
Total well lengt Water table der Water column I WELL PURG Purge Method Acceptance C - Temperature - pH - D.O Spec. Cond	h: Q 4,4 oth: \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	7.441 7.441 PA Reg 6 or - 0.1	Screen interval Casing type\di Pump intake of ap & dedicated tion I low flow	tubing (-)	Steel / Steel / Steflor teflor rater san	Tui Here Min Fit hijs	cedure) 10 mV t		24 6.375 (calculations on reverse)	(ft) (inches) (liters)
Field Testing		used:	Make		Mod		-	Serial	number	
			YSI YSI		6101	DM O or 6920				
			LaMotte) Turbidim	eter			
			Photovac		12020	PID :				<u></u>
Time Remov	ed Temp.	рH	Spec. Cond	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comment	H
(24hr) (liters 0.00	12.93 (°C)	6,33		177.	3,53	17.75	aso	17,73	Flow cell full	D:2-3 ppm:
				100	2 22	65 (AC)	120	/8:03		
905 3	12.7	5.96	441	135.1	3.03	36	120	18.11	PID=1.600	·~
910 3.5	12.69	5.93	437	1737	3.50	38	130	18:17		
7976 6	13.70	5.93	- 4	163.6	3.83	28	150	18.23		
925 3	12.54	5.93	432	141.1	3.30	23	150	13,30		
930	12.61	5.94	437	123.5	3.23	27	150	18.34		
1935 10	12.6	15.94	440	109.3	3.90	121	160	13.39	<u> </u>	
1940 13	12.64	5.93	439	103.4	2.58		150	13.44	ļ	
945	12.75	5.93	440	97.0	3.66		150	13.48		
0950 15	12.29	5.93	443	91.7	3.44	14	150	13.20	<u> </u>	
	F 7"	un,	Ems.	tu.	For	rack	orgo.	pury	ola) 25 ~ 3.	5 gals
0955 50	~ ~~				,		 	 		
0955 Sw	- 34	-	1,1			L	<u> </u>			
0955 54	100									
0955 SW	194									

Well ID: M W-6(5

-	Volume	(continu	ued fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp. (°C)	рH	Spec. Cond. (µS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
ļ										

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
MW-615-GW-05300		40 ml	HCL	TCL NOCS =	1025
MIN-615-6W-05300	3 <u>2 </u>	11	4°C	2-Methinaphhalene	1035
MW-615		500 ML Dingtic	400	1-05+ kits	1



Calculations:

tubing length = $\frac{3}{x}$ (add 3ft for pump) x $\frac{0.0217}{x}$ Liters per foot

tubing vol. = 0.065

+ 0.25 (flow cell vol., L) system vol. = 0.315 (liters)

Volume per linear ft of tubing							
Gallon	Liter						
0.0025	0.0097						
0.0057	0.0217						
0.0102	0.0386						
0.0229	0.0869						
0.0408	0.1544						
0.0637	0.2413						
0.0918	0.3475						
0.1632	0.6178						
0.2550	0.9653						
0.3672	1.3900						
0.6528	2.4711						
1.4688	5.5600						
	Gallon 0.0025 0.0057 0.0102 0.0229 0.0408 0.0637 0.0918 0.1632 0.2550 0.3672 0.6528						

Comments: A flow rate around 180 ml/min is	s appropriate
PID reading of purge water =	ppm

Collector(s): M. Creenberg Date: 5-3



Well ID: MW - 625

ge 1 of 2

Ground Water Sample Collection Record

Client: Navy (Foster Wheel Project No: 5060-068-02840-0		ə: <u>5-29-03</u> Tim	ne: Start <u>1312</u> (24hr) Finish <u>1441</u>									
Site Location: NWIRP Bedford - S Weather Conds: Survey	ite 4	lector(s): M. Greenb	erg, L. Burdick									
WATER LEVEL DATA: (measured from Top of Casing) Total well length: 25.55 11CScreen interval: 16-26 Total tubing length: 24 (ft) Water table depth: 12.79 16Casing type\diameter: Steel / 2" Tubing internal diam.: 6.3+5 (inches) Water column length: Pump intake depth: 22+1 / 25 Minimum purge volume: (alculations on reverse)												
2. WELL PURGE DATA Purge Method: Peristaltic pump of	& dedicated tubing (+e	flon										
Acceptance Criteria (EPA Region - Temperature 3% - pH + or - 0.1 t - D.O. 10% (0.5 m - Spec. Cond. 3%	- ORP - Drawdo	+ or - 10 mV own < 0.3 ft	•									
Field Testing Equipment used:	Make	Model	Serial number									
	YSI	610DM										

<u>استنتا</u>	001113 = 4			YSI		6101	DM			
				YSI		6820	or 6920			
			LaMotte) Turbidim	eter		
				Photovac		2020) PID			
Ī	Volume						!			
Time (24hr)	Removed (liters)	Temp.	pН	Spec. Cond.	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
374	0.00	13.67	6.57	252	4158	3,69	50	3-00	17.72	Flow cell full
12713	2	12.56	296	176	91.7	2,93	4.5	110	18.61	
	2.3 Me		5.98		88.1					

(24hr)	(liters)	(°C)		(μS/cm)	(mV)	(mq/L)		(m/min)	(reer)	
1314	0.00	13.67	6.57	⊋ 5 3	4158	3,69	50	3-00		Flow cell full
1274	2	12.56	C.96	176	917	2,93	4.5	170	18.61	·
1330	2-2-Me	12.72	3.43	176	88.1	2.96		100	13.73	
331	- 1 AC	12.75	5.94	177	72.1	2.94		130	19.08	PID=NAB
1344	W.	12.61	5.99	173	69.5	2.85		200		PI D=NAB
1350	3.300	2.35	6.23	171	53,6	2.68	13	ವರ್ಣ	19.47	
1355	C ₂	12.57	6,03	175		2.49		180	19.62	
1404	R	12.29	6.0	137	16.7	7.05	11	200	19.84	
1412	8//	12.32	615	700	7.1		9,5		10, 33	
1418	12	12.37			0.3	1.61	6.9	150	19.39	
1423	15	12.23	6.34		79,5	1.44	6.0	150	19.39	
1428	77	17.26	630	272	-30.5	1.36		170	19.91	
1433	20	12.22	26.3	277	-31.5	1.40	5.9	170	14.94	
133	22	1378	6.75	236	-30.1	1.45	5.4	170	19.95	
1			1							
ापपा	EN B	-00	To	見がっ	4 note	Alisa	ten re	herao.		
 ` ` ` ` 		1			J.		.	0		
										<u> </u>

continued on back)

Sample Collector(s): M. Granding L. Burliel Date: 5-29-03

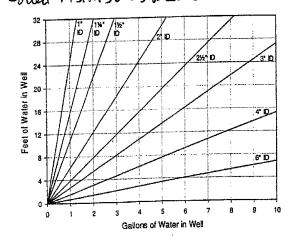
Well ID: MW-625

Ţ	Volume	(continu	ed fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp.	рН	Spec. Cond. (μS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
(2-4117)										
					·					
 					·····					
					·					
			·				<u> </u>			
l							<u> </u>			

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
day it had all a	3 3 9	40 ml	HCL	TCL NOCS -	1600
MW-625-6W-052903		16	4°C	2-Methlnasthalene	1600
1 W. C*7 200 03X10		Scomb plastic	400	lest leits	1600

Collect MS/MSD as well (total of 9-40mL viols, 6-12 jars), 1600



Calculations:

tubing length = 3 (add 3ft for pump) x 0.0217 Liters per foot tubing vol. = 0.065 + 0.25 (flow cell vol., L)

	+	0.25 (flow cell vo
system vol.	=	0.315 (liters)

Volume p	er linear ft	of tubing
ID (in)	Gallon	Liter
0.250	0.0025	0.0097
0.375	0.0057	0.0217
0.500	0.0102	0.0386
0.750	0.0229	0.0869
1.000	0.0408	0.1544
1.250	0.0637	0.2413
1.500	0.0918	0.3475
2.000	0.1632	0.6178
2.500	0.2550	0.9653
3.000	0.3672	1.3900
4.000	0.6528	2.4711
6.000	1.4688	5.5600

Comments: A flow rate around 180 ml/min is appropriate

PID reading of purge water = ppm

Collector(s): M. Greenberg, L. Burdick Date: 5-29-03



Well ID: MW-635 .

Page 1 of 2

Ground Water Sample Collection Record

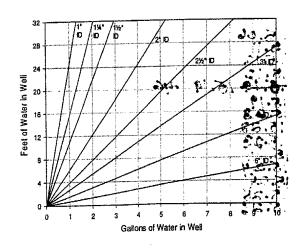
Client:_	Navy (Date: _	5-3-0	3	Time:	Start	1010	_(24hr)
Project I				<u> </u>	<u>>\</u>					Finish	1136	
Site Loc				-8:tc 4			1.	1 -	λ		^ .	
Weathe	r Conds:	SUNY	14.1	c0s		Collect	or(s): 🔼	1. Gre	whier	<u>., L.</u>	Burlick	<u> </u>
			4 7	<u> </u>						+		
1. WAT	ER LEVEL	DATA:	: (mea:	sured from T	op of Ca	sing)						
				Screen interva			bas To	tal tubing l	enath:		7 3	(ft)
						Steel	72 [™] Tu	bing intern	al diam.	: -	375	(inches)
Water table depth: いって Casing type\diameter: Steel / 3 ¹¹ Tubing internal diam.: 6 3 + 5 (inches Water column length: Pump intake depth: 3 0 5 5 4 Minimum purge volume: (liters)												 '
water column length: Pump intake depth: 30 635 willithrum purge volume: (liters)												
	L PURGE I						\			- "		
Purg	e Method:	Perista	ltic pun	np & dedicated	tubing (teflo	n					
_				-! ! 1 £!			0	I V				~
				jion I low flow	groundw ORf							
	nperature	3%	6 or - 0.1	,		wdown	+ or - < 0.3 f					/
pH - D.C)			້ 5 mg/L if <1)	- Turk			in 10%				
	ec. Cond.	3%		z mg/= = 1/	- ruit	, only	~ *********	1070				
Field	Testing Equ	uipment	used:	Make		Mod	lei		Se	erial nun	nber	
				YSI			DM			H .		
				YSI		6820 or 6920				02 F 03 2 9 A)		
				LaMotte		2020 Turbidimeter 2020 PID			0634-1248			
	F	i		Photovac		1202	U PID					****************
	Volume			Spec. Cond.	600		· •	71 D-1-	D			
Time (24hr)	Removed (Temp. (°C)	pН	(μS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdo (feet)		Commen	TS
1013	0.00	113.25		267	1931	1,25		180	14.8	3 Flo	ow cell full	
1023		12.42		166	50.0	1.57		190	15.	36		
1028		12.53		180	20.0		550	140	15.11			
1033	1.0	12.67			3.0	1.69		150	15.1			
1038	177	12.13	_		-23.4	1.45	650	160	13.1		2 10 (2)	
10तंत्र		12.73		351	37.5	1.35	550	770	+6-1		5.19 MG	•
/ठतेहें	1.3	12.77		277	-48,9 -681	1.03	300	160	12.3			
1053		12.74		287	~64. 9	0.90	210	160	15.0			*****
1103	2.0	a.75		290		0.85		160	5.2			
108	2.3	12.85				0.30	110	160	15.2	7		
1113	2.5	12.76	7	294		0.73	70	160	15.2			
1118	2.7	12.21		298	-79.9	0.68	60	1.50	15.24			_
1123	20	13.88		292		0.61	39	170	15.2	5		
1138	3.2	12.92		_ <u></u>		0.64	39	160	12.3			
1133	3.5	12.83	كالوط	290	84.5	0.65	32~	170	is.as	<u> </u>		
11:22	6 EN		C10	- A-4-	18) 1	دي د د						
	16 EN	للله	<u>y 44</u>	· 37 121	ا ک حق	3.79	<u>5 30/45</u>					
				•	1		4				entinued on back)	
	ample Celle		-M	GADA	\ ^			_	ata:	F -	2-03	

Well ID: MW-635

	Volume	(continu	ued fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp.	рH	Spec. Cond. (µS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
1-111										
·							<u> </u>			
						 	<u> </u>			
		t				<u> </u>	1	<u> </u>		

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
MW-635-6W-06030	2 3	40 ml	HCL	TCL WOCS =	1205
MW-635-GW-0602		16	40	2-MethInaDthalene	1205
MW-635 GW-0808	1	500ml plastic	4 °C	test kits	:205



<u>Calcula</u>	ations:	4.31	ಠ, ಇನ್	,	٠,	
tubing	length	×	: 3, 3£	(add 3it f Liters be	or pun	np)
tubing	C dow	7.6. 3.4.	0.825	flow ce	~	S
system			0.33.52	(liter\$)?) L	1
		07.0	3.77	· Air		
35	200			30) \$ 1.0 \$ 1.0

volume p	er imear it	or tubing
<u>+</u> 1Ω-(in)	• Gallon	Liter
F.G.250	~ ,0:00 2 5;<	0.0097
0.375	2 0.0057	0.0217
ຼີ 0:500	0.0102	0.0386
9.750	0.0229	0.0869
£\$.Ω00	Ω.0408-	0.1544
41.250	0.0637	- 0.2413
:500 ;	0.0948	0.3475
32: 000 (2	0.1632	.0.6178
2.500	0.2550, ,	0.9653
₹8.000	∵0 , 367≥ ु	1.3900
64.000	70.6528	
6.000	1.4688	5.5600

Comments: A flow rate around 180 ml/min is	appropriate	 		
PID reading of purge water =	ppm		 	
			 	,
	:			

Collector(s): M. Greenser Date: 62-03



Ground Water Sample Collection Record

Client: Navy (Foster Wheeler)	Date: 3 - 30 - 10 - 5	Time: Start <u>3055</u> (24nr)
Project No: 5060-068- 02840-006	<u>-366</u>	Finish
Site Location: NWIRP Bedford - 3:4c		enborg, L. Burliak
Water column length: Pump int	om Top of Casing) Interval: 1424 865 Total tubin Interval: Steel / 2" Tubing intervals Interval: 17.5 hg Minimum p	ernal diam.: <u>6.375</u> (inches)
2. WELL PURGE DATA Purge Method: Peristaltic pump & dedi	rated tubing (LaClan)	
Purge Method: Feristande pump & dedi	cated tubing Cressisti	
Acceptance Criteria (FPA Region Llow	flow groundwater sampling procedure)	
- Temperature 3%	- ORP + or - 10 mV	
- pH + or - 0.1 t	Drawdown < 0.3 ft	
- D.O. 10% (0.5 mg/L if	<1) - Turbidity < within 10%	
- Spec. Cond. 3%		
Field Testing Equipment used: Make	Model	Serial number
Field Testing Equipment used: Make YSI	610DM	0280435AD
YSI	6820 or 6920	99812788
LaMo		3542-3502
Photo	vac 2020 PID	

Photovac

_	Volume						:	,			1
Time (24hr)	Removed (liters)	Temp. (°C)	рH	Spec. Cond.	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments .	
6902	0.00	12.42	6.05	413		a.570		300	0,05		@9°c
GIPO	0.35	11.78	590	276	33.4	1.77	3,0	300	0.10	5901 5160C	į
0917	0.50	11.63	593	みずる	25.4	206	1.8	360	0.11	PID 14.5, odor e	lear
0933	0,75	11.54	5.94	378	22.4	2.03	2.1	240	0.12	Odor clear	•
1027	1.00	11.104	5,97	38	20.7	2,42	2.5		91.0	PID 6.0 Odorie	ear
0032	1.25	11.69	5.98	284	18,3	2.43	33	900	6.17	Clear ober	
0027	1,50	11.73	5,99	286	16.2	3.02	3.5	200	21.0	PID I.4, clear	
0042	1,75	18.11	10,01	288	14.7	3,75	3.3	900	0.18	, clear, some od	r
0947	200	11.84	10.01	989	14.3	85,6	3,4	900	0.80	PIDO8 clear	
3955	2.25	11.94	6.03	295	13.4	ひけん	28	950	0.20	croc ,	
CQ 5.7	A.50	13.06			13.6	9.99	PE	900	0.21	clear	
600	3.00	12.64	624	296	14.0	2.69	13.1	<u> 1</u> 00	0.39	Noa	
1005	7ea	30	10	Sans	10.						
		1			7						
···							-				1
									<u> </u>]
										Vesstinuad on book	

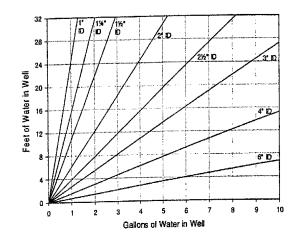
(continued on back)

Well ID: MW-645

[Volume	(conting	ued fron	n front)						Page 2 of 2
Time (24hr)	Removed (literss)	Temp.	pН	Spec. Cond. (µS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	Drawdown (feet)	Comments
				1						
				Zoi:	12	1				
				·		Loch	k			
ļ										
								<u>L</u>		

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
MW-645-66 0530	3 3	40 ml	HCL	TCL NOCS 12	1005
MW-645-6 W-0530	03 0	11	4°C	2-MethInadthalene	1005
MW 645 6 10 00 00 00 00 00 00 00 00 00 00 00 00	7 7	500 m 1 D/05	me you	lest lits	1005



Calculations:

tubing length = $\frac{3}{x}$ (add 3ft for pump) x 0.0217 Liters per foot

tubing vol. = 0.065

+ <u>0.25</u> (flow cell vol., L)

system vol. = 0.315 (liters)

Volume per linear ft of tubing						
ID (in)	Gallon	Liter				
0.250	0.0025	0.0097				
0.375	0.0057	0.0217				
0.500	0.0102	0.0386				
0.750	0.0229	0.0869				
1.000	0.0408	0.1544				
1.250	0.0637	0.2413				
1.500	0.0918	0.3475				
2.000	0.1632	0.6178				
2.500	0.2550	0.9653				
3.000	0.3672	1.3900				
4.000	0.6528	2.4711				
6.000	1.4688	5.5600				

Comments: A flow rate around 180 ml/min is	s appropriate
PID reading of purge water =	bom
1 ID Teaching of parge mater	

Collector(s): Las Brudik Date: 5/30/03



Well ID: MW-655
Page 1 of 2

(continued on back)

	Ground Water Sample Collection Record									
Client: Project N)ර8 ල	284c	eler) 3-006-30 3:te 4	Δ		2-2-		Time: Sta Finis	sh
Site Loca Weather		YKP Be Sunu			(Collecto	r(s):	1. Green	berg L.	Bortick .
1. WATER LEVEL DATA: (measured from Top of Casing) Total well length: 3.61 TIC Screen interval: 13-23 has Total tubing length: 20 (ft) Water table depth: \(\frac{\lambda_0 \frac{\gamma_1 \text{TIC}}{\gamma_0 \text{TIC}}\) Casing type\(\diam\text{diameter:}\) Water column length: Pump intake depth: \(\frac{13 \cdot \gamma_0 \frac{\gamma_0 \text{TIC}}{\gamma_0 \text{TIC}}\) WELL PURGE DATA Purge Method: Peristaltic pump & dedicated tubing \(\frac{\gamma_0 \text{TIC}}{\gamma_0 \text{TIC}}\) Peristaltic pump & dedicated tubing \(\frac{\gamma_0 \text{TIC}}{\gamma_0 \text{TIC}}\) 13-23 has Total tubing length: \(\frac{\gamma_0 \text{3-5}}{\gamma_0 \text{5-5}}\) (inches) (inches) (inches)										
- Tem - pH - D.O.	Acceptance Criteria (EPA Region I low flow groundwater sampling procedure) - Temperature 3% - ORP + or - 10 mV									
Field	Testing Equ	ipment	used:	Make		Mode	el			number
L				YSI		610I				BOHZZAD
				YSI			or <u>(6920</u>)		1797	11377AA
				LaMotte) Turbidim	eter	-+	49 - 2260
		7		Photovac	× 	12020	PID ;			
	Volume	Ļ		01				E1 E1-4-	Drawdown	Comments
Time	Removed	Temp. (°C)	pН	Spec. Cond. (μS/cm)	ORP (mV)	DO (mg/L)	Turbidity (NTU)	Flow Rate (ml/min)	(feet)	Comments
(24hr)	(liters) 0.00	1195	1. 58	1071	-130 3	14.8)	9.5	380	1.0	Flow cell full
1036 1036	0.35		lo51	373	-315.5	7,11	11	330		cleas
1041	8.50		6:47	273	⊋34.ı	7.85	08.i	150	しらる	()
1046	(5.75	11.98	6.45	370	-335.k	3.91	₹.5	150	1.44	11 12
1051	1.00	106	64.4	ედე	244.0	1.03	X +	450	1.44	11 (3
1056	1.25		6.38	360	<u>- مالاه- ۲</u>	liets	13	150	1.46	
1101	1.50	10,01	634	363	-548.1	1.10	10	150	1,47	(V/ /X
2001	1,75		15.0	92.F	-520 je		10	160	1.53	1 1 1 02
1111	2.00	118+	1	365	~249.4 ~243.4		18	150	1,51	1 6
1116	3.32	-	6.33	363	~242.4 -234.7		18	150	1, 53	1 6
7181	2.50	11.61		253 333	-236.7		19	130	1.53	1 3
iigle	2,75	10.14		335 355	-3378 -336.T		18	150	1.53	h / .
1131 1136	3.85	13.0		341	-337.7		16	150	1.53	11/
1130	2.92	1020	~ 10.7	<u> </u>		2.5			T	

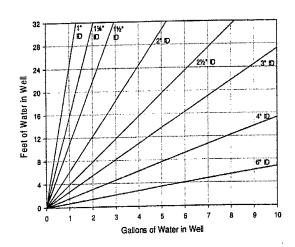
Sample Collector(s): La Buduk Date: 06/02/03 **30.04**

Well ID: MW-655

	Volume	(continu	ued fron	n front)		-				Page 2 of 2
Time	Removed	Temp.	рH	Spec. Cond.	ORP	DO	Turbidity	Flow Rate	Drawdown	Comments
(24hr)	(literss)	(°C)		(µS/cm)	(mV)	(mg/L)	(NTU)	(ml/min)	(feet)	
				1						
					<u> </u>					
				~	trust.					
						WE_				
 										
 										
 										

SAMPLE COLLECTION DATA

Sample ID	No. of Containers	Container Type	Preservation	Analysis	Time (24 hr)
20.00	n3 3	40 ml	HCL	TCL NOCS is	1908
Mill-622 310 1000	3	J. L	4°C	2-Methinaphhalene	1908
NW-1055	1	500mi Mastic	براص	Lest kits	1908



Calculations:

tubing length = 3 (add 3ft for pump) x 0.0217 Liters per foot tubing vol. = 0.065 + 0.25 (flow cell vol., L)

	+	0.25 (flow cell vo
system vol.	=	0.315 (liters)

Values per linear ft of tubing									
Volume per linear ft of tubing									
Gallon	Liter								
0.0025	0.0097								
0.0057	0.0217								
0.0102	0.0386								
0.0229	0.0869								
0.0408	0.1544								
0.0637	0.2413								
0.0918	0.3475								
0.1632	0.6178								
0.2550	0.9653								
0.3672	1.3900								
0.6528	2.4711								
1.4688	5.5600								
	Gallon 0.0025 0.0057 0.0102 0.0229 0.0408 0.0637 0.0918 0.1632 0.2550 0.3672 0.6528								

Comments:	A flow rate around 180 ml/min is appropriate
	PID reading of purge water = ppm

Collector(s): La Bundin Date: 0(d02/03

Well I.D.: <u>IW-5</u>	Date: 6/30/03	
Well Depth (from T.O.C.) = $\frac{Q \cdot Q \cdot Q \cdot Q}{Q \cdot Q}$ ft	Well Diameter (d) =	
Static Water Level (WL) = 10.80 ft (from T.O.C.)	FWENC Sampler(s): Yixian Thang	Matt Greenber
Height of Water in Well (T):	Parameters Sampled: Ph. Conductivity	DO ORP A
T = depth (ft) - Static Water Level (ft)	Tobing intake at 18541	TCL VOG, 2 methylapy

Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (<u>± 10%)</u>	D.O. (mg/l) (±10%)	ORP (mV) (± 10%)	Flow Rate (ml/min)	Static Water <u>Level</u>	Comments (Vol Rangued)
11=50	18.58	6.60	0.842		0.5 mg/c;2<1 2.47	<u>-169.3</u>	175	11.70	Grown, Lurbid
12:00	15.90	6.26	0.907		1.62	-143. 8	120	11-50	
12:05	15.99	6.214	0.919		1055	-118.0	130	11.20	
12:10	17.10	6.27	0.926		1.50	-101.3	140	11.80	
12:15	15.32	<u>6.2</u>	0-911		1.42	-83.8	150	11.80	
17:70	15.16	6.23	0.890		1.28	<u>-79.9</u>	140	11.80	
1217	15.40	6.24	0.884	****	1.21	<u>-77.</u> 5	130	11.80	Becoming Jearer
12-30	15.30	6.26	0.862		1.14	<u>-75.</u> 0	130	11.85	7.
12.235	15055	6.26	0.844	- /	1.11	<u> - 70.9</u>		4.90.	
12:40	15.87	<u> </u>	<u>8-8-0</u>		1.09	-70.4	150	11.95	Network and the state of the st
12:45	15.13	6.24	0.800		1.08	7.76-	100	1:.90	
12:50	11.6	6.25	0. 782		1.04	-66-7	100	11.90	
12255	15.16	6.24	0.778		1.02	-64.8		11.90	
		-							***************************************
\355				8.36		Total	Volume R	emoved: 15	i 2 gols

P:/Sciences/Science.geo/Sci-form/LOWFLOW2.DOC

1400 Collect sample. Lobel 05 IW-5-6W-063003.
To reidity Meter had broken; waiting for a replacement. W. Ucollect 1 to reidity reading prior to sampling.

Well I.D.: MW - 658	Date: 6-30)-03
Well Depth (from T.O.C.) =	Well Diameter (d) =	2"
Static Water Level (WL) = 11.30 ft (from T.O.C.)	FWENC Sampler(s):	M. Grownbarg, Y. Zhang
Height of Water in Well (T):		TCC VOCs, 2-methyl napthalone
T = depth (ft) - Static Water Level (ft) T = ft	Tubing intokat	17ft bg9.

Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (± 10%)	D.O. (mg/l) (±10%) or.5m	ORP (mV)(46)	Flow Rate (ml/min)	Static Water <u>Level</u>	Comments (16/2	Pemorel)
1415	16.68	6.37	0.551	<u> 13.9 </u>	<u>2.35</u>	-44.6	200	11.82		
14-20	14.16	6.35	0.433	14.2	1.28	-46.2	20 V	12.75		
1425	15.09	6.38	0.432	14.1	1.02	-49.2	160	12.80	-	
1630	14.96	6.3	0.446	8.80	1.06	-419	140	12.85		
1431	14-74	6.38	0418	7.43	0.92	-49.0	120	12-85		
1440	14.58	6.41	0.457	7.15	0.84	<u>-52.}</u>	150	12.85		i .
1445	14.8	6.40	0.461	6.28	0.87	<u>-56.</u> }	150	13.00		
1450	.14-09	6.43	0.461	_6.81	_0.75	<u> -184</u>	1.50	13.05		
1455	14.2	6.41	0.452	10.41	0.76	56.0	170	书13.10		
# 1500		6.37	0.440	14.2	0.74	-42.9	160	13.10		
1505	14.6]	6.34	0.430	<u> 185</u>	0.7/	-24.6	120	13.25	····	
15.10	15.3 +	6-34	0.466	16.6	0-73	-21.9	<u> </u>	· 13.30		
1315	15.28	6.34	0.478	16.8	0.76	-28.5	120	13.37		
1520	14.9	6.35	0.488	14.6	0.72	<u> </u>	<u>0 L/</u>	13.30		•
ا سر، بر	15157 1		00 v	.1		Total	Volume R	emoved:	~2.5 gols	

Well I.D.	: <u>MW</u>	-66S				Date:	6/30/	103			
Well Dep	th (from T.O.C	c.) =	· 20 ft			Well Diame	eter (d) = _	2 "	,		i e
Static Wa	nter Level (WL D.C.))= [0.	<u>44 </u>			FWENC Sa	ampler(s):	Matt Gre	een berg,	Yixian	zhang
Height of	Water in Well	(T):				Parameters	Sampled:	pH, ()	industricity	700 :-	ORPEN
-	(ft) - Static Water	• •				Tchi	na inta	he at a 15	ft bos	الله الالكي	2-nethylmap
T =	- <u>-</u>						\mathcal{J}		9,		
Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (± 10%)	D.O. (mg/l) (<u>±10%)</u> 0 ros.f<!--</b-->	ORP (mV) _m √ (± 10 %)	Flow Rate (ml/min)	Static Water <u>Level</u>	Comm	<u>ients</u>	
1425	17.72	6.72	0.517	11.8	4.21	-293.1	130	10.61		,,	
1430	18.22	6.35	0.485	9.04	3.03	-274.1	175	10.82			
1435	15.97	6.26	0.472	<u>8.26</u> 41.9	2,65	-279.3	130	11,18		***************************************	
<u>1440</u> <u>1445</u>	15.51 \5.13	6.27	<u>0.470</u>	30.2	2.42	-263.7 -240.2	180	11.52			
1455	15,93	6.35	0.482	19.2	2.52	-198, 2	150	11.89	*** **********************************		•
1500	15.10	6,29	0.475	9.62	2.35	-208.2	220	12,16			
505	15.16	6.21	824.0	9.73	2.20	-195.5	50	12,25			
1210	15.75	6.22	0.473	9.13	5.23	71965	140	12/31			
1515	16.15	6.24	0,474	4.81	3,35	755.1	700	12.59	<u></u>		
1520	15.71	6.22	0.470	3.88	3,46	<u>-133.1</u>	180	1251			
1525 1530	15.42 15.11	6.24	9.471	<u>4.60</u>	<u> 3.68</u> <u>3.64</u>	7/31,4	170	12.70			
<u>1535</u>	(5.22	6,23	0.473	6.49	3.61	-126.4 -126.4	, <u>7</u>	12.77			
	1538 E		et well.				ıl Volume l		~ 2.5	pols.	
	1700 0	Lallot 5	Dolal Sam	city . L	1-65-6	10-0631m2			(J	

P:/Sciences/Science.geo/Sci-form/LOWFLOW2.Doc , labelled as MW 665-6W-063003.

1110 Duplicate sample time MW-665-6W-063003D.

				LOW	-FLOW E	PATA SHE	ŒT					
Well I.D	.: <u>MW-</u>	185R	1			Date: _9/	9/03					
Well De	pth (from T.O.C.	·)= <u>27.</u>	<i>33</i> ft			Well Diameter (d) =						
Static W (from T.	ater Level (WL)	=	<i>52</i> ft	from 5	129/03		-	m. Ekas				
-	Water in Well (Г):				Parameters	Sampled:	Vacis				
T = depth $T = 2$ $T = -2$	(ft) - Static Water 7.33 - 16 ft	Level (ft)				Tubing Ry	on ~	25FL TIC.				
<u>Time:</u>	Temp.(°C) (±3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (± 10%)	D.O. (mg/l) (±10%)	ORP (mV) (<u>± 10%)</u>	Flow Rate (ml/min)	Static Water <u>Level</u>	<u>Com</u>	uments		
0934	52.95	6.19	254	644	3.23	25.1	500		DUCKE P	13016 11		
1023	21.74	6.30	461	17.6	4.14	25.0	100		PID	0.0	ey, at 0940	
1029	<u> 26.50</u>	_ الط	236	1.85	3.37	-28.8	100					
038	21.17	6.10	451	9.44	3.20		10-0	-			,	
1046	18.94	6.08	449	9.51	3.27	43.2	10-0					
1055	18.57	6.50	450	8.64	5.04	69.2	100				•	
1105	20.43	5.99	450	13.0	2.92	<u>59.8</u>	100					
1118	49.70	6.14	467	27.8	1.16	44.3	100	***************************************				
1124	35.45	6.05	470	28 E	1.93	44.7	100	-				
1133	25.05	6.03	459	30.5	3.29	<u>66.3</u>	100					
1139	25.08	6.14	459	43.4	4.28	76.7	100					
1149	25.12	6.13	457	53.9	5.19	111.0	100		tand pu	rge.		
1155	Samole	collecte	d nor	TCA VOC	'S				7			

Total Volume Removed:

~2,75 gals

P:/Sciences/Science.geo/Sci-form/LOWFLOW2.DOC

A flow though cell not used were peeted high temperatures.

Well I.D	: <u>MW-</u>	635				Date:	1-9-0=	3			
Well De	pth (from T.O.C.)= 24.	[3] f	t meason 5-	29-03	Well Diam	eter (d) =	2°			
Static W (from T.	ater Level (WL)		.36 f	t meas on E	5-29-03		FWENC Sampler(s): M. Greenburg Parameters Sampled: VOCs				
_	f Water in Well (*) (ft) - Static Water ft	·		AM CONTRACTOR	so can be	of the series	w through being if	h coll was	as used for tear causing stamage than another putof Flow-		
Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (<u>± 10%)</u>	D.O. (mg/l) (<u>±10%)</u>	ORP (mV) (<u>± 10%)</u>	Flow Rate (ml/min)	Static Water <u>Level</u>	<u>Comments</u>		
1130 1137 147 157 1207 1219	31.73 24.95 25.55 23.63 21.19 21.65	5.98 5.56 5.51 5.47 5.51	771 750 741 741 738 749	5.91 12.2 18.8 31.9 42.6 67.5	5.92 6.18 7.87 6.65 7.24 1.92	137.0 138.1 132.4 135.5 136.3 149.4	125 150 140 150 110 125 720	NM NM NM NM	Vater is slightly gellow.		
1327	almost drie	has far	os con be	told with	n <u>i PIGI</u> t retor tus	brolne	ter. Will	allow of	romwell; it has scharge for 15 nimetes;		
1255	Colort	5 auple	MW-63	S-6W-C	09 <u>0903</u> , 20909	3D.					
						Tota	ıl Volume R	emoved:	~2 gals.		

Well I.D.:	nw-	655				Date:	9191	03		
Well Dep	th (from T.O.C.	.)= <u>ಇನ್.(</u>		ft, mea s. on 5	29.13	Well Diam	eter (d) =	2"		
Static Wa	ter Level (WL) D.C.)	= 11.2.	5	ft, meas. On 5-2	1-03	FWENC Sampler(s):			3	
Height of	Water in Well (Γ):				Parameters	Sampled:	TE VO	<u>دځ</u>	
T = depth ((ft) - Static Water	Level (ft)						(100)		
T =	n									
Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)		D.O. (mg/l) (<u>±10%)</u>	ORP (mV) (<u>± 10%)</u>	Flow Rate (ml/min)	Static Water <u>Level</u>	<u>Comments</u>	
1337	44.45	6.76	443	25.6	1.38	50.3	180			
1345	34.22	5.74	458	21.0	3.29	45.1	, 50			
1350	27.64	5.84	452	17.2	2.97	40.3	150		· · · · · · · · · · · · · · · · · · ·	
<u> 1355</u>	25.87	5.74	429	17.9	1.87	48.4	150			
1400	25.30	5.75	425	17.2	1.85	48.7	150			
1406	24.68	5.69	437	17.7	1.70	56.3	150		The assect to	Conl
1410	21.68	5.66	423	18.4	1.96	<u>55.2</u>	150			·
1415	.20.54	5.67	422	16.3	1.87	70.1	150		`	
1420	20.97	5,94	417	16.2	1.48	73.9	150			
1425	19.62	6.00	414	16.8	1.51	59.8	150			
1430	21.24	5.96	416	15.1	1.47	68.1	150			
1435	21:83	6.03	414	16.2	1.40	70.5	150			
 .	1440	Sampled	1 Label	as MW-	<u> 55-</u> 6	5 <u>W-0909</u>	03.			
	1445	Samples	(Dup)	L. Labell a	SMW.	-65S-C	W-09	0 <u>903D.</u>		
						_	Volume R		2 gallon.	

						DIREIR DIR	TORY I			
Well I.D	D.:MW	1-185	R			Date:	09-	30-02	3	
Well De	pth (from T.O.0	C.) =	f	t		Well Dian	neter (d) =	2"		
Static W (from T.	ater Level (WL O.C.))= _2	0,98 f	t	·	FWENC S	Sampler(s):	9.1	Verban	
	f Water in Well					Parameter	s Sampled:	V.	OC	· · · · · · · · · · · · · · · · · · ·
T = depth T = T =	n (ft) - Static Wate 	er Level (ft)								
Time:	Temp.(°C)	pH (SU) (<u>± 0.1)</u>	Spec. Cond. (Mahos/cm) (±3%)	Turbidity (NTUs) (<u>± 10%)</u>	D.O. (mg/l) (<u>±10%)</u>	ORP (mV)	Flow Rate	Static Water		
1050	32.93	8.60	1.895	0.50	5.32	$(\pm 10\%)$ -180.2	(ml/min) 150.	<u>Level</u> 21.02	Replaced well	tubin
1055	<u>46,87</u> <u>34.82</u>	6.40	1.668	0.90	<u>4.48</u> 5.28	<u>-88.0</u> -29.0	<u>200.</u> 200.	21.06		
1105 1110	31.55 31.09	5.87 6.10	1.862 1.860	<u> 1.0</u> _0.60	5,72 5,56	-3.6 -8.1	200 ·	21.28		
1115	30.47	<u>5,92</u> 5,78	1.859	0.50	5.01	31.5	200:	21.29		
1125	29.63	5.72	1.853	0.60	4.95	<u>43.8</u> <u>39.8</u>	<u>200.</u> 200.	21.29		
1135	0-110	2,71	1.859	0,50	4.94	38,2	200:	21.29		

Total Volume Removed:

2.25 gd

1135

•,				LOY	Y-TLUW	DATA SI	IEET		, and
Well I.D).: <u>MW-</u> 2	12 SR				Date:	9/30/0	ζ	
Well De	pth (from T.O.	C.) =	ft				meter (d) =	2"	· ·
Static W (from T.	ater Level (WI O.C.)	L) = ZE	5.56 ft			FWENC	Sampler(s):	John	lmhoff
	f Water in Well					Paramete	rs Sampled: _	VOC	5
T = depth T = T =	(ft) - Static Wat	er Level (ft)		·			·		
Time:	Temp.(°C) (±3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (± 10%)	D.O. (mg/l) (±10%)	ORP (mV) (± 10%)	Flow Rate (ml/min)	Static Water Level	Comments
11:58 12:00 12:05 12:10 12:15 12:20 12:25 12:30 12:35	19.74 16.50 16.89 16.93 16.77 16.54 16.23 15.98 16.3	5.86 5.61 5.61 5.68 5.54 5.51 5.47	0.814 ms/cmc 0.767ms/cmc 0.769 0.769 0.771 0.773 0.777 0.775 0.773	3.1 2.3 2.1 2.3 2.5 2.4 2.3 1.8	0.68 0.80 0.92 0.88 0.87 0.89 0.91 0.92	-26.3	30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min 30 me/min		Sample

Total Volume Removed:

Well I.D.: $MW - 60S$ Well Depth (from T.O.C.) = 27 . ft Static Water Level (WL) = 22.88 ft (from T.O.C.) Date: $09-29-03$ Well Diameter (d) = 2^{11} FWENC Sampler(s): $9 \times \sqrt{94}$	**			LOV	V-FLOW	DATA SH	EET		e ^c
Static Water Level (WL) = $\frac{22.88}{1}$ ft						Date:	09-	29-03	
Static Water Level (WL) = 22.88 ft	Well Depth (from	T.O.C.) =	<u>27.</u> ft			Well Diam	eter (d) =	2"	
(from T.O.C.)	Static Water Leve (from T.O.C.)	el (WL) = 2	.2.88 _{ft}			FWENC S	ampler(s):	\bigcirc \downarrow /	bon
Height of Water in Well (T): T = depth (ft) - Static Water Level (ft) T =	T = depth (ft) - Stati					Parameters	Sampled:	Voc	
Temp.(°C) pH (SU) (Mahos/cm) (NTUs) (mg/l) (mV) Rate Water (±3%) (±0.1) (±3%) (±10%) (±10%) (±10%) (±10%) (ml/min) Level Comments 1615 14.71 8.79 0.662 8.2 1.17 -170.9 NM 24.93 WL Stable 1620 13.17 9.63 0.663 6.60 0.60 -177.0 24.93 1630 11.09 13.93 0.665 6.0 0.49 -242.4 24.93 1635 10.76 17.43 0.666 5.1 0.53 -224.6 24.93	T= Temp(Time: (±3% 1615 14.7 1620 13.1 1625 11.3 1630 11.0 1636 10.7	PH (SU) (± 0.1) 1 8.79 7 9.53 5 12.62 9 13.93 16 17.43	(Manhos/cm) (± 3%) 0.662 0.663 0.664 0.665 0.666	(NTUs) (± 10%) 8.2 6.0 6.4 6.0 5.1	(mg/l) (±10%) 1.17 0.60 0.49 0.47 0.53	(mV) (±10%) -170.9 -177.0 -242.4 -224.6 -235.6	Rate (ml/min)	Water Level 24.93 24.93 24.93 24.93	we stable
1690 10.57 15.88 0.667 4.3 0.69 -206.5 24.93 Saupling			0,007	7.3	<i>O</i> .69			24.93	Saupling

Total Volume Removed:

Well I.D	D.:	1-615				Date:	09-29	-02	
Well De	epth (from T.O.C	C.) =	<mark>(0</mark> ft			Well Dian	neter (d) =	2"	
Static W (from T.	ater Level (WL O.C.))= 21	. 19 ft				Sampler(s):	J. Ver	la
Height o	f Water in Well ((T):				Parameter	s Sampled:	Voc	
	ı (ft) - Static Wate								
T =	ft								
Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (mhos/cm) (±3%)	Turbidity (NTUs) (± 10%)	D.O. (mg/l) (<u>±10%)</u>	ORP (mV) (<u>± 10%)</u>	Flow Rate (ml/min)	Static Water Level	Comments
1530	14.45	6.11	0.657	5.4	0.92	126.3	_NM	23.75	23.75 is
									bottom of tube
									1.5 gal removed
0915	35.79	5.95	1.304		2.99	40.2	300. m/in	23,09	
0930		-							Sarphy
							·		10
78-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1		•							
									<u> </u>
								1	
						Tota	l Volume Re	moved:	

Well I.I	D.:MU	1-62	5			Date:	<u>(1)</u> -01	- 03	
Well D	epth (from T.O.C	C.) =	ft			Well Diar	neter (d) =	2"	
Static V (from T	Vater Level (WL CO.C.))= 22	<u>2.10</u> n			FWENC S	Sampler(s):	~ /	erlan
	of Water in Well (Parameter	s Sampled:	V00	,
T = dept T = T =	h (ft) - Static Wate	er Level (ft)							
Time: 1030 1036 1046 1045 1050 1100 1110	Temp.(°C) (±3%) [9.3] [7.49 [6.64 [4.46 [3.53 [4.97 [6.22	pH (SU) (±0.1) 6.20 6.08 6.02 5.96 5.96 5.98	Spec. Cond. (umhos/cm) (±3%) 0.565 0.577 0.551 0.547 0.553 0.56 (0.589	Turbidity (NTUs) (± 10%) 3,7 5.7 7.9 10: 12. 13.	D.O. (mg/l) (±10%) 4,91 0.97 1.16 0.69 0.60 0.48	ORP (mV) (±10%) -10.2 -35.3 -34.8 -35.0 -32.7 -34.0 -35.7	Flow Rate (ml/min) 200. 100. 100. 100. 100.	Static Water Level 22.54 22.88 23.01 23.21 24.21 24.66	Wh continues to drop regardless of flow rate Well Dry Sampled
								•	

Total Volume Removed:

2. gol

						DIXITY DI	TIPID I		,e*	
Well I.I	D.: <u>MW-(</u>	038				Date:	9/30/0	W 3 10-0	11-03	
Well Do	epth (from T.O.		fi	<u>.</u>		Well Dia	meter (d) =	2"	05	
Static V (from T	Vater Level (WI .O.C.)	.)= 20.4	H 20.51 A				Sampler(s):		on J. Vuba	u
Height o	of Water in Well	(T):				Parameter	rs Sampled:	Voc		
	h (ft) - Static Wate									
T =	ft T	-								
Time: 920 925 930 935 940	Temp.(°C) (±3%) 2242 18.64 17.65 16.84	pH (SU) (±0.1) 5.94 6.90 6.88 5.84	Spec. Cond. (Mhhos/cm) (±3%) 1.490 1.492 1.503	Turbidity (NTUs) (± 10%) 0,95 1,1 3,0 2,7	D.O. (mg/l) (±10%) 4.22 4.34 4.50 4.41	ORP (mV) (± 10%) 101.8 107.1 108.5 111.6	Flow Rate (ml/min) [OO . [OO . [OO .	Static Water Level 21.15 21.17 21.17 21.17	Samply	-
						Tota	l Volume Re	emoved:	-	•

	Well I.D	: <u>MW-64</u>	13				Date:	9/29/0	3		
. <i>S</i>	Well De	oth (from T.O.0	C.) =	ft			Well Diar	neter (d) =	2"		
ਵੰ	Static Water T.C.	ater Level (WL O.C.)		5 c 0910 7/30	E.0			Sampler(s):		hoff	
	Height of	Water in Well	(T):		,		Parameter	s Sampled:	VOCs		
		(ft) - Static Water									
	Time:	Temp.(°C) (± 3%)	pH (SU) (± 0.1)	Spec. Cond. (umhos/cm) (± 3%)	Turbidity (NTUs) (<u>± 10%)</u>	D.O. (mg/l) (±10%)	ORP (mV) (<u>± 10%)</u>	Flow Rate (ml/min)	Static Water Level	Comments	
129/03	1620	50.84	6.30	0.644 /cm		1.43	- 4.2	******	22.47	dry, in AM.	of Smpl
130/03	19	28.48	6,03	0,650 /cm	10	2.60	29.6		20.52	Burnt odor	
		1			***************************************						
-									•		·
-											
-	· ·										
-											· ·
_			,								_
-	· · · · · · · · · · · · · · · · · · ·										
-	<u>:</u>										
-	ş.								1		
-	<i>k</i>										
	P:/Sciences	(Colonos /0 ! /					Tota	l Volume Re	emoved:	2.0 gallons	

inlet of pump - day @ 1620

Static Wa	oth (from T.O.C)=	n. 89 n			FWENC S	oneter (d) = Sampler(s): s Sampled:	0-03 2' J.Ve	Wan	
T = depth T = T = Time: 1545 1550 1550 1605 1605 1610 1615 1620 1645		pH (SU) (± 0.1) \$.31 9.68 [4.07 15.21 11.01 6.62 8.18 9.64 8.07	Spec. Cond. (umhos/cm) (± 3%) 1.420 1.422 1426 1.426 1.446 1.458 1.466 1.473 1.479	Turbidity (NTUs) (± 10%) 1.1 1.0 1.6 0.95 0.95 0.90 0.60 0.50 0.50	D.O. (mg/l) (±10%) 0.79 0.61 0.35 0.37 0.63 0.76 0.46 0.89	ORP (mV) (± 10%) -90.2 -106, -168. -187, -136, -95.9 -113.6 -112.7 -111.2	Flow Rate (ml/min) 200. 200, 200, 200, 100. 100.	Static Water Level 19.50 19.57 19.78 19.78 19.96 20.00 20.00 20.00	Comments Aspated Flow Sampling	
						Tota	l Volume Re	emoved:		

				LOT	Y-PLO YY	DATASE	TEE.T.		8
Well I.D	P.:M	W- 60	o S			Date:	10-	01-03	
Well De	epth (from T.O.	C.) =	ft			Well Dia	meter (d) =	2"	
Static W (from T.	⁷ ater Level (WI .O.C.)	.)= [3	8,71 n				Sampler(s):		luban
Height of	f Water in Well	(T):				Paramete	rs Sampled:	Voc	
	ı (ft) - Static Wate								
Time: 1200 1205 1210 1220 1230 1236	Temp.(°C) (±3%) 21.41 17.99 17.36 17.96 21.44	PH (SU) (±0.1) 6.48 6.44 6.46 6.46	Spec. Cond. (umhos/cm) (± 3%) 0.560 0.548 0.548 0.551 0.556	Turbidity (NTUs) (± 10%) 5.2 16. 13, 5.0 2.8	D.O. (mg/l) (±10%) O.58 O.48 O.45	ORP (mV) (± 10%) 9,2 13,6 13,1 13.8 5.9	Flow Rate (ml/min) 200, 200, 200, 200.	Static Water Level 14.76 15.35 15.59 16.20 17.28 17.40	Comments WL contains to drop W/Slow recharge Well dry (below toke) Sarphy Perplicate Here
P:/Sciences/	/Science.geo/Sci-fc	orm/LOWFi Owa	boc			Tota	 l Volume Re	moved:	3gal

				LOW	-FLOW i	DATA SH	ELI			
Project N	ame: Bedfor	d, MA				Project No	o.:2	282.0891.920	2.00000	_
Well I.D.	: <u>18 SR</u>	·				Date:		4/14/04		_
Well Dep	oth (from T.O.C	.)= 27,4	ft			Well Dian	neter (d) =			_ ft
Static Wa	ater Level (WL) O.C.)	= 15.0	ft.			FWENC Sampler(s): Mance Ekas (TTFW), Lo			orie Burdick (ENSR)	
Height of	Water in Well ((T):								
$T = \frac{\pi}{4}$ $T = \frac{\pi}{4}$	(ft) - Static Wate 1.4 - 15 49 ft	er Level (ft)								
Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	<u>Comments</u>
12924	32.68	662	1.22	47	-3 Ai	-1/ O Q	0.03	W ED	- اه	-1 3 1.1

Time: Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	Color	<u>Comments</u>
0934 33.68 0934 34.93 0939 35.08 0944 35.34 0949 35.36 0954 35.39 0959 35.45 1004 35.50	6.63 6.72 6.73 6.73 6.73 6.73 6.73 70m	633 623 623 624 623 620 621	4.2 5.8 6.0 5.6 4.3 4.4 3.5 2.9	-3.01 -1.86 -1.72 -1.53 -1.52 -1.42 -1.45 -1.41	-169.9 -215.6 -233.5 -217.8 -219.0 -214.9 -214.9 -210.6		16.53 16.63 16.63 16.69 16.70 16.71 16.72	clear clear clear clear clear clear	odor - oil-like

Total	Volume R	emoved:		

Project Name: Bedford, MA						Project No.	: 22	282.0891.9202	.00000		
Well I.D.:	mw 1	BSR				Date:	: 	4/14/04			
Well Dept	th (from T.O.C.) =	ft			Well Diame	eter (d) = _		ft.		
Static Wa (from T.C	ter Level (WL) O.C.)	***************************************	ft	. ft FV			FWENC Sampler(s): Mance Ekas			Lorie Burdick (ENSR)	
	Water in Well ((ft) - Static Wate ft	•									
Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments	
1025 1030 1035 1040 1045	24.97 25.24 25.31 25.42 25.42 Ne @	6,75 6.74 6,73 6,73	626 626 624 625 623	2.2 1.2 1.6 0.75 0.80	-0.3/ -0.73 -1.02 -1.01 -0.91	-208.6 -215.0 -216.4 -210.7 -311.5		16.64 16.64 16.65 16.70			
The state of the s		****		P-07-1			Tota	al Volume Re	moved:	5 agl	

Field Forms Templates (FF-4 Lowflow)
Proprietary Information

Version Date: 08/01/2001

Revision 1

Project Na	ame: <u>Bedford</u>	, MA				Project No.: 2282.0891.9202.00000					
Well I.D.:	N/W-L/2	SE				Date:		4/\3/04			
Well Dep	th (from T.O.C.)= 15.39	€ 24.63 A			Well Diame	eter (d) = _			ft	
Static Wa	ter Level (WL) 0.C.)	= 15.33	ft .			FWENC Sampler(s) Mance Ekas (TTFW), Lorie Burdick (ENSR)					****
Height of	Water in Well (T):							"		
	(ft) - Static Wate 03 - 15 31 ft			1			•			sample @	
Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh <u>(mV)</u>	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments	
1348	15.13	6.45	47	126	0.97	<u>-104.7</u>	180	15.68		Flow cell Full	
<u>1358</u> 1403	18.30	<u>5.97</u> 5.91	<u>37</u> 40	<u>90</u> 105	1.30	<u>-100.1</u> -136.1	300 180	15.98 ilo.05	- (l		
1408	13.28	5,86	44	45	1.17	-1577	180	16.14	\ <u>'</u>	•	
7414	13:30	5.3	53	<u>36</u>	<u>49.0</u>	-160.0	300	16.21	Mear	light rain	
_1433 _1418	18,45	<u>5.82</u>	<u>59</u> 	<u>35</u> 32	18.0 17.0	<u>~ 157,3</u> -157,3	081	16.25	<u> </u>		
1438	18.35	5,81	76	19	0,14	<u>-153.7</u>	180	86.01 56.01	·		
1433		5.81	88	19	0.57	-152,8	180	16.37	u		
1438	18.25	5.8	95	14	0.44	<u>-151,4</u>	180	16.37		raining harder	
1443	17.26	5.81 E81	103	14	0.43	<u>-148,2</u>	180	16.29	<u></u>	·	

Field Forms Templates (FF-4 Lowflow) Proprietary Information

Version Date: 08/01/2001 Revision 1

180 Total Volume Removed:

Project N	ame: Bedfore	d, MA				Project No.	.:22	282.0891.9202	.00000		
Well I.D.	: <u>mu</u>	05	***			Date:	***************************************	4/ 1 /04			
Well Dep	th (from T.O.C	.)=	ft			Well Diam	eter (d) = _	,		<u>f</u> t	
Static Wa	ater Level (WL) O.C.)	= 19.18	n fi			FWENC S	ampler(s):	Mance Ekas	(TTFW), L	Lorie Burdick (ENSR)	*
Height of	Water in Well	(T):									
_	(ft) - Static Water						•				
T = T =		<u></u>									
	MATERIA MATERI		Spec.				Flow	Static			
Time:	Temp. (°C)	pH (SU)	Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Rate (ml/min)	water <u>Level</u>	Color	Comments	
0920	20.12	6.18	367	2.8	1.25	-51.4	150	19.30	Clear		
0925	21.28	6-17	362	2.7	0.83	-46.8	180	19.41	4 0		
0930	2232	6.14	34/	2,7	0.68	-502	180	19.75	14 . 4		
0935	21.83	6.14	340	4.3	0.63	-61.3	190	19.80	<i>"</i> "		
0940	21.61	6.13	33Z	5.1	0.54	-62.4	150	19.80	<i>i i</i> •		
0945	21,96	6.12	323	5.0	0.43	-67.7	150	19.89	<i>y</i> ()	,	
69F)	21.99	6.12	323	4.2	0.38	-76.4	150	20:14	n +1		
1000	22.00	6.13	327	5.7	0.30	-880	150	20:00	24 × 23		
1005	22.11	6.19	330	4.5	0.30	-95.7	150	20.27	1, 11		
1010	22.11	6.14	332	4.3	0.29	-102.5	150	20.30	11.11		
1015	22.17	6.15	336	4.3	0.28	-103.9	150	20.41	11 11		
1020	Samp	Ced.			,1						
	*						Tota	al Volume Re	emoved:		

Field Forms Templates (FF-4 Lowflow)
Proprietary Information

Version Date: 08/01/2001 Revision 1

Project Na	ame: Bedford	l, MA				Project No	o.: <u>22</u>	82.0891.9202.	00000	_
Well I.D.:	mu	اص ب	<u>S</u>			Date:		4/ 13/04	-	
Well Dep	th (from T.O.C.)=	ft			Well Diam	neter (d) =			ft
Static Wa	ater Level (WL) O.C.)	= /6	-29 ft			FWENC S	Sampler(s):	Mance Ekas (TTFW), I	Lorie Burdick (ENSR)
Height of	Water in Well ((T):					-	······································	· · · · · · · · · · · · · · · · · · ·	
T = depth $T =$	(ft) - Static Wate	er Level (ft)								
T =	ft									
Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments
1113	18.02	5.71	436	14	0.62	72.3	2,000	16.57	clem	
1118	20.18	5.70	432	15	0.62	73.4	180	16.82	11 11	
1126	2026	5.69	428	17	0.56	81.0	200	17.16	- si el	
1132	19.42	5.68	427	21	0.46	82.9	200	17.56	<i>a</i> u	
1138	1289	5.69	427	22	0.48	77.7	890	12.77		
-	1145	Suple	丛					Market and a second		4-44
		Markedo Tr. Handle To Market						-		
			<u> </u>		#TM-12-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1					
			***************************************	***						
							Tota	al Volume Re	moved:	

Field Forms Templates (FF-4 Lowflow)
Proprietary Information

Version Date: 08/01/2001 Revision 1

Project N	ame: Bedford	l, MA				Project No	.:22	282.0891.9202	.00000	
Well I.D.	mw 62	.5				Date:	·····	4/ <i>1</i> 3/04		
Well Dep	th (from T.O.C.) =	ft.			Well Diam	eter (d) = _			_ ft
Static Wa	ater Level (WL) O.C.)	=	<i>0</i> 6 ft			FWENC S	ampler(s):	Mance Ekas	(TTFW), L	orie Burdick (ENSR)
_	Water in Well ((ft) - Static Water in ft	•								
Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments
1350	19.74	5.33	444	0.85	0.45	1233	200	17.32	clear-	
1400	21.08	5.34	445	1-3	0.25	129.0	180	17.75	17.17	
1405	21,10	5.33	443	2.6	0.19	131,1	180	17.95	" "	
1411	20,75	5,30	447	3,9	0.19	132.2	200	18.29	U 11	
1417	20.83	5.29	454	5.3	0.16	130 2	200	18 47	<i>u 11</i>	***************************************
1422	21:1	5.30	459	5.5	0.28	126.0	180	18.59	<u> </u>	
1427	20.82	5.32	460	5.5	0.18	,23.9	180	18.70	****	
	<u>San</u>	pled of	1435	2.17	Toler					
							<u> </u>			
		Marie Marie	***************************************			-				
	destate and the second				*****	• 				11777-1171-1171
							Tota	al Volume Re	moved:	

Field Forms Templates (FF-4 Lowflow)
Proprietary Information

Version Date: 08/01/2001 Revision 1

Project Name: Bedford, MA	Project No.: 2	282.0891.9202.00000
Well I.D.: <u>MW - 63 S</u>	Date:	4/\4/04
Well Depth (from T.O.C.) = 24.04 ft	Well Diameter (d) =	ft
Static Water Level (WL) = 1478 ft (from T.O.C.)	FWENC Sampler(s):	Mance Ekas (TTFW), Lorie Burdick (ENSR)
Height of Water in Well (T):		

T = depth (ft) - Static Water Level (ft) $T = \frac{34.04}{9.36} - \frac{14.78}{ft}$ $T = \frac{9.36}{100} ft$

<u>Time</u>	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments
2111	20.94	6,62	388	45	<u>-1,75</u>	-101.6	250	15.12	Uear	flow cell full
1118	21.78	<u>6,39</u>	367	37	-1.10	-91,9	250	15,25	Ϋ́	
1193	21.91	<u>6.34</u>	365	<u>33</u>	<u>-0.91</u>	-98.7	250	15.55	clear	
1158	91.93	6.34	368	24	<u> 19.0-</u>	-99.0	256	15,92	clear	
1133	21.96	6.34	372_		<u>-0.83</u>	-116.4	250	61.01	clear	
1138	21.98	6.37	384	13	<u>-0,13</u>	<u>6.261-</u>	250	16.26	clear	
1143	80.66	6.41	401	10	-0.46	-131.8	250	16,34	clear	
1148	<u>77.66</u>	6.43	413	0.8	<u> 20,0-</u>	P.681-	250	16.45	clear	
1153	76.66	6.46	427	6.3	<u>-0.54</u>	-142,6	250	16.53	Clear	
<u> 1158</u>	99.37	6:50.	439	5.6	<u>-0.63</u>	4.747	250	16.58	clear	
7903	22,50	6,52	452	4.2	60.0-	-152.3	250	60,01	clear	
1908	<u>22.55</u>	6,55	467	<u>3,5</u>	<u>-0,5%</u>		250	16.00	clear	
1913	84.66	6.55	479	I, \mathcal{E}	PQ,0-	-157.1	Total	Volume Re	-	<u> 59</u>
				^						7

Field Forms Templates (FF-4 Lowflow)
Proprietary Information

Sample @ 1220

Version Date: 08/01/2001

Revision 1



Project N	Name: Bedford	l, MA				Project No.	:22	82.0891.9202	.00000	
Well I.D	: <u>mw</u>	645				Date:		4/14/04		:
Well Dep	oth (from T.O.C.)=	ft			Well Diam	eter (d) =			ft
Static W (from T	ater Level (WL) O.C.)	= 14.	52 ft			FWENC S	ampler(s):	Mance Ekas	(TTFW),	Lorie Burdick (ENSR)
-	f Water in Well (1 (ft) - Static Water	•								
<u>Time:</u>	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (<u>mV)</u>	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments
1105	20.53	6.05	325	1.20	6.75	-21.8	200	14.60	Cley	~
1110	21.26	6.05	320	1.29	0.59	-23.5	200	14.60	1. 11	
1115	21.67	6.03	317	1.01	0.42	-22.8	180	14.66		
1120	21.63	6.03	316	1.13	0.43	-23.0	200	14.70	., //	
1125	21.53	6.00	3:3	0.92	0.34	-21.4	200	1476		
1130	21.41	5.98	311	0.96	0.27	-19.8	200	14.80	11.16	
1135	21.25	5.96	310	0.59	0.23	-17.1	200	14.85	411	
1140	20:98	5.93	309	0.94	0.24	-12.8	200	14.87)ı **	
1145	20,99	5.92	308	1.24	0.29	-10.5	200	14.90		
1150	21.00	5.91	309	1.08	0.29	- 9.4	200	14.90	**************************************	
<i>5</i> a.	model at	1155			******					
						·····				

Total Volume Removed:

Project N	ame: Bedfo	rd, MA				Project No.	:22	282.0891.9202	.00000	
Well I.D.	:	MW 65	5			Date:		4/14/04		
Well Dep	oth (from T.O.	C.) =	ft			Well Diame	eter (d) = _			ft
Static Wa	ater Level (WL O.C.)	.)= <u>(1.35</u>	ft			FWENC S	ampler(s):	Mance Ekas	(TTFW), 1	Lorie Burdick (ENSR)
Height of	Water in Well	(T):							····	
T = depth T =	(ft) - Static Wa	ter Level (ft)				•				
T =	ft									
Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (mV)	Flow Rate (ml/min)	Static water <u>Level</u>	<u>Color</u>	Comments
1225	16.84	6.69	452	3.99	2.16	-136.9	3 <i>5</i> 0	12.65	clear	
1230	19.55	6.79	453	3.09	6.72	-166.6	180	12.64): *f	
235	17.52	6.80	457	2.68	0,32	-173.9	180	13.15	11 11	
1240	17.41	6.8i	461	1.70	025	-180.7	150	13 22	,, 46	***************************************
1245	17.52	6,82	466	1.69	0.25	-1844	150	13.30		***
1250	17.70	6.82	468	1,05	0.23	-187.1	150	13.20		
1255	17.84	6.82	472	1,91	0.19	-189.9	150	13.21		
1300	17.85	6.82	474	1.87	0.19	-196.8	150	13.21		
1305	17.86	6.83	475	1,34	0.18	-191.3	150	13.21		
	1340	Sappled.								
	· · · · · · · · · · · · · · · · · · ·			· .						
		***************************************					Tota	al Volume Re	moved:	

Field Forms Templates (FF-4 Lowflow)
Proprietary Information

Version Date: 08/01/2001

Revision 1

|--|

6	89
W	60)
i	00

Project Name: Bedford, MA

Well I.D.: MW - 6005

Well Depth (from T.O.C.) = $\frac{18}{18}$, $\frac{15}{18}$

Static Water Level (WL) = \6 37 (from T.O.C.)

Project No.:

2282.0891.9202.00000

Date:

Well Diameter (d) =

FWENC Sampler(s): Mance Ekas (TTFW), Lorie Burdick (ENSR)

Height of Water in Well (T):

T = depth (ft) - Static Water Level (ft)

T = 18.45 - 10.37

Time:	Temp. (°C)	pH (SU)	Spec. Conduct (umhos/cm)	Turbidity (NTUs)	D.O. (mg/l)	Eh (<u>mV)</u>	Flow Rate (ml/min)	Static water <u>Level</u>	Color	Comments
1030 1040 1050 1055 1100 1105	11.65 12.23 12.23 12.23 12.27	6.60 6.60 6.60 6.60		13 7.3 7.3 5.6 5.3 4.4	-1.00 -1.00 -1.00 -1.00 -1.00	-110.3 -98.4 -96.3 -95.8 -96.8	180 180 180 180 180	10.60 10.85 11.10 11.24 11.45 11.75	brown blear elear elear elear alear	odor? -can't fell whot
			ingle							

Total Volume Removed:

Version Date: 08/01/2001 Revision 1

Field Forms Templates (FF-4 Lowflow) **Proprietary Information**

APPENDIX E

Summary of Analytical Results – Soil

Table E-1 Soil Analytical Results Site 4 ERH Remediation Bedford NWIRP Site Bedford, Massachusetts

Sample ID	MW-60S-SBC-051403 MW-61S-SBA-051503 MW-62S-SBA		A-051503	MW-62S-SBA-0	51503D	MW-63S-SBA-051603		MW-64S-SBA-051603		MW-65S-SBA-051703		MW-66S-SBA-062603				
Date Collected	5/14/20	003	5/15/20	003	5/15/2	003	5/15/2003	}	5/16/200	03	5/16/20	003	5/17/20	03	6/26/2	2003
Depth Collected (ft bgs)	25.5	;	20.0		21.5	5	21.5		17.5		16.5	;	16.0		4.	5
Analyte	ug/kg	Qual.	ug/kg	Qual.	ug/kg	Qual.	ug/kg	Qual.	ug/kg	Qual.	ug/kg	Qual.	ug/kg	Qual.	ug/kg	Qual.
TCL VOCs			- 5 5		- 5 5	-,	- 3 3	-,			- 5 5					
1.1.1-Trichloroethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
1.1.2.2Tetrachloroethane	1400	Ü	1600	Ü	740	Ü	480		2800	Ū	760	Ü	2700	Ü	75	
1,1,2-Trichloroethane	1400	Ū	1600	Ū	740	Ū	480	Ū	2800	Ū	760	Ū	2700 U		75	
1,1-Dichloroethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
1,1-Dichloroethene	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
1,2-Dichloroethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
1,2-Dichloropropane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
2-Butanone	3400	U	4100	U	1900	U	1200	U	7000	U	1900	U	6700	U	75	U
2-Hexanone	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
4-Methyl-2-pentanone	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Acetone	3400	U	3200	U	1900	U	1000	U	3700	U	850	U	6700	U	180	U
Benzene*	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Bromodichloromethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Bromoform	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Bromomethane	3400	U	1100	J	410	U	1200	U	7000	U	1900	U	6700	U	190	U
Carbon disulfide	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Carbon tetrachloride	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Chlorobenzene	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Chloroethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Chloroform	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Chloromethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Cis-1,2-Dichloroethene	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Cis-1,3-dichloropropene	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Dibromochloromethane	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	U
Ethylbenzene*	23000		1800		740	U	480	U	42000		2400		50000		40	J
Methylene chloride	3400	U	4100	U	1900	U	1200	U	7000	U	1900	U	6700	U	190	U
Methyl-tert-butyl ether	1400	U	1600	U	740	U	480	U	2800	U	760	U	2700	U	75	
Naphthalene	6500		5300		540		390		16000		3500		17000		75	
Styrene	1400		1600		740		480		2800		760		2700		75	
Tetrachloroethene	1400		1600	U	740		480		2800	U	760	U	2700	U	75	
Toluene*	7600		7600		740		480		31000		2300		30000		75	
Trans 1,2-dichloroethene	1400		1600		740		480		2800		760		2700		75	
Trans-1,3-dichloropropene	1400		1600		740		480		2800		760		2700		75	
Trichloroethene	1400		1600		740		480		2800	U	760		2700		75	
Vinyl chloride	1400	U	1600	U	740		480		2800	U	760	U	2700	U	75	
p/m - Xylene*	86000		69000	-	790	-	510	-	260000		61000		210000	-	150	
o-Xylene*	23000		35000		740	U	480	U	86000		22000		56000		75	U
Total VOCs	146100		119800		1330		900		435000		91200		363000		40	1
Total BTEX	139600		113400		790		510		419000		87700		346000		40	
SVOCs																
2-Methylnaphthalene	340		330		120	J	190	J	770		450		320		53	U
2 Montylliaphinalene	340	l	330		120	<u> </u>	190		, ,,,,		+30		320			

Notes:

Analyte with "*" indicates that it is a Contaminant of Concern (COC).

U = Non-detect

J = Analyte was detected below its reporting limit. The result was estimated.

ft bgs = feet below ground surface

APPENDIX F

 $Summary\ of\ Analytical\ Results-Groundwater$

Table F-1 Groundwater Analytical Results Site 4 ERH Remediation Bedford NWIRP Site Bedford, Massachusetts

Bedford, Massachusetts																		
Sample Location		MW-1	8SR		MW-42SR			MW	/-60S			MW-61S			MW-62S			
									5/29/2003,									4/13/2004,
Date Collected	6/2/2003	9/9/2003	9/30/2003	4/14/2004	6/2/2003	9/30/2003	4/13/2004	5/29/2003	Duplicate	9/29/2003	4/14/2004	5/30/2003	9/30/2003	4/13/2004	5/29/2003	10/2/2003	4/13/2004	Duplicate
Sampling Event	Pre-Treatment	Mid-Process	Post-Treatment	Long-Term Monitoring	Pre-Treatment	Post- Treatment	Long-Term Monitoring	Pre-Treatmer	nt Pre-Treatment	Post- Treatment	Long-Term Monitoring	Pre-Treatment	Post- Treatment	Long-Term Monitoring	Pre-Treatment	Post-Treatment	Long-Term Monitoring	Long-Term Monitoring
Cumping Event	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic
Sample Collection Method	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump	pump
	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.
Analyte	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qua		(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	
TCL VOCs	1		1 1															
1,1,1-Trichloroethane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
1,1,2,2,-Tetrachloroethane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
1,1,2-Trichloroethane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
1,1-Dichloroethane	40 U	2.0 U	4.0 U	1.4 J	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
1,1-Dichloroethene 1,2-Dichloroethane	40 U 40 U	2.0 U 2.0 U	4.0 U 4.0 U	1.6 J 2 U	2.0 U 2.0 U	10 U	2 U 2 U	40 U 40 U	40 U	40 U	2 U 2 U	100 U 100 U	20 U 20 U	2 U 2 U	20 U 20 U	100 U	2 U 2 U	2 U 2 U
1,2-Dichloropropane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
2-Butanone	40 0	12	91	4.4	8.7	11	2.5	46	110	26 J	1.8 J	110	97	2 J	20 U	63 J	2	2.6
2-Hexanone	40 U	5.0 U	2.7 J	1.3 J	2.0 U	10 U	2 U	40 U	40 U	40 U	1.6 J	100 U	20 U	4	20 U	250 U	2 U	2 U
4-Methyl-2-pentanone	40 U	5.0 U	4.0 U	3.7	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	1 J	20 U	100 U	2 U	2 U
Acetone	99 J	180	760	11	29	39	8.5	110	210	73 J	4.1 J	190 J	320	4 J	51	310	2.7 J	2.6 J
Benzene*	220	2.0 U	3.3 J	41	14	20	2.2	250	250	140	7.6	76 J	14 J	2 U	59	66 J	3.4	3.5
Bromodichloromethane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Bromoform	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Bromomethane Carbon disulfide	100 U 40 U	5.0 U 1.0 J	4.0 U 4.0 U	2 U 2 U	5.0 U 2.0 U	10 U 10 U	2 U 2 U	100 U 40 U	100 U 40 U	40 U 40 U	2 U 2 U	250 U 100 U	20 U 20 U	2 U	50 U 20 U	100 U	2 U 2 U	2 U 2 U
Carbon disulfide Carbon tetrachloride	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Chlorobenzene	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Chloroethane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Chloroform	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	26	100 U	2 U	2 U
Chloromethane	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
1,2-Dichloroethene (total)	40 U	2.0 U	4.0 U	16	2.0 U	10 U	2 U	40 U	40 U	40 U	4.5	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Cis-1,3-dichloropropene	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Dibromochloromethane	40 U	2.0 U	4.0 U	2 U 650	2.0 U 34	10 U 65	2 U	40 U	40 U	40 U 2100	2 U 97	100 U 290	20 U	2 U 2 U	20 U	100 U	2 U	2 U 12
Ethylbenzene* Methylene chloride	1200 100 U	3.1 5.0 U	15 10 U	650 5 U	34 5.0 U	65 25 U	15	1600 100 U	1700 100 U	100 U	97 5 U	290 250 U	650 50 U	2 U 5 U	110 50 U	790 100 U	12 5 U	12 5 U
Methyl-tert-butyl ether	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Naphthalene	290	2.5 J	40.0	390	11	28	5.1	320	380	600	52	240	170	1.2 J	89	340	15	15
Styrene	40 U	5.0 U	4.0 U	3.2	2.0 U	10 U	2 U	U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Tetrachloroethene	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Toluene*	2200	6.8	24	13	1.5 J	7.4 J	2 U	1800	2300	670	1.3 J	3800	830	2 U	85	230	17	17
Trans-1,3-dichloropropene	40 U	2.0 U	4.0 U	2 U	2.0 U	10 U	2 U	40 U	40 U	40 U	2 U	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Trichloroethene	29 J 40 U	2.0 U	4.0 U	1.9 J	1.2 J	10 U	2 U 2 U	40 U	40 U	40 U	1.4 J	100 U	20 U	2 U	20 U	100 U	2 U	2 U
Vinyl chloride p/m - Xylene*	3600	2.0 U	4.0 U	2 U 800	2.0 U 22	10 U	2 U 14	40 U 3500	40 U 3800	40 U 4600	2 U 26	100 U 7800	20 U 3300	2 U 34	20 U 410	100 U 2000	2 U 47	2 U 48
o-Xylene*	1500	2.7	40	50	1.2 J	18	2 U	1200	1800	1100	6.5	4800	1900	16	150	710	20	19
- 197010	1000		, , ,	- 55			2 0	1230		1100	5.5	4000	1000	ı ' <u>"</u>	1 .50			,
Total VOCs	9180	226.1	1040	1961	122.6	259.4	51.3	8826	10550	9309	196.3	17306	7281	63.2	980	4509	119.1	119.7
Total BTEX	8720	30.6	146	1554	72.7	181.4	35.2	8350	9850	8610	138.4	16766	6694	56	814	3796	99.4	99.5
																		, ,
svoc			1												1			
2-Methylnaphthalene	42	NA	NA	37	5.8	NA	0.27 U	30	39	NA	6.9	42	NA	0.25 U	29	NA	4.6	2.2
Ronzono % Poduction (from 5/2/02)		99%	90%	81%		-43%	84%			44%	070/		920/	97%	T T	-120/	94%	040/
Benzene % Reduction (from 6/2/03) Total BTEX % Reduction (from 6/2/03)	+	100%	99%	81% 82%		-43% -150%	52%		+ +	-3%	97% 98%		82% 60%	100%	+ +	-12% -366%	94% 88%	94% 88%
Total BTEX /6 Reduction (Ironi 0/2/03)	1 1	10070	3070	O£ /0		1 30 /0	J£ /0	<u> </u>		-J /0	30 /0	<u> </u>	00 /0	10070	1	-300 /0	00 /0	00 /0
Low Flow Parameters																		
Temp (C)	13.5	25.1	29.6	25.4	14.4	16.3	17.3	13.1	13.1	10.6	22.2	12.8	35.8	20.0	12.2	16.2	20.8	20.8
pH Spec. Conductivity (umhos/cm)	6.28 431	6.13 457	5.71 1859	6.73 623	6.60 121	5.47 773	5.81 118	6.21 783	6.21 783	5.88 667	6.15 336	5.93 443	5.95 1304	5.69 427	6.25 286	5.98 5809	5.32 460	5.32 460
Turbidity (NTUs)	6.0	53.9	0.5	0.8	45.0	1.8	13.0	4.8	4.8	4.3	4.3	14.0	5.4	22.0	5.4	17.0	5.5	5.5
D.O. (mg/l)	0.48	5.19	4.94	-0.91	1.50	0.92	0.36	0.37	0.37	0.69	0.28	2.44	2.99	0.48	1.45	0.48	0.18	0.18
ORP (mV)	-150.0	111.0	38.2	-211.5	-7.0	17.3	-142.0	-127.2	-127.2	-206.5	-103.9	91.7	40.2	79.7	-30.1	-35.7	128.9	128.9
Flow Rate (ml/min)	150	100	200	250	160	30	180	150	150	NR	150	150	300	200	170	100	180	180

Table F-1 Groundwater Analytical Results Site 4 ERH Remediation Bedford NWIRP Site Bedford, Massachusetts

Bedford, Massachusetts																				
Sample Location		M	N-63S			MW-64S					MW	V-65S			IW-5	MW-66S				
												9/9/2003,						10/1/2003,		
Date Collected	6/2/2003	9/9/2003	10/1/2003	4/14/2004	5/30/2003	9/30/2003	4/14/2004	6/2/2003	6/30/	/2003	9/9/2003	Duplicate	9/30/2003	4/14/2004	6/30/2003	6/30/20		Duplicate	4/14/2004	
Sampling Event	Pre-Treatment	Mid-Process	Post- Treatment	Long-Term Monitoring	Pre-Treatment	Post-Treatment	Long-Term Monitoring	Pre-Treatment	Pre-Tre	eatment	Mid-Process	Mid-Process	Post-Treatment	Long-Term Monitoring	Pre-Treatment	Pre-Treat	Post- tment Treatment	Post- Treatment	Long-Term Monitoring	
Gamping Event	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	_	taltic	peristaltic	peristaltic	peristaltic	peristaltic	peristaltic	perista		peristaltic	peristaltic	
Sample Collection Method	pump	pump	pump	pump	pump	pump	pump	pump	pu	mp	pump	pump	pump	pump	pump	pum	p pump	pump	pump	
	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.		Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	Conc.	
Analyte	(ug/L) Qual.	(ug/L) Qua		1		(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.		Qual.	(ug/L) Qual.		(ug/L) Qual.	(ug/L) Qual.	(ug/L) Qual.	(ug/L)			(ug/L) Qual.	
TCL VOCs	, , , , , , , , , ,	(0)	1,0,1	, , ,	, , , , , , , , ,	, ,	, , , , , , , , , , , , , , , , , , , ,	(0)	, ,		, ,	1, 0, 1	1,0,1	, , , , , , , , , , , , , , , , , , , ,	1 (0)	, , ,	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	, , , , , , , , , , , ,	, , , ,	
1,1,1-Trichloroethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U	100) U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
1,1,2,2,-Tetrachloroethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U	100	U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
1,1,2-Trichloroethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U	100	U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
1,1-Dichloroethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		U	20 U	20 U	10 U	2 U	20 U	4 l		10 U	2 U	
1,1-Dichloroethene	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U) U	20 U	20 U	10 U	2 U	20 U	4 l		10 U	2 U	
1,2-Dichloroethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		U	20 U	20 U	10 U	2 U	20 U	4 (J 10 U	10 U	2 U	
1,2-Dichloropropane 2-Butanone	100 U	10 U 250	20 U 92	2 U	40 U 150	40 U 460	2 U 7.5	100 U		0 U 9 J	20 U	20 U	10 U	2 U 6.6	20 U 39	4.8	J 10 U 9.8 J	10 U 9.3 J	2 U	
2-Butanone 2-Hexanone	100 U	25 U	50 U	2.2	40 U	22 J	4.2	100 U	_	0 U	50 U	50 U	25 U	1.1 J	20 U	4.6		25 U	2 U	
4-Methyl-2-pentanone	100 U	25 U	20 U	2.8	40 U	40 U	1.7 J	100 U		o U	50 U	50 U	10 U	2 U	20 U	4 (7.2 J	2 U	
Acetone	220 J	2000	620	24	210	2400	13	200 J	220		840	710	370	16	100	18	25	23 J	5 U	
Benzene*	180	10 U	20 U	26	43	32 J	4.4	320	27		18 J	14 J	6.2 J	40	360	52	32	32	91	
Bromodichloromethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U	100) U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
Bromoform	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		U	20 U	20 U	10 U	2 U	20 U	4 l		10 U	2 U	
Bromomethane	250 U	25 U	20 U	2 U	100 U	40 U	2 U	250 U	250		50 U	50 U	10 U	2 U	50 U	10 l		10 U	2 U	
Carbon disulfide	100 U	13	20 U	2 U	40 U	40 U	2 U	100 U	_) U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
Carbon tetrachloride	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
Chlorobenzene	100 U	10 U	20 U 20 U	2 U 2 U	40 U 40 U	40 U 40 U	2 U 2 U	100 U 100 U		ว U ว U	20 U 20 U	20 U 20 U	10 U	280 2 U	20 U 20 U	4 l		10 U	2 U 1.6 J	
Chloroethane Chloroform	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		บบ	20 U	20 U	10 U	2 U	20 U	4.1	10 U	10 U	1.6 J	
Chloromethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		טט	20 U	20 U	10 U	2 U	20 U	4.1		10 U	2 U	
1,2-Dichloroethene (total)	100 U	10 U	20 U	6.8	40 U	40 U	2 U	100 U		υ	20 U	20 U	10 U	4.4	20 U	4 (10 U	2.7	
Cis-1,3-dichloropropene	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		D U	20 U	20 U	10 U	2 U	20 U	4 (- 1	10 U	2 U	
Dibromochloromethane	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U	100) U	20 U	20 U	10 U	2 U	20 U	4 l	J 10 U	10 U	2 U	
Ethylbenzene*	1600	6.0 J	25	430	280	1000	130	1500	230	0	420	370	78	2 U	800	210	26	26	240	
Methylene chloride	250 U	25 U	20 U	5 U	100 U	100 U	5	250 U	250	U	50 U	50 U	10 U	5 U	50 U	10 l	J 10 U	10 U	5 U	
Methyl-tert-butyl ether	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		U	20 U	20 U	10 U	2 U	20 U	4 l		10 U	2 U	
Naphthalene	410	11 J	21	500	360	1700	470	360	620	_	790	670	90	190	190	31	8.7 J	8.6 J	40	
Styrene	100 U	25 U	20 U	2 U	40 U	40 U	2 U	100 U		U	50 U	50 U	10 U	2 U	20 U	4 l		10 U	2 U	
Tetrachloroethene	100 U	10 U	20 U 27	2 U 27	40 U 920	40 U 1000	2 U 13	100 U 5900	100 660		20 U 600	20 U 520	10 U	2 U 250	20 U 1400	4 l 24	J 10 U 91	10 U 86	2 U 46	
Trans-1,3-dichloropropene	100 U	10 U	20 U	2 U	40 U	40 U	2 U	100 U		D U	20 U	20 U	10 U	2 U	20 U	4 1	J 10 U	10 U	2 U	
Trichloroethene	100 U	10 U	20 U	1.2 J	40 U	40 U	2 U	100 U		D U	20 U	20 U	6.9 J	5.6	16 J	5.4	6.7 J	6.3 J	3.5	
Vinyl chloride	100 U	10 U	20 U	2 U	24 J	40 U	2 U	100 U	100		20 U	20 U	10 U	2 U	20 U	4 (10 U	2 U	
p/m - Xylene*	8700	31	62	1300	6700	4900	1100	6200	800		1800	1600	330	650	1800	130	260	250	190	
o-Xylene*	4200	7.0 J	24	290	4200	2600	260	2600	290	0	910	780	120	400	600	43	93	90	88	
											,									
Total VOCs	19785	2332.0	871	2582	12887	14114	2002.1	17080	2099		5488	4764	1124.1	1560.2	5305	522.3	559.7	538	719.5	
Total BTEX	19080	58.0	138	2073	12143	9532	1507.4	16520	2007	0	3748	3284	615.2	1342	4960	459	502	484	655	
avec	1	<u> </u>	1 1	1	1	1 1	ı	ı			1	 	 		1	1		1	 	
SVOC 2-Methylnaphthalene	44	NA	N/A	60	60	N/A	76	34	80	1	NA	NA NA	NA	14	41	4.4	NA	NA	1.5	
<u>z-мешушарнинанене</u>	44	INA	NA	ויס	60	NA	70	34	1 8	ν	INA	INA	INA	14	41	1.1	INA	AVI	1.6	
Benzene % Reduction (from 6/2/03)		94%	89%	86%		26%	90%		169	%	94%	96%	98%	88%			38%	38%	-75%	
Total BTEX % Reduction (from 6/2/03)	1	100%	99%	89%	1 1	22%	88%		-219	_	77%	80%	96%	92%			-9%	-5%	-43%	
		- = 7 = 1				7		ı I		1	7	7		- /기	<u> </u>				1	
Low Flow Parameters																				
Temp (C)	12.8	NA	16.8	22.5	12.0	28.5	21.0	12.1	15.0		21.8	21.8	25.5	17.9	15.2	15.2	21.4	21.4	12.3	
pH Spec. Conductivity (umhos/cm)		NA NA	5.84 1503	6.55 472	6.04 296	6.03 658	5.91 309	6.24 241	6.3	_	6.03 414	6.03 414	8.07 1479	6.83 475	6.24 778	6.23 471	6.51 556	6.51 556	6.60 372	
Turbidity (NTUs)		NA	2.7	3.1	3.1	10.0	1.1	16.0	14.0		16.2	16.2	0.5	1.3	NR NR	6.5	2.8	2.8	4.4	
D.O. (mg/l)	0.65	NA	4.41	-0.64	2.69	2.60	0.29	-237.70	0.72		1.40	1.40	0.89	0.18	1.02	2.61	0.45	0.45	-1.00	
ORP (mV)		NA	111.6	-157.1	14.0	29.6	-9.4	1.3	-30.		70.5	70.5	-111.2	-191.3	-64.8	-123.2	5.9	5.9	-96.8	
Flow Rate (ml/min)	170	NA	100	250	200	NR	200	150	120	J	150	150	100	150	100	120	200	200	180	

APPENDIX G

Summary of Analytical Results – Vapor

Table G-1 Vapor Analytical Results Site 4 Remediation Influent (Vapor Samples Collected Using Summa Canisters)

•	Site 4 II	NF	Site 4 INF		VR-INFL4-081403		VR-INFL4-082203		VR-INFL4-082803		VR-INFL4-	090603	VR-INFL4-09110	
Date Collected	7/31/20		8/7/20	003	8/14/2	003	8/22/2	003	8/28/20	03	9/6/20	03	9/11/2	003
Analyte (TCL VOCs)	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.
1,1,1-Trichloroethane		U		U		U		U		U		U		U
1,1,2,2,-Tetrachloroethane		U		U U		U		U		U		U		U
1,1,2-Trichloroethane 1,1-Dichloroethane		U		U		U		U		U		U		U
1,1-Dichloroethene		U		U		U		U		U		U		U
1,2-Dichloroethane		Ü		U		U		U		U		U		U
1,2-Dichloropropane		Ū		U		Ū		Ū		U		U		U
2-Butanone		Ū		U		Ū		Ū		U		U		U
2-Hexanone		Ū		Ū		U		U		U		U		Ū
4-Methyl-2-pentanone		U		U		U		U		U		U		U
Acetone		U		U		U		U		U		U	1300	
Benzene*	92		12		16		32		520		38		220	
Bromodichloromethane		U		U		U		U		U		U		U
Bromoform		U		U		U		U		U		U		U
Bromomethane		U		U		U		U		U		U		U
Carbon disulfide		U		U		U		U		U	240			U
Carbon tetrachloride		U		U		U		U		U		U		U
Chlorobenzene		U		U		U		U		U		U		U
Chloroethane		U		U		U		U		U		U		U
Chloroform Chloromethane		U		U		U		U		U	35	U		U
Cis-1,2-Dichloroethene		U		U		U		U		U	აე	U		U
Cis-1,2-Dichloroetherie Cis-1.3-dichloropropene		U		U		U		U		U		U		U
Dibromochloromethane		U		U		U		U		U		U		U
Ethylbenzene*	260	•	66	•	30	•	170	J	4900	-	400	<u> </u>	9700	
Methylene chloride	200	U	- 00	U	30	U	170	U	7300	U	+00	U	3700	U
Methyl-tert-butyl ether		U		U		U		U		U		U		Ü
Naphthalene		U		U		U		U		U	160	_	7800	-
Styrene		U		Ü		U		U		Ü		U		U
Tetrachloroethene		U		U		U		U		U		U		U
Toluene*	1600		330		140		650		13000		2100		12000	
Trans 1,2-dichloroethene		U		U		U		U		U		U		U
Trans-1,3-dichloropropene		U		U		U		U		U		U		U
Trichloroethene		U		U		U		U		U	50			U
Vinyl chloride		U		U	7.2			U		U		U		U
p/m - Xylene*	9200		3000		2300		5200		45000		6700		61000	
o-Xylene*	3600		1400		1300		2400		16000		2700		24000	
TVO (Total VOCs)														
T-1-I DTEV	14752		4808		3793.2		8452		79420		12423		116020	
Total BTEX	14752		4808 4808		3793.2 3786		8452 8452		79420 79420		12423 11938		116020 106920	
Tentatively Identified Compound	14752												106920	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl-	14752						8452						106920 24000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl-	14752		4808		3786						11938		106920 24000 22000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl-	14752						8452						24000 22000 87000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl-	14752		2300		3786		8452				11938		24000 22000 87000 32000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl-	14752		4808		3786		8452				11938		24000 22000 87000 32000 89000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl	14752		2300		3786		8452				11938		24000 22000 87000 32000 89000 29000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl-	14752		2300		3786		8452				11938		24000 22000 87000 32000 89000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl	14752 s (TICs)		2300		1400		3800		79420		11938		24000 22000 87000 32000 89000 29000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane	14752 s (TICs)		2300		1400		3800		79420		11938		24000 22000 87000 32000 89000 29000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl-	14752 s (TICs)		2300		1400		3800 3800 6300 2800		79420 63000		5600 5100		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl-	14752 s (TICs) 6400		2300		1400 2200 2000		3800 3800 6300 2800 6200		79420 63000		5600 5100 5000		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 3-ethyl-	14752 s (TICs) 6400 15000 6800		2300 1400		1400 2200 2000		6300 2800 6200 2700		63000 120000		5600 5100 5000 2500		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 3-ethyl- Pentane, 2,2,4-trimethyl-	14752 s (TICs) 6400 15000 6800 7600		2300 1400		1400 2200 2000		6300 2800 6200 2700 2400		63000 120000 76000		5600 5100 5000 2500 3600		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl-	14752 s (TICs) 6400 15000 6800 7600 7500		2300 1400		1400 2200 2000		6300 2800 6200 2700 2400 2700		63000 120000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 3-ethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane	14752 s (TICs) 6400 15000 6800 7600 7500		2300 1400		1400 2200 2000		6300 2800 6200 2700 2400 2700		63000 120000 76000		5600 5100 5000 2500 3600		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane Heptane, 2-methyl-	14752 s (TICs) 6400 15000 6800 7600 7500		2300 1400 1400 1600		1400 2200 2000		6300 2800 6200 2700 2400 2700		63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,2,4-trimethyl- Heptane, 2-methyl- Heptane, 2-methyl- Heptane, 2-methyl- Heptane, 2-methyl- Heptane, 4-methyl-	14752 s (TICs) 6400 15000 6800 7600 7500		1400 1400 1200		1400 2200 2000		6300 2800 6200 2700 2400 2700		63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 3-ethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane Heptane, 4-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl-	14752 s (TICs) 6400 15000 6800 7600 7500		1400 1600 1200 1100		1400 2200 2000		6300 2800 6200 2700 2400 2700		63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 3-ethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane Heptane, 2-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl-	14752 s (TICs) 6400 15000 6800 7600 7500		1400 1400 1200		2200 2000 980		6300 2800 6200 2700 2400 2700		63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,2,4-trimethyl- Heptane Heptane, 2-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl-	14752 s (TICs) 6400 15000 6800 7600 7500		1400 1600 1200 1100		2200 2000 980		6300 2800 6200 2700 2400 2700		63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,2,4-trimethyl- Heptane Heptane, 2-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl-	14752 s (TICs) 6400 15000 6800 7500 13000		1400 1600 1200 1100		2200 2000 980		6300 2800 6200 2700 2400 2700		79420 63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane Heptane, 2-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclopentane, methyl-	14752 s (TICs) 6400 15000 6800 7500 13000		1400 1600 1200 1100		2200 2000 980		6300 2800 6200 2700 2400 2700		79420 63000 120000 76000 72000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclopentane, methyl- Hexane	14752 s (TICs) 6400 15000 6800 7500 13000		1400 1400 1600 1200 1100 2600		2200 2000 980		6300 2800 6200 2700 2400 2700		79420 63000 120000 76000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-ethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3,3-trimethyl- Heptane, 4-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclopentane, methyl- Hexane Hexane, 2,2-dimethyl-	14752 s (TICs) 6400 15000 6800 7500 13000		1400 1400 1600 1200 1100 2600		2200 2000 980		6300 2800 6200 2700 2400 2700		79420 63000 120000 76000 72000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-trimethyl- Pentane, 2,3-trimethyl- Heptane, 2-methyl- Heptane, 4-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclopentane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl-	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		2200 2000 980 970 2100		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-ethyl- Pentane, 2,3-dimethyl- Pentane, 2,3-trimethyl- Pentane, 2,3-trimethyl- Heptane, 2-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 2-methyl- Cyclobutane, ethyl- Cyclopentane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2-methyl-	14752 s (TICs) 6400 15000 6800 7500 13000		1400 1400 1600 1200 1100 2600		970 2100		6300 2800 6200 2700 2400 2700		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-ethyl- Pentane, 2,3-dimethyl- Pentane, 2,3-trimethyl- Pentane, 2,3-trimethyl- Heptane, 2-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclobutane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2-methyl- Hexane, 2-methyl- Hexane, 2-methyl- Hexane, 2-methyl- Hexane, 3-methyl-	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		970 2100 1700 1800		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-ethyl- Pentane, 2,3-dimethyl- Pentane, 2,3-trimethyl- Pentane, 2,3-trimethyl- Heptane, 2-methyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclobutane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 3-methyl- Hexane, 3-methyl- Hexane, 3-methyl- Hexane, 3-methyl- Hexane, 2,2,5,5-tetramethyl-	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		970 2100		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200 2800		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,2,4-trimethyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclobutane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,5-5-tetramethyl- Octane, 2,2,6-trimethyl-	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		970 2100 1700 1800 1900		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 2,3-dimethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,2,4-trimethyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclobutane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,5-5-tetramethyl- Octane, 2,2,6-trimethyl- Octane, 4-methyl- Octane, 4-methyl-	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		970 2100 1700 1800		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200 2800 3700		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-ethyl- Pentane, 2,3-dimethyl- Pentane, 2,3-trimethyl- Pentane, 2,3-trimethyl- Heptane, 2-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Cyclobutane, ethyl- Cyclobutane, ethyl- Cyclopentane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,5-5-tetramethyl- Octane, 2,2,6-trimethyl- Octane, 4-methyl- Pyrrolidine	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		970 2100 1700 1800 1900		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000 61000		5600 5100 5000 2500 3600 4200 2800		24000 22000 87000 32000 89000 29000 46000	
Tentatively Identified Compound Benzene, 1-ethyl-2-methyl- Benzene, 1-ethyl-3-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1-ethyl-4-methyl- Benzene, 1,2,3-trimethyl- Benzene, 1,3,5-trimethyl- Benzene, 1-methyl-3-propyl Benzene, 1-ethyl-3,5-dimethyl- Butane, 2-methyl- Pentane Pentane, 2-methyl- Pentane, 3-methyl- Pentane, 3-ethyl- Pentane, 2,3-dimethyl- Pentane, 2,2,4-trimethyl- Pentane, 2,3-trimethyl- Heptane, 4-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3-methyl- Heptane, 3,4-dimethyl- 1-Pentene, 2-methyl- Cyclobutane, ethyl- Cyclobutane, methyl- Hexane Hexane, 2,2-dimethyl- Hexane Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,3-dimethyl- Hexane, 2,5-5-tetramethyl- Octane, 2,2,6-trimethyl- Octane, 4-methyl- Octane, 4-methyl-	14752 s (TICs) 6400 15000 6800 7500 13000 5500 4900		1400 1400 1600 1100 2600 2500 1700		970 2100 1700 1800 1900		8452 3800 6300 2800 6200 2700 2400 4300		79420 63000 120000 76000 72000 53000 46000		5600 5100 5000 2500 3600 4200 2800 3700		24000 22000 87000 32000 89000 29000 46000	

Notes:

U = Non-detect

 $\ensuremath{\mathsf{J}}$ = Analyte was detected below its reporting limit. The result was estimated.

NA = Not analyzed

Analyte with * indicates that it is a Contaminant of Concern (COC).

Table G-2 Vapor Analytical Results Combined Effluent for Site 3 and Site 4 Operation (Vapor Samples Collected Using Summa Canisters)

Sample ID	GAC E		GAC E		VR-EFFL-		VR-EFFL-0		VR-EFFL-0		VR-EFFL-		VR-EFFL-	
Date Collected	7/31/20				8/14/20		8/22/200		8/28/20		9/6/2003		9/11/20	
Analyte (TCL VOCs)	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.	ppbv	Qual.
1,1,1-Trichloroethane		U		U		U	2100		4700		5.4		15	
1,1,2,2,-Tetrachloroethane		U		U		U		U		U		U		U
1,1,2-Trichloroethane 1,1-Dichloroethane		U		U U	6.8	U	600	U	710	U		U	26	•
1,1-Dichloroethane		U		U	4.1		7200		9100		10	U	240	
1,2-Dichloroethane		U		U	4.1	U	7200	U	9100	U	10	U		U
1,2-Dichloropropane		U		U		U		U		U		U		U
2-Butanone	8.1	U		U		U		U		U		U		U
2-Butanone	_	U		U		U		U		U		U		U
		U		U		U		U		U		U		U
4-Methyl-2-pentanone Acetone	20	-	4.0	U	3.9	U		U		U	4.2	U		U
Benzene	20		4.0	U	3.9	U		U		U	4.2	U		U
Bromodichloromethane		U		U		U		U		U		U		U
Bromoform		U		U		U		U		U		U		U
Bromomethane		U		U		U		U		U		U		U
Carbon disulfide		U		U		U		U		U		U	19	_
Carbon disulide Carbon tetrachloride		U		U		U		U		U		U	19	U
Chlorobenzene		U		U		U		U		U		U		U
Chloroethane		U	0.90	U		U		U		U		U		U
Chloroform Chloroform		U	0.90	11		U		U		U	<u> </u>	U		U
Chloromethane		U		U U		U		U		U	7.1	U	3.2	U
Cis-1,2-Dichloroethene		U		U		U	52	U	3900	J	13		3.2 55	
,		U		U		U	52	U	3900	U	13	U		U
Cis-1,3-dichloropropene		U		_		U		U		U		U		U II
Dibromochloromethane				U		•		·		•		•		U
Ethylbenzene Methylene ehleride		U		U	4.0	U		U		U		U	6.3	
Methylene chloride		U		U	10			U		U		U		U
Methyl-tert-butyl ether		U		U		U		U		U:		U		O
Naphthalene		U		U		U		U		U		U	20	
Styrene		U		U		U		U		U		U		U
Tetrachloroethene		U		U		U		U		U	9.9		9.2	
Toluene		U		U		U		U		U	2.9		4.2	
Trans 1,2-dichloroethene		U		U		U		U		U		U		U
Trans-1,3-dichloropropene		U		U		U		U		U		U		U
Trichloroethene		U		U		U		U		U	160		63	
Vinyl chloride		U	17.0		28		42			U		U	23	
p/m - Xylene		U		U		U		U	110			U	43	
o-Xylene		U		U		U		U		U		U	18	
TVO (Total VOCa)	20.4		24.0	1	F0.0		0004		40500	1	040.5		F44.0	
TVO (Total VOCs)	28.1		21.9		52.8		9994		18520		212.5		544.9	
Tentatively Identified Compounds (TIC	Cs)													
Benzene, 1-ethyl-2-methyl-													120	
Benzene, 1,3,5-trimethyl-													160	
Benzene, 1-ethyl-2,4-dimethyl-													95	
Butane					230		1400						82	
Butane, 2-methyl-					470		9900		58000				880	
1-Butene					28		0000		00000				555	1
1-Butene, 3-methyl-					20		880				<u> </u>			
Cyclobutanone							1100							
Cyclopropane, ethyl-					85									
Cyclopropane, 1,1-dimethyl-									6100					
Cyclohexane													76	
Ethane, 1,2-dichloro-1,1,2-trifluoro-					8.6									
Hexane									4500		32			
Hexane, 2-methyl-											38			
Heptane											32			
Cyclopentane, methyl-							5000				34		160	1
1-Pentene, 2-methyl-							3000		17000				.00	
2-Pentene							1000		17000		<u> </u>			
							1000		4000					
2-Pentene, (Z)-									4800					
2-Pentene, 4-methyl-, (Z)-									8100					
Pentane					4.1		5500		24000				280	
Pentane, 2-methyl-									49000		78		100	
Pentane, 3-methyl-							1200		21000		40			
Propane, 2-methyl-					770									
Pentane, 2,3-dimethyl-					-						39			
Pentane, 2,4-dimethyl-											19			
											61			
Pantana 77/4-trimatni/i-														
Pentane, 2,2,4-trimethyl-							l.				^^			
Pyrrolidine	0.0		40		745.0		F000		4400		39			
	6.6		12		715.9		5060		4100		39			

Notes:

U = Non-detect

J = Analyte was detected below its reporting limit. The result was estimated.

NA = Not analyzed

Note that effluent vapor data represent a combined vapor mass from the Site 3 pilot test and Site 4 remediation.

APPENDIX H

Waste Management Tracking Sheets

WASTE TRACKING TABLE ERH REMEDIATION BEDFORD NWIRP SITE BEDFORD, MASSACHUSETTS

Waste Stream	# of Containers	Total Quantity	Ship Date	State Manifest Doc. #	Generator Manifest Doc. #	Treatment, Storage and Disposal Facility	USEPA Waste Code(s)	State Waste Code(s)	Complete Manifest Package #	Transfer Facility	Transfer Facility State Manifest Doc. #
Non-Hazardous Soil Cuttings	10 roll-off dumpsters	130.94 tons	10/20/03 - 10/23/03	N/A	00193	Waste Management of New Hampshire - Gonic, NH	N/A	N/A	N/A	N/A	N/A
Soil Cuttings Shipped for Asphalt Batching	1 roll-off dumpster	12.55 tons	10/24/03	N/A	N/A	Environmental Soil Management, Inc. – Loudon, NH	N/A	N/A	N/A	N/A	N/A
Spent Vapor-Phase Granular Activated Carbon	2 bags, 4 vessels	Approximately 8,600 lbs.	11/12/03	K003339	03339	Westates Carbon Arizona – Parker, AZ	D040, D039	N/A	1	N/A	N/A
Spent Non- Hazardous Liquid- Phase Granular Activated Carbon	3 55-gallon drums	Approximately 1,200 lbs.	11/19/03	N/A – Bill of Lading	N/A	US Filter – Avon, MA	N/A	N/A	N/A	N/A	N/A

Notes: